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Space Shuttle Main Engine
High Pressure Fuel Pump
Aft Platform Seal Cavity
Flow Analysis

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SPACE SHUTTLE MAIN ENGINE HIGH PRESSURE FUEL PUMP AFT PLATFORM SEAL CAVITY FLOW ANALYSIS

I. INTRODUCTION

In working to improve the performance of the Space Shuttle Main Engine (SSME), the engineer is confronted with the difficult task of analyzing a complex engine system running under extreme operating conditions. The temperatures in the Shuttle's engines range from 37°R up to 5000°R, pressure vary from 20 to 8000 psi, and the engines' pumps rotate at speeds up to 37,000 rpm. Direct measurement of the engine environment is often impractical. Indeed, the particular area under consideration may be virtually inaccessible to instrumentation. Fortunately, the capability of modeling heat and mass transfer using computers has advanced to the point where computational fluid dynamics (CFD) can provide an alternate method of analyzing the engine. When used to model the various components and processes in the engine, numerical analysis can provide the engineer with valuable insight by allowing him or her to examine a wide range of operating conditions. The effect of a change in geometry, of a change in flowrate, or of a change in any parameter can be examined. Even a simple numerical model can demonstrate the sensitivity of the engine system to such changes, and a sophisticated numerical model, especially when used in conjunction with measured data, is a highly effective analytical tool.

In the current application, a general-purpose CFD code named PHOENICS, developed by CHAM Inc., is used to model the temperatures, pressures, and velocities in the SSME's High Pressure Fuel Turbopump (HPFTP) aft-platform seal cavity for a variety of boundary conditions and geometries. This cavity is located downstream of the fuel pump's second turbine disk, between the disk and the aft platform seal (Figs. 1 to 4). It is an annular cavity where 1400°R combustion products and 150°R coolant hydrogen mix in a complex flow pattern and then are vented into the pump's turbine exhaust. An understanding of the flow field in this cavity is critical since there are at least two known problems in the High Pressure Fuel Pump which may be linked to the environment in this region. Specifically, these problems are (1) cracking of the second stage turbine blade shanks, and (2) hot gas leakage into the stack behind the aft platform seal (Fig. 4). The first problem, blade cracking, can severely limit the time a pump can operate before it must be rebuilt. The second problem, that of hot gas leakage, is potentially more severe since, in the extreme, it may cause the pump to shut down prematurely if the temperatures or pressures in the coolant liner behind the aft-platform seal exceed certain redlines.

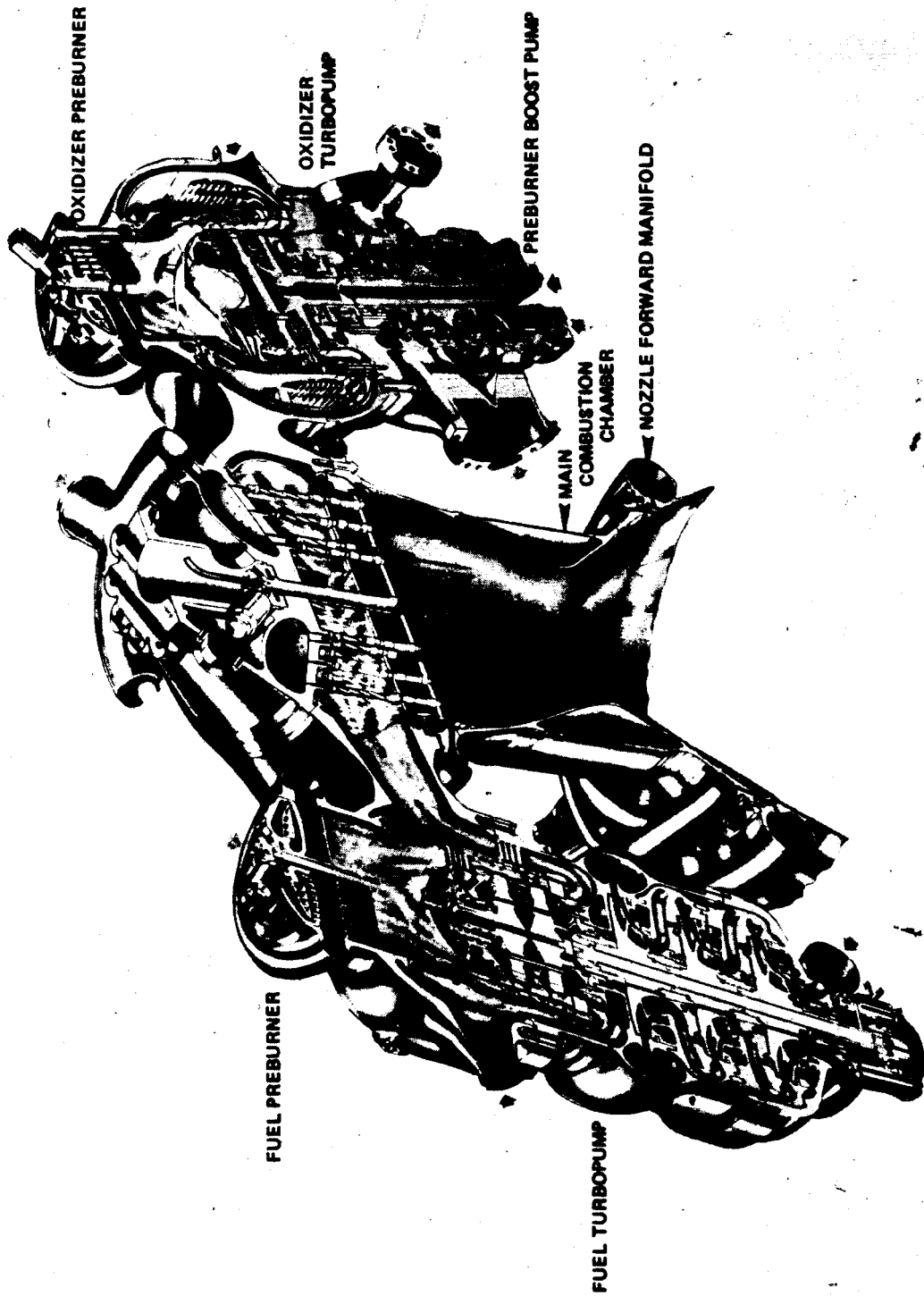
Accordingly, the primary purpose of the present analysis is to investigate the two problem areas mentioned above. In doing so, the study addresses the following questions:

- 1) How severe is the temperature gradient in the region where the turbine blades are cracking?
- 2) What would be the temperature of any fluid which leaked from the cavity into the coolant liner?

The analysis addresses these questions, not only for the pump operating under normal conditions, but also for a range of off-design conditions since even a slight departure from the norm might have a radical effect on the flow pattern and temperatures in the aft-platform seal cavity. As such, the broad objective of this study is to develop a model flexible enough that it can examine the effect that boundary parameters such as clearances, pressures, and flowrates have on the flow pattern and temperatures in the cavity. Such a model must be general enough that it can support future analytical and experimental investigations of the HPFTP aft-platform seal cavity.

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SSME POWERHEAD



968-90305



Figure 1. The Space Shuttle Main Engine.

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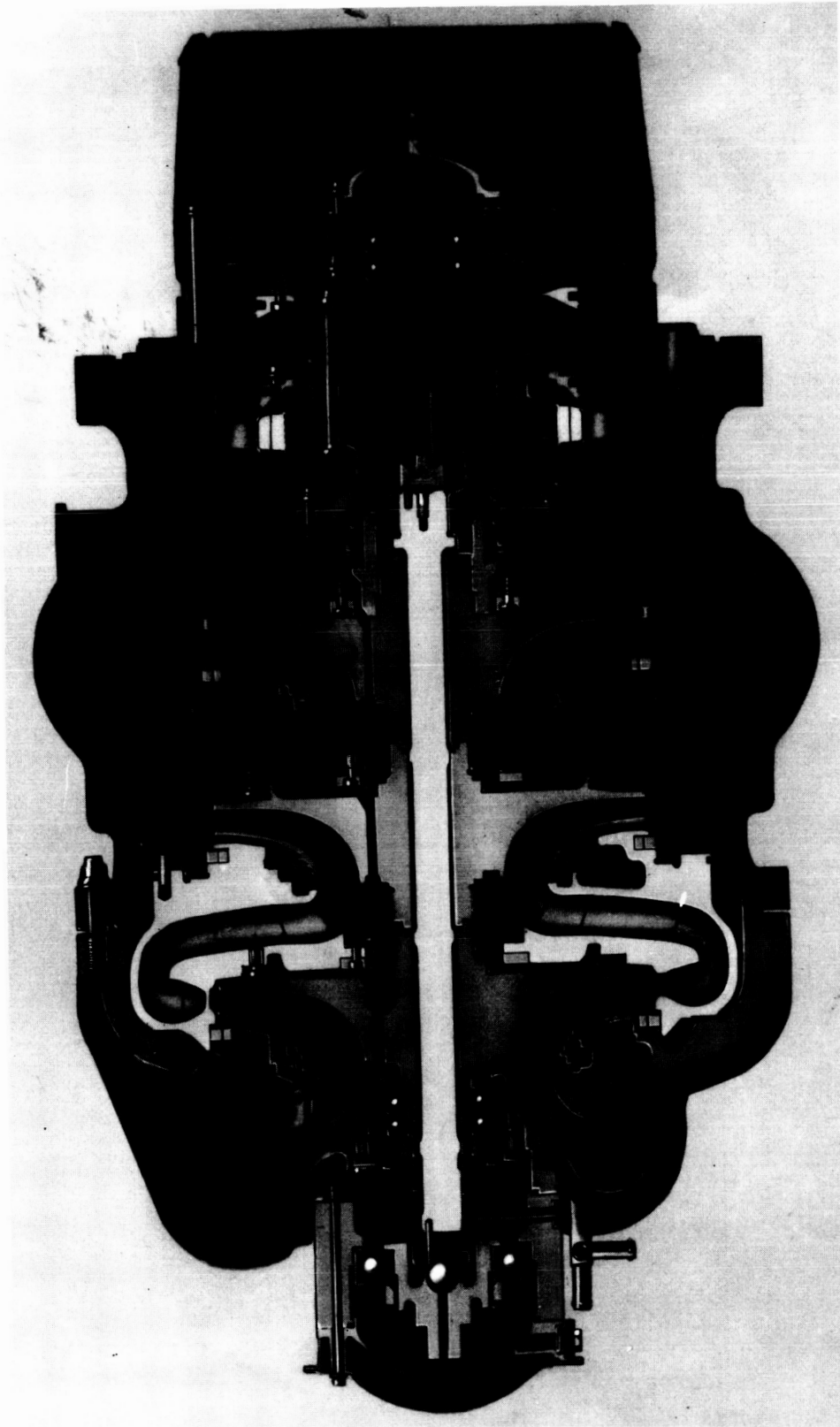


Figure 2. SSME High Pressure Fuel Turbopump.

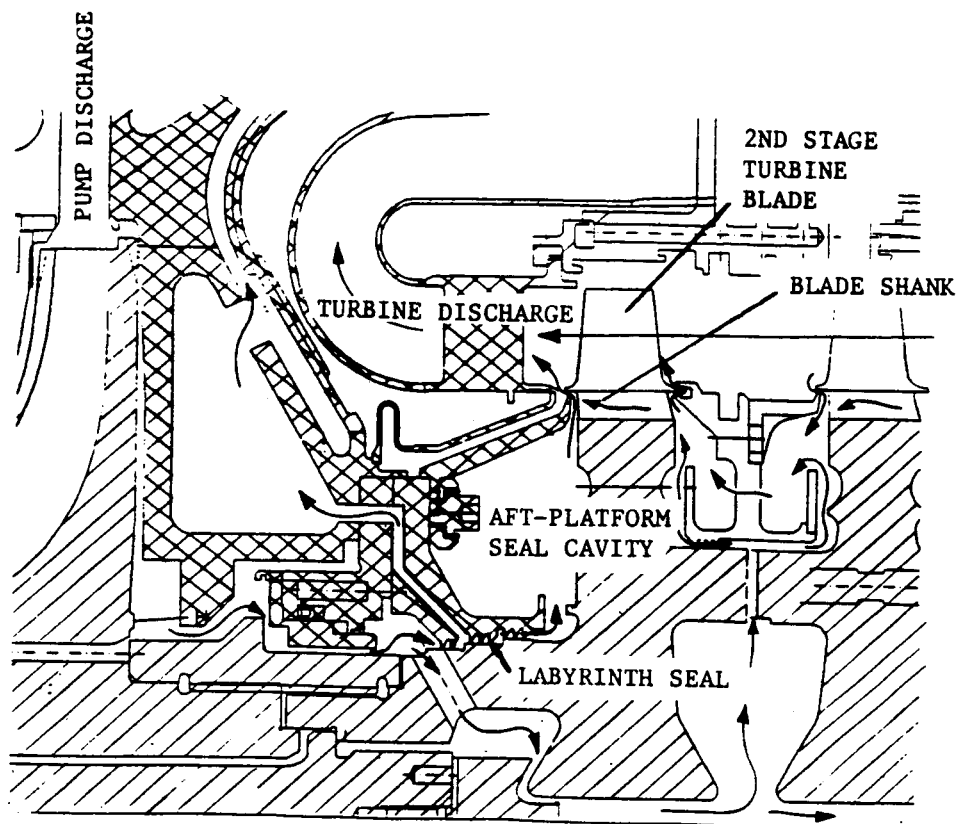


Figure 3. HPFTP turbine flow paths.

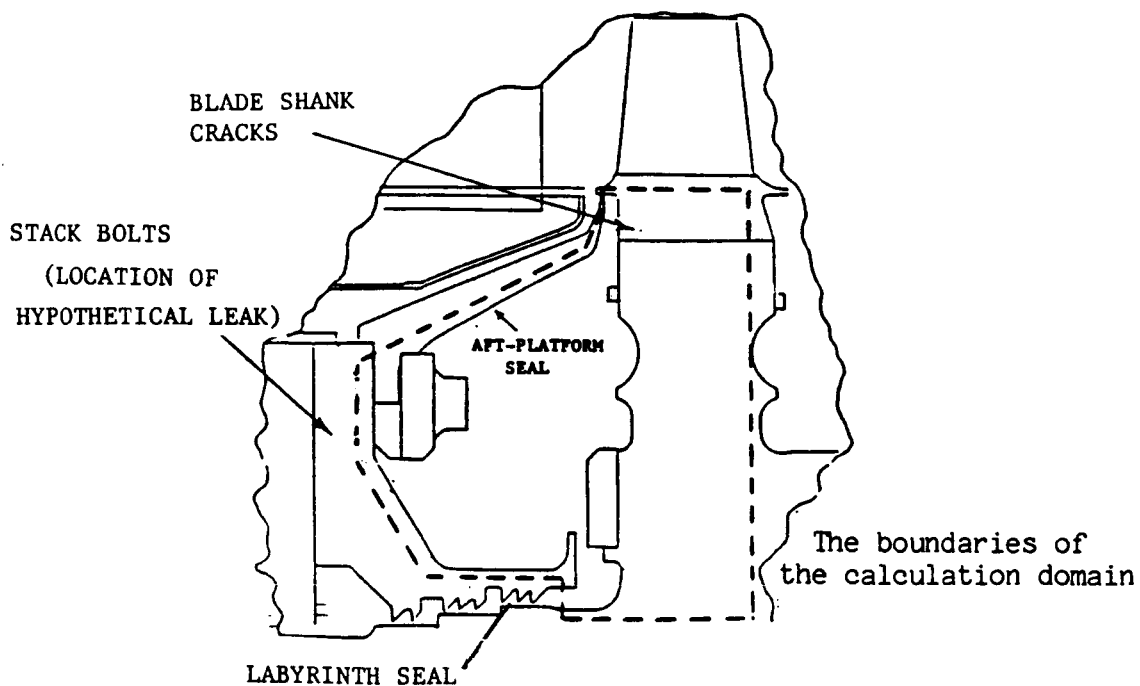


Figure 4. Aft-platform seal cavity.

II. PROBLEM DESCRIPTION

The region being modeled is the aft-platform seal cavity downstream of the second-stage turbine in the Space Shuttle's HPFTP. A close-up of the aft-platform seal cavity is provided in Figure 4. General views of the shuttle engine, the fuel pump, and the fuel pump turbine section are given in Figures 1 to 3. The dashed lines in the close-up view, Figure 4, represent the limits of the problem as specified in the model. The fluid properties and either the pressures or the flowrates at the boundaries must be input into the program. Unfortunately, the only available measurements of these parameters (i.e., temperature and pressure) are far removed from the inlets and exits of the aft-platform seal cavity. As such, the boundary conditions chosen as inputs rely heavily on an existing one-dimensional analysis of the HPFTP and must be used with caution [1].

Inspection of Figure 2, the HPFTP, will show that the aft-platform seal cavity is an axisymmetric annular cavity defined by stationary walls on one side and a rotating disk on the other. Flow enters the cavity through two inlets, one at the inner radius of the cavity and one near the outer radius of the disk. The flow leaves the region via the gap between the outer radius of the aft-platform seal and the blade lips. At high rpm (up to 37,000) the flow is a turbulent mixture of hydrogen and water at temperatures ranging from approximately 140°R to possibly as high as the turbine exhaust at 1700°R. Flowrates are on the order of 1 lbm/sec and pressures are in the range of 4000 psi.

The inlets and exits of the aft-platform seal cavity are described qualitatively below. The specific numbers used in this study, e.g., flowrates, pressures, etc., and the assumptions used in defining these numbers, can be found in the section on numerical model set-up.

A. Inlets

1. Coolant Inlets

At the inner radius of the cavity, approximately 0.3 lbm/sec of liquid hydrogen flows into the aft-platform seal cavity through a labyrinth seal. The source of this hydrogen is the coolant circuit which is fed by the discharge of the HPFTP (Fig. 3). In the two-dimensional model, this flowrate is calculated implicitly based on the pressure drop through the labyrinth seal. In the three-dimensional model, in the interest of computational economy, the coolant flowrate through the labyrinth seal is not calculated internally, but is simply set to the value predicted by the two-dimensional model operating with the same average clearances and flowrate through the blade shanks.

2. Hot Gas Inlet at the Blade Shanks

One wall of the aft-platform seal cavity is formed by the rotating disk upon which are mounted the second stage turbine blades. At the periphery of this disk, a mixture of coolant hydrogen and combustion products enters the cavity through the gap between the shank of one turbine blade and the next (Fig. 5). Since there are 58 blades in the second stage disk, there are, accordingly, 58 holes available for this hot gas mixture to flow through into the aft platform seal cavity from the high pressure side of the turbine disk. The flow pattern of the fluid entering through these holes is complex since the shanks of the blades are curved and the disk itself is rotating at up to 37,000 rpm.

In modeling this inlet, the 58 separate streams entering through the disk have been "smeared" in the circumferential direction into a single, continuous axisymmetric source. The flowrate and fluid properties at this inlet are prescribed based on predicted values, and the angular velocity of the fluid entering the cavity through these passages is assumed to have the same angular velocity as the disk.

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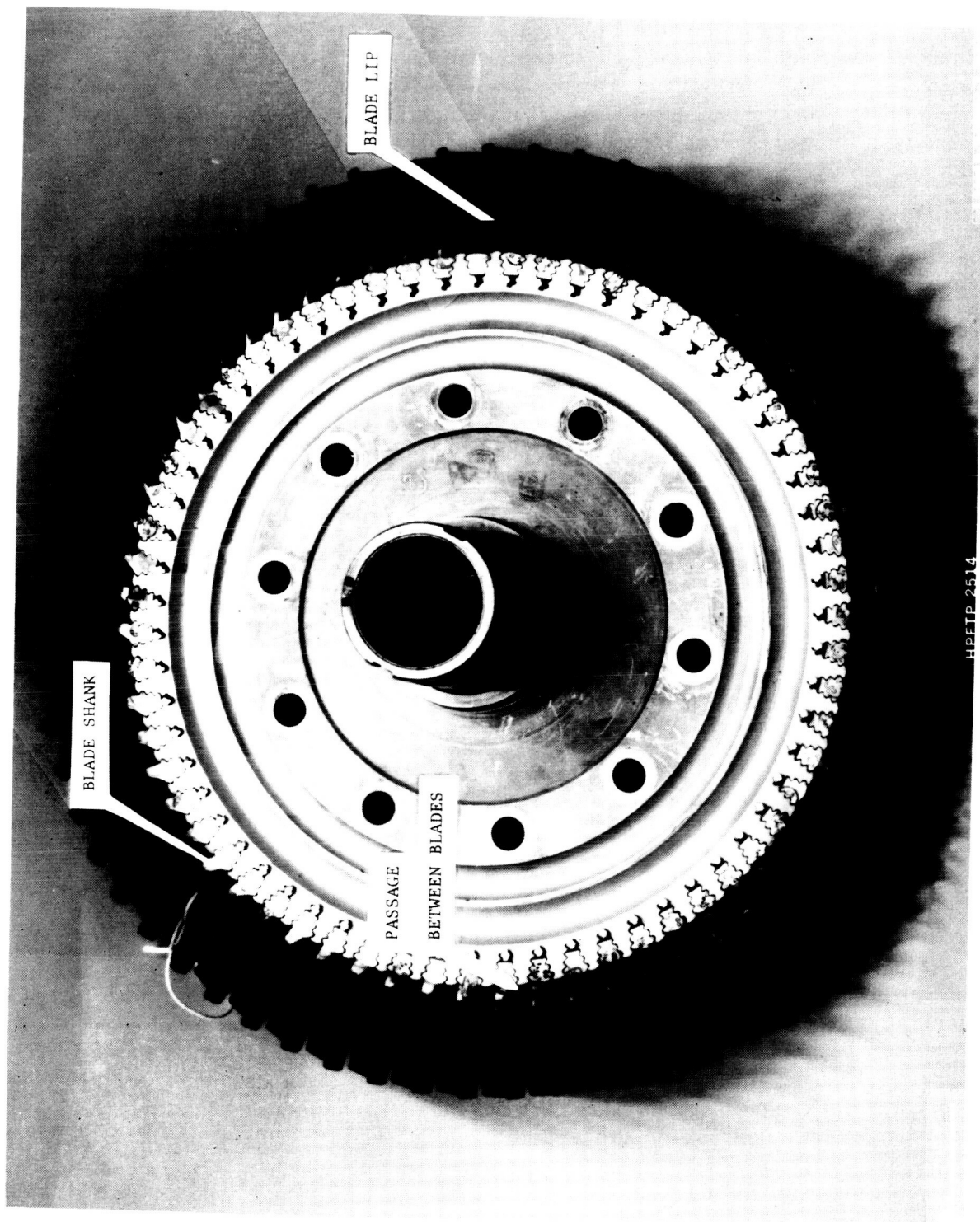


Figure 5. HPFTP second stage turbine disk with blades.

B. Exits

1. Exit Gap Between the Outer Diameter of the Aft-Platform Seal and the Blades

In this study, the single most important parameter which affects the flow pattern in the aft-platform seal cavity is the gap between the outer diameter of the aft platform seal and the lip of the turbine blades. This gap is very small, on the order of one hundredth of an inch, and it supports a high pressure drop of over 500 psi between the aft-platform seal cavity and the turbine exhaust. Any slight variation in this gap clearance will have a strong effect on the total flow and overall flow pattern in the cavity. In general, the actual flow exiting through this gap at a given location will respond to changes in the overall turbine discharge pressure, the circumferential variation in turbine discharge pressure, and any changes in the width of the gap. The latter could be due to a number of different causes, including: sideloads, dynamics, machining tolerances, eccentricity, or thermal expansion.

In the model, the exit pressure outside the gap is fixed at the best estimate for the turbine discharge pressure. The pressure drop across this exit is then related to the flowrate based on a loss coefficient times the local dynamic head.

2. Secondary Exit Hole

In one of the test runs discussed in this report, the aft-platform seal is modeled with a second exit in order to simulate a postulated leak. The leak was assumed to be around the bolts which secure the aft-platform seal to the lift-off seal stack (Fig. 4). The hole size, loss coefficient, and exit pressure of this second exit were chosen such that the resulting calculated flowrate would be approximately 0.2 lbm/sec. The leak rate of 0.2 lbm/sec was chosen because it is the maximum flowrate which could be leaking past the bolts. This last conclusion is based on experimental measurements of the pressure drops in the coolant liner cavity which is downstream of the postulated leak.

III. NUMERICAL MODEL SET-UP

CHAM Inc.'s general purpose computational fluid dynamics code, PHOENICS [2], has been employed for all the numerical studies described herein. To use PHOENICS, special purpose "satellite" and "ground station" sub-programs must be formulated whereby the built-in features can either be turned on or off or modified, as necessary. One set of the sub-programs adapted specifically for the HPFTP aft-platform seal cavity three-dimensional studies is listed, in full, in Appendix A. Full listings of the other adapted sub-programs used in this study are given in a separate CHAM report [3]. All of these sets of sub-programs are extensively annotated (via built-in "COMMENT" statements) so as to make them self-explanatory when read in conjunction with the PHOENICS User's Manual [4]. Consequently, no detailed line-by-line description is given here; however, the most relevant features are described below.

The two-dimensional calculations described herein have been performed by using the two-dimensional y/z, polar coordinate option of the code. Figure 6 shows the selected two-dimensional grid distribution. There are 1120 control cells, with 40 and 28 cells in the radial (IY) and (IZ) directions, respectively. Due to the (initially) assumed cyclic symmetry of the problem, only one control cell is required in the circumferential (IX) direction. However, to enable correct account to be taken of the wall shear stresses acting on the fluid entering between the blade shanks, the circumferential extent of the calculation domain is taken to be equal to the space between 2 consecutive blades (i.e., an angle of $1/58 \times 2\pi$ deg, where $58 = \text{total number of blades}$).

In the three-dimensional calculation, the full three-dimensional x/y/z coordinate capabilities of PHOENICS were employed. The identical y/z grid distribution of the 2-dimensional calculations was retained with, in addition, 8 cells in the circumferential (IX) direction, such that a total of $8 \times 40 \times 28 = 8960$ control cells is used.

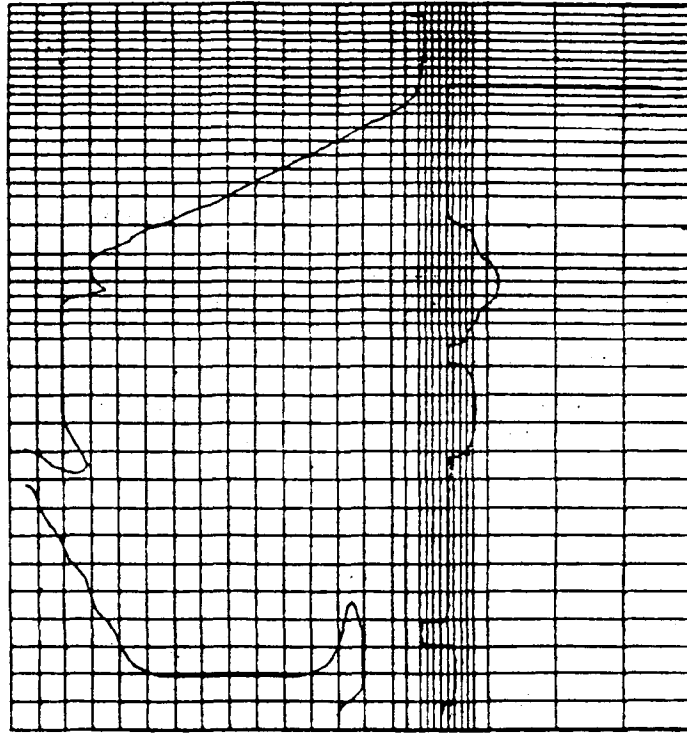


Figure 6. Computational grid.

As depicted in Figure 3, the “cold” liquid hydrogen coolant enters axially, through the labyrinth seal, at the inner radius of the cavity. This “cold” hydrogen then joins with the mixture of “hot” hydrogen and water that flows into the cavity from between the blade shanks located at the outer radius of the rotating disk. The combined streams of fluid then exit beneath the blade lips, as also shown in Figure 3.

A. Assumptions/Model Details

The major assumptions and salient features of the physical models and the boundary conditions employed are described below.

- 1) All boundary surfaces (both stationary and rotating) have been assumed to be adiabatic.
- 2) The hydrogen and water mixture are treated as a single homogeneous fluid with mixture properties (density and laminar viscosity) and temperature deduced from the calculated mixture enthalpy and specified hydrogen and water property curve fit data as described in Appendix B.
- 3) The turbulence effects are presented by way of the two-equation (k - ϵ) model of turbulence. In this model, two parameters, viz: the turbulence kinetic energy, k , and its dissipation rate, ϵ , are computed from differential transport equations. Thus, it has the capability of representing both the local and history effects. The effective viscosity is expressed as:

$$\mu_{\text{eff}} = \mu_{\text{L}} + C_{\mu} \rho k^2/\epsilon$$

where μ_l is the laminar viscosity, C_μ is an empirical constant and ρ is the local mixture density. In addition, four other empirical constants are assigned the values as recommended in original publications [4].

4) All boundary surfaces of irregular shape are accommodated in the present calculations by use of "cell porosities." In this approach, each control cell is characterized by a set of fractions, in the range from 0 to 1. These fractions determine the proportion of the cell volume which is available for flow from the cell to its neighbor in a given direction. This practice is much more rigorous and accurate than the practice of using rectangular steps.

5) The wall shear stress is calculated by using the conventional wall functions which are based on the assumption of the logarithmic law of the wall. For partially blocked control cells, the wall stress is calculated for the projected surfaces parallel to the velocity components.

It should be noted that the PHOENICS (1981 version) built-in process for determining wall shear stress is restricted to a finite number of special regions, to be set via the satellite subroutine. For the complex aft-platform seal geometry, many such special regions would be necessary, in excess of the built-in maximum, and a special PHOENICS user subroutine program was written for the current problem to overcome this restriction. This user sub-program (GWALL) performs the identical job as the built-in PHOENICS "WALL" subroutine but is used via the PHOENICS ground station. A listing of GWALL is included in Appendix A.

6) In PHOENICS, an iterative finite-difference solution procedure is employed to solve the governing differential equations together with the above mentioned relations. The method is based on a fully implicit, conservative formulation. As a result there is no restriction on the selection of the grid and the magnitude of the time steps.

The variables calculated and/or solved for (and printed) in the seal cavity flow calculation include the following:

- a. The fluid velocities in the 3 coordinate directions
- b. The mixture enthalpy and deduced temperature
- c. The (mass) concentration of water vapor
- d. The turbulent kinetic energy and its dissipation rate
- e. The static and total pressures
- f. The mixture density and separate densities of both the hydrogen and water
- g. The effective viscosity.

7) Boundary conditions are:

a. Prescribed mass flowrate, velocities, enthalpy, mixture ratio, and turbulence parameters at all inlets except for the two-dimensional solutions, in which case the flowrate through the labyrinth seal was computed based on a prescribed inlet pressure.

b. Prescribed exit pressure at all outlets, with the pressure drop related to the flowrate based on a specified loss coefficient times the dynamic head.

c. The incoming fluid enclosed between the blade shanks is assumed to rotate at the same speed as the adjacent disk surface.

8) The (phase change) freezing of the water is not accounted for; any water at temperatures below freezing is given the properties (density, etc.) of liquid water at freezing.

9) The effects of viscous heating have been ignored.

IV. TWO-DIMENSIONAL TEST RUNS

Three different two-dimensional test cases were run. The first of these was considered to be the basecase using the best estimate of the average conditions for the pump operating at the full power level (FPL). A second test run was made with a reduced amount of coolant entering through the labyrinth seal in order to determine the sensitivity of the solution to the ratio of hot gas flowing in at the blades relative to the hydrogen entering at the labyrinth seal. Finally, a third two-dimensional test run was made in order to see what effect a postulated leak through the stack bolts would have on the calculated cavity temperatures and flows. These three test runs and results are described in more detail below.

A. Two-Dimensional Test Runs: Boundary Conditions

1. Basecase 2-D

The basecase two-dimensional run uses boundary conditions and operating clearances taken from a one-dimensional flow analysis provided by Lockheed, Inc. [1]. These boundary conditions are tabulated in Table 1. It should be noted that for this particular run, the boundary condition specified at the labyrinth seal is that of a prescribed pressure boundary from which the flowrate is then deduced based on the following relationship [5]:

$$\text{MASSFLOW} = \text{FC} * \text{AREA} * \text{SQRT} \left(\left(\text{RHO} * \text{P0} \left(1 - \left(\text{PN} / \text{P0} \right) ** 2 \right) \right) / \left(\text{NUMBER OF TEETH} + \text{ALOG} \left(\text{P0} / \text{PN} \right) \right) \right)$$

WHERE P0 = UPSTREAM PRESSURE; PN = DOWNSTREAM PRESSURE; FC = FLOW COEFF.

(Note that for the basecase test run, the above equation when coupled with the PHOENICS two-dimensional model predicts a slightly lower flowrate through the labyrinth seal (0.26 lbm/sec versus 0.36 lbm/sec) as compared to the Lockheed one-dimensional model predictions.)

2. Reduced Coolant (Labyrinth) Flow

In the second run, the basecase two-dimensional model was modified by reducing the clearance at the outer diameter of the aft-platform seal while leaving all the other boundary conditions, including the hot gas flowrate, the same. When the gap size is reduced, the pressure in the cavity goes up and the coolant through the labyrinth seal decreases. The purpose here was to determine the effect that a reduction in coolant flow would have on the temperature field in the cavity.

3. Leak Through the Stack Bolts

The final two-dimensional run of the current study simulated a 0.2 lbm/sec leak through the stack bolts. The boundary conditions for this run were the same as the basecase but with a "hole" at the location shown in Figure 4. The loss coefficient at this hole and the hole size were chosen such that they dictated a leak rate of approximately 0.2 lbm/sec.

TABLE 1. TWO-DIMENSIONAL BOUNDARY CONDITIONS

<u>Variable</u>	<u>Basecase</u>	<u>Reduced Coolant</u>	<u>Leak</u>
Rotational speed of the disk (RPM)	37,000	37,000	37,000
Gap size at the labyrinth seal (in.)	0.1069	0.1069	0.1069
Total flow area (360°) between the blade shanks (in. ²)	3.877	3.877	3.877
Clearance between the aft-platform seal and blades (in.)	0.0108	0.0102	0.0108
Loss coefficient at the exit near the blade shanks	1.5	1.5	1.5
Enthalpy of the H ₂ upstream of the labyrinth seal (Btu/lbm) (Resultant calculated temperature – degrees Rankine)	278.3 (145°R)	278.3 (145°R)	278.3 (145°R)
Enthalpy of H ₂ and H ₂ O entering through the blades (Btu/lbm) (Resultant calculated temperature – degrees Rankine)	3558 (1466°R)	3558 (1466°R)	3558 (1466°R)
Density of the H ₂ upstream of the labyrinth seal (lbm/ft ³)	3.574	3.574	3.574
Density of H ₂ and H ₂ O entering through the blades (lbm/ft ³)	0.931	0.931	0.931
Mass flowrate of H ₂ and H ₂ O entering past the blades (lbm/s)	3.649	3.649	3.649
Mass fraction of H ₂ O entering through the blades	0.474	0.474	0.474
Pressure at the turbine discharge (psi)	3582	3582	3582
Pressure at the labyrinth seal inlet (psi)	4254	4254	4254
Loss coefficient for the second (leak) exit	1.5	1.5	1.5
Total flow area at the second (leak) exit (in. ²)	0	0	0.00019

B. Two-Dimensional Test Runs: Results and Observations

1. Basecase

According to the model, when the HPFTP is operating at full power, centrifugal force dominates the flow field and pressure field in the aft-platform seal cavity. This is not surprising when one considers that at 37,000 rpm and a radius of 4.5 in., the hot gas exits the blade shanks with a centrifugal force equal to approximately 175,000 g's. Figures 7 and 8 show that there is virtually no penetration of the hot gas down into the aft-platform seal cavity and, as a result, the temperature in the cavity remains cold, at approximately 375°R (-85°F). The flow pattern in the main cavity consists of two large co-rotating vortices which maintain the cavity at a relatively uniform temperature. The liquid hydrogen which enters through the labyrinth seal at the inner radius of the cavity flows radially outward along the face of the disk and then abruptly merges with the hot fluid stream exiting from between the shanks. While it appears from the drawing that the cold flow then recirculates, in fact all of the coolant which enters through the labyrinth seal must, by continuity, mix and then exit with the hot stream, resulting in the sharp temperature gradient at the blade shanks especially evident in the close-up view provided in Figure 8. The actual local gradients that the blade shanks would see would be more severe than predicted here since, in the model, the hot gas flow is treated as an axisymmetric source which would tend to smooth out the temperature gradients at the trailing edge of the blade shanks. In reality, there are 58 blades shanks between which the hot gas flows into the cavity. The cold fluid which is slung off the disk, up behind the trailing edge of the blade shanks, will be sheltered from the hot flow entering from between the blade shanks. As a result, the local mixing of hot and cold fluid will be delayed, and the local temperature gradient will be even more severe than shown here.

2. Reduced Coolant (Labyrinth) Flow

During the course of the study the question was raised as to what would happen if the proportion of coolant to hot gas flow were different than that predicted by the one-dimensional model used to define the boundary conditions [1]. In order to answer this question, the boundary conditions in the model are manipulated in a somewhat contrived manner in order to change the proportion of hot gas flow to coolant flow, viz: the coolant flowrate is reduced by slightly reducing the clearance between the aft-platform seal and the blade lips. The result is that a reduction of only six ten-thousandths of an inch (6 percent) of this clearance reduces the coolant flow by over half. This change, however, has little effect on the flow field in the cavity. As with the basecase, the flow in the cavity remains dominated by the centrifugal force. As shown in Figures 9 and 10, the temperature in the cavity has risen by only approximately 150 deg, up to 525°R, which is a moderate increase when compared with the hot gas inlet temperature of 1466°R. The conclusion is that the flow field and temperature field of the aft-platform seal cavity is relatively insensitive to the amount of coolant entering at the labyrinth seal relative to the amount of hot gas mixture entering through the blade shanks. However, the pressure and coolant flowrate are extremely sensitive to the exit clearance at the outer diameter of the aft-platform seal for a fixed hot gas inlet flow.

3. Leak Through the Stack Bolts

For the third two-dimensional test run, a "hole" is simulated underneath the bolts which secure the lift-off stack. The rationale behind such a study is that a flow leaking past these bolts into the coolant liner might be one explanation for the erratic temperatures and pressures sometimes recorded in the coolant liner. The exit area and loss coefficient at this hole are adjusted so that the calculated leakage rate is 0.2 lbm/sec. The flowrate of 0.2 lbm/sec comes from the best estimate of the upper limit of what the leak rate could be, based on the known temperature and pressure measurements in the liner [6].

Figures 11 and 12 show that a leak of 0.2 lbm/sec through the stack bolts does not dramatically change the flow field or temperature field as compared with the no-leak, baseline case. The temperature of the main cavity and the fluid leaking out past the bolts remains relatively unchanged at around 375°R (-85°F).

BASECASE

DSK 2D BC

2-D SOLUTION

O.D. GAP =
.0109"

EXIT PRESSURE = 3558 PSI

FLOWRATE THROUGH THE BLADE SHANKS = 3.65 lbm/s

RESULTANT LABYRINTH FLOWRATE = .26 lbm/s

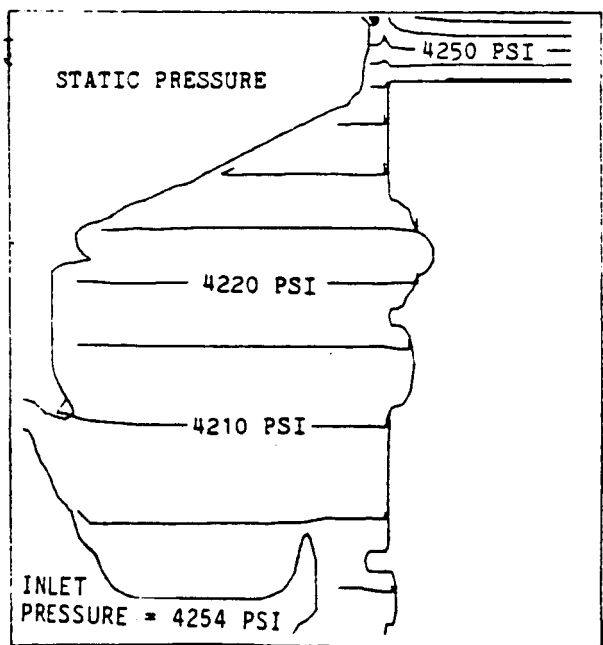
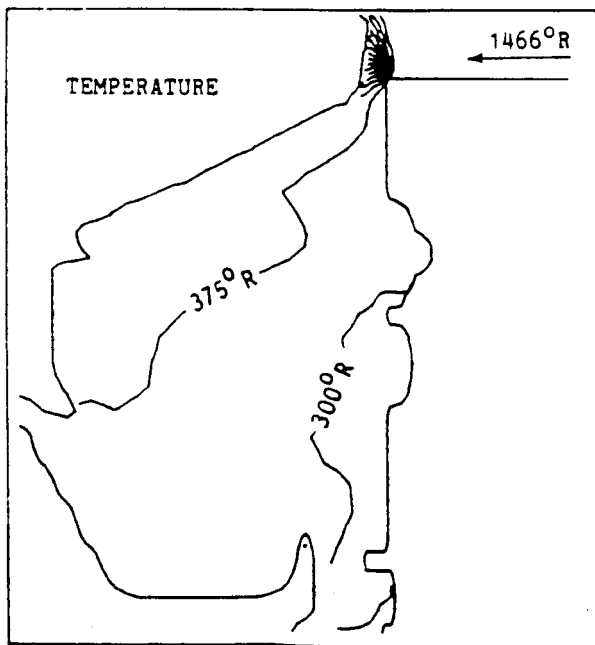
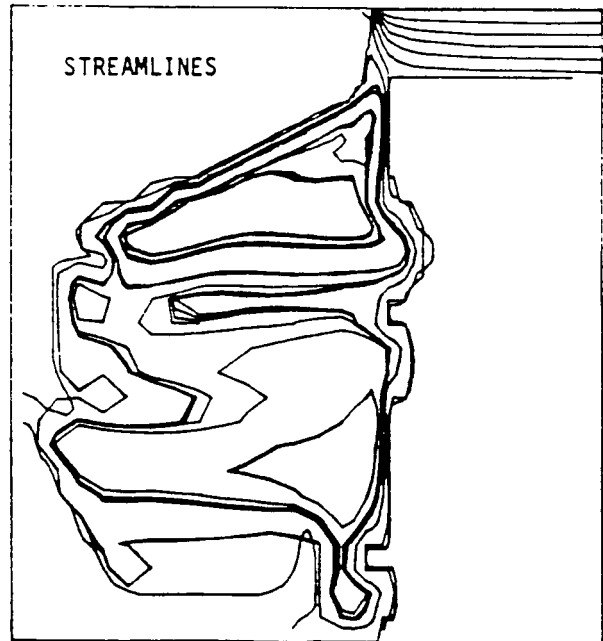
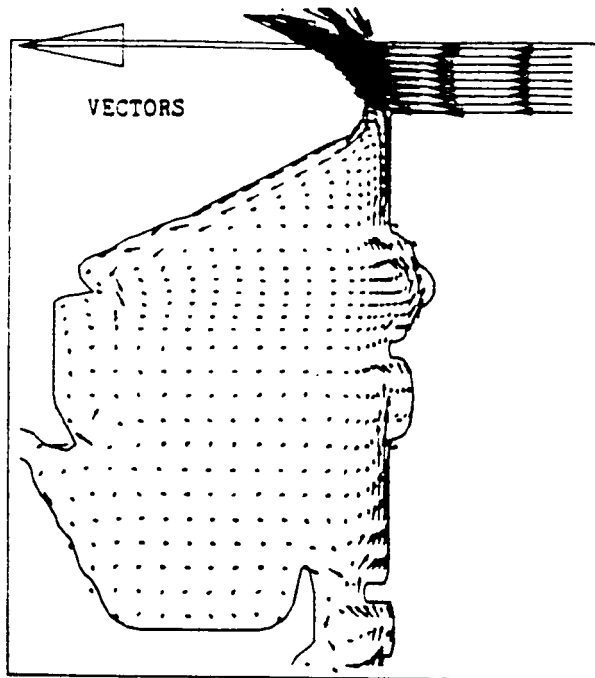


Figure 7. Two-dimensional basecase results.

BASECASE
 DSK 2D BC
 2-D SOLUTION

 O.D. GAP =
 .0108"

 EXIT PRESSURE = 3558 PSI
 FLOWRATE THROUGH THE BLADE SHANKS = 3.65 lbm/s
 RESULTANT LABYRINTH FLOWRATE = .26 lbm/s

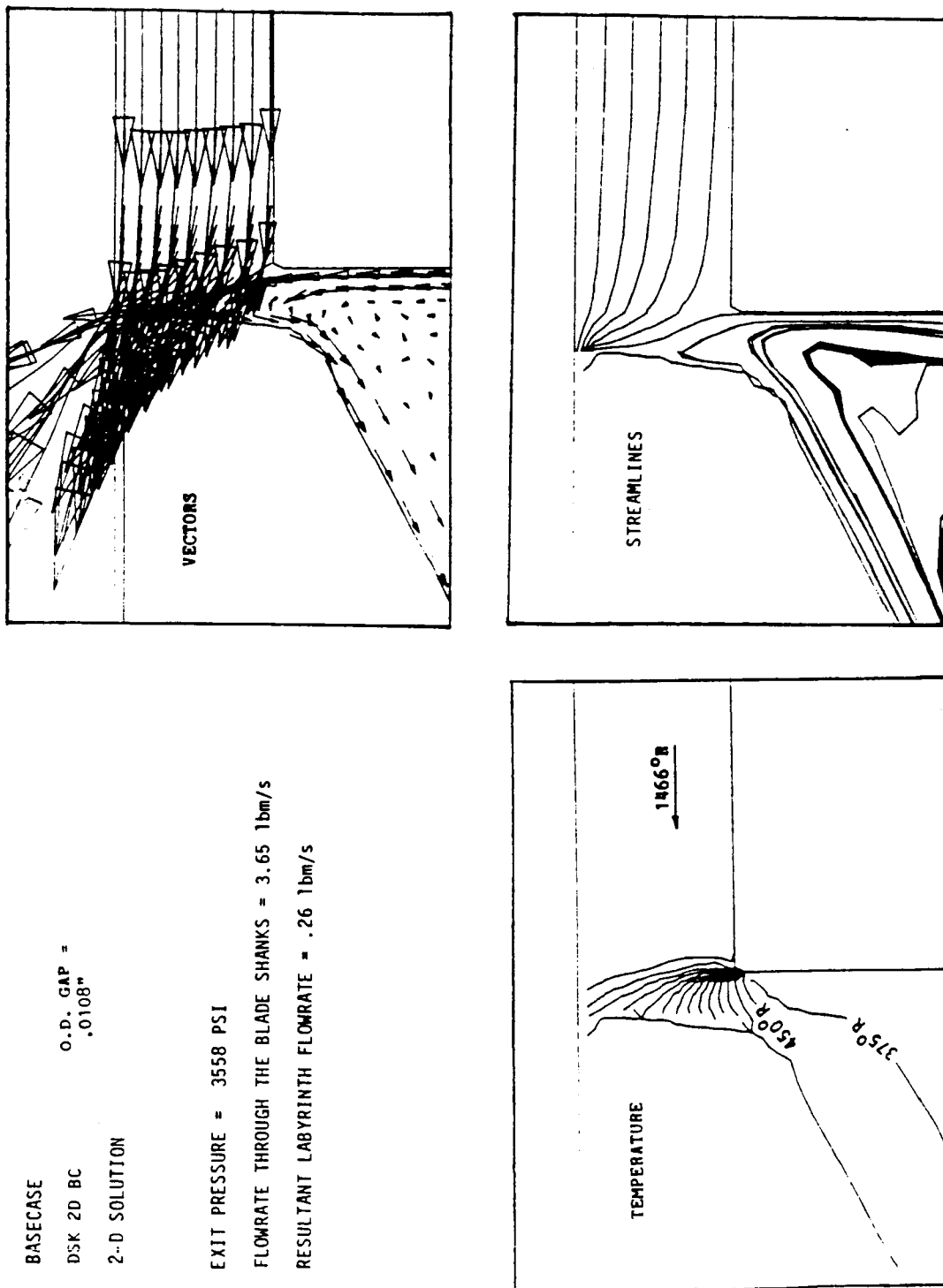


Figure 8. Two-dimensional basecase results, expanded view.

DSK 2D B

O.D. GAP = .0102"

2-D SOLUTION

(.0108" - .0006")

EXIT PRESSURE = 3558 PSI

FLOWRATE THROUGH THE BLADE SHANKS = 3.65 lbm/s

RESULTANT LABYRINTH FLOWRATE = .12 lbm/s

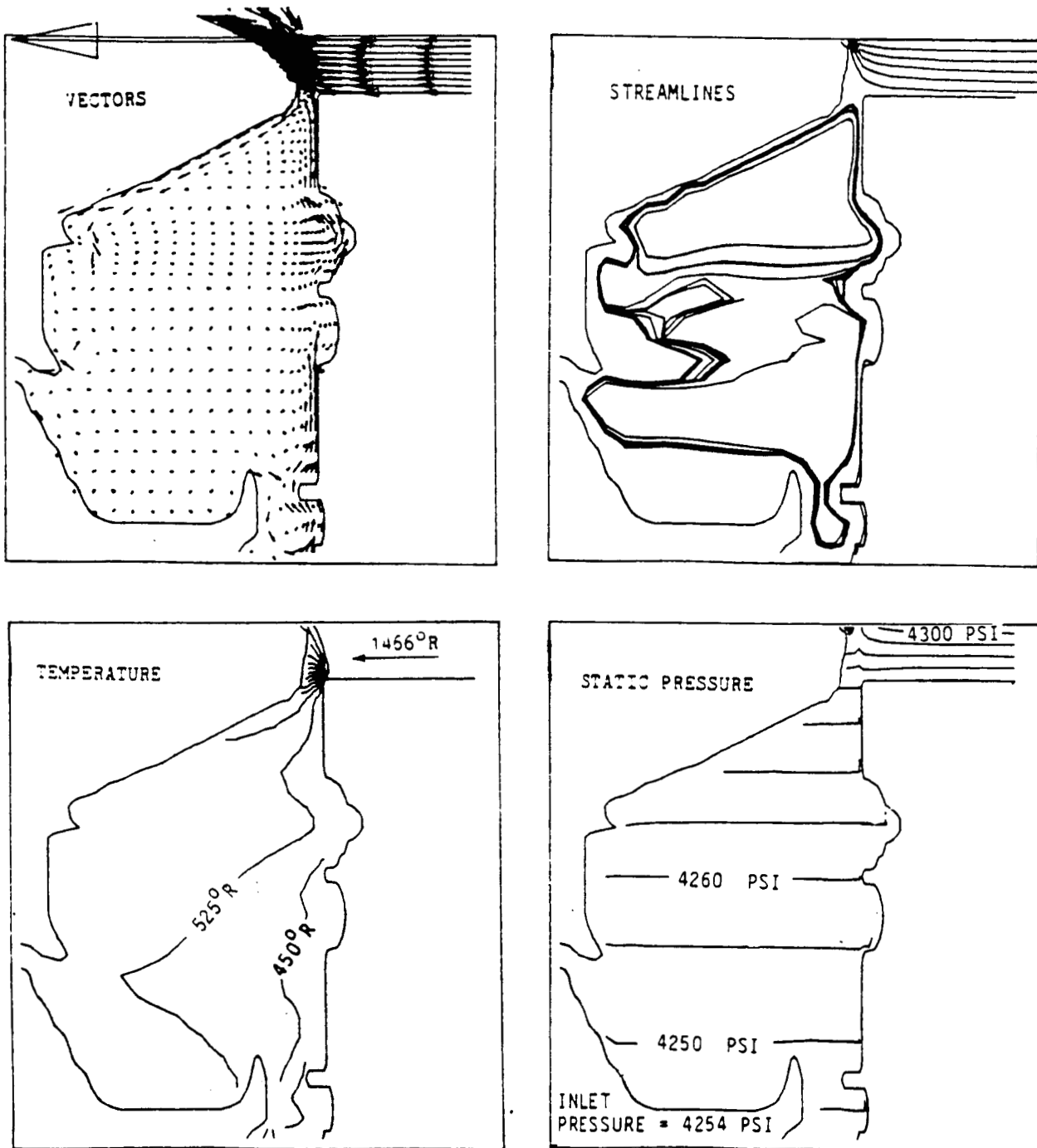


Figure 9. Two-dimensional reduced coolant flow results.

DSK 2D B

O.D. GAP = .0102"

EXIT PRESSURE = 3558 PSI

2-D SOLUTION

(.0108" - .0006")

FLOWRATE THROUGH THE BLADE SHANKS = 3.65 lbm/s

RESULTANT LABYRINTH FLOWRATE = .12 lbm/s

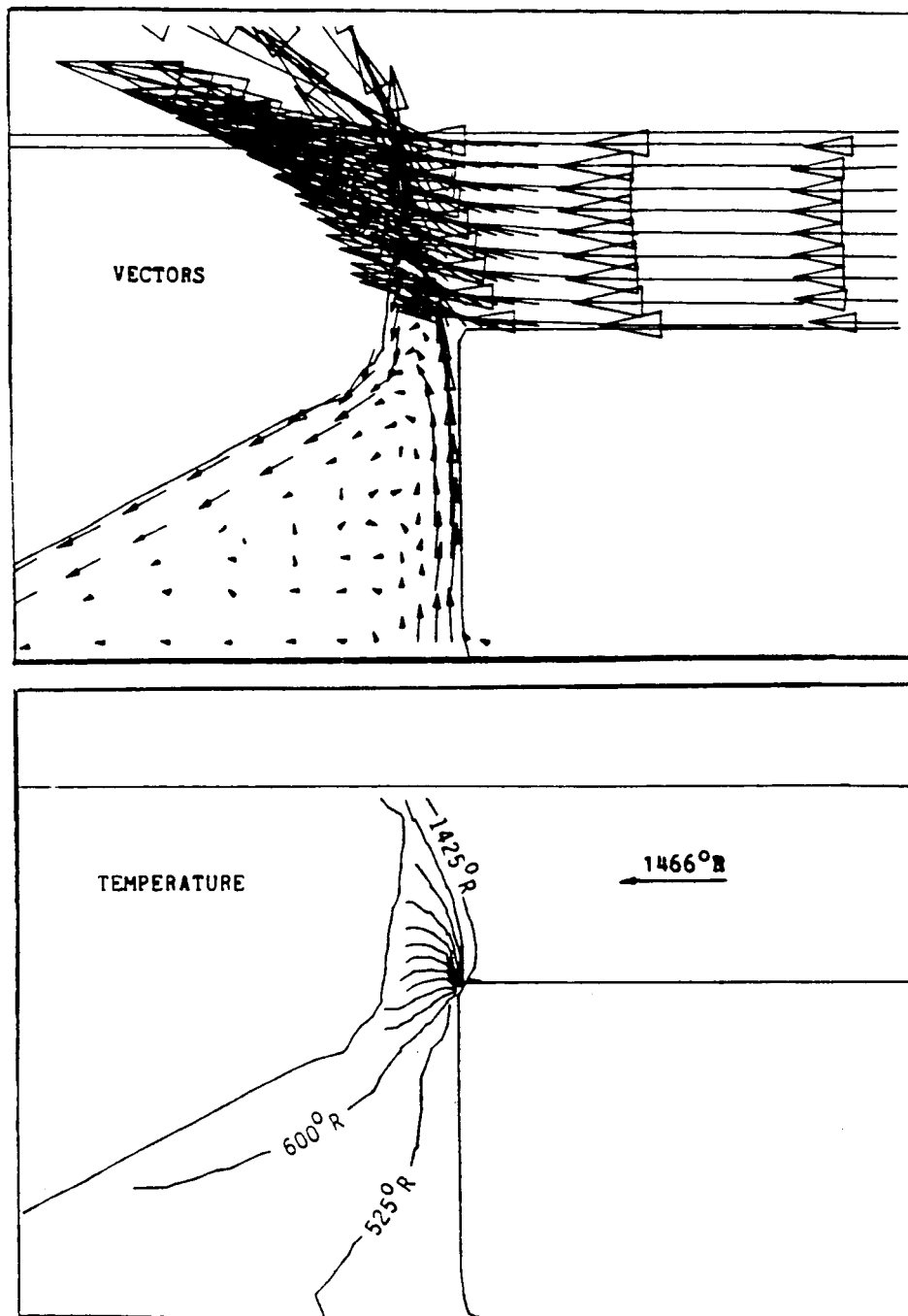


Figure 10. Two-dimensional reduced coolant flow, expanded view.

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SECOND EXIT

DSK 2D 2H

2-D SOLUTION

O.D. GAP =
.0108"

EXIT PRESSURE = 3558 PSI

FLOWRATE THROUGH THE BLADE SHANKS = 3.65 lbm/s

RESULTANT LABYRINTH FLOWRATE = .34 lbm/s

SECOND EXIT HOLE FLOWRATE = .20 lbm/s

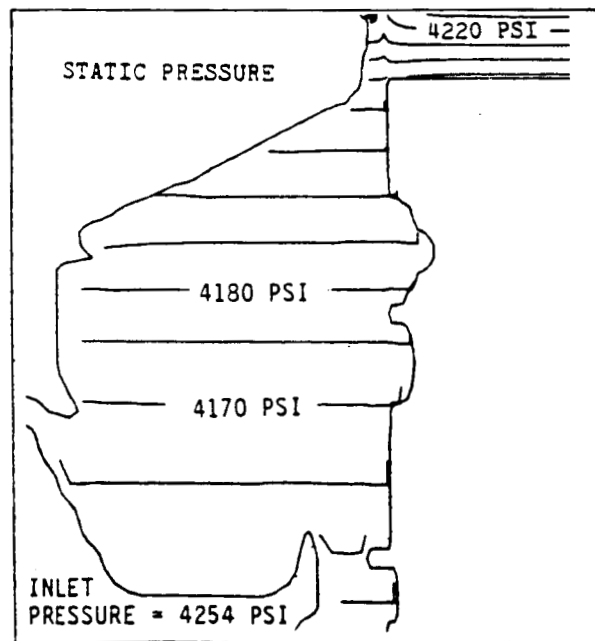
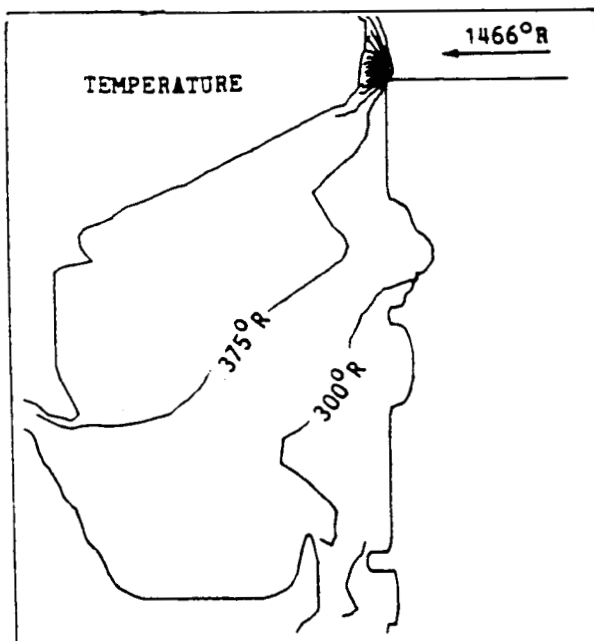
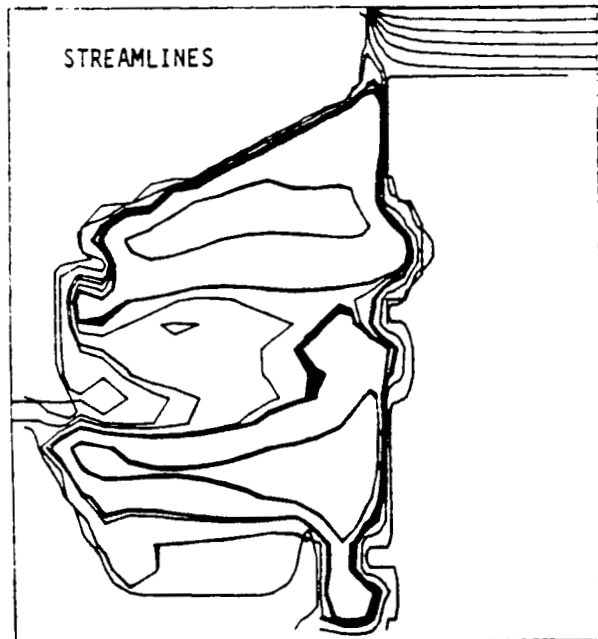
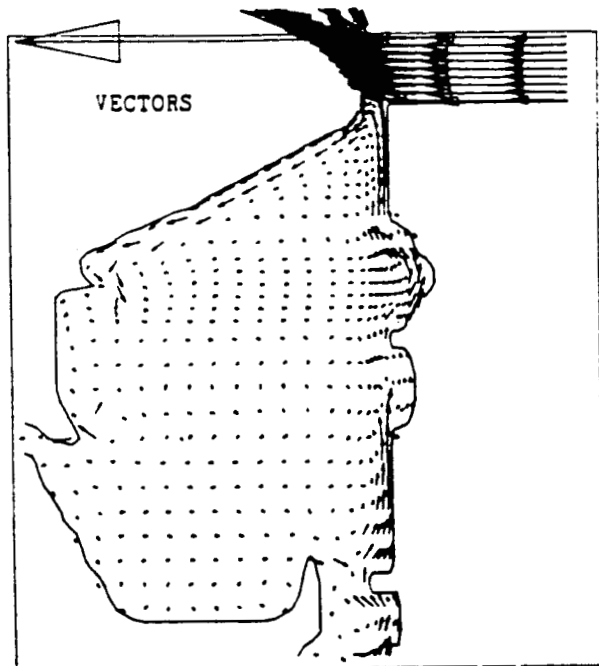


Figure 11. Two-dimensional 0.2 lbm/s leak flow results.

SECOND EXIT
DSK 2D 211
2-D SOLUTION

O.D. GAP =
.0158"

EXIT PRESSURE = 3558 PSI
FLOWRATE THROUGH THE BLADE SHANKS = 3.65 lbm/s
RESULTANT LABYRINTH FLOWRATE = .34 lbm/s
SECOND EXIT HOLE FLOWRATE = .20 lbm/s

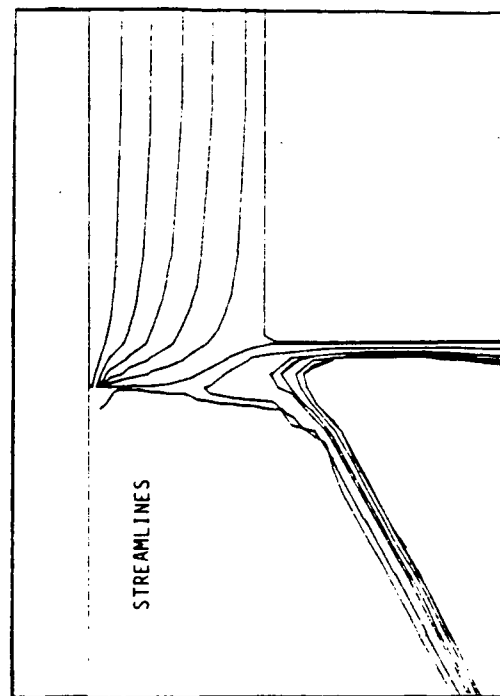
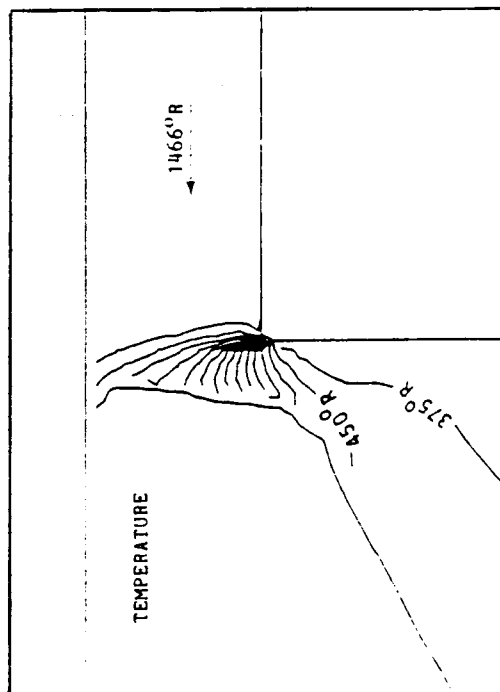
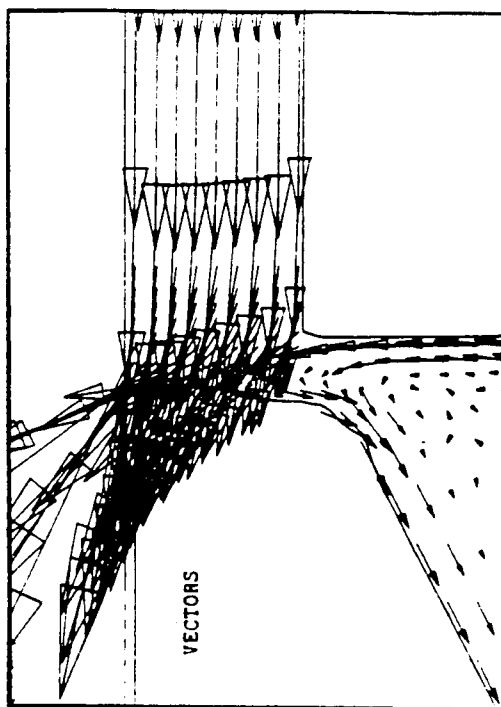


Figure 12. Two-dimensional 0.2 lbm/s leak flow, expanded view.

C. Convergence Characteristics and Computer Time

Numerical solutions of flows involving rotating boundaries are notoriously slow to converge for a variety of reasons (not to be discussed here) and so it was deemed essential that careful checks be made to ensure that the PHOENICS solutions being obtained were meaningful. Thus, before the two-dimensional production runs described above were fully completed, a series of test calculations were performed to ensure that the solutions were converged to an acceptable degree. To this end, various runs were made for the basecase setup with different initial guess/starting solutions that were quite extensive. The results of these investigations are presented and discussed in Appendix C. As shown in the latter, the PHOENICS solutions are clearly converging to an identical solution in each case, as should (and must) be expected.

As depicted in Appendix C, the two-dimensional basecase was run for a total of 500 sweeps, at which time all calculated monitor flow variables had settled to an acceptable degree (Figs. C-1 to C-8). All the other 2-dimensional runs reported here were restarted from this basecase solution (i.e., the initial fields for the starting of the iterative calculation procedure were taken to be the basecase solution, rather than some simple initial guess) and then run on until, again, the solution monitor values were suitably settled. This usually required another 150 to 200 sweeps, at most. Computer times for these restart runs were approximately 35 CPU minutes on CHAM's Perkin Elmer 3251 mini-computer.

All the 3-dimensional calculations described in the next section were also restarted from the 2-dimensional basecase solution which was symmetrically duplicated in the circumferential IX-direction. Again, converged solutions then took approximately 150 to 200 more sweeps and required approximately 5 CPU hours of computer time on the Perkin-Elmer 3251 machine.

V. THREE-DIMENSIONAL TEST RUNS

The disadvantage of the preceding axisymmetric analysis is that, by definition, it does not include the three-dimensional effects either known or suspected to exist in the pump. One of the most important of these asymmetries left unaccounted for by the two-dimensional analysis is the circumferential variation in pressure which has been measured downstream of the exit of the fuel turbine. This exit pressure serves as one of the boundary pressures which regulates the flow in the aft-platform seal cavity. In addition to this known pressure variation, there may be variations in clearances or other parameters which could radically alter the flow pattern in the cavity. As such, a three-dimensional model is an essential tool for a proper study of this cavity. As a starting point, three different three-dimensional cases were run and are presented here. The first is the basecase which uses the same set of flowrates, fluid properties, and clearances as used in the two-dimensional basecase. The only difference between the two is that the three-dimensional basecase also includes a prescribed asymmetrical turbine exit pressure based on pressure measurements taken during a full scale test of the shuttle engine. The second three-dimensional case was set-up to simulate a 0.003 in. shift in the rotor position with a corresponding change in the clearance at the labyrinth seal and at the exit gap between the aft-platform seal and the blade lip. This shift is relative to the average labyrinth seal clearance of 0.003 in. and the average exit gap of 0.0108 in. The last three-dimensional run presented here simulates a relatively large eccentricity of the aft-platform seal alone, such that the exit clearance is skewed to one side by 0.0081 in., which is 75 percent of its average clearance.

A. Three-Dimensional Test Runs: Boundary Conditions

1. Basecase (Geometrically Axisymmetric with Asymmetric Exit Pressures)

As its boundary conditions, the basecase three-dimensional run uses the same operating clearances, flowrates, pressures, mixture ratios, and enthalpies, etc., as used by the two-dimensional basecase analysis. The

only exception is that the exit pressure of the turbine is no longer uniform but varies circumferentially based on data taken during Rocketdyne's engine test 902-279 [7]. These boundary conditions are the best estimate of the operating conditions in the fuel pump at full power (109 percent). The specific numbers used for this run, and for the subsequent three-dimensional runs, are listed in Table 2.

2. Eccentric Rotor (Rotor Shift of 0.003 in.)

The Eccentric Rotor (0.003 in.) case was set up to simulate the effect that a rotor shift of 0.003 in. would have on the flow field in the cavity. The shift of 0.003 in. was chosen because it is an upper limit on the distance the rotor can shift before the shaft starts rubbing against the labyrinth seal. Such a rotor shift in a given direction would open up the exit clearance between the aft-platform seal and the blade lips, while at the same time it would close down the clearance at the labyrinth seal. This effect is simulated in the model by, on the one hand, directly adjusting the clearances at the outer diameter of the aft-platform seal and, on the other, by adjusting the flow rate at the labyrinth seal. All the other inputs remain the same as for the three-dimensional basecase.

TABLE 2. THREE-DIMENSIONAL BOUNDARY CONDITIONS

Variable	Basecase	Rotor Eccentricity = 0.003 in.	Aft-Platform Eccentricity = 0.0081 in.
Rotational speed of the disk (RPM)	37,000	37,000	37,000
Flowrate at the labyrinth seal (lbm/sec)			
1:00	0.0323	0.0095	0.0323
2:30	0.0323	0.0323	0.0323
4:00	0.0323	0.0551	0.0323
5:30	0.0323	0.0646	0.0323
7:00	0.0323	0.0551	0.0323
8:30	0.0323	0.0323	0.0323
10:00	0.0323	0.0095	0.0323
11:30	0.0323	0.0000	0.0323
Total Mass Flowrate	0.258	0.258	0.258
Total flow area (360°) between the blade shanks (in. ²)	3.877	3.877	3.877
Clearance between the aft-platform seal and blades (in.)			
1:00	0.0108	0.0129	0.0165
2:30	0.0108	0.0108	0.0108
4:00	0.0108	0.0087	0.0051
5:30	0.0108	0.0078	0.0027
7:00	0.0108	0.0087	0.0051
8:30	0.0108	0.0108	0.0108
10:00	0.0108	0.0129	0.0165
11:30	0.0108	0.0138	0.1800
Total Area	0.307	0.307	0.307
Loss coefficient at the exit near the blade shanks	1.5	1.5	1.5
Enthalpy of the H ₂ entering at the labyrinth seal (Btu/lbm) (Resultant calculated temperature – degrees Rankine)	278.3 (145°R)	278.3 (145°R)	278.3 (145°R)
Enthalpy of H ₂ and H ₂ O entering through the blades (Btu/lbm) (Resultant calculated temperature – degrees Rankine)	3380 (1466°R)	3380 (1466°R)	2280 (1466°R)
Density of the H ₂ entering at the labyrinth seal (lbm/ft ³)	3.574	3.574	3.574
Density of H ₂ and H ₂ O entering through the blades (lbm/ft ³)	0.931	0.931	0.931
Mass flowrate of H ₂ and H ₂ O entering past the blades (lbm/s)	3.649	3.649	3.649
Mass fraction of H ₂ O entering through the blades	0.474	0.474	0.474
Pressure at the turbine discharge (psi)			
1:00	3451	3451	3451
2:30	3541	3541	3541
4:00	3697	3697	3697
5:30	3622	3622	3622
7:00	3606	3606	3606
8:30	3592	3592	3592
10:00	3476	3476	3476
11:30	3481	3481	3481
Average Exit Pressure	3558	3558	3558

3. Eccentric Aft-Platform Seal (Aft-Platform Seal Shift of 0.0081 in.)

The third three-dimensional test run models the flow field for a highly eccentric (75 percent) aft-platform seal. In this run the clearance at the gap between the aft-platform seal and the blade lips is adjusted so that it models what the gap would be if the aft-platform seal had moved laterally 0.0081 in. in the 11:30 direction. Note that the rotor itself has not moved but is still concentric with the labyrinth seal so that the gap between the labyrinth seal and the rotor axle remains at a uniform 0.003 in. (In general, the clocking positions used in this report correspond to the convention adopted by Rocketdyne in Reference 7, however, in this particular test run the decision to move the aft-platform seal in the 11:30 direction is arbitrary, and is based on convenience rather than any physical justification.) The choice of the magnitude of the eccentricity is also somewhat arbitrary but the reasoning behind the shift of 0.0081 in. was the desire to choose a large aft-platform eccentricity in order to observe extreme effects. An aft-platform shift of 0.0081 in. is 75 percent of the total aft-platform seal clearance.

B. Three-Dimensional Test Runs: Results and Observations

1. Basecase

A comparison of the three-dimensional basecase results (Figs. 13 to 21) with the two-dimensional basecase results (Figs. 7 and 8) shows that the addition of an asymmetric pressure distribution at the exit of the turbine has had little effect on the flow pattern in the aft-platform seal cavity. While some evidence of the influence of the external pressure distribution can be seen at the outer diameter of the disk near the blade shanks (e.g., Fig. 16), this effect is small; toward the center of the cavity the results are nearly identical to the two-dimensional solution. At the flowrates and small clearances of the aft-platform seal cavity running at full power, a circumferential pressure difference of 220 psi as modeled here represents only a fraction of the over 600 psi pressure drop between the aft-platform seal cavity and the turbine exhaust. As a result, the 220 psi circumferential variation on the outside of the cavity has little effect on the flow pattern inside. In addition, even with the circumferential variation in turbine exhaust pressure, the centrifugal force in the aft-platform seal cavity still dominates the flow such that the influence that is felt due to the pressure variation is confined to the periphery of the cavity. For an example of this effect, examine the lines of constant temperature given in the close-up view in Figure 17.

2. Eccentric Rotor (Rotor Shift of 0.003 in.)

Perhaps the most notable feature of the aft-platform seal cavity flow field (Figs. 22 to 30) with a 0.003 in. eccentric rotor is the small change as compared to the three-dimensional basecase with its centered rotor. Even with an eccentric rotor, the temperatures in the cavity have risen just 75°R, indicating only a slight increase in the heat transferred down into the cavity. Again, the only significant effect is felt at the outer diameter of the turbine disk where, at the 5:30 clock position, the hot gas actually flows down into the cavity causing a local hot spot. This hot spot will be felt by the blade shanks once per revolution, with a corresponding cooling in between. In general, therefore, a rotor shift of 0.003 in. results in a slight warming of the average cavity temperature, and a cyclical variation of temperature at the outer diameter of the disk of approximately 600°R.

3. Eccentric Aft-Platform Seal (Aft-Platform Seal Shift of 0.0081 in.)

Of the six different two-dimensional and three-dimensional test runs investigated during this study, the most dramatic results (Figs. 31 to 39) come from running the model with an aft-platform seal that has been shifted to one side by 3/4 of the exit clearance (i.e., by 0.0081 in.). With the exit gap substantially closed down on one side, the hot gas which would normally exit through that gap must, instead, exit at a different location. The centrifugal force

BASECASE

DSK 32 BC

3-D SOLUTION

ASYMMETRICAL

PRESSURE

VECTORS

SIDE VIEW

SYMMETRICAL

GAP (= .0108")

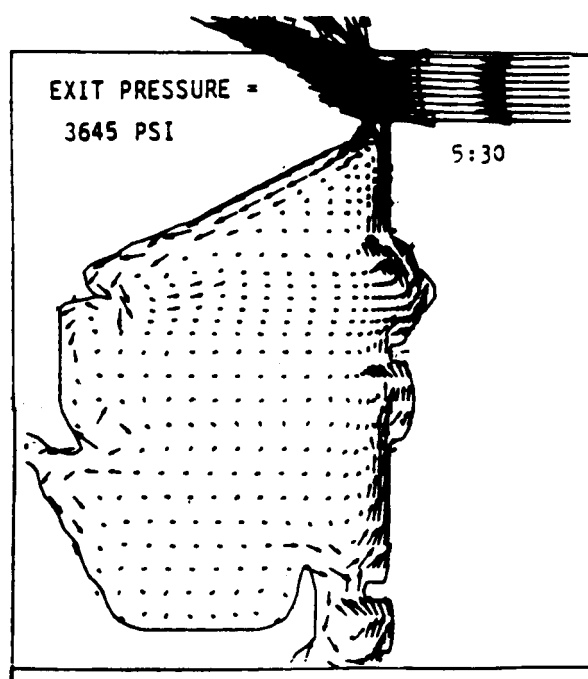
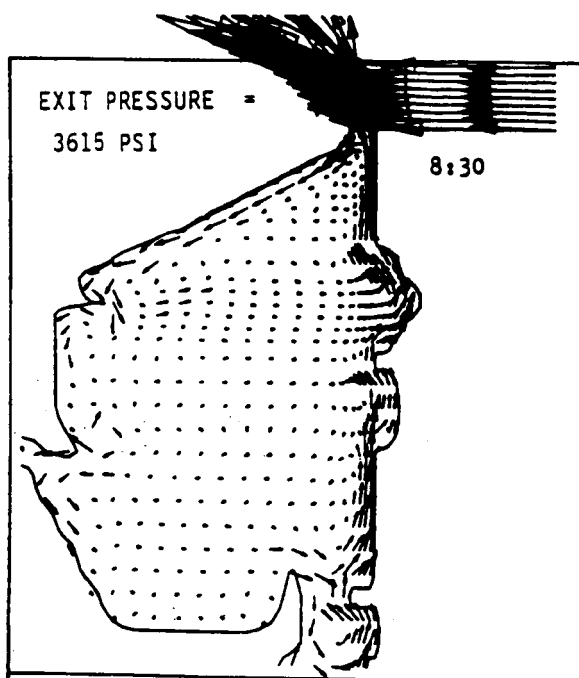
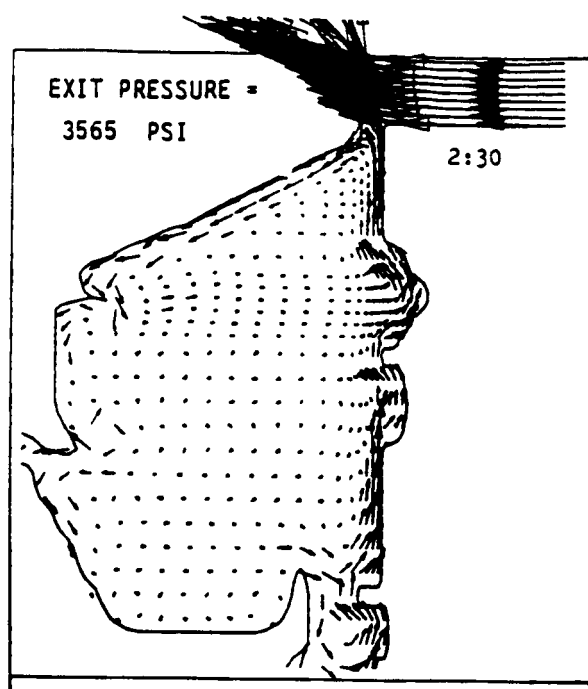
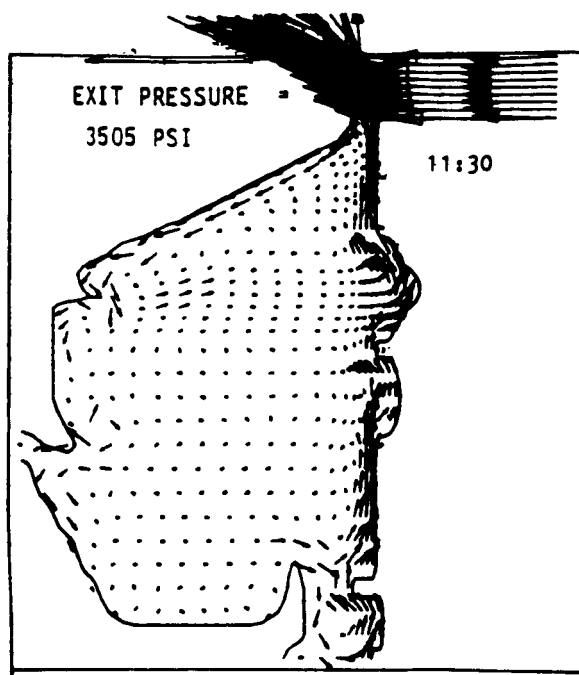


Figure 13. Three-dimensional basecase results: vectors.

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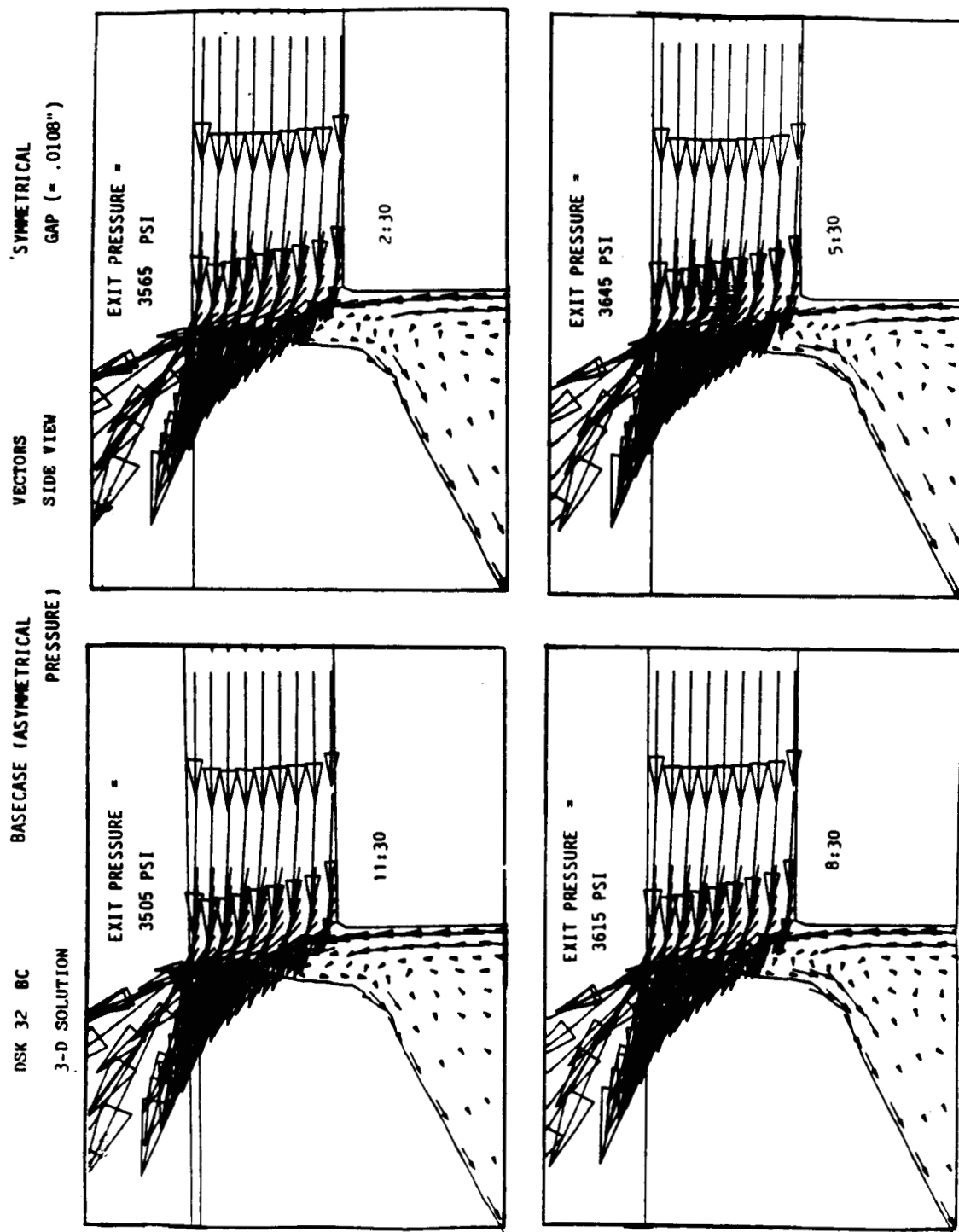


Figure 14. Three-dimensional basecase results: vectors (close-up).

BASECASE

DSK 32 8C

3-D SOLUTION

ASYMMETRICAL

EXIT PRESSURE

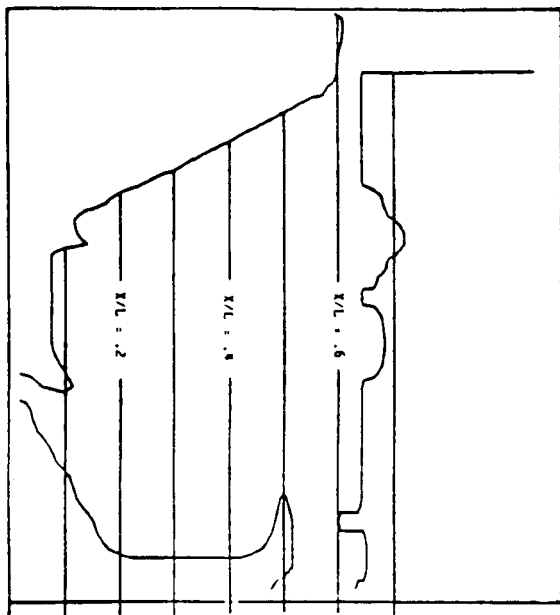
VECTORS

END VIEW

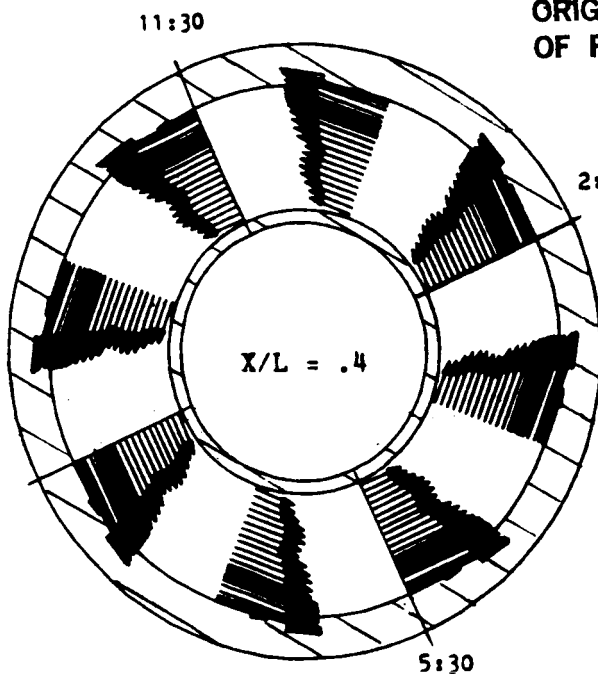
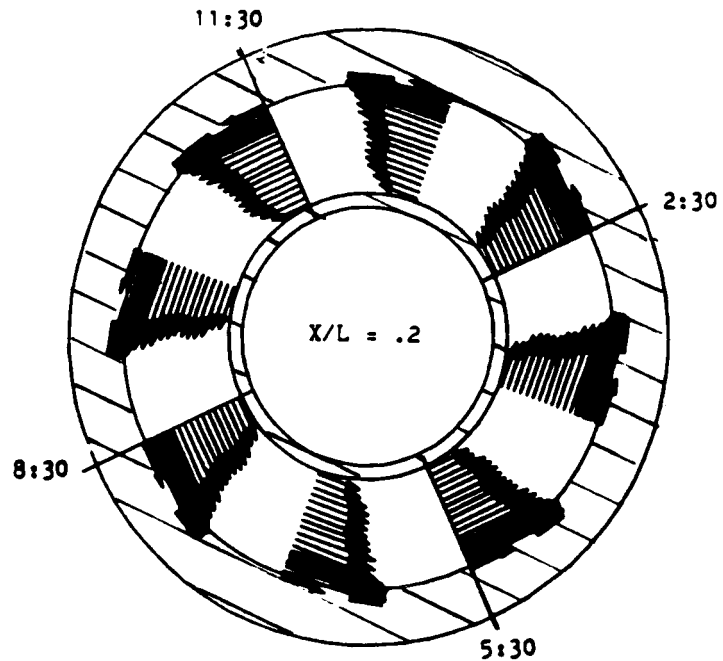
(FROM THE TURBINE END)

SYMMETRICAL

GAP (= .0108")



CROSS SECTIONS USED IN END VIEW



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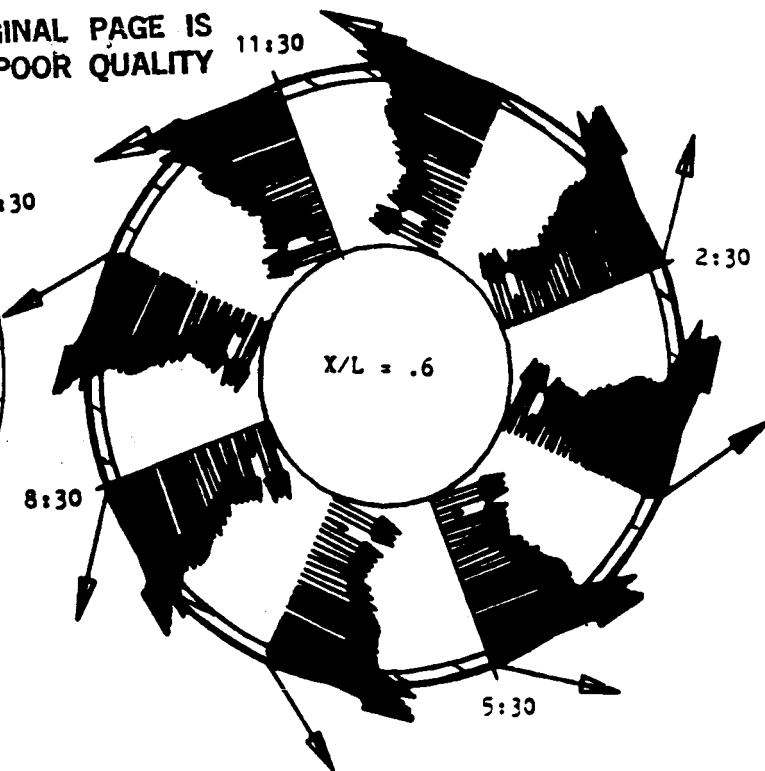


Figure 15. Three-dimensional basecase results: vectors (end view).

BASECASE

DSK 32 BC

3-D SOLUTION

ASYMMETRICAL

PRESSURE

TEMPERATURE

SIDE VIEW

SYMMETRICAL

GAP (= .0108")

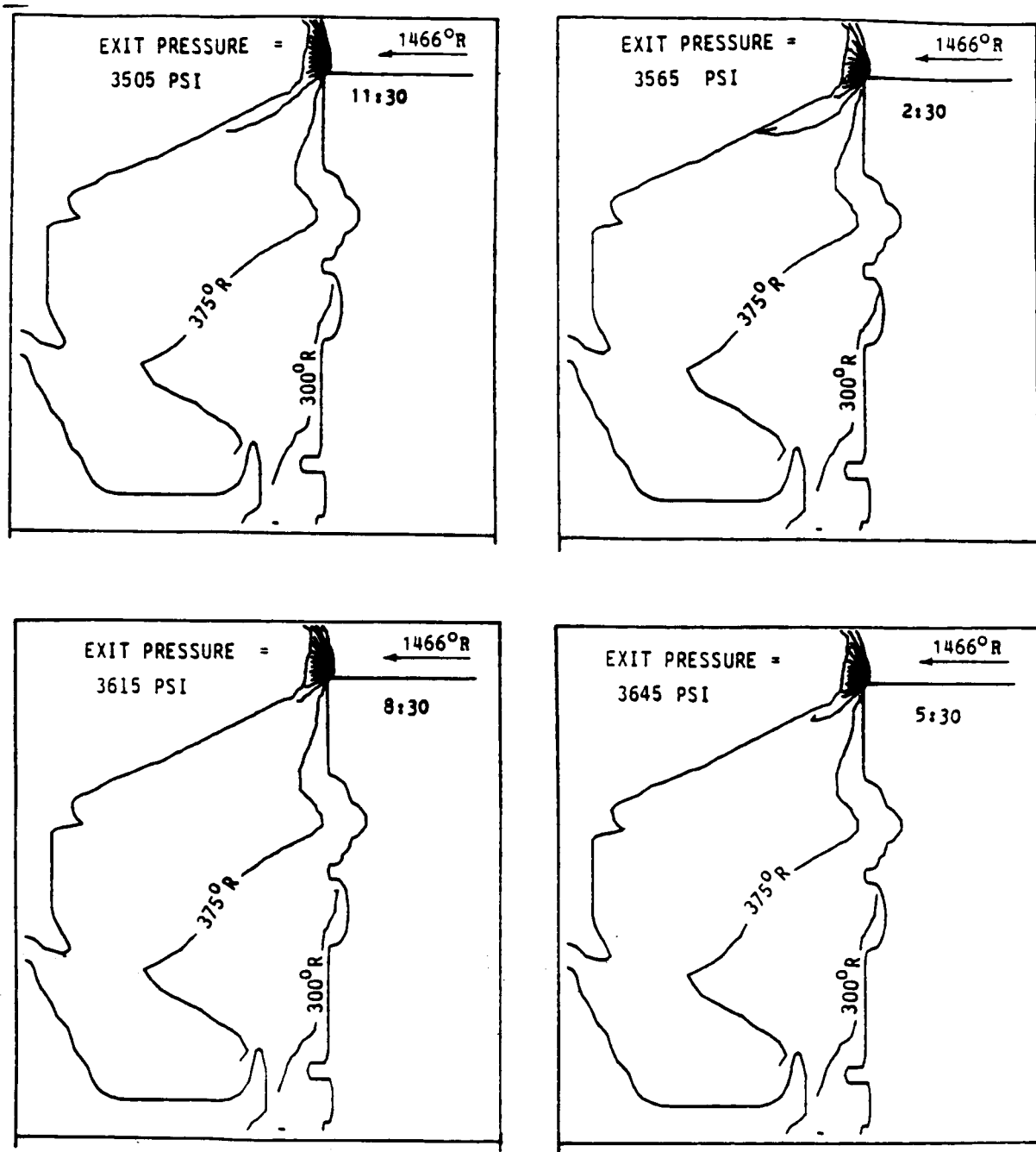


Figure 16. Three-dimensional basecase results: temperature.

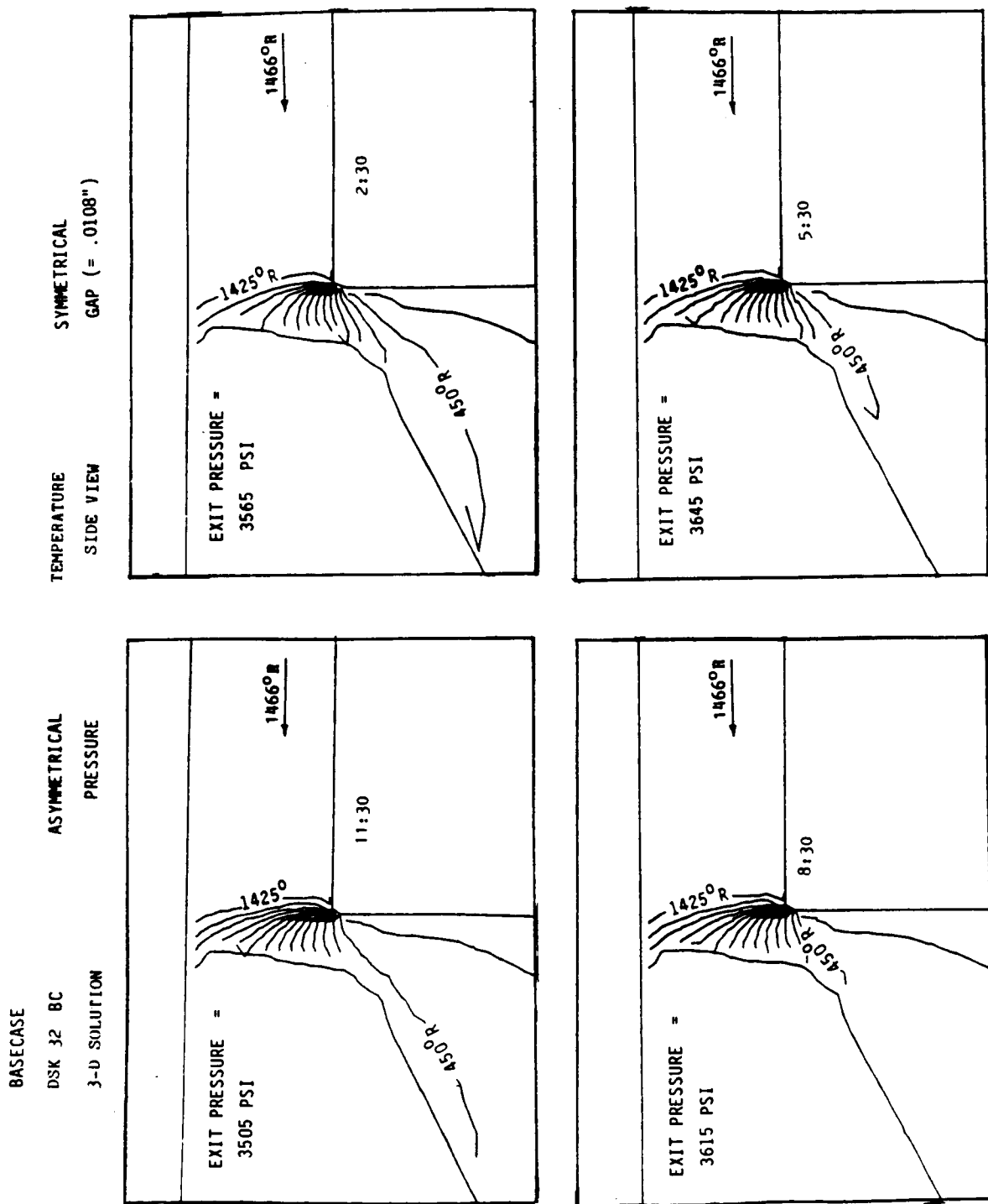


Figure 17. Three-dimensional basecase results: temperature (close-up).

BASECASE

DSK 32 BC

3-D SOLUTION

ASYMMETRICAL

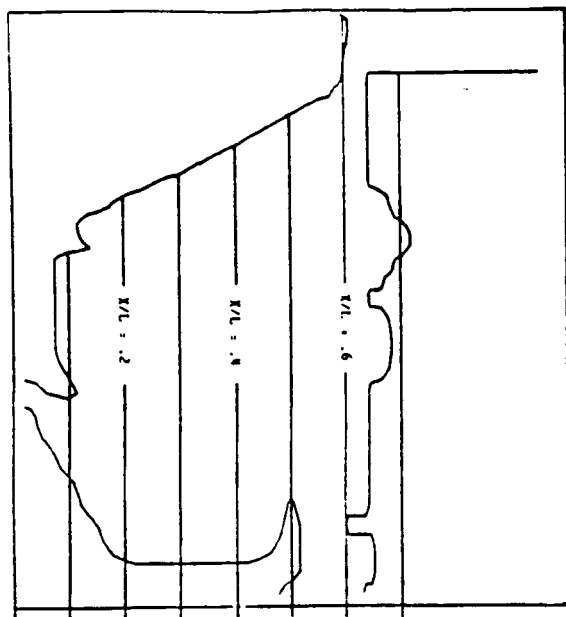
PRESSURE

TEMPERATURE

END VIEW

SYMMETRICAL

GAP (= .0108")



CROSS SECTIONS USED IN END VIEW

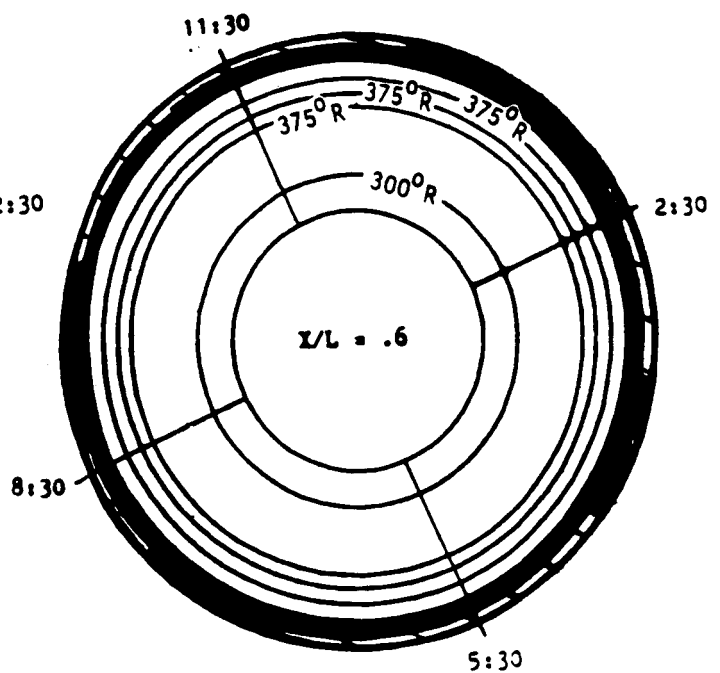
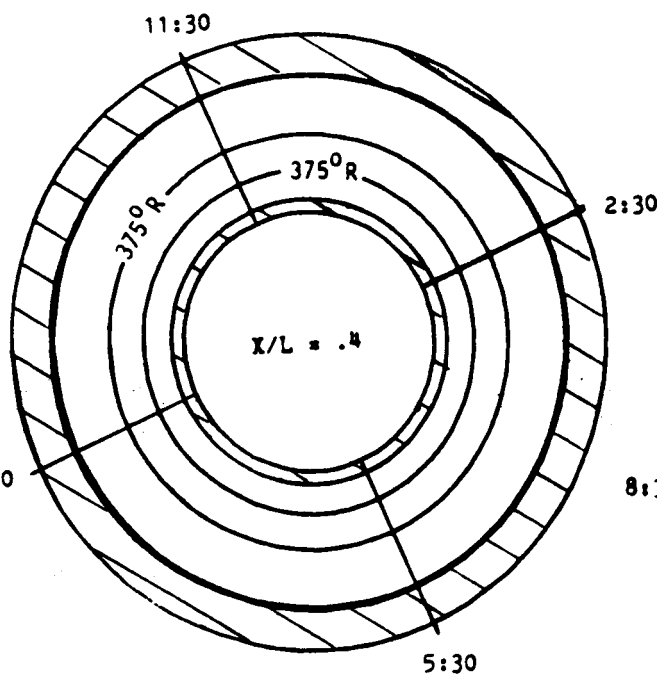
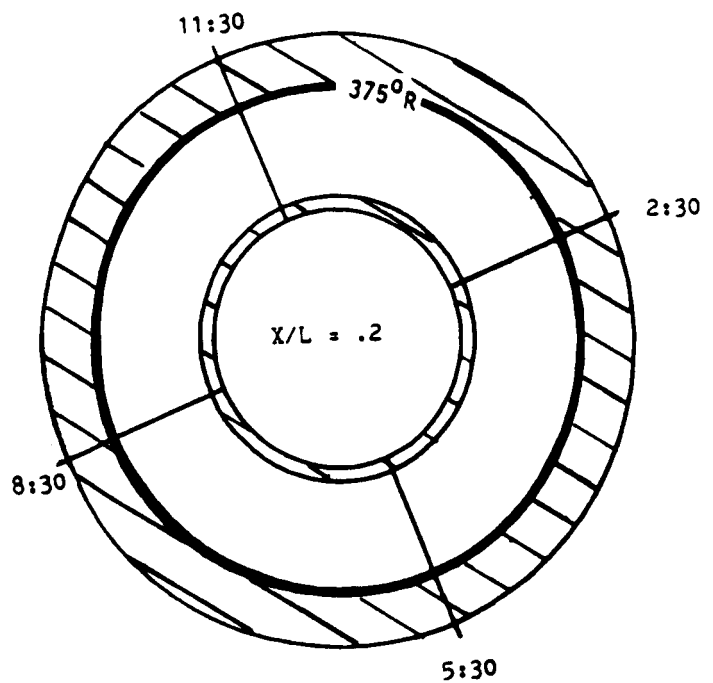


Figure 18. Three-dimensional basecase results: temperature (end view).

BASECASE

DSK 32 BC

3-D SOLUTION

ASYMMETRICAL

PRESSURE

H₂O

MASS CONCENTRATION

SIDE VIEW

SYMMETRICAL

GAP (= .0108")

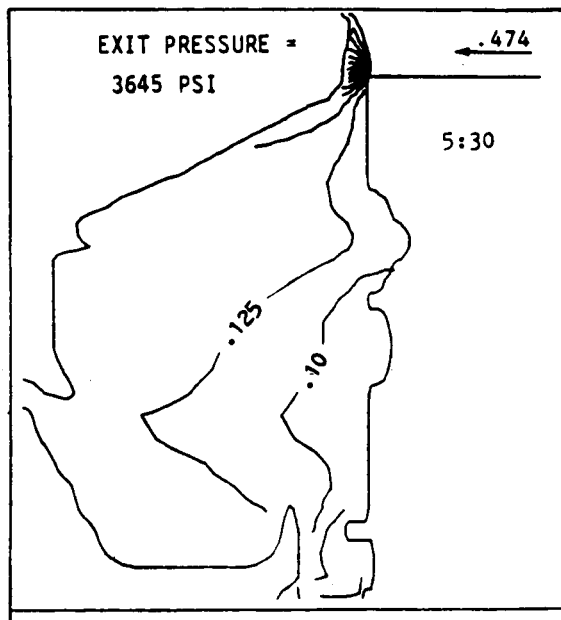
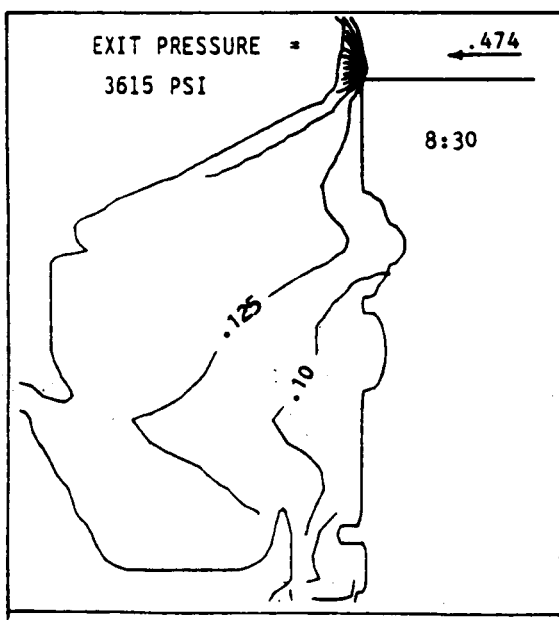
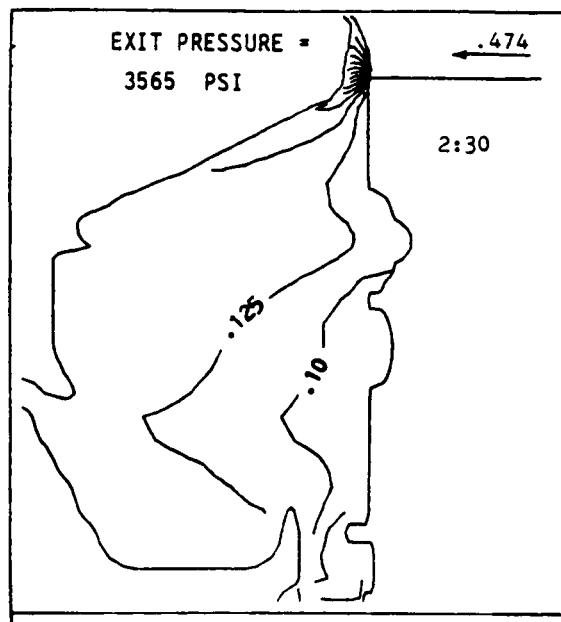
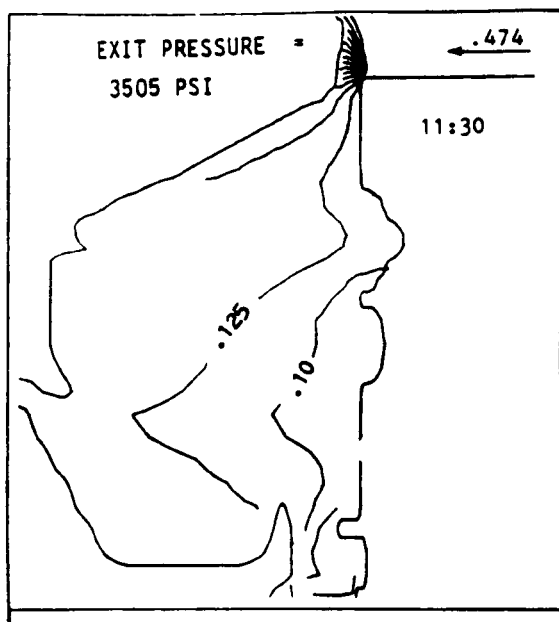


Figure 19. Three-dimensional basecase results: mass concentration.

BASECASE

DSK 32 BC
3-D SOLUTION

ASYMMETRICAL
EXIT PRESSURE

STATIC PRESSURE (PSI)
SIDE VIEW

SYMMETRICAL
GAP (= .0108")

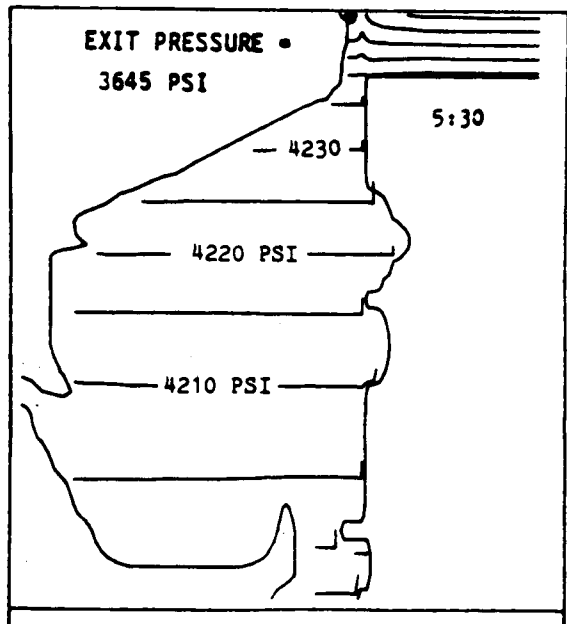
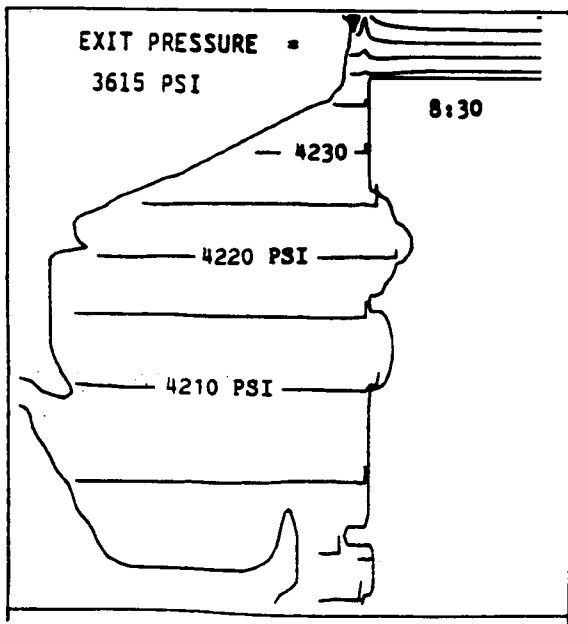
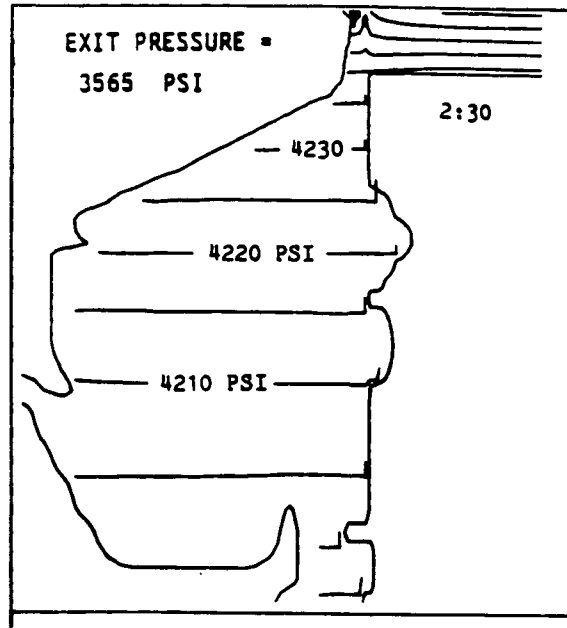
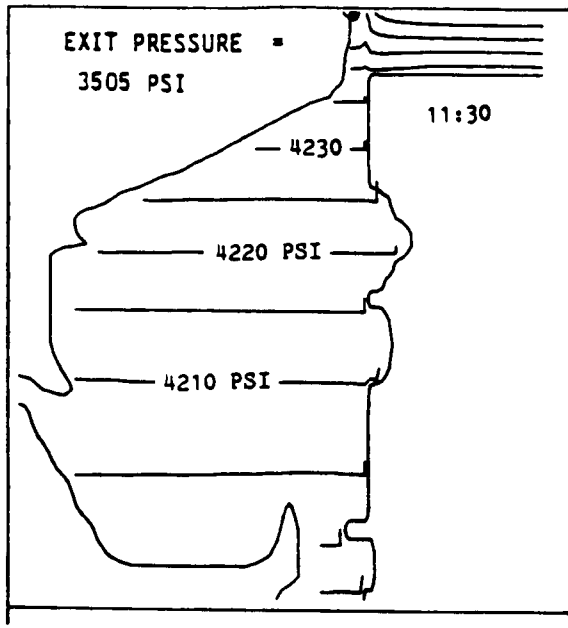


Figure 20. Three-dimensional basecase results: static pressure.

BASECASE

DSK 32 8C

ASYMMETRICAL

TOTAL PRESSURE (PSI)

SYMMETRICAL

3-D SOLUTION

EXIT PRESSURE

SIDE VIEW

GAP (= .0108")

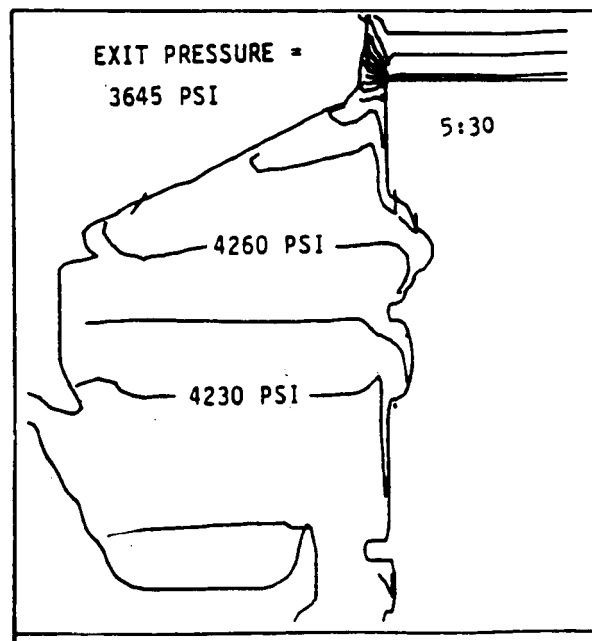
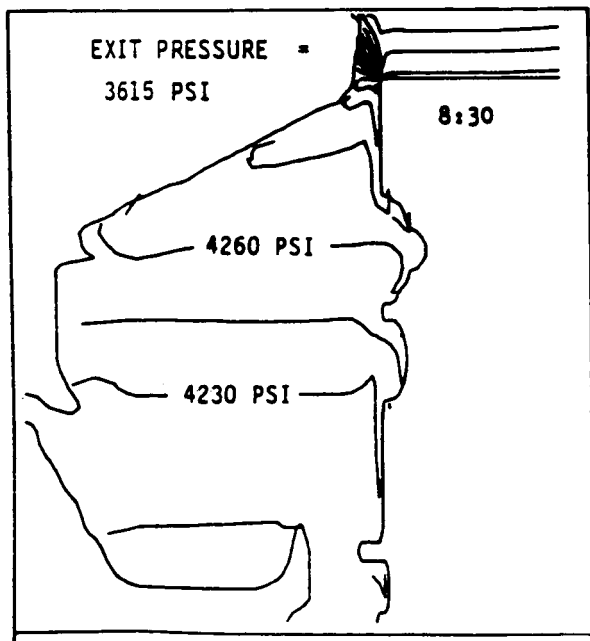
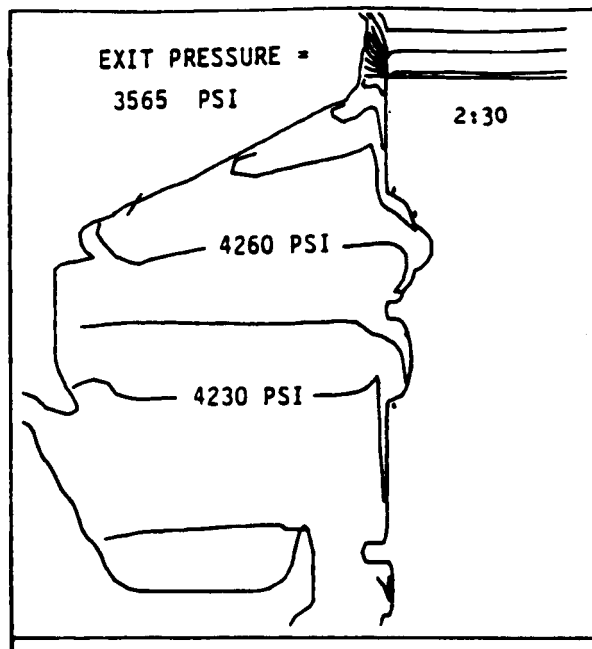
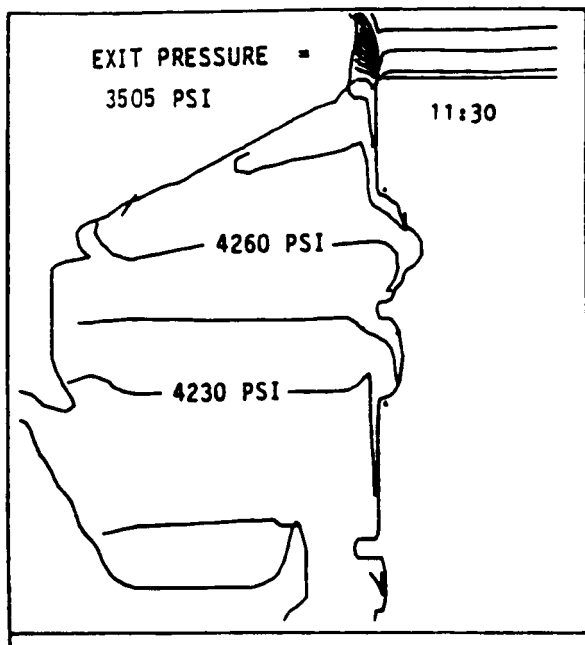


Figure 21. Three-dimensional basecase results: total pressure.

DSK 32 EC

ASYMMETRICAL GAP

VECTORS

SYMMETRICAL EXIT

3-D SOLUTION

ECCENTRICITY = .003"

SIDE VIEW

PRESSURE = 3558 PSI

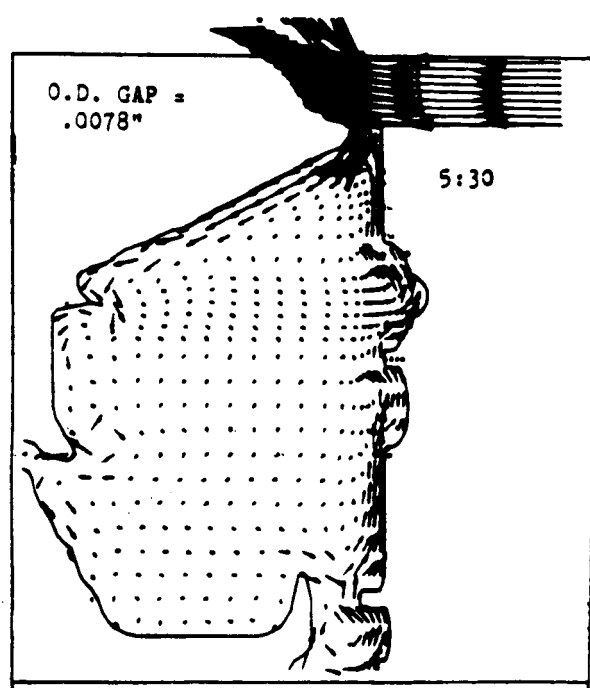
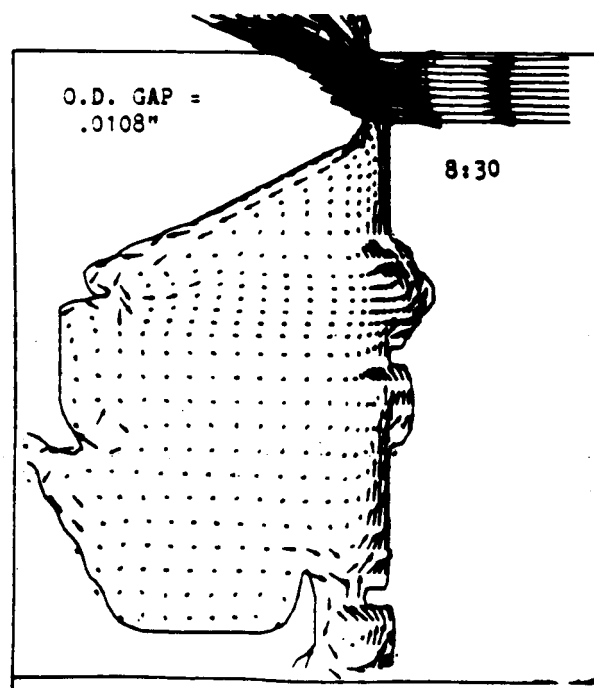
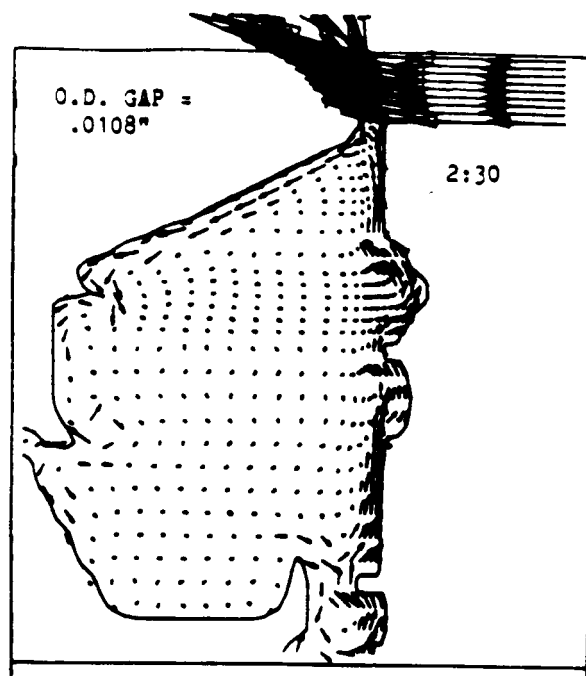
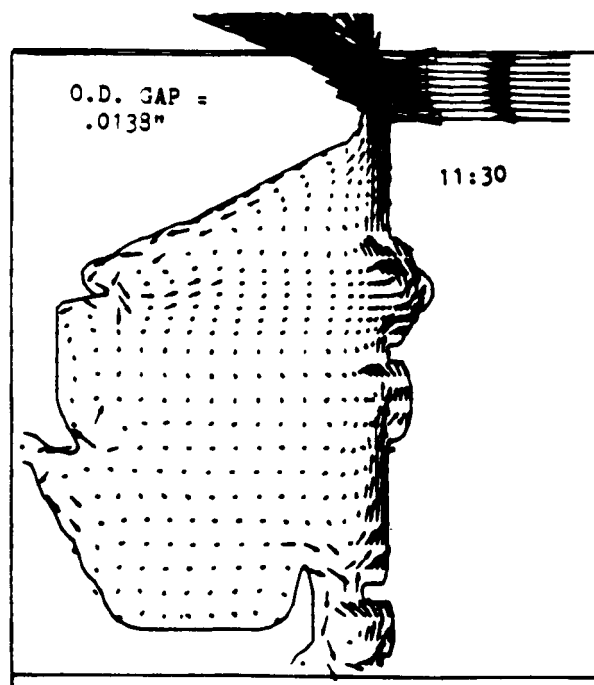


Figure 22. Three-dimensional eccentric (0.003 in.) rotor: vectors.

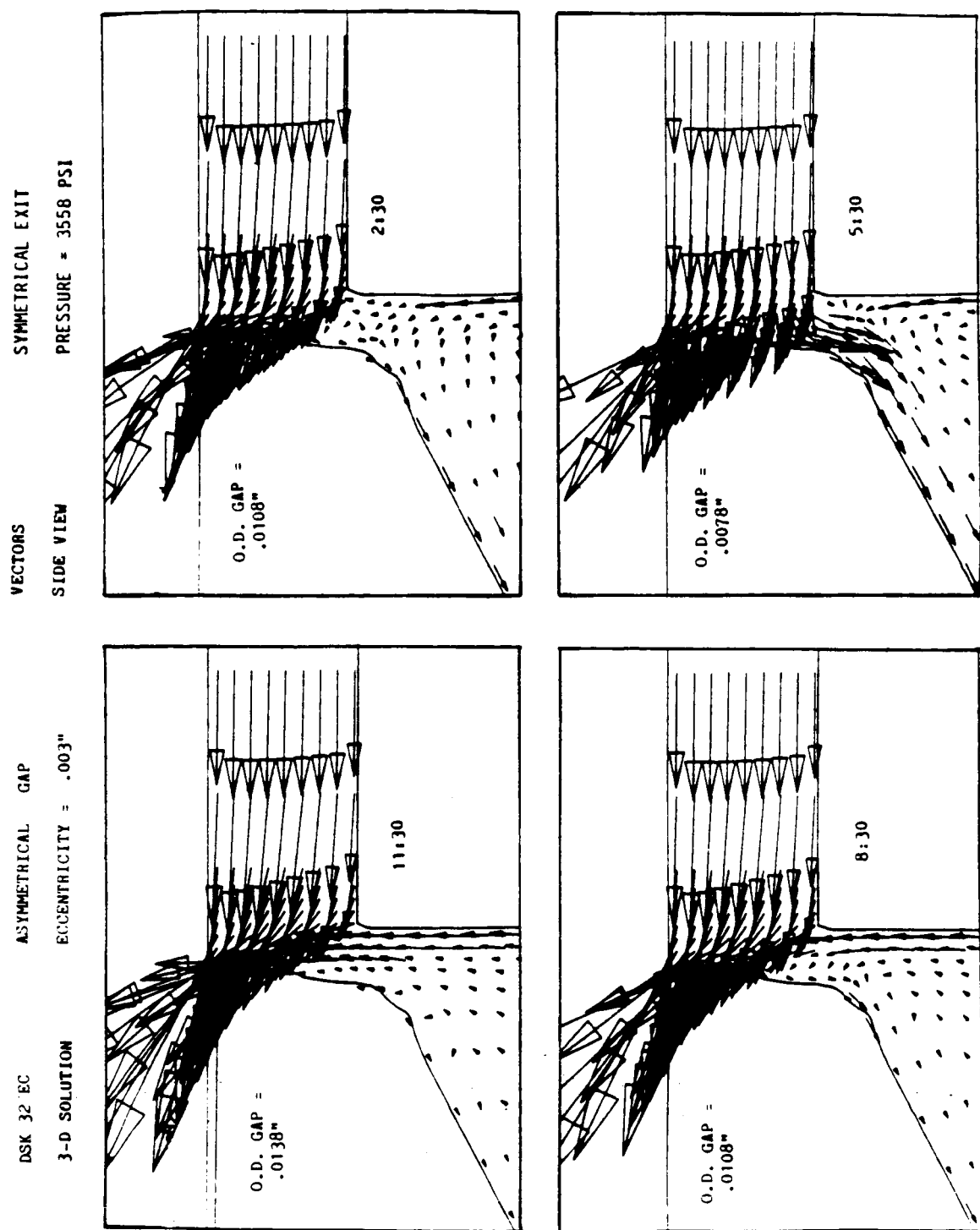


Figure 23. Three-dimensional eccentric (0.003 in.) rotor: vectors (close-up).

VECTORS

DSK 32 EC

ASYMMETRICAL GAP

END VIEW

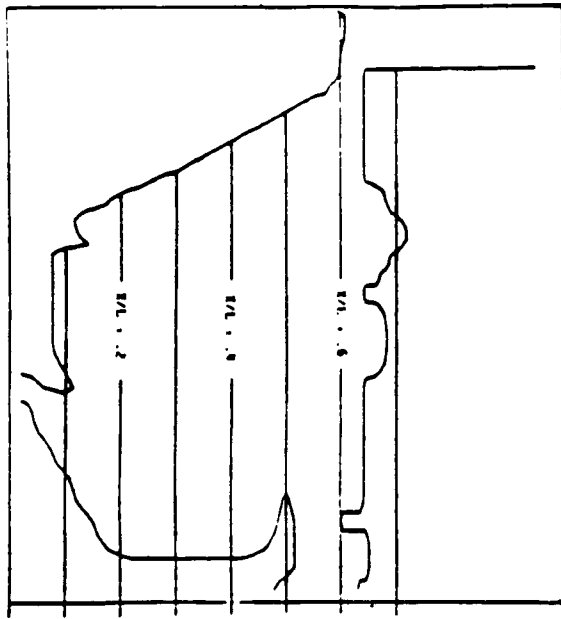
SYMMETRICAL EXIT

3-D SOLUTION

ECCENTRICITY = .003"

(FROM THE TURBINE END)

PRESSURE = 3558 PSI



CROSS SECTIONS USED IN END VIEW

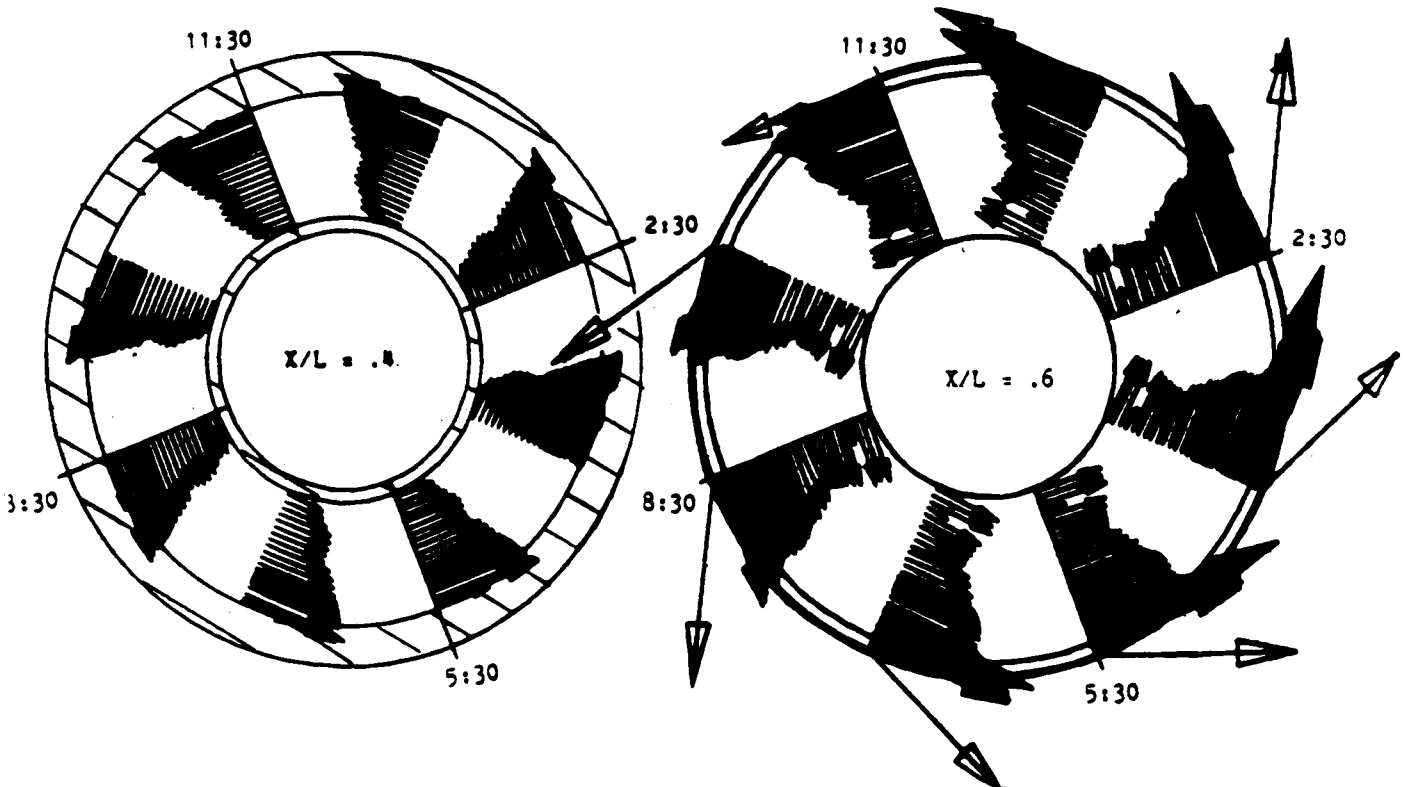
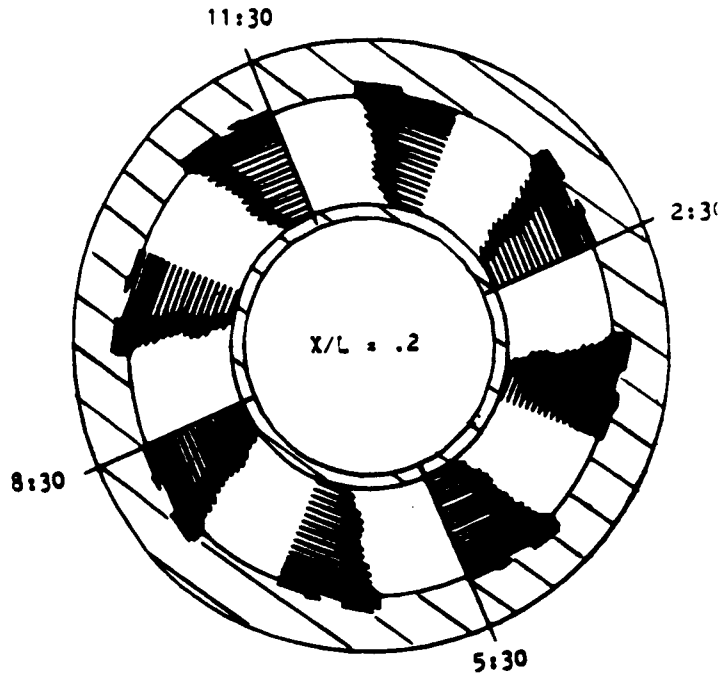


Figure 24. Three-dimensional eccentric (0.003 in.) rotor: vectors (end view).

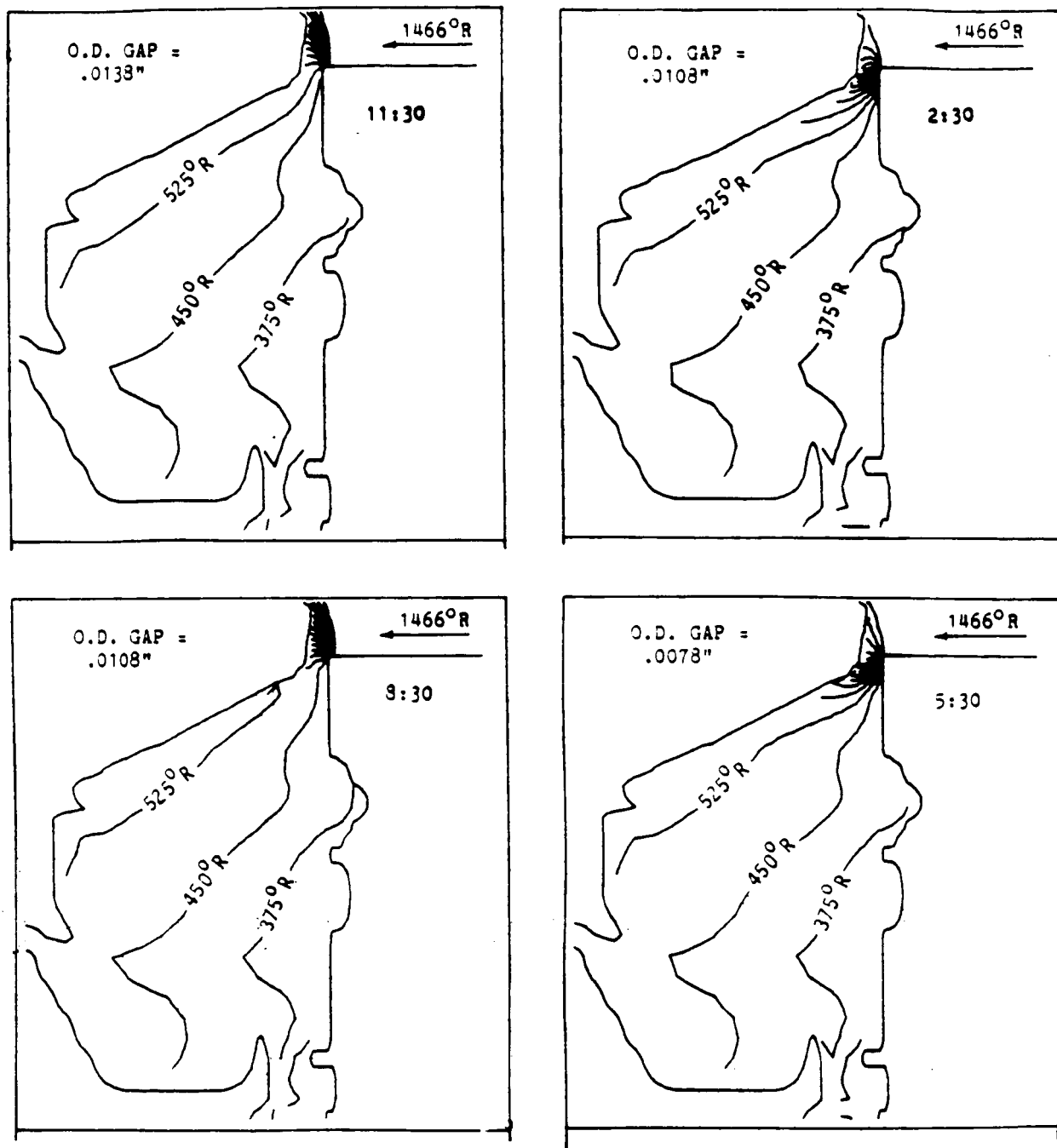


Figure 25. Three-dimensional eccentric (0.003 in.) rotor: temperature.

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DSK 3.2 EC. ASYMMETRICAL GAP TEMPERATURE SYMMETRICAL EXIT
3-D SOLUTION ECCENTRICITY = .003" SIDE VIEW PRESSURE = 3558 PSI

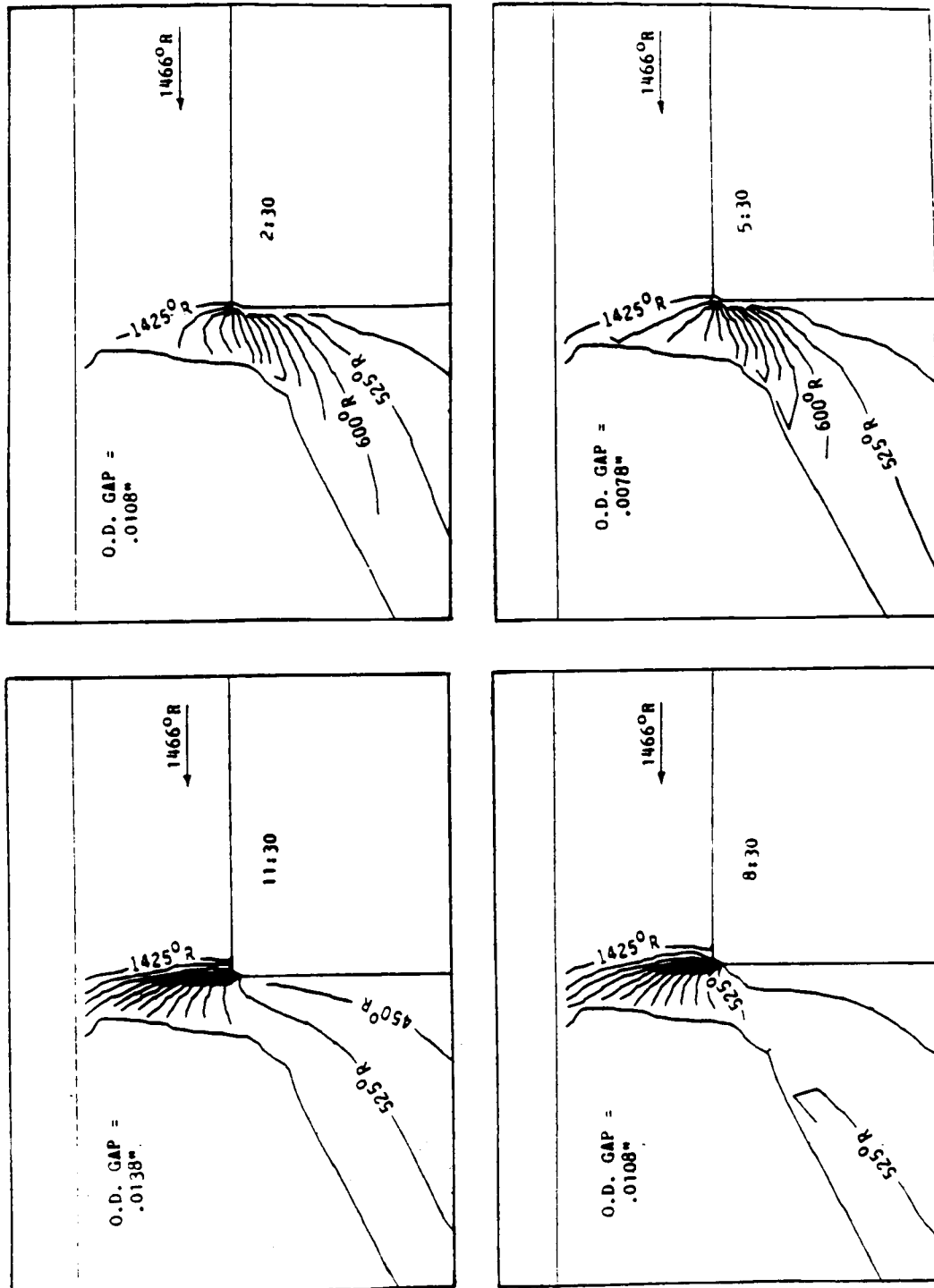


Figure 26. Three-dimensional eccentric (0.003 in.) rotor: temperature (close-up).

DSK 32 EC
3-D SOLUTION

ASYMMETRICAL GAP
ECCENTRICITY = .003"

TEMPERATURE

END VIEW
(FROM THE TURBINE END)

SYMMETRICAL EXIT
PRESSURE = 3558 PSI

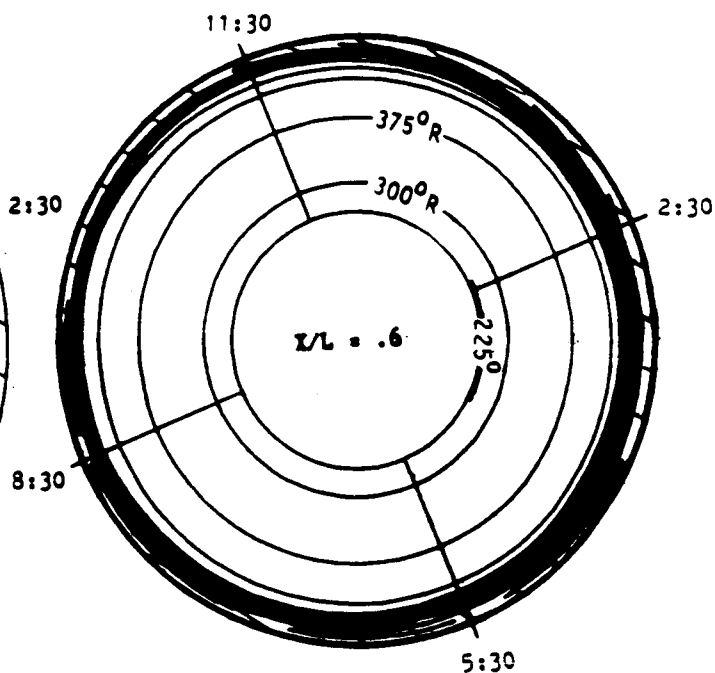
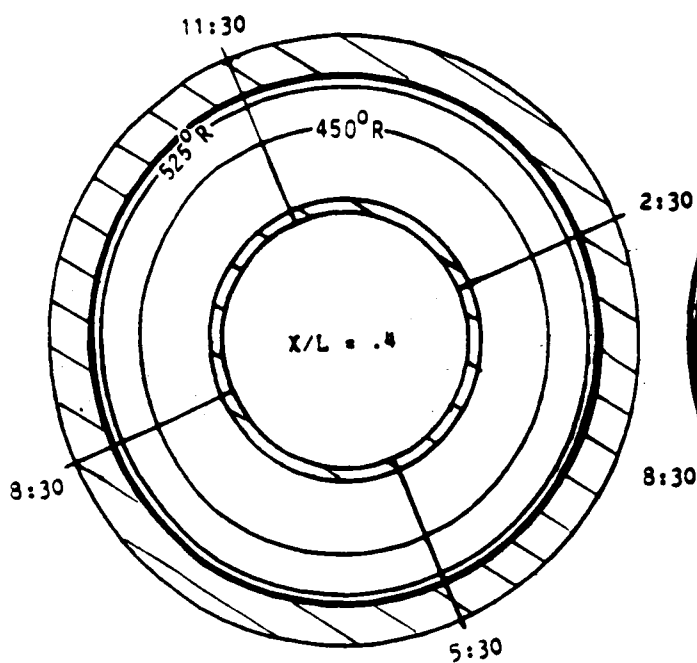
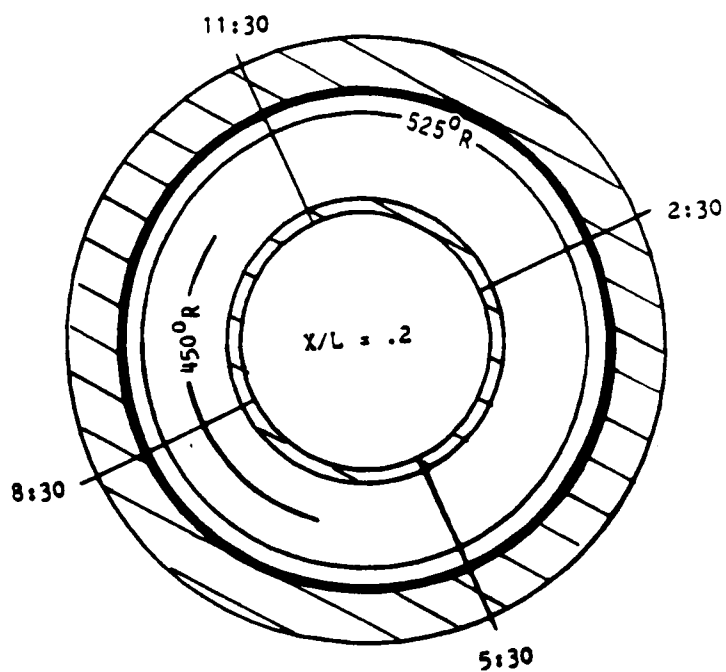
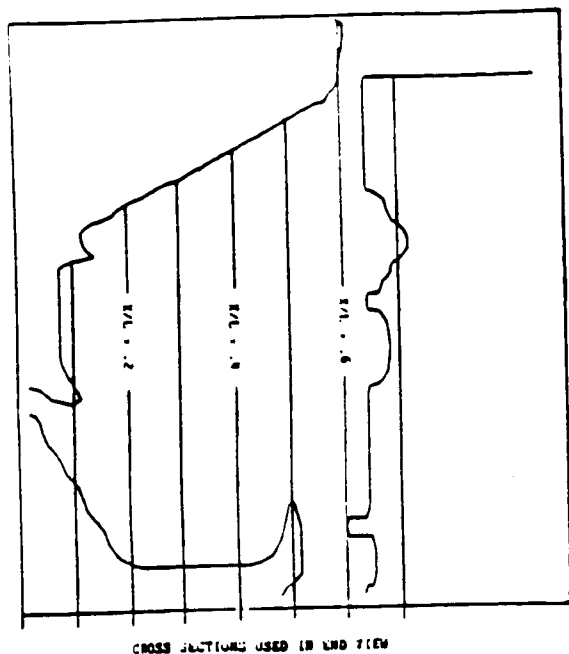


Figure 27. Three-dimensional eccentric (0.003 in.) rotor: temperature (end view).

H₂O

DSK 32 EC

ASYMMETRICAL GAP

MASS CONCENTRATION

SYMMETRICAL EXIT

3-D SOLUTION

ECCENTRICITY = .003"

SIDE VIEW

PRESSURE = 3558 PSI

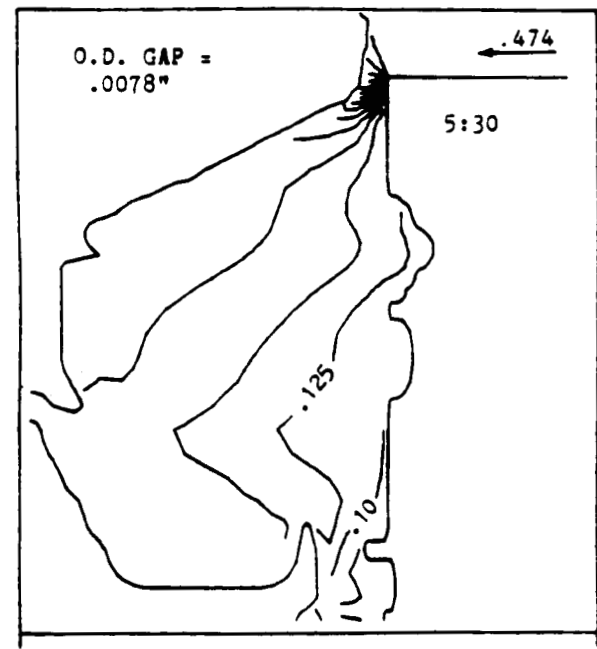
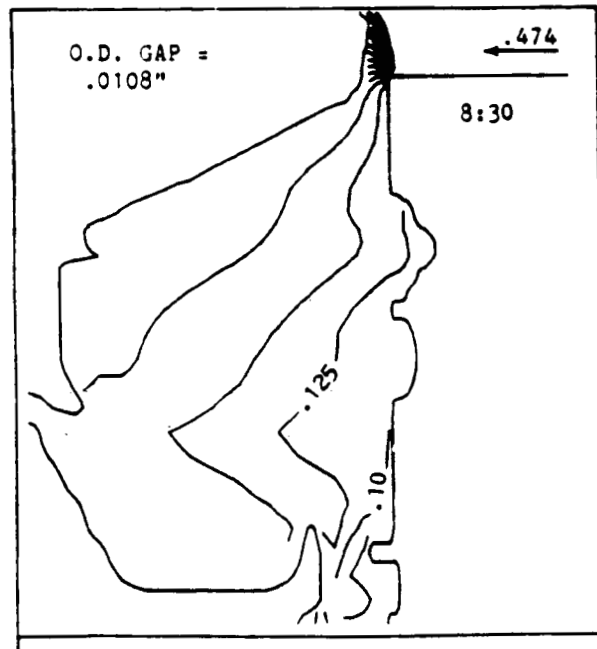
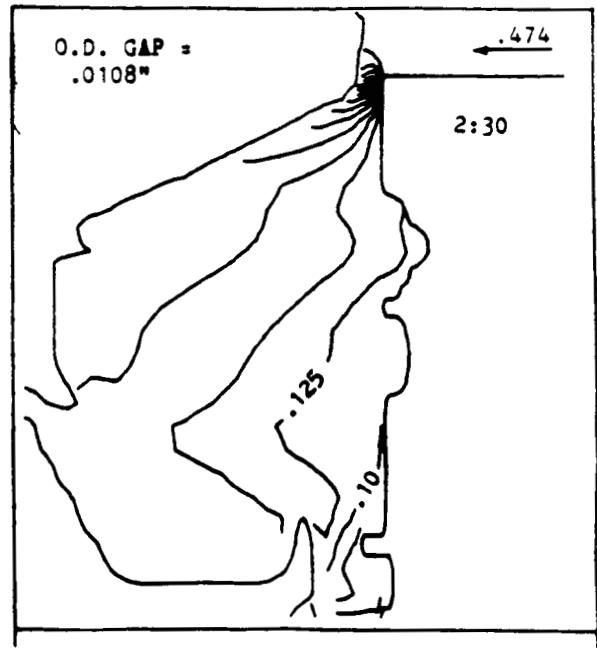
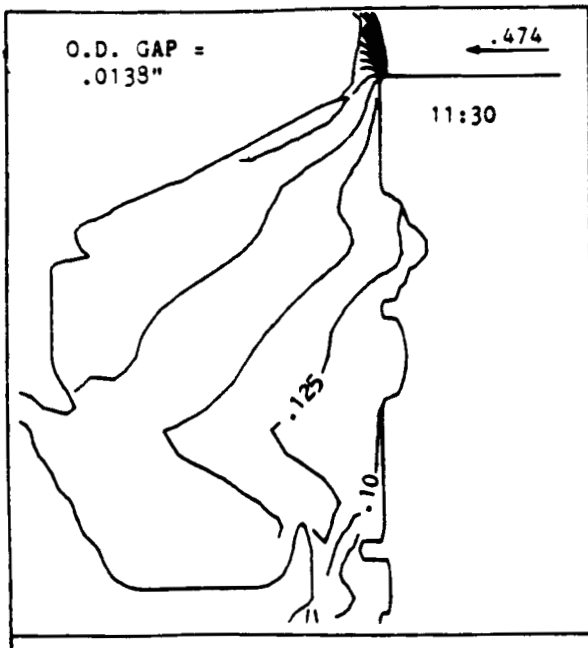


Figure 28. Three-dimensional eccentric (0.003 in.) rotor: Mass concentration.

DSK 32 EC
3-D SOLUTION

ASYMMETRICAL GAP
ECCENTRICITY = .003"

STATIC PRESSURE (PSI)
SIDE VIEW

SYMMETRICAL EXIT
PRESSURE = 3558 PSI

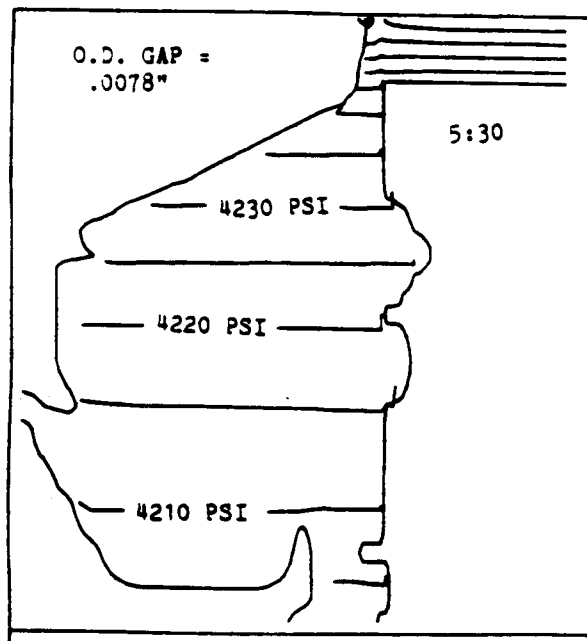
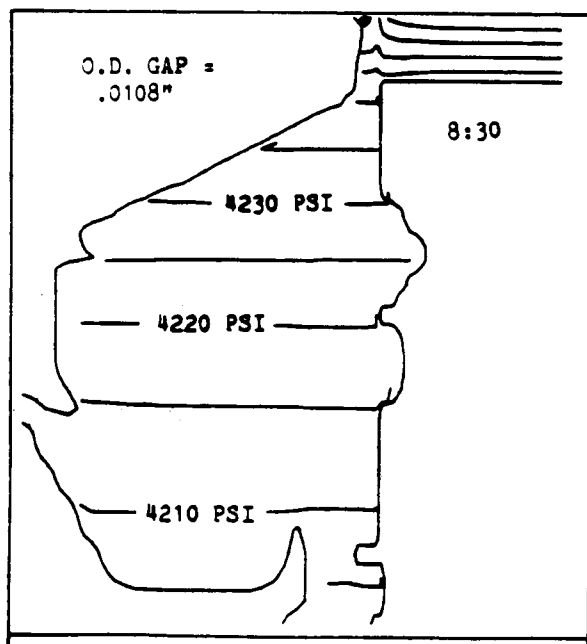
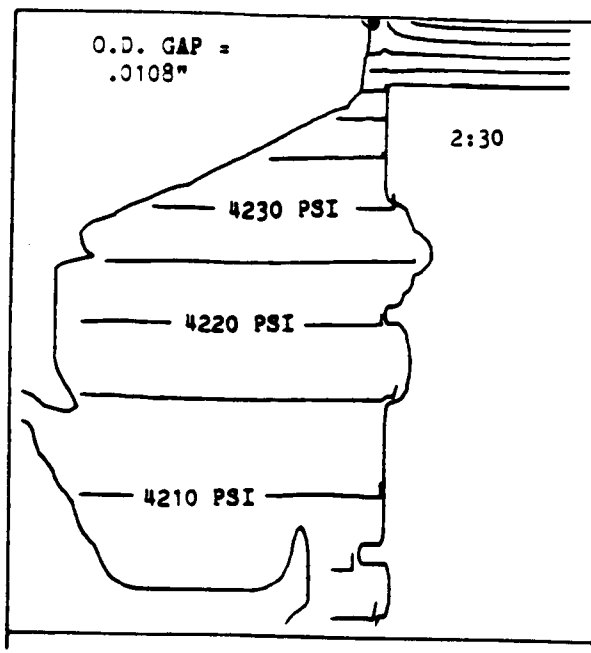
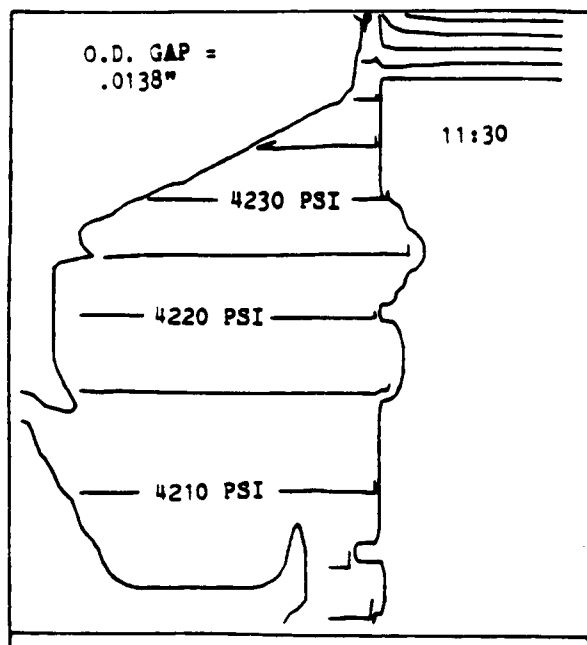


Figure 29. Three dimensional eccentric (0.003 in.) rotor: static pressure.

DSK 32 EC

ASYMMETRICAL GAP

TOTAL PRESSURE (PSI)

SYMMETRICAL EXIT

3-D SOLUTION

ECCENTRICITY = .003"

SIDE VIEW

PRESSURE = 3558 PSI -
STATIC

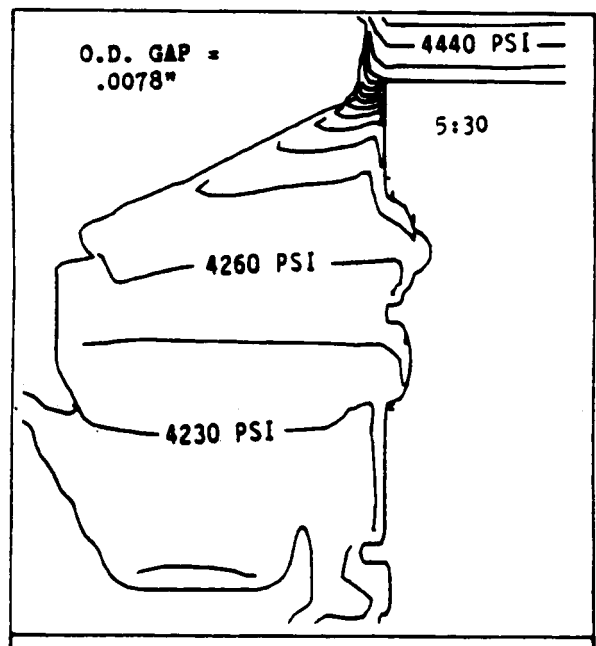
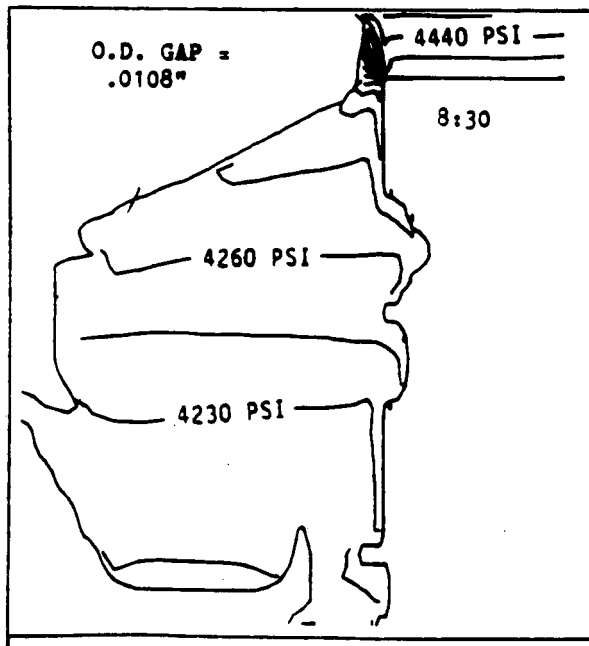
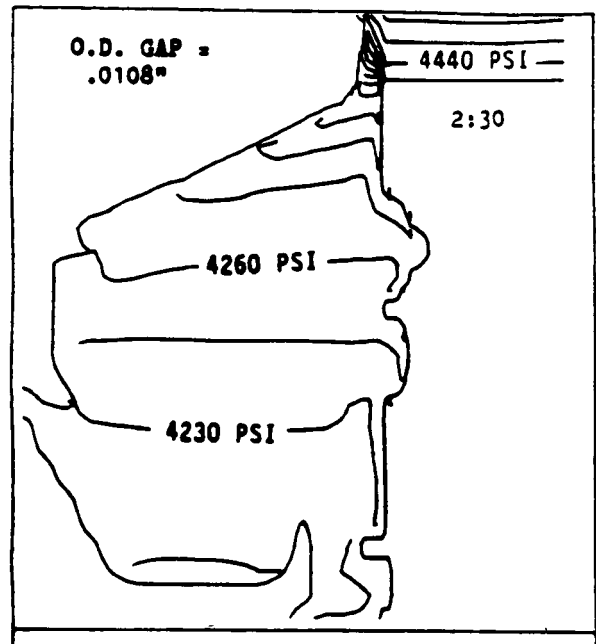
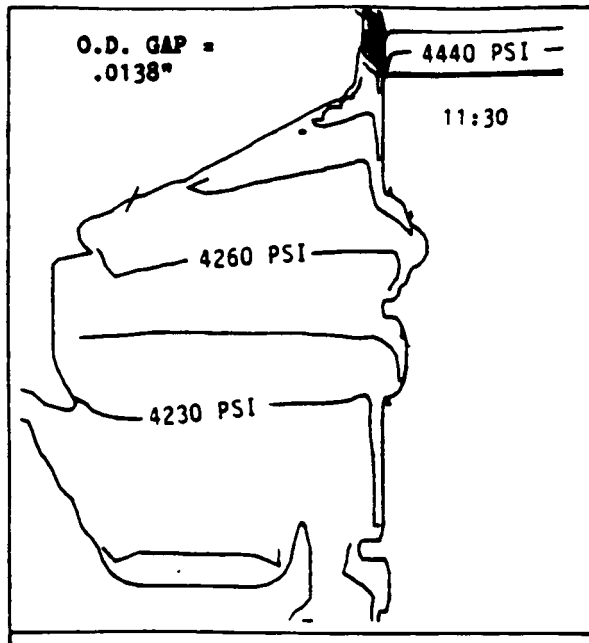


Figure 30. Three-dimensional eccentric (0.003 in.) rotor: total pressure.

DSK 32 ASH
3-D SOLUTION

ASYMMETRICAL GAP
ECCENTRICITY = .0081"

VECTORS
SIDE VIEW

SYMMETRICAL EXIT
PRESSURE = 3558 PSI

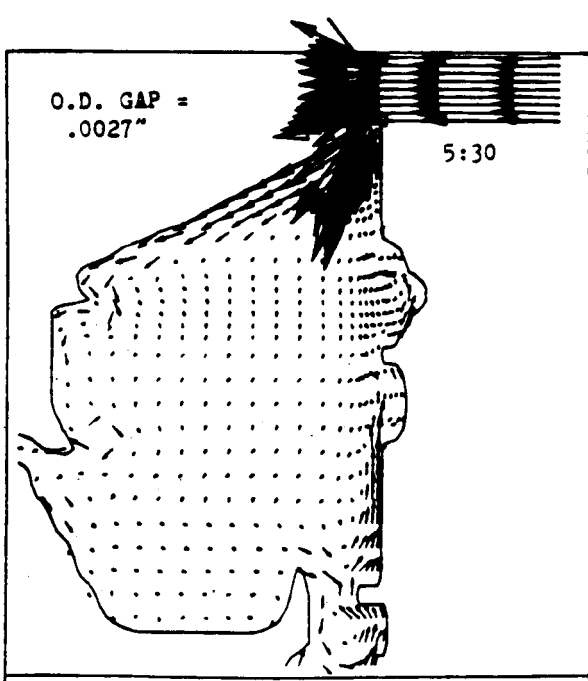
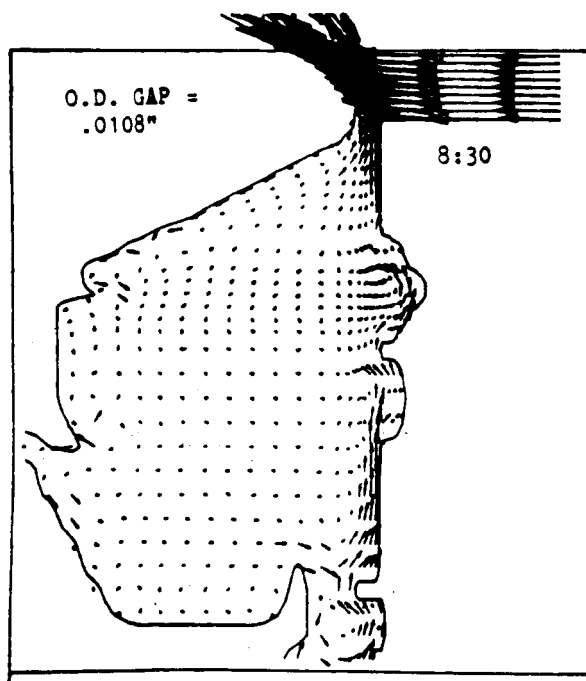
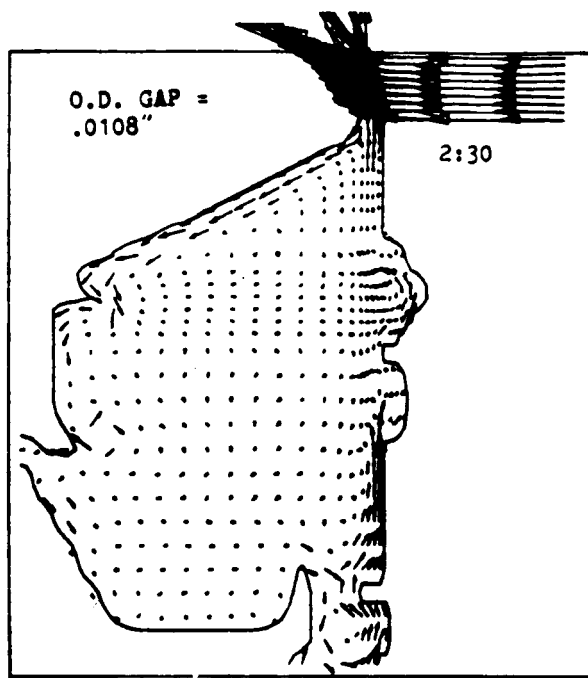
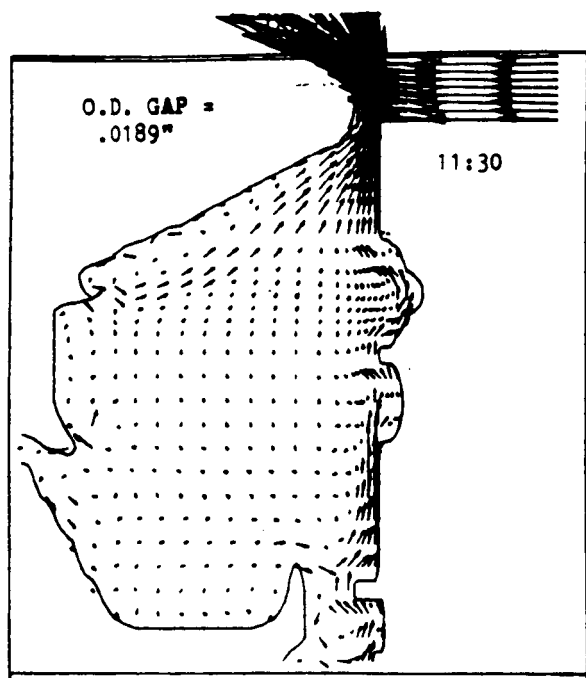


Figure 31. Three-dimensional eccentric (0.0081 in.) aft-platform seal: vectors.

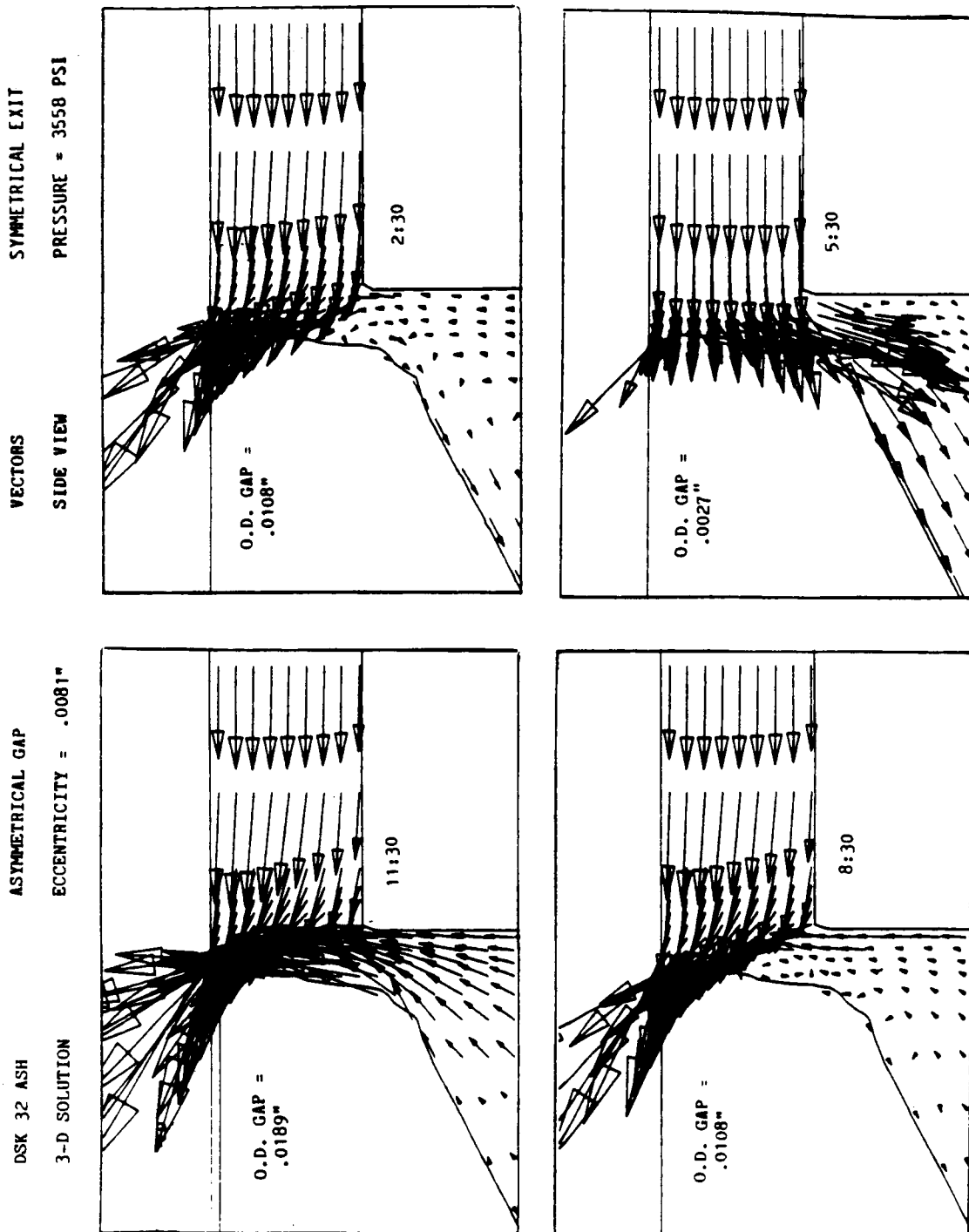


Figure 32. Three-dimensional eccentric (0.0081 in.) aft-platform seal: vectors (close-up).

DSK 32 ASH
3-D SOLUTION

ASYMMETRICAL GAP
ECCENTRICITY = .0081"

VECTORS
END VIEW
(FROM THE TURBINE END)

SYMMETRICAL EXIT
PRESSURE = 3558 PSI

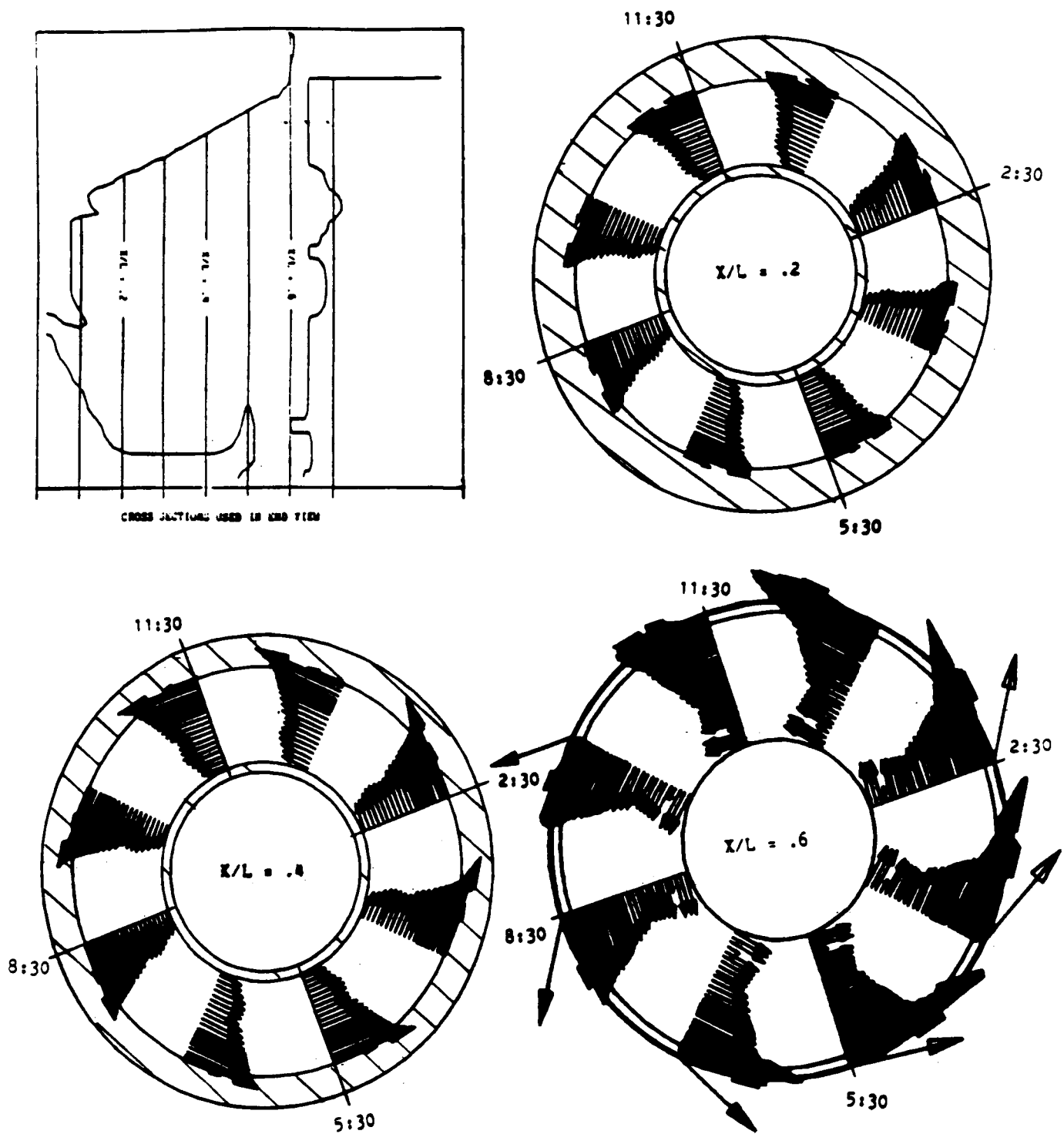


Figure 33. Three-dimensional eccentric (0.0081 in.) aft-platform seal: vectors (end view).

DSK 32 ASH

ASYMMETRICAL GAP

TEMPERATURE

SYMMETRICAL EXIT

3-D SOLUTION

ECCENTRICITY = .0081"

SIDE VIEW

PRESSURE = 3558 PSI

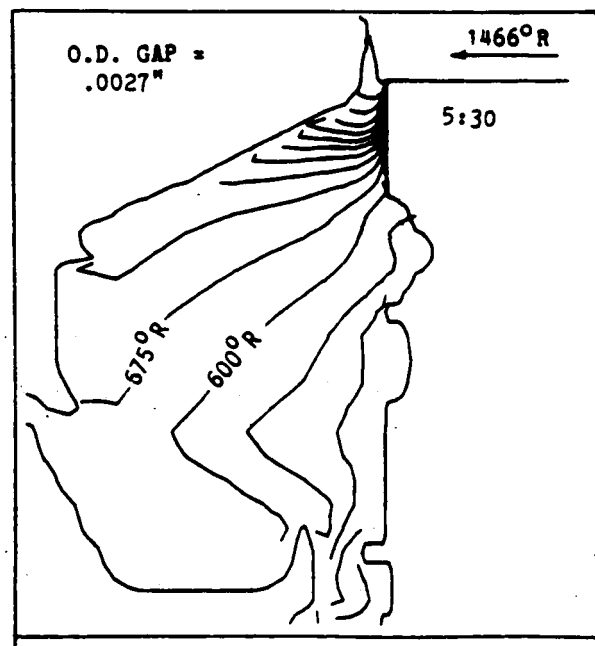
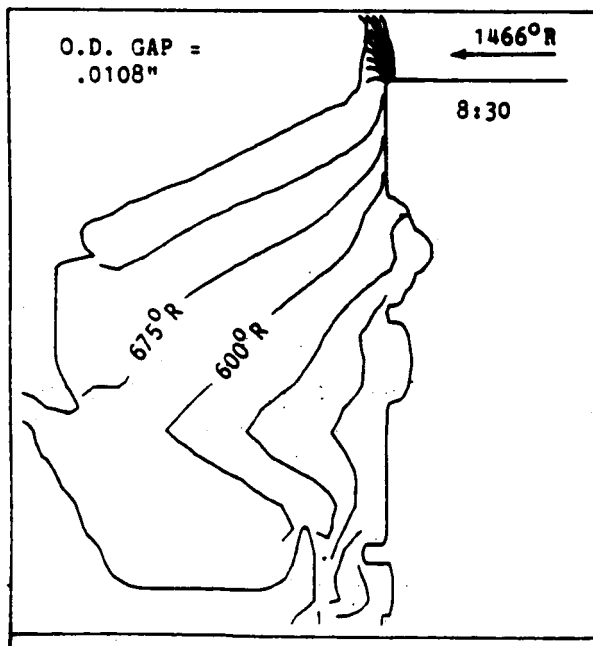
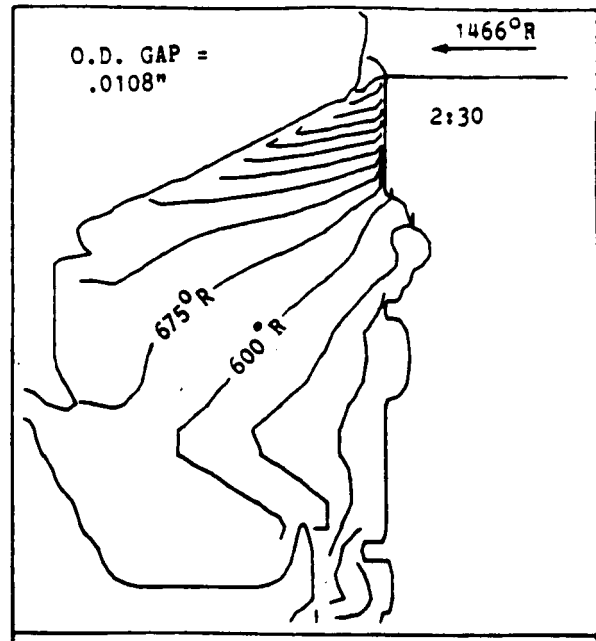
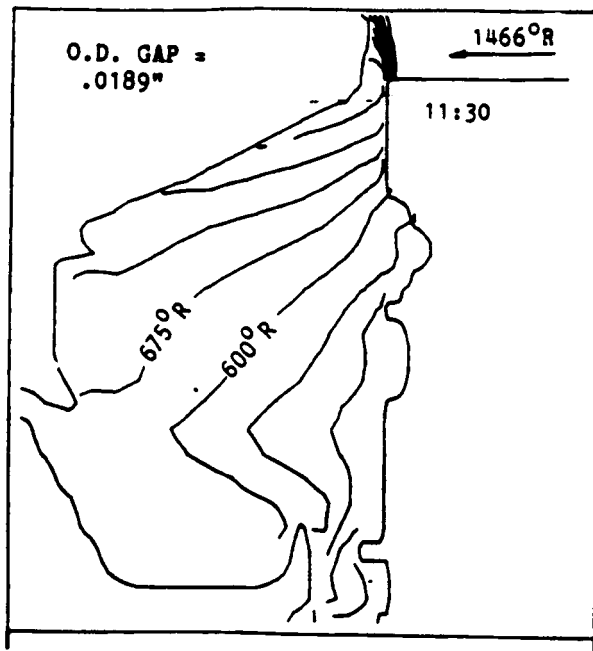


Figure 34. Three-dimensional eccentric (0.0081 in.) aft-platform seal: temperature.

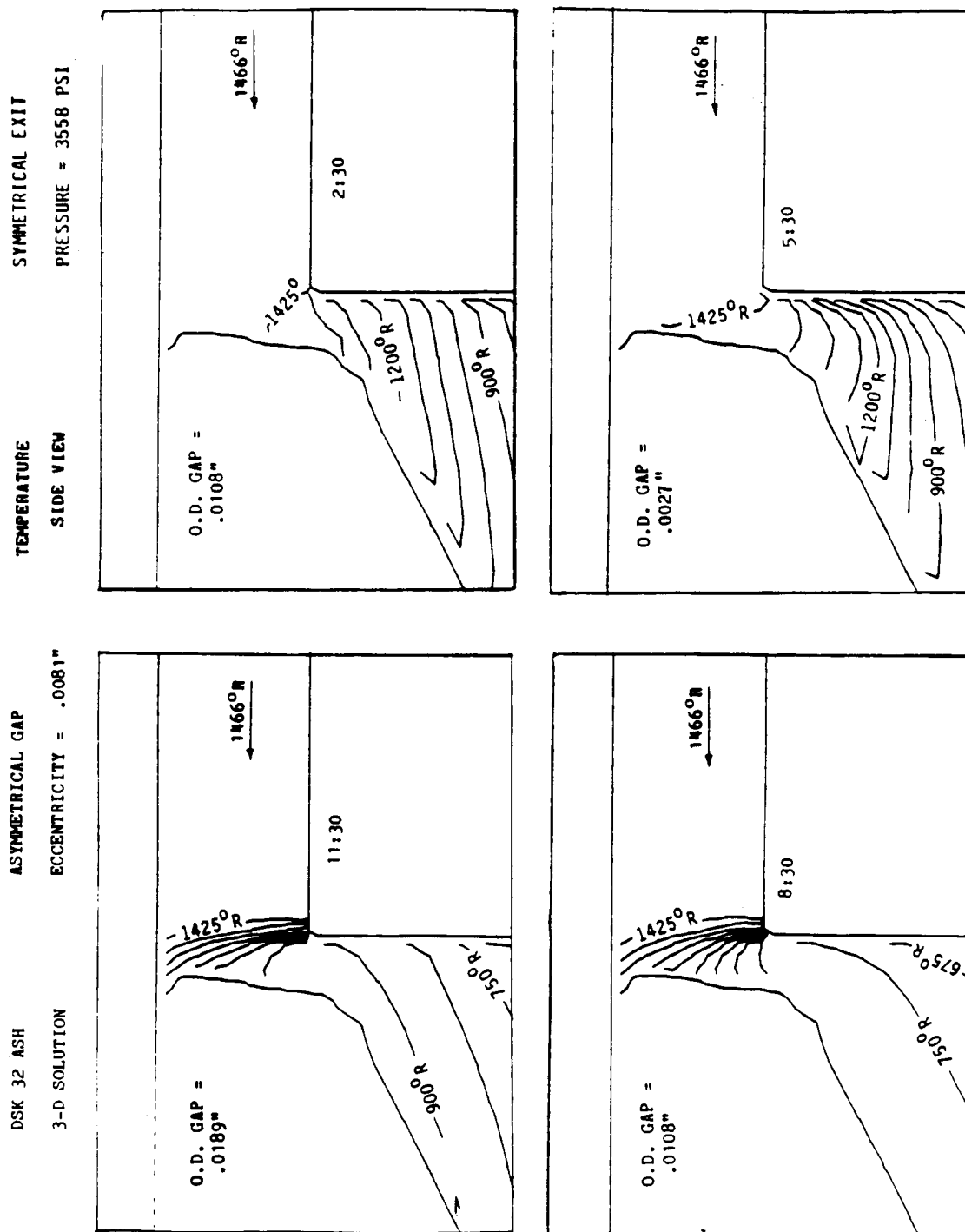


Figure 35. Three-dimensional eccentric (0.0081 in.) aft-platform seal: temperature (close-up).

DSK 32 ASH

ASYMMETRICAL GAP

TEMPERATURE

END VIEW

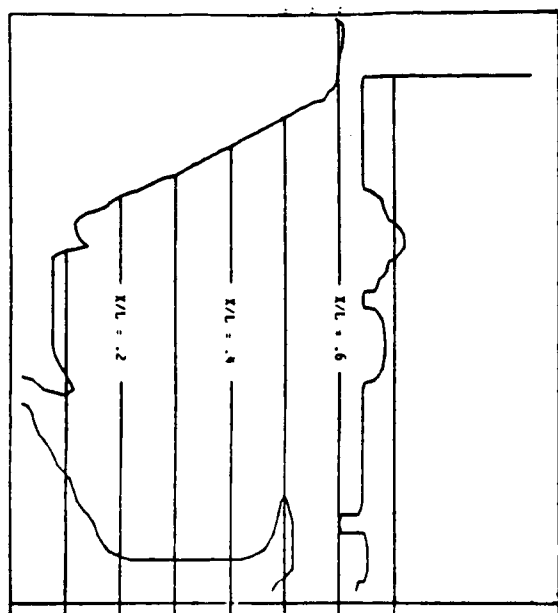
SYMMETRICAL EXIT

3-D SOLUTION

ECCENTRICITY = .0081"

(FROM THE TURBINE END)

PRESSURE = 3558 PSI



CROSS SECTIONS USED IN END VIEW

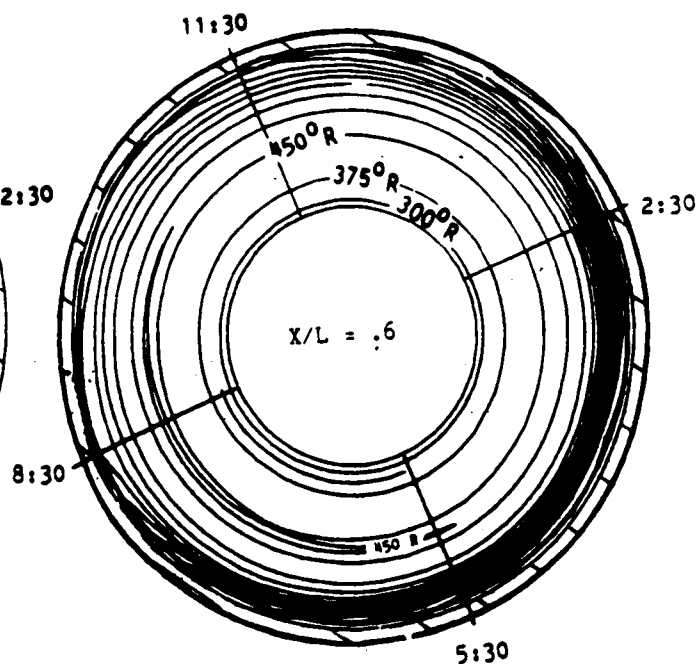
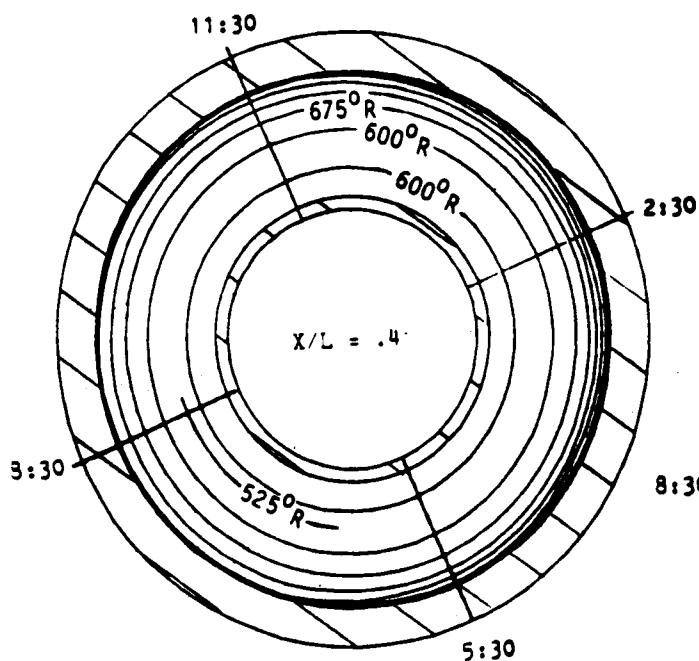
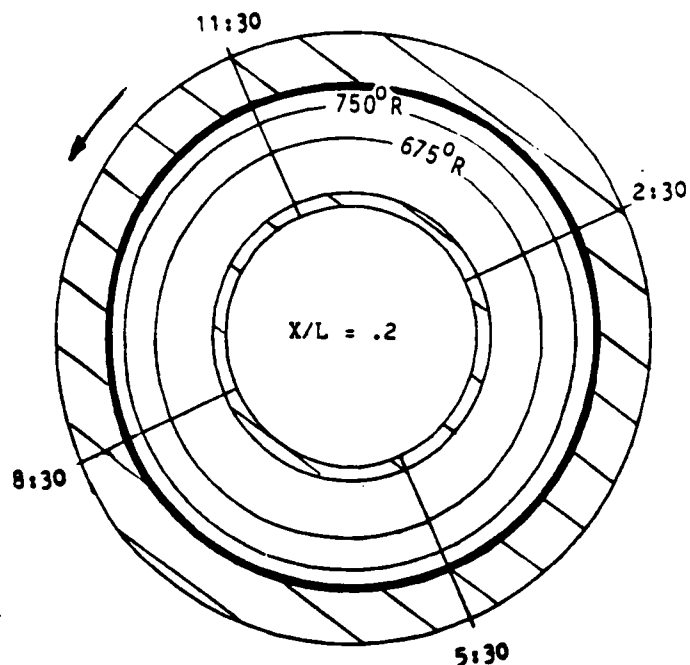


Figure 36. Three-dimensional eccentric (0.0081 in.) aft-platform seal: temperature (end view).

DSK 32 ASH

ASYMMETRICAL GAP

3-D SOLUTION

ECCENTRICITY = .0081"

H₂O

MASS CONCENTRATION

SIDE VIEW

SYMMETRICAL EXIT

PRESSURE = 3558 PSI

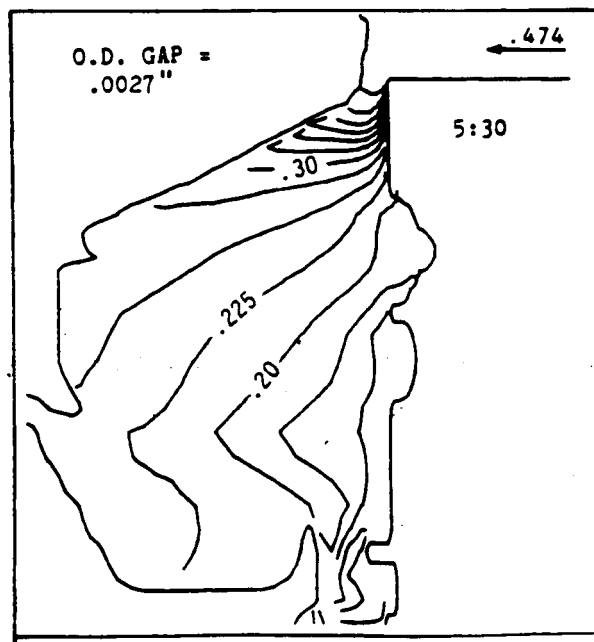
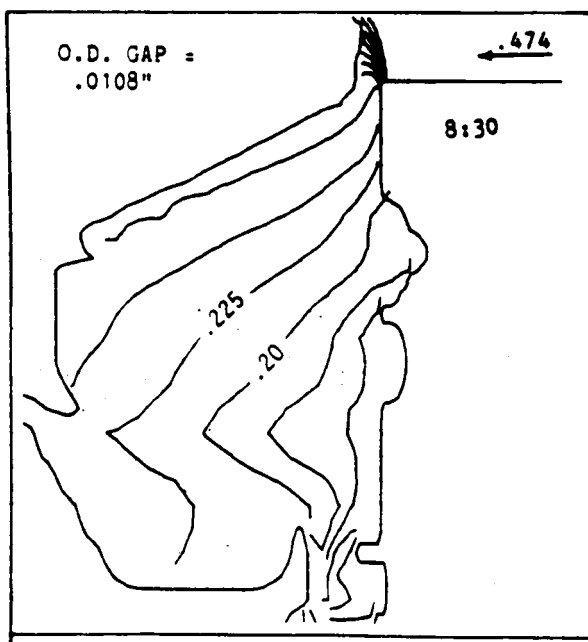
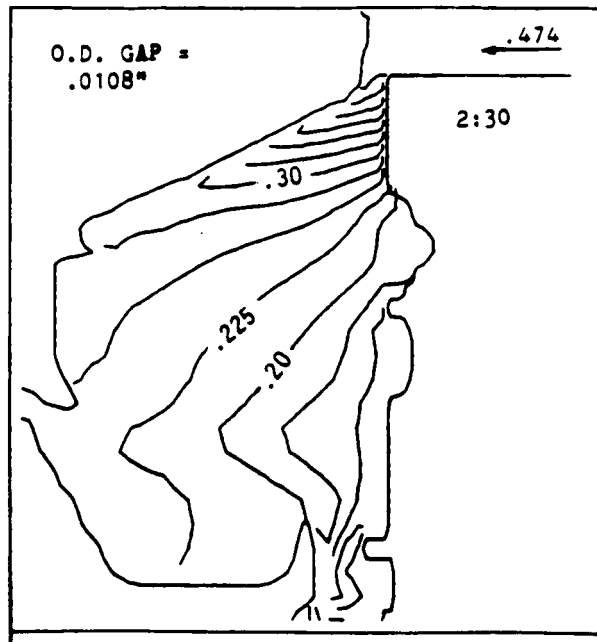
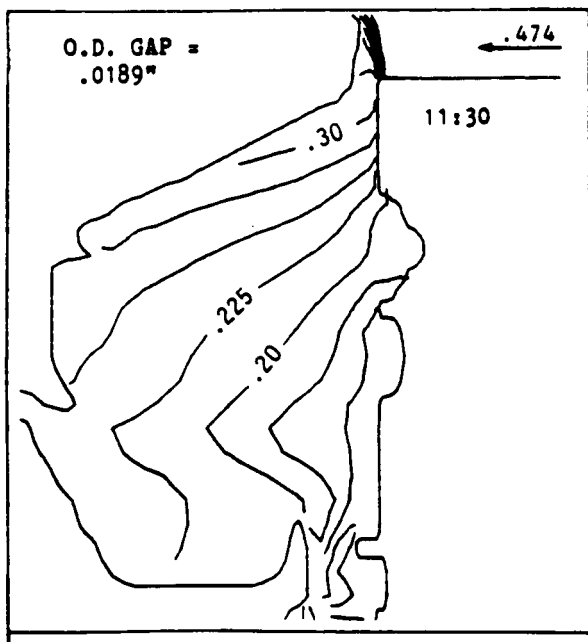


Figure 37. Three-dimensional eccentric (0.0081 in.) aft-platform seal: mass concentration.

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DSK 32 ASH

ASYMMETRICAL GAP

STATIC PRESSURE (PSI)

SYMMETRICAL EXIT

3-D SOLUTION

ECCENTRICITY = .0081"

SIDE VIEW

PRESSURE = 3558 PSI

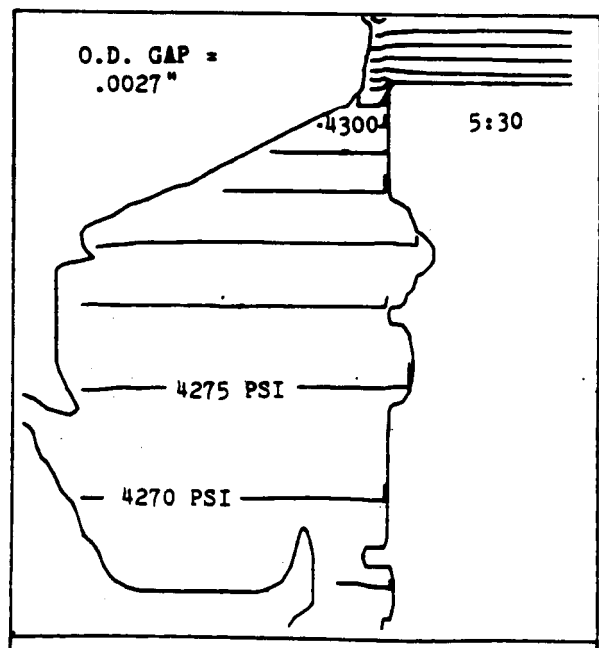
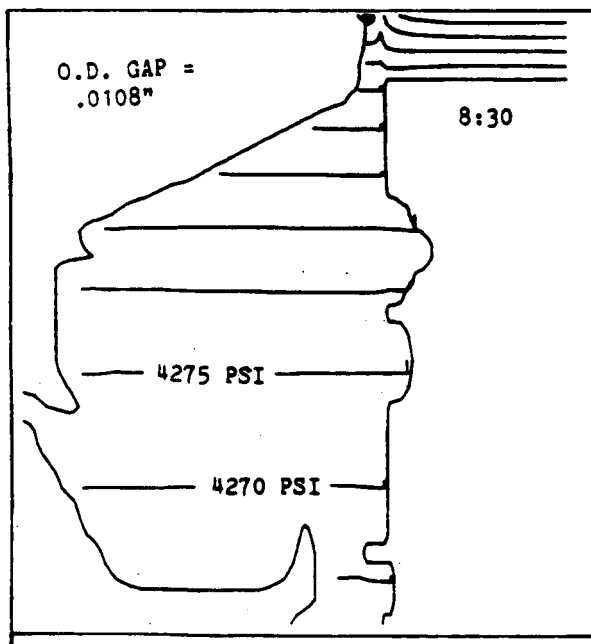
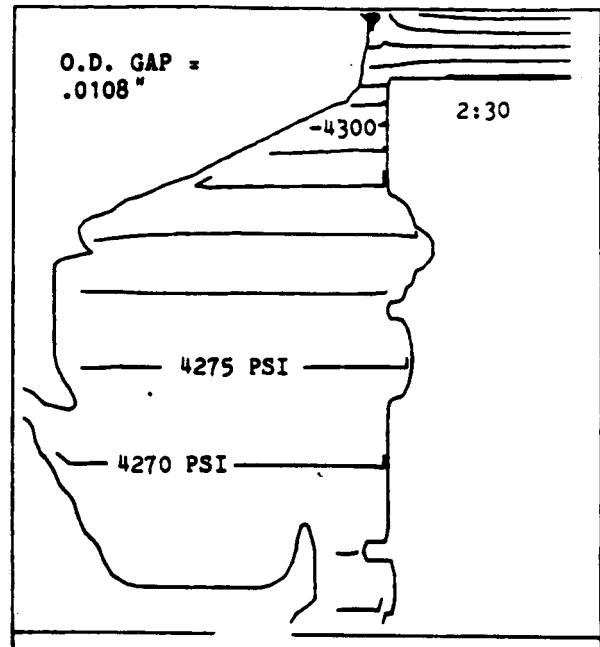
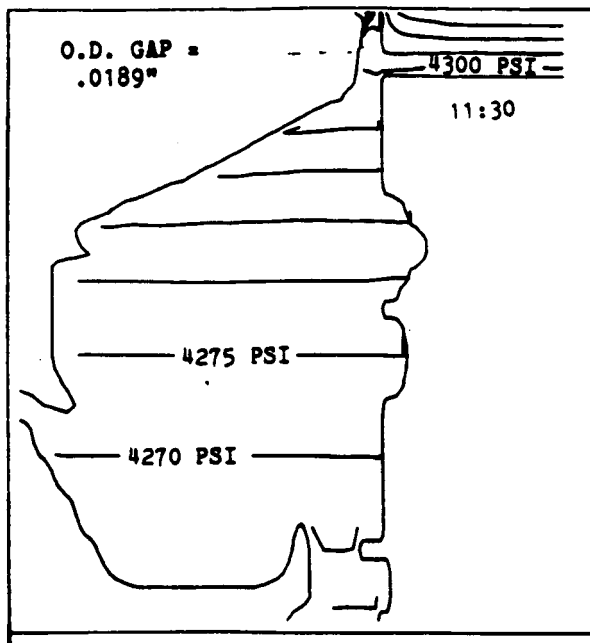


Figure 38. Three-dimensional eccentric (0.0081 in.) aft-platform seal: static pressure.

DSK 32 ASH

~~ASYMMETRICAL~~ GAP

TOTAL PRESSURE (PSI)

SYMMETRICAL EXIT

3-D SOLUTION

ECCENTRICITY = .0081"

SIDE VIEW

PRESSURE = 3558 PSI
STATIC

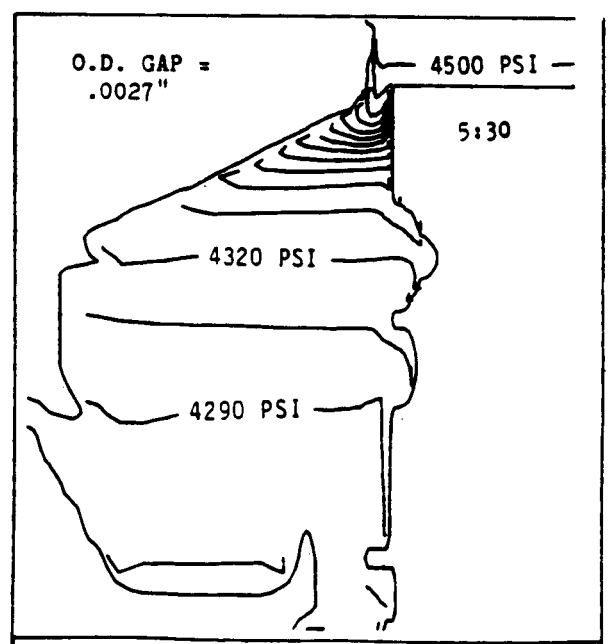
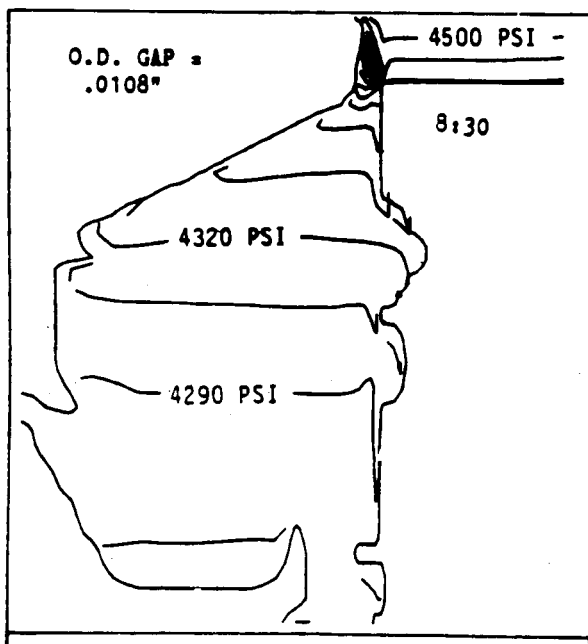
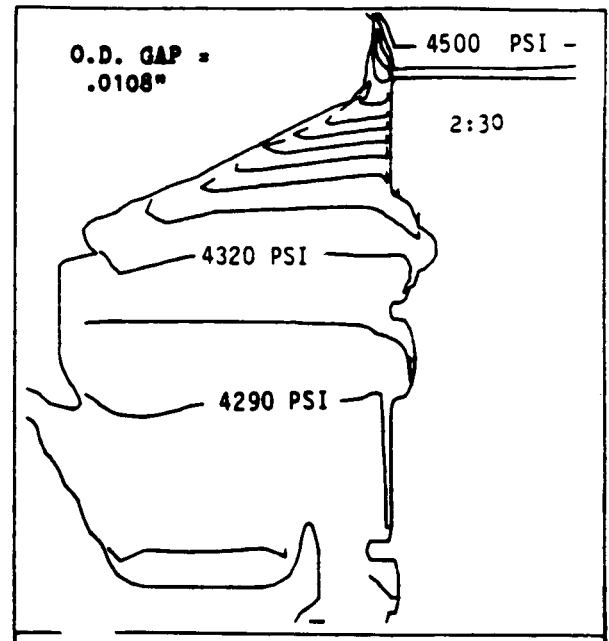
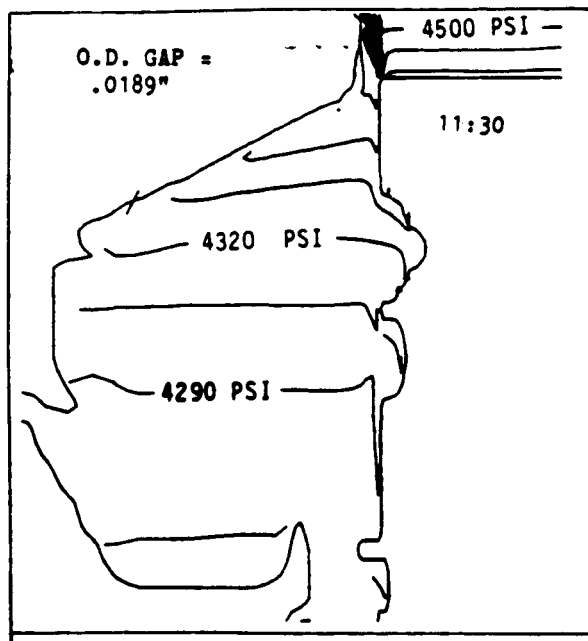


Figure 39. Three-dimensional eccentric (0.0081 in.) aft-platform seal: total pressure.

on this hot gas still works to confine it to the outer radius of the cavity. However, the pressure differences in the radial direction are, in this case, becoming large enough that they are forcing more and more hot gas down into the cavity. This is clearly evident in the velocity diagrams (Figs. 31 and 32) where, at the 5:30 clock position, there is a strong inward flow of hot gas down into the cavity. The temperature profiles also indicate a dramatic increase in hot gas in the cavity. The temperatures at the center of the cavity are now up to 675°R (215°) which is 300° warmer than for the basecase. As with the other three-dimensional runs, the most pronounced effects can still be seen at the outer radius of the cavity. Here at the outer radius of the disk near the blade shanks, there is a large circumferential variation in both temperature and pressure with the temperature cycling 600°R and the pressure varying by 20 psi.

One further observation on the results from this test run has to do with the static pressure. The observation is that for a 0.0081 in. eccentric aft-platform seal, the pressure in the cavity has gone up by 80 psi relative to the three-dimensional basecase. The implications of this pressure rise are not simple to determine. The difficulty lies in the fact that such a pressure in the cavity would reduce the flow rate through the labyrinth seal, which, for the three-dimensional model is (numerically) fixed based on the flowrates calculated earlier in the two-dimensional basecase. Since the total exit areas and average turbine discharge pressure for all the three-dimensional runs are the same as for the two-dimensional basecase, this is a reasonable assumption. In this final three-dimensional case, however, the assumption leads to a contradiction. For the eccentric aft-platform seal case, using the flowrates from the two-dimensional basecase, the pressure at the exit of the labyrinth seal is calculated as being higher than the pressure at the labyrinth inlet. In other words, if in the three-dimensional model this boundary had been specified as a fixed pressure instead of a fixed flowrate, the model would have predicted reverse flow through the labyrinth seal. That there could actually be reverse flow through the labyrinth seal is considered extremely unlikely. What would more likely occur is that an eccentricity in the aft-platform seal would raise the pressure in the aft-platform seal cavity, reducing both the hot gas flow past the blade shanks and the labyrinth seal flow.

VI. SUMMARY OF THE CURRENT TEST RUN RESULTS AND OBSERVATIONS

The axisymmetric computer model of the aft-platform seal cavity indicates that at 37,000 rpm the flow in the aft-platform seal cavity is dominated by the centrifugal force caused by the rotating turbine disk. The disk drives a recirculating flow in the central region of the cavity, creating a core of nearly uniform temperature. In general, the temperature field throughout the aft-platform seal cavity is dictated primarily by convection (as opposed to conduction) as indicated by the fact that little heat from the hot gas at the periphery of the cavity is conducted down into the isothermal core. As a result, the core stays relatively cold, even when the coolant flowrate is reduced by over 50 percent.

The most severe temperature gradient in the aft-platform seal cavity occurs at the outer diameter of the turbine disk, near the blade shanks. At this location, the hot gas entering from between the blade shanks mixes with the coolant flow that is being slung off the face of the disk. The temperature difference between the two streams is over 1000°R.

The three-dimensional computer model of the aft-platform seal cavity shows that, for normal clearances and operating conditions, the flow field in the cavity is relatively insensitive to the circumferential pressure variation known to exist in the turbine discharge. The flow field is shown to be sensitive, however, to eccentricities of the exit gap between the aft-platform seal and the blade shanks. But in both cases, it is the centrifugal force which still dominates the flow pattern, such that any perturbation of the flow field or temperature field which results from either pressure changes or geometrical changes are, for the most part, confined by centrifugal force to the outer diameter of the cavity.

In addition to the above, the study also reveals that, for fixed flow through the blade shanks, the labyrinth flowrate is extremely sensitive to the exit area at the outer diameter of the aft-platform seal. While this result is somewhat misleading, since it is based on the unrealistic boundary condition of a fixed flowrate through the blade shanks, it nevertheless merits further consideration especially with regard to transient phenomena. Finally, as a related observation, the flowrate through the labyrinth seal is also sensitive to the eccentricity of the aft-platform seal clearance, even for a constant exit area. This sensitivity is something which has yet to be included in the current one-dimensional models of the flow through the pump's turbine section.

VII. CONCLUSIONS

The results of the study summarized above provide the following insight into the specific problems which initiated the study, i.e., (1) the cracking of the HPFTP second stage blades, and (2) the suspected hot gas leakage into the coolant cavity behind the aft-platform seal bolts.

As far as the blade cracking is concerned, the model has shown that the second stage blade shanks are subjected to varying degrees of thermal stress, both steady state and once per revolution. The severity of this gradient has been shown to be sensitive to asymmetries in the external pressure and to variations in the geometrical clearances. At the time of this writing, however, it is believed that the primary cause of cracking is not due to thermal effects but is the result of a very high mean mechanical stress coupled with the moderate thermal stress. The proposed solution to alleviate the cracking is to recontour the shank in the high stress area, to shot-peen the surface to reduce the surface mean operating stress, and to coat the shanks to reduce the thermal stress [8].

As for the variations in coolant liner pressure and temperature thought to be indicative of a leak into the coolant liner, they remain an enigma. In order to gain a clearer understanding of this problem, the fluid temperatures calculated in the current study will be used as an input to the thermal stress analysis of the hardware. Prior to this study it was believed that the temperatures in the cavity were on the order of 900°R hotter than predicted here [8]. With a better estimate of the fluid temperature, the thermal stress analysis will be better able to predict the deformation of the aft-platform seal and the other components neighboring the aft-platform seal cavity. This will, in turn, generate improved estimates of the clearances and flowrates in the region.

The new flowrates estimated from the above will be fed back into the PHOENICS model for an improved analysis of the flow and temperature field in the cavity. Other changes which could be incorporated into the model would be to include the effect of heat transfer into the cavity and the viscous heating of the fluid itself, both of which will result in increases in the cavity temperature.

In addition to further analytical studies and improvements, there are plans to build a fuel pump that has pressure and temperature measurements built into the aft-platform seal, the labyrinth seal, the lift-off seal stack, and the coolant liner [8]. The test data from this instrumented pump, in conjunction with the computer model predictions should greatly increase the level of understanding of the operating environment of the high pressure fuel pump aft-platform seal cavity.

REFERENCES

1. Lockheed Missiles and Space Company, Inc.: Fluid Flow Analysis of the SSME High Pressure Fuel Turbo-pump Operating at Full Power Level. LMSC-MSFC TR D697954, May 1980.
2. Spalding, D. B.: General Computer Program for Fluid Flow Heat Transfer and Chemical Reaction Process. International Finite Element Congress, Baden-Baden, West Germany, November 1980.
3. Keeton, L. W., Lowry, S. A., and Wayden, L.: Listings of Phoenix 2-D and 3-D Satellites and Ground Stations as Adapted for the SSME Aft-Platform Seal Cavity Flow Model. CHAM 4045/21, June 1985.
4. Rosten, H. I., Spalding, D. B., and Tatchell, D. G.: PHOENICS - An Instruction Manual. CHAM Report TR/75, January 1982.
5. Morrison, G. L., et al.: Labyrinth Seals for Incompressible Flow. NAS8-34536 Final Report, April 1983, p. 63.
6. Conversation with Garry Lyles, EP26, Marshall Space Flight Center, NASA, January 1985.
7. Wineland, D. L. and Cramer, K.: HPFTP Instrumented Turbine Test Data. Rockwell International, September 12, 1982, p. F3.
8. Conversation with Rick Ryan, EP23, Marshall Space Flight Center, NASA, June 1985.

**APPENDIX A: PHOENICS COMPUTER CODE
SATELLITE AND GROUND ADAPTATIONS
FOR THE SPACE SHUTTLE MAIN ENGINE HPFTP
AFT-PLATFORM SEAL CAVITY 3-D MODEL**

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1 \$BATCH
2 C\$DIRECTIVE**SATLIT
3 C ***
4 C *FILE NAME: DSK32SAT.FTN
5 C ***
6 C *ABSTRACT: SATELLITE FOR SSME AFT-PLATFORM SEAL 3-D MODEL (2 EXITS)
7 C ***
8 C *DOCUMENTATION: PHOENICS INSTRUCTION MANUAL (SPRING 1983).
9 C *AUXILIARY SUBROUTINES (TAPES, ETC.) ARE IN SATELLITE LIBRARY
10 C SERVICEU, WHICH MUST BE INCLUDED IN LINK EDIT TO RUN.
11 C CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX STANDARD SECTION 1 STARTS:
12 C-----
13 C
14 C CHAPTER 1 COMMON BLOCKS AND USER'S DATA.
15 C-----
16 C \$INCLUDE 9.CMNGUSST.FTN/G
17 C \$INCLUDE 9.GUSSEQUI.FTN/G
18 C \$INCLUDE 9.CMNGRFIC.FTN/G
19 C COMMON/GPI/IPWRIT.IDUM(243)
20 C DIMENSION GOTAPE(3),DFAULT(4)
21 C DIMENSION ARRAY1(309),ARRAY2(194),ARRAY3(421)
22 C LOGICAL ARRAY1,LSPDA,WRT,RD,NAMLST
23 C INTEGER ARRAY2,XPLANE,YPLANE,ZPLANE
24 C INTEGER P1,PP,U1,U2,V1,V2,W1,W2,R1,R2,RS,EP,H1,H2,H3,C1,C2,
25 C &C3,C4
26 C REAL NORTH,LOW
27 C EQUIVALENCE (ARRAY1(1),CARTES), (ARRAY2(1),NX)
28 C EQUIVALENCE (ARRAY3(1),SPARE1(1)), (M1,R1), (M2,R2)
29 C EQUIVALENCE (LSTRUN,INTGR(12)), (NAMLST,LOGIC(88))
30 C CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX STANDARD SECTION 1 ENDS.
31 C CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX USER SECTION 1 STARTS:
32 C C GRAFFIC ARRAYS DIMENSIONED AS NEEDED...
33 C ***
34 C COMMON/GRAF1/PHI1(134500) /GRAF2/PHI2(239500)
35 C COMMON/GRAF1/PHI1(1) /GRAF2/PHI2(1)
36 C ***
37 C POROSITY & SPECIAL DATA ARRAYS DIMENSIONED AS NEEDED...
38 C ***
39 C DIMENSION PE(8,40,28),PN(8,40,28),PH(8,40,28),PC(8,40,28)
40 C DIMENSION LSPDA(1),ISPDA(1),RSPDA(37)
41 C DIMENSION PEXIT(8),GEXIT(8)
42 C ***
43 C USER PLACES HIS VARIABLES, ARRAYS, EQUIVALENCES ETC. HERE.
44 C ***
45 C DATA NLSP,NLSP,NRSP/1,1,37/
46 C EQUIVALENCE (RSPDA(17),PEXIT(1)), (RSPDA(30),GEXIT(1))
47 C ***
48 C USER PLACES HIS DATA STATEMENTS HERE.
49 C ***
50 C DATA PI,G,TINY/3.1416,32.174,1.E-10/
51 C CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX USER SECTION 1 ENDS.
52 C CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX STANDARD SECTION 2 STARTS:
53 C C-----
54 C CHAPTER 2 SET CONSTANTS, AND ARRANGE FILE MANIPULATIONS.
55 C-----
56 C PLEASE DO NOT ALTER, OR RE-SET, ANY OF THE REMAINING
57 C STATEMENTS OF THIS CHAPTER.
58 C DATA CELL,EAST,WEST,NORTH,SOUTH,HIGH,LOW,VOLUME/
59 C & O..1..2..3..4..5..6..7. /

```

60 DATA P1,PP,U1,U2,V1,V2,W1,W2,R1,R2,RS,KE,EP,H1,H2,H3,C1,C2,
61 &C3,C4/1,2,3,4,5,6,7,8,9,10,11,12,13,14,15,16,17,18,19,20/
62 DATA FIXELU, FIXVAL, ONLYMS, WALL/1,E-10,1,E10,O.O,-10.O/
63 DATA IPLANE, YPLANE, ZPLANE/O,1,2,3/
64 DATA WRT, RD, DFAULT/.TRUE.,.FALSE.,.4HDEFA,4HULT.,.4HDTA/,1HG/
65 DATA GDTAPE/4HGUSI,4HE1,D,2HTA/
66 DATA NLDATA,NIDATA,NRDATA/309,194,421/
67 DATA NLCREG,NICVRG/60,350/
68 CALL TAPES(10,GDTAPE,3,1,4*NRDATA)
69 C-----READ DEFAULT FILE IF BLOCKDATA ABSENT
70 IF (INTGR1(29).NE.10) GO TO 2
71 CALL WRIT40(40HDATA ESTABLISHED IN BLOCK DATA. )
72 GO TO 3
73
74 2 CALL TAPES(1,DFAULT,4,2,4*NRDATA)
75 CALL DATAIO(RD,1)
76
77 3 CALL WRIT40(40HFILE MODSTL.FTN IS THE SATLIT USED. )
78 C-----
79 CHAPTER 3 DEFINE DATA FOR NRUN RUNS.
80 C-----
81 CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX STANDARD SECTION 2 ENDS.
82 CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX
83
84 LOGIC(89)=.TRUE.
85 DO 410 II=1,1
86 410 RUN(II)=.TRUE.
87 C *****
88 C ***** INPUTS *****
89 C *****
90 C *****
91 C *****
92 C ***** GEOMETRY *****
93 C *****
94 C ** SET GINC1 TO THE (LARGE) GAP HT (IN) AT THE COLD INLET
95 GINC1 = .10693
96
97 C ** SET GEXIT1 = THE AVERAGE GAP CLEARANCE AT THE EXIT (INCHES)
98 NB. SHOULD NOT BE LARGER THAN CELL WIDTH (=0.03333)
99 GEXIT1 = .0108
100
101 C ** SET ECCENT = THE RADIAL ECCENTRICITY (INCHES) OF THE ROTOR IN
102 THE CELL 1 (11:30) DIRECTION. THIS ECCENTRICITY WOULD NORMALLY
103 BE LIMITED BY THE CLEARANCE OF THE LABYRINTH SEAL (GINC1S) AT
104 ITS NARROWEST (IE WHERE "TEETH" MEET SHAFT).
105 THE ECCENTRICITY EFFECTS BOTH THE EXIT GAP AT THE HOT GAS EXIT
106 AND THE DISTRIBUTION OF FLOW AT THE LABYRINTH SEAL INLET.
107 GINC1S=0.003
108
109 C ECCENT = GINC1S
110
111 C ** SET GEXIT ARRAY TO ACTUAL REQUIRED GAP CLEARANCE AT EXIT (FEET)
112 (SEE DESCRIPTION OF PEXIT ARRAY BELOW FOR CLOCKING CONVENTION)
113
114 C NB. GEXIT ARRAY CALCULATIONS BELOW ARE GRID DEPENDENT!!!
115
116 C SET GEXIT(1) TO AVERAGE GAP CLEARANCE AT 11:30
117 GEXIT(1)=(GEXIT1+COS(O.)*ECCENT)/12.
118
119 C SET GEXIT(2) TO AVERAGE GAP CLEARANCE AT 10:00
120 GEXIT(2)=(GEXIT1+COS(2.*PI/8.)*ECCENT)/12.

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120 C SET GEXIT(3) TO AVERAGE GAP CLEARANCE AT 8:30
121 GEXIT(3)=(GEXIT1+COS(2.*PI/4.)*ECCENT)/12.
122 C SET GEXIT(4) TO AVERAGE GAP CLEARANCE AT 7:00
123 GEXIT(4)=(GEXIT1+COS(2.*PI*3./8.)*ECCENT)/12.
124 C SET GEXIT(5) TO AVERAGE GAP CLEARANCE AT 5:30
125 GEXIT(5)=(GEXIT1+COS(PI)*ECCENT)/12.
126 C SET GEXIT(6) TO AVERAGE GAP CLEARANCE AT 4:00
127 GEXIT(6)=(GEXIT1+COS(2.*PI*5./8.)*ECCENT)/12.
128 C SET GEXIT(7) TO AVERAGE GAP CLEARANCE AT 2:30
129 GEXIT(7)=(GEXIT1+COS(2.*PI*3./4.)*ECCENT)/12.
130 C SET GEXIT(8) TO AVERAGE GAP CLEARANCE AT 1:00
131 GEXIT(8)=(GEXIT1+COS(2.*PI*7./8.)*ECCENT)/12.
132 C
133 CC ** SET AINHI TO THE AREA (SQ IN) AT THE HOT INLET
134 AINHI = 3.877
135 CC ** SET ARGDD1 = THE HIGH FACE GRID AREA (SQ IN) AT THE HOT INLET
136 ARGDD1 = 8.143
137 CC ** 1/SLICES = THE FRACTION OF 360 DEGREES BEING MODELLED
138 SLICES=1.0
139 CC
140 CC *** PROPERTIES
141 CC
142 CC ** SET H1INC1 TO THE ENTHALPY (BTU/LBM) AT THE COLD INLET
143 H1INC1=278.3
144 CC ** SET H1INH1 TO THE ENTHALPY (BTU/LBM) AT THE HOT INLET
145 H1INH1=3380.
146 CC ** SET HEXIT1 TO THE ENTHALPY (BTU/LBM) OF THE TURBINE EXIT
147 HEXIT1=3895.4
148 CC ** SET ROINC1 TO THE DENSITY (LBM /CU FT) AT THE COLD INLET
149 ROINC1 =3.574
150 CC ** SET ROINH1 TO THE DENSITY ( LBM /CU FT) AT THE HOT INLET
151 ROINH1 = .931
152 C *** NOTE: THE DIRECTION OF ROTATION OF THE TURBINE IS
153 C COUNTERCLOCKWISE ACCORDING TO THE CLOCKING CONVENTION
154 C USED IN ROCKETDYNE HPFTP INSTRUMENTED TURBINE TEST
155 C DATA REPORT P9-17-82
156 C THE PRESSURE OF 3582 IS AN AVERAGE OF
157 C THE 3D DATA (3505,3500,3615,3630,3645,3720,3565,3475) WHICH
158 C COMES FROM TEST #902-279 FPL DATA - IT CORRESPONDS TO AN
159 C AVERAGE COOLANT LINER PRESSURE OF 3800 PSI
160 C !!! NB. VALUES BELOW INCREMENTED IN ACCORDANCE WITH NEW DATA
161 C
162 CC ** SET PEXIT(1) TO THE PRESSURE (PSF) AT 11:30
163 PEXIT(1)= 144.0 * 3481.4
164 CC ** SET PEXIT(2) TO THE PRESSURE (PSF) AT 10:00
165 PEXIT(2)= 144.0 * 3476.4
166 CC ** SET PEXIT(3) TO THE PRESSURE (PSF) AT 8:30
167 PEXIT(3)= 144.0 * 3591.4
168 CC ** SET PEXIT(4) TO THE PRESSURE (PSF) AT 7:00
169 PEXIT(4)= 144.0 * 3606.4
170 CC ** SET PEXIT(5) TO THE PRESSURE (PSF) AT 5:30
171 PEXIT(5)= 144.0 * 3621.4
172 CC ** SET PEXIT(6) TO THE PRESSURE (PSF) AT 4:00
173 PEXIT(6)= 144.0 * 3696.4
174 CC ** SET PEXIT(7) TO THE PRESSURE (PSF) AT 2:30
175 PEXIT(7)= 144.0 * 3541.4
176 CC ** SET PEXIT(8) TO THE PRESSURE (PSF) AT 1:00
177 PEXIT(8)= 144.0 * 3451.4
178 C
179 CC ** SET PEXITA TO THE AVERAGE TURBINE DISCHARGE PRESSURE (PSF)
```

```

180 PEXITA= 144.0 * 3558.4
181
182 C
183 C*****
184 C SET UP EXIT PRESSURES AS UNIFORM
185 PEXIT(1)=PEXITA
186 PEXIT(2)=PEXITA
187 PEXIT(3)=PEXITA
188 PEXIT(4)=PEXITA
189 PEXIT(5)=PEXITA
190 PEXIT(6)=PEXITA
191 PEXIT(7)=PEXITA
192 PEXIT(8)=PEXITA
193
194 C*****
195 C *** BOUNDARY CONDITIONS
196
197 C ** INPUT RPM
198 RPM= 37000.
199
200 C ** SET FEEDC1 TO THE TOTAL MASS FLOWRATE (LBM/S)
201 AT THE COLD INLET
202 FEEDC1 = .2582
203
204 C ** SET FEEDH1 TO THE TOTAL MASS FLOWRATE (LBM/S)
205 AT THE HOT INLET
206 FEEDH1 = 3.649
207
208 C ** SET H2OINH TO THE H2O MASS FRACTION AT THE HOT INLET
209 H2OINH = .474
210
211 C ** SET H2OXIT TO THE H2O MASS FRACTION AT THE TURBINE EXIT
212 H2OXIT = .5
213
214 C ** SET GLOSK1 TO LOSS COEFFICIENT FOR LOSSES AT EXIT
215 NEAR BLADE ROOTS
216 GLOSK1=1.5 + TINY
217
218 C
219 C*****
220 C*****
221 C*****
222 C*****
223 C*****
224 C*****
225 C*****
226 C*****
227 C*****
228 C*****
229 C*****
230 C*****
231 C*****
232 C*****
233 C*****
234 C*****
235 C*****
236 C*****
237 C*****
238 C*****
239 C*****

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'TYPE' = EAST.

*DIMENSION ARRAYS PE(NX,NY,NZ), PN(NX,NY,NZ), PII(NX,NY,NZ), &
C OVER REGION IXF,...,IZL.
C WEST, NORTH, SOUTH, HIGH, LOW & CELL. 'VALUE' = WANTED POROSITY
C IR=RUN SECTION NUMBER, E.G. 1 FOR RUN1 SECTION
C CALL CONPOR(IR,TYPE,VALUE,IXF,IXL,IYF,IYL,IZF,IZL), WHERE:
C *SET CONSTANT POROSITIES OVER SUB-DOMAINS USING:
C --- GROUP 7. BLOCKAGE: BLOCK<F>.,IPLANE,IPWRIT
C --- MGRID,IZW1,IZW2,AZW2,BZW2,CZW2,PINT,ZW2M1T
C --- GROUP 6. MOVING GRID :
C --- ZWLAST= 2.5/12.1
C ZFRAC(1)= -14.0
C ZFRAC(2)= 2.0+1./50.0
C ZFRAC(3)= 2.0
C ZFRAC(4)= 1.0/50.0
C ZFRAC(5)= 8.0
C ZFRAC(6)= 1.0/(2.0+50.0)
C ZFRAC(7)= 1.0
C ZFRAC(8)= 1.0/50.0
C ZFRAC(9)= 3.0
C ZFRAC(10)= 5.0+1./50.0
C --- GROUP 5. Z-DIRECTION :
C NZ<1>.,ZWLAST<1.0>.,ZFRAC(1-30)
C SERVICE SUBROUTINE FOR POWER-LAW GRID:
C CALL GRODPR(3,NZ,ZWLAST,POWER)
C NZ= 28
C *** 2.5= DISTANCE FROM THE LEFT WALL OF THE CAVITY
C TO THE RIGHT SIDE OF THE GRID (INCHES).
C ZWLAST= 2.5/12.1
C ZFRAC(1)= -14.0
C ZFRAC(2)= 2.0+1./50.0
C ZFRAC(3)= 2.0
C ZFRAC(4)= 1.0/50.0
C ZFRAC(5)= 8.0
C ZFRAC(6)= 1.0/(2.0+50.0)
C ZFRAC(7)= 1.0
C ZFRAC(8)= 1.0/50.0
C ZFRAC(9)= 3.0
C ZFRAC(10)= 5.0+1./50.0
C --- GROUP 4. Y-DIRECTION :
C NY<1>.,YVLAST<1.0>.,YFRAC(1-30),RINNER,SNALFA
C SERVICE SUBROUTINE FOR POWER-LAW GRID:
C CALL GRODPR(2,NY,YVLAST,POWER)
C NY= 40
C *** 2.6 = DISTANCE FROM THE INNER CAVITY RADIUS
C TO THE OUTER RADIUS (INCHES)
C YVLAST= 2.6/12.
C YFRAC(1)= -14.0
C YFRAC(2)= 1./26.0
C YFRAC(3)= 6.0
C YFRAC(4)= 1./(2.0+26.0)
C YFRAC(5)= 2.0
C YFRAC(6)= 1./26.0
C YFRAC(7)= 6.0
C YFRAC(8)= 1.0/(2.0+26.0)
C YFRAC(9)= 12.0
C YFRAC(10)= 1.0/(3.0+26.0)
C RINNER= 1.87/12.
C --- GROUP 3. X-DIRECTION :
C NX<1>.,XULAST<1.0>.,XFRAC(1-30)
C SERVICE SUBROUTINE FOR POWER-LAW GRID:
C CALL GRODPR(1,NX,XULAST,POWER)
C NX= 8
C XFRAC(1)= -8.0
C XFRAC(2)= 1./8.0
C XULAST= 2.*PI/SLICES
C --- CALL GRODPR(O,NT,TLAST,POWER)
C ---

```

300 C PC(NX,NY,NZ) ABOVE.
301 C FOR FULLY-BLOCKED CELLS (IE. 'VALUE' = 0.0) USER NEED SET ONLY
302 C THE 'CELL' POROSITY (TO ZERO), AS CELL-FACE AREAS ARE THEN
303 C AUTOMATICALLY ZEROED.
304 C *FOR SATELLITE PRINTOUT OF ALL POROSITIES IN DOMAIN, 'IPLANE' =
305 C XPLANE YPLANE OR ZPLANE, FOR DESIRED CROSS-SECTION DIRECTION.
306 C *FOR EACH 'TYPE' A MAXIMUM OF 10 CALLS TO CONPOR IS ALLOWED.
307 C BUT IF REQUIREMENTS EXCEED THIS PROVISION SET BLOCK=.T. &
308 C IPWRIT=-1, AND SET POROSITY ARRAYS EXPLICITLY HERE AS WANTED.
309 C IN THIS CASE, THE USER MUST SET ALL ELEMENTS OF
310 C ARRAYS PE, PN, PH, PC (MANY MAY BE 0.0 OR 1.0). HE MAY USE:
311 C CALL CR(PARRAY,VALUE,IXL,IYF,IYL,IZF,IZL,NX,NY,NZ)
312 C ANY NUMBER OF TIMES, TO SET 'PARRAY' (= PE, ETC.) TO
313 C 'VALUE' OVER RANGE IXF TO IXL, IYF TO IYL, IZF TO IZL.
314 C *CONPOR MUST NOT BE USED IN CONJUNCTION WITH EXPLICIT
315 C SETTINGS OF THE ARRAYS (INCLUDING SETTINGS VIA CR).
316 C BLOCK= .TRUE.
317 C IPWRIT= -1
318 C *** INITIALIZE ALL POROSITIES TO 1.0 (OPEN)
319 C DO 70 IX = 1,NX
320 C DO 70 IY = 1,NY
321 C DO 70 IZ = 1,NZ
322 C PE(IX,IY,IZ) = 1.0
323 C PN(IX,IY,IZ) = 1.0
324 C PH(IX,IY,IZ) = 1.0
325 C PC(IX,IY,IZ) = 1.0
326 C
327 C *** ROW 1 (BOTTOM)
328 C CALL CR(PC,O.O,1,NX, 1, 1, 1,12,NX,NY,NZ)
329 C CALL CR(PN,O.O,1,NX, 1, 1, 1,13,NX,NY,NZ)
330 C CALL CR(PE,O.O,1,NX, 1, 1, 1,12,NX,NY,NZ)
331 C CALL CR(PH,O.O,1,NX, 1, 1, 1,12,NX,NY,NZ)
332 C
333 C CALL CR(PC,O.O,1,NX, 1, 1,20,28,NX,NY,NZ)
334 C CALL CR(PN,O.O,1,NX, 1, 1,20,28,NX,NY,NZ)
335 C CALL CR(PE,O.O,1,NX, 1, 1,20,28,NX,NY,NZ)
336 C CALL CR(PH,O.O,1,NX, 1, 1,19,28,NX,NY,NZ)
337 C
338 C *** ROW 2
339 C CALL CR(PC,O.O,1,NX, 2, 2, 1,13,NX,NY,NZ)
340 C CALL CR(PN,O.O,1,NX, 2, 2, 1,13,NX,NY,NZ)
341 C CALL CR(PE,O.O,1,NX, 2, 2, 1,13,NX,NY,NZ)
342 C CALL CR(PH,O.O,1,NX, 2, 2, 1,13,NX,NY,NZ)
343 C
344 C CALL CR(PC,O.O,1,NX, 2, 2,22,28,NX,NY,NZ)
345 C CALL CR(PN,O.O,1,NX, 2, 2,22,28,NX,NY,NZ)
346 C CALL CR(PE,O.O,1,NX, 2, 2,22,28,NX,NY,NZ)
347 C CALL CR(PH,O.O,1,NX, 2, 2,21,28,NX,NY,NZ)
348 C
349 C *** ROW 3
350 C CALL CR(PC,O.O,1,NX, 3, 3, 1, 4,NX,NY,NZ)
351 C CALL CR(PN,O.O,1,NX, 3, 3, 1, 4,NX,NY,NZ)
352 C CALL CR(PE,O.O,1,NX, 3, 3, 1, 4,NX,NY,NZ)
353 C CALL CR(PH,O.O,1,NX, 3, 3, 1, 4,NX,NY,NZ)
354 C
355 C CALL CR(PC,O.5,1,NX, 3, 3, 5, 5,NX,NY,NZ)
356 C CALL CR(PN,1.0,1,NX, 3, 3, 5, 5,NX,NY,NZ)
357 C CALL CR(PE,O.5,1,NX, 3, 3, 5, 5,NX,NY,NZ)
358 C CALL CR(PH,1.0,1,NX, 3, 3, 5, 5,NX,NY,NZ)
359 C
360 C CALL CR(PC,O.5,1,NX, 3, 3,12,12,NX,NY,NZ)

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360 CALL CR(PN, 1, 0, 1, NX, 3, 3, 12, 12, NX, NY, NZ)
361 CALL CR(PE, 0, 5, 1, NX, 3, 3, 12, 12, NX, NY, NZ)
362 CALL CR(PH, 0, 0, 1, NX, 3, 3, 12, 12, NX, NY, NZ)
C
363
364 CALL CR(PC, 0, 0, 1, NX, 3, 3, 13, 13, NX, NY, NZ)
365 CALL CR(PN, 0, 0, 1, NX, 3, 3, 13, 13, NX, NY, NZ)
366 CALL CR(PE, 0, 0, 1, NX, 3, 3, 13, 13, NX, NY, NZ)
367 CALL CR(PH, 0, 0, 1, NX, 3, 3, 13, 13, NX, NY, NZ)
C
368
369 CALL CR(PC, 0, 0, 1, NX, 3, 3, 22, 28, NX, NY, NZ)
370 CALL CR(PN, 0, 0, 1, NX, 3, 3, 17, 28, NX, NY, NZ)
371 CALL CR(PE, 0, 0, 1, NX, 3, 3, 22, 28, NX, NY, NZ)
372 CALL CR(PH, 0, 0, 1, NX, 3, 3, 21, 28, NX, NY, NZ)
C
373
C *** ROW 4
374
375 CALL CR(PC, 0, 0, 1, NX, 4, 4, 1, 3, NX, NY, NZ)
376 CALL CR(PN, 0, 0, 1, NX, 4, 4, 1, 3, NX, NY, NZ)
377 CALL CR(PE, 0, 0, 1, NX, 4, 4, 1, 3, NX, NY, NZ)
378 CALL CR(PH, 0, 0, 1, NX, 4, 4, 1, 3, NX, NY, NZ)
C
379
380 CALL CR(PC, 15, 1, NX, 4, 4, 4, 4, NX, NY, NZ)
381 CALL CR(PN, 0, 5, 1, NX, 4, 4, 4, 4, NX, NY, NZ)
382 CALL CR(PE, 15, 1, NX, 4, 4, 4, 4, NX, NY, NZ)
383 CALL CR(PH, 75, 1, NX, 4, 4, 4, 4, NX, NY, NZ)
C
384
385 CALL CR(PC, 0, 0, 1, NX, 4, 4, 13, 13, NX, NY, NZ)
386 CALL CR(PN, 0, 0, 1, NX, 4, 4, 13, 13, NX, NY, NZ)
387 CALL CR(PE, 0, 0, 1, NX, 4, 4, 13, 13, NX, NY, NZ)
388 CALL CR(PH, 0, 0, 1, NX, 4, 4, 12, 13, NX, NY, NZ)
C
389
390 CALL CR(PC, 0, 0, 1, NX, 4, 4, 17, 28, NX, NY, NZ)
391 CALL CR(PN, 0, 0, 1, NX, 4, 4, 17, 28, NX, NY, NZ)
392 CALL CR(PE, 0, 0, 1, NX, 4, 4, 17, 28, NX, NY, NZ)
393 CALL CR(PH, 0, 0, 1, NX, 4, 4, 16, 28, NX, NY, NZ)
C
394
C *** ROW 5
395
396 CALL CR(PC, 0, 0, 1, NX, 5, 5, 1, 3, NX, NY, NZ)
397 CALL CR(PN, 0, 0, 1, NX, 5, 5, 1, 3, NX, NY, NZ)
398 CALL CR(PE, 0, 0, 1, NX, 5, 5, 1, 3, NX, NY, NZ)
399 CALL CR(PH, 0, 0, 1, NX, 5, 5, 1, 3, NX, NY, NZ)
C
400
401 CALL CR(PC, 75, 1, NX, 5, 5, 4, 4, NX, NY, NZ)
402 CALL CR(PN, 1, 0, 1, NX, 5, 5, 4, 4, NX, NY, NZ)
403 CALL CR(PE, 75, 1, NX, 5, 5, 4, 4, NX, NY, NZ)
404 CALL CR(PH, 1, 0, 1, NX, 5, 5, 4, 4, NX, NY, NZ)
C
405
406 CALL CR(PC, 30, 1, NX, 5, 5, 13, 13, NX, NY, NZ)
407 CALL CR(PN, 1, 0, 1, NX, 5, 5, 13, 13, NX, NY, NZ)
408 CALL CR(PE, 30, 1, NX, 5, 5, 13, 13, NX, NY, NZ)
409 CALL CR(PH, 30, 1, NX, 5, 5, 12, 13, NX, NY, NZ)
C
410
411 CALL CR(PC, 0, 0, 1, NX, 5, 5, 21, 28, NX, NY, NZ)
412 CALL CR(PN, 0, 0, 1, NX, 5, 5, 21, 28, NX, NY, NZ)
413 CALL CR(PE, 0, 0, 1, NX, 5, 5, 21, 28, NX, NY, NZ)
414 CALL CR(PH, 0, 0, 1, NX, 5, 5, 20, 28, NX, NY, NZ)
C
415
C *** ROW 6
416
417 CALL CR(PC, 0, 0, 1, NX, 6, 6, 1, 2, NX, NY, NZ)
418 CALL CR(PN, 0, 0, 1, NX, 6, 6, 1, 2, NX, NY, NZ)
419 CALL CR(PE, 0, 0, 1, NX, 6, 6, 1, 2, NX, NY, NZ)

420	C	CALL CR(PH,O.O,1,NX, 6, 6, 1, 2,NX,NY,NZ)
421		
422		CALL CR(PC,.25,1,NX, 6, 6, 3, 3,NX,NY,NZ)
423		CALL CR(PN,O.5,1,NX, 6, 6, 3, 3,NX,NY,NZ)
424		CALL CR(PE,.25,1,NX, 6, 6, 3, 3,NX,NY,NZ)
425		CALL CR(PH,1.O,1,NX, 6, 6, 3, 3,NX,NY,NZ)
426	C	
427		CALL CR(PC,O.O,1,NX, 6, 6,21,28,NX,NY,NZ)
428		CALL CR(PN,O.O,1,NX, 6, 6,21,28,NX,NY,NZ)
429		CALL CR(PE,O.O,1,NX, 6, 6,21,28,NX,NY,NZ)
430		CALL CR(PH,O.O,1,NX, 6, 6,20,28,NX,NY,NZ)
431	C	
432	C ***	ROW 7
433		CALL CR(PC,O.O,1,NX, 7, 7, 1, 2,NX,NY,NZ)
434		CALL CR(PN,O.O,1,NX, 7, 7, 1, 2,NX,NY,NZ)
435		CALL CR(PE,O.O,1,NX, 7, 7, 1, 2,NX,NY,NZ)
436		CALL CR(PH,O.O,1,NX, 7, 7, 1, 2,NX,NY,NZ)
437	C	
438		CALL CR(PC,.85,1,NX, 7, 7, 3, 3,NX,NY,NZ)
439		CALL CR(PN,1.O,1,NX, 7, 7, 3, 3,NX,NY,NZ)
440		CALL CR(PE,.85,1,NX, 7, 7, 3, 3,NX,NY,NZ)
441		CALL CR(PH,1.O,1,NX, 7, 7, 3, 3,NX,NY,NZ)
442	C	
443		CALL CR(PC,O.O,1,NX, 7, 7,21,28,NX,NY,NZ)
444		CALL CR(PN,O.O,1,NX, 7, 7,21,28,NX,NY,NZ)
445		CALL CR(PE,O.O,1,NX, 7, 7,21,28,NX,NY,NZ)
446		CALL CR(PH,O.O,1,NX, 7, 7,20,28,NX,NY,NZ)
447	C	
448	C ***	ROW 8
449		CALL CR(PC,O.O,1,NX, 8, 8, 1, 1,NX,NY,NZ)
450		CALL CR(PN,O.O,1,NX, 8, 8, 1, 1,NX,NY,NZ)
451		CALL CR(PE,O.O,1,NX, 8, 8, 1, 1,NX,NY,NZ)
452		CALL CR(PH,O.O,1,NX, 8, 8, 1, 1,NX,NY,NZ)
453	C	
454		CALL CR(PC,O.5,1,NX, 8, 8, 2, 2,NX,NY,NZ)
455		CALL CR(PN,.75,1,NX, 8, 8, 2, 2,NX,NY,NZ)
456		CALL CR(PE,O.5,1,NX, 8, 8, 2, 2,NX,NY,NZ)
457		CALL CR(PH,1.O,1,NX, 8, 8, 2, 2,NX,NY,NZ)
458	C	
459		CALL CR(PC,O.O,1,NX, 8, 8,21,28,NX,NY,NZ)
460		CALL CR(PN,O.O,1,NX, 8, 8,21,28,NX,NY,NZ)
461		CALL CR(PE,O.O,1,NX, 8, 8,21,28,NX,NY,NZ)
462		CALL CR(PH,O.O,1,NX, 8, 8,20,28,NX,NY,NZ)
463	C	
464	C ***	ROW 9
465		CALL CR(PC,O.O,1,NX, 9, 9, 1, 1,NX,NY,NZ)
466		CALL CR(PN,O.O,1,NX, 9, 9, 1, 1,NX,NY,NZ)
467		CALL CR(PE,O.O,1,NX, 9, 9, 1, 1,NX,NY,NZ)
468		CALL CR(PH,O.O,1,NX, 9, 9, 1, 1,NX,NY,NZ)
469	C	
470		CALL CR(PC,O.O,1,NX, 9, 9,21,28,NX,NY,NZ)
471		CALL CR(PN,O.O,1,NX, 9, 9,21,28,NX,NY,NZ)
472		CALL CR(PE,O.O,1,NX, 9, 9,21,28,NX,NY,NZ)
473		CALL CR(PH,O.O,1,NX, 9, 9,20,28,NX,NY,NZ)
474	C	
475		CALL CR(PC,.90,1,NX, 9, 9,2,2,NX,NY,NZ)
476		CALL CR(PN,1.O,1,NX, 9, 9,2,2,NX,NY,NZ)
477		CALL CR(PE,.90,1,NX, 9, 9,2,2,NX,NY,NZ)
478		CALL CR(PH,1.O,1,NX, 9, 9,2,2,NX,NY,NZ)
479	C	

C *** ROW 10
480 CALL CR(PC, .40, 1, NX, 10, 10, 2, 2, NX, NY, NZ)
481 CALL CR(PN, 0, 0, 1, NX, 10, 10, 1, 2, NX, NY, NZ)
482 CALL CR(PE, .40, 1, NX, 10, 10, 2, 2, NX, NY, NZ)
483 CALL CR(PH, .20, 1, NX, 10, 10, 2, 2, NX, NY, NZ)
484 CALL CR(PC, .20, 1, NX, 10, 10, 3, 3, NX, NY, NZ)
485 CALL CR(PN, 0, 0, 1, NX, 10, 10, 3, 3, NX, NY, NZ)
486 CALL CR(PE, .20, 1, NX, 10, 10, 3, 3, NX, NY, NZ)
487 CALL CR(PH, .30, 1, NX, 10, 10, 3, 3, NX, NY, NZ)
488 CALL CR(PC, .80, 1, NX, 10, 10, 4, 4, NX, NY, NZ)
489 CALL CR(PN, .35, 1, NX, 10, 10, 4, 4, NX, NY, NZ)
490 CALL CR(PE, .80, 1, NX, 10, 10, 4, 4, NX, NY, NZ)
491 CALL CR(PH, 1, 0, 1, NX, 10, 10, 4, 4, NX, NY, NZ)
492 CALL CR(PC, 1, 0, 1, NX, 10, 10, 20, 20, NX, NY, NZ)
493 CALL CR(PN, 1, 0, 1, NX, 10, 10, 20, 20, NX, NY, NZ)
494 CALL CR(PE, 1, 0, 1, NX, 10, 10, 20, 20, NX, NY, NZ)
495 CALL CR(PH, .20, 1, NX, 10, 10, 20, 20, NX, NY, NZ)
496 CALL CR(PC, .20, 1, NX, 10, 10, 21, 21, NX, NY, NZ)
497 CALL CR(PN, 1, 0, 1, NX, 10, 10, 21, 21, NX, NY, NZ)
498 CALL CR(PE, .20, 1, NX, 10, 10, 21, 21, NX, NY, NZ)
499 CALL CR(PH, .15, 1, NX, 10, 10, 21, 21, NX, NY, NZ)
500 CALL CR(PC, .10, 1, NX, 10, 10, 22, 22, NX, NY, NZ)
501 CALL CR(PN, 1, 0, 1, NX, 10, 10, 22, 22, NX, NY, NZ)
502 CALL CR(PE, .10, 1, NX, 10, 10, 22, 22, NX, NY, NZ)
503 CALL CR(PH, 0, 0, 1, NX, 10, 10, 22, 22, NX, NY, NZ)
504 CALL CR(PC, .10, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
505 CALL CR(PN, 0, 0, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
506 CALL CR(PE, .10, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
507 CALL CR(PH, 0, 0, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
508 CALL CR(PC, .10, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
509 CALL CR(PN, 0, 0, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
510 CALL CR(PE, .10, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
511 CALL CR(PH, 0, 0, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
512 CALL CR(PC, .10, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
513 CALL CR(PN, 0, 0, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
514 CALL CR(PE, .10, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
515 CALL CR(PH, 0, 0, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
516 CALL CR(PC, .10, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
517 CALL CR(PN, 0, 0, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
518 CALL CR(PE, .10, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
519 CALL CR(PH, 0, 0, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
520 CALL CR(PC, .10, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
521 CALL CR(PN, 0, 0, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
522 CALL CR(PE, .10, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
523 CALL CR(PH, 0, 0, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
524 CALL CR(PC, .10, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
525 CALL CR(PN, 0, 0, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
526 CALL CR(PE, .10, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
527 CALL CR(PH, 0, 0, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
528 CALL CR(PC, .10, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
529 CALL CR(PN, 0, 0, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
530 CALL CR(PE, .10, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
531 CALL CR(PH, 0, 0, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
532 CALL CR(PC, .10, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
533 CALL CR(PN, 0, 0, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
534 CALL CR(PE, .10, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
535 CALL CR(PH, .80, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
536 CALL CR(PC, .10, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
537 CALL CR(PN, 0, 0, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
538 CALL CR(PE, .10, 1, NX, 10, 10, 23, 28, NX, NY, NZ)
539 CALL CR(PH, 0, 0, 1, NX, 10, 10, 23, 28, NX, NY, NZ)

CALL	CR(PH,O.O,1,NX,11,11,24,24,NX,NY,NZ)
CALL	CR(PC,O.O,1,NX,11,11,25,28,NX,NY,NZ)
CALL	CR(PN,O.O,1,NX,11,11,25,28,NX,NY,NZ)
CALL	CR(PE,O.O,1,NX,11,11,25,28,NX,NY,NZ)
CALL	CR(PH,O.O,1,NX,11,11,25,28,NX,NY,NZ)
ROW 12	
CALL	CR(PC,O.O,1,NX,12,12,1,2,NX,NY,NZ)
CALL	CR(PN,O.O,1,NX,12,12,1,2,NX,NY,NZ)
CALL	CR(PE,O.O,1,NX,12,12,1,2,NX,NY,NZ)
CALL	CR(PH,O.O,1,NX,12,12,1,2,NX,NY,NZ)
CALL	CR(PC,O.O,1,NX,12,12,25,28,NX,NY,NZ)
CALL	CR(PN,O.O,1,NX,12,12,25,28,NX,NY,NZ)
CALL	CR(PE,O.O,1,NX,12,12,25,28,NX,NY,NZ)
CALL	CR(PH,O.O,1,NX,12,12,28,NX,NY,NZ)
ROW 13	
CALL	CR(PC,O.O,1,NX,13,13,1,2,NX,NY,NZ)
CALL	CR(PN,O.O,1,NX,13,13,1,2,NX,NY,NZ)
CALL	CR(PE,O.O,1,NX,13,13,1,2,NX,NY,NZ)
CALL	CR(PH,O.O,1,NX,13,13,1,2,NX,NY,NZ)
CALL	CR(PC,.90,1,NX,13,13,23,23,NX,NY,NZ)
CALL	CR(PN,O.O,1,NX,13,13,23,23,NX,NY,NZ)
CALL	CR(PE,.90,1,NX,13,13,23,23,NX,NY,NZ)
CALL	CR(PH,.80,1,NX,13,13,23,23,NX,NY,NZ)
CALL	CR(PC,O.5,1,NX,13,13,24,24,NX,NY,NZ)
CALL	CR(PN,O.O,1,NX,13,13,24,24,NX,NY,NZ)
CALL	CR(PE,O.5,1,NX,13,13,24,24,NX,NY,NZ)
CALL	CR(PH,O.O,1,NX,13,13,24,24,NX,NY,NZ)
CALL	CR(PC,O.O,1,NX,13,13,25,28,NX,NY,NZ)
CALL	CR(PN,O.O,1,NX,13,13,25,28,NX,NY,NZ)
CALL	CR(PE,O.O,1,NX,13,13,25,28,NX,NY,NZ)
CALL	CR(PH,O.O,1,NX,13,13,25,28,NX,NY,NZ)
ROW 14	
CALL	CR(PC,O.O,1,NX,14,14,1,2,NX,NY,NZ)
CALL	CR(PN,O.O,1,NX,14,14,1,2,NX,NY,NZ)
CALL	CR(PE,O.O,1,NX,14,14,1,2,NX,NY,NZ)
CALL	CR(PH,O.O,1,NX,14,14,1,2,NX,NY,NZ)
CALL	CR(PC,O.O,1,NX,14,14,21,28,NX,NY,NZ)
CALL	CR(PN,O.O,1,NX,14,14,21,28,NX,NY,NZ)
CALL	CR(PE,O.O,1,NX,14,14,21,28,NX,NY,NZ)
CALL	CR(PH,O.O,1,NX,14,14,20,28,NX,NY,NZ)
ROW 15	
CALL	CR(PC,O.O,1,NX,15,15,1,2,NX,NY,NZ)
CALL	CR(PN,O.O,1,NX,15,15,1,2,NX,NY,NZ)
CALL	CR(PE,O.O,1,NX,15,15,1,2,NX,NY,NZ)
CALL	CR(PH,O.O,1,NX,15,15,1,2,NX,NY,NZ)
CALL	CR(PC,.75,1,NX,15,15,23,23,NX,NY,NZ)
CALL	CR(PN,O.O,1,NX,15,15,23,23,NX,NY,NZ)
CALL	CR(PE,.75,1,NX,15,15,23,23,NX,NY,NZ)
CALL	CR(PH,O.5,1,NX,15,15,23,23,NX,NY,NZ)

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C 600 CALL CR(PC, .15, 1, NX, 15, 15, 24, 24, NX, NY, NZ)
601 CALL CR(PN, O.5, 1, NX, 15, 15, 24, 24, NX, NY, NZ)
602 CALL CR(PE, .15, 1, NX, 15, 15, 24, 24, NX, NY, NZ)
603 CALL CR(PH, O.1, NX, 15, 15, 24, 24, NX, NY, NZ)
604
605
C 606 CALL CR(PC, O.O, 1, NX, 15, 15, 25, 28, NX, NY, NZ)
607 CALL CR(PN, O.O, 1, NX, 15, 15, 25, 28, NX, NY, NZ)
608 CALL CR(PE, O.O, 1, NX, 15, 15, 25, 28, NX, NY, NZ)
609 CALL CR(PH, O.O, 1, NX, 15, 15, 25, 28, NX, NY, NZ)
610
C *** ROW 16
611 CALL CR(PC, O.O, 1, NX, 16, 16, 16, 1, 2, NX, NY, NZ)
612 CALL CR(PN, O.O, 1, NX, 16, 16, 1, 2, NX, NY, NZ)
613 CALL CR(PE, O.O, 1, NX, 16, 16, 1, 2, NX, NY, NZ)
614 CALL CR(PH, O.O, 1, NX, 16, 16, 1, 2, NX, NY, NZ)
615
616
C 617 CALL CR(PC, .15, 1, NX, 16, 16, 25, 25, NX, NY, NZ)
618 CALL CR(PN, .30, 1, NX, 16, 16, 25, 25, NX, NY, NZ)
619 CALL CR(PE, .15, 1, NX, 16, 16, 25, 25, NX, NY, NZ)
620 CALL CR(PH, O.O, 1, NX, 16, 16, 25, 25, NX, NY, NZ)
621
622 CALL CR(PC, O.O, 1, NX, 16, 16, 26, 28, NX, NY, NZ)
623 CALL CR(PN, O.O, 1, NX, 16, 16, 26, 28, NX, NY, NZ)
624 CALL CR(PE, O.O, 1, NX, 16, 16, 26, 28, NX, NY, NZ)
625 CALL CR(PH, O.O, 1, NX, 16, 16, 26, 28, NX, NY, NZ)
626
C *** ROW 17
627 CALL CR(PC, O.O, 1, NX, 17, 17, 1, 2, NX, NY, NZ)
628 CALL CR(PN, O.O, 1, NX, 17, 17, 1, 3, NX, NY, NZ)
629 CALL CR(PE, O.O, 1, NX, 17, 17, 1, 2, NX, NY, NZ)
630 CALL CR(PH, O.O, 1, NX, 17, 17, 1, 2, NX, NY, NZ)
631
632 CALL CR(PC, 1.O, 1, NX, 17, 17, 4, 4, NX, NY, NZ)
633 CALL CR(PN, O.4, 1, NX, 17, 17, 4, 4, NX, NY, NZ)
634 CALL CR(PE, 1.O, 1, NX, 17, 17, 4, 4, NX, NY, NZ)
635 CALL CR(PH, 1.O, 1, NX, 17, 17, 4, 4, NX, NY, NZ)
636
C 637 CALL CR(PC, O.5, 1, NX, 17, 17, 25, 25, NX, NY, NZ)
638 CALL CR(PN, .70, 1, NX, 17, 17, 25, 25, NX, NY, NZ)
639 CALL CR(PE, O.5, 1, NX, 17, 17, 25, 25, NX, NY, NZ)
640 CALL CR(PH, O.O, 1, NX, 17, 17, 25, 25, NX, NY, NZ)
641
642 CALL CR(PC, O.O, 1, NX, 17, 17, 26, 28, NX, NY, NZ)
643 CALL CR(PN, O.O, 1, NX, 17, 17, 26, 28, NX, NY, NZ)
644 CALL CR(PE, O.O, 1, NX, 17, 17, 26, 28, NX, NY, NZ)
645 CALL CR(PH, O.O, 1, NX, 17, 17, 26, 28, NX, NY, NZ)
646
C *** ROW 18
647 CALL CR(PC, O.O, 1, NX, 18, 18, 1, 3, NX, NY, NZ)
648 CALL CR(PN, O.O, 1, NX, 18, 18, 1, 3, NX, NY, NZ)
649 CALL CR(PE, O.O, 1, NX, 18, 18, 1, 3, NX, NY, NZ)
650 CALL CR(PH, O.O, 1, NX, 18, 18, 1, 3, NX, NY, NZ)
651
652 CALL CR(PC, .40, 1, NX, 18, 18, 4, 4, NX, NY, NZ)
653 CALL CR(PN, O.4, 1, NX, 18, 18, 4, 4, NX, NY, NZ)
654 CALL CR(PE, .40, 1, NX, 18, 18, 4, 4, NX, NY, NZ)
655 CALL CR(PH, 1.O, 1, NX, 18, 18, 4, 4, NX, NY, NZ)
656
C 657 CALL CR(PC, .75, 1, NX, 18, 18, 25, 25, NX, NY, NZ)
658
659

660	CALL CR(PN,.75,1,NX,18,18,25,25,NX,NY,NZ)
661	CALL CR(PE,.75,1,NX,18,18,25,25,NX,NY,NZ)
662	CALL CR(PH,O,O,1,NX,18,18,25,25,NX,NY,NZ)
663	C
664	CALL CR(PC,O,O,1,NX,18,18,26,28,NX,NY,NZ)
665	CALL CR(PN,O,O,1,NX,18,18,26,28,NX,NY,NZ)
666	CALL CR(PE,O,O,1,NX,18,18,26,28,NX,NY,NZ)
667	CALL CR(PH,O,O,1,NX,18,18,26,28,NX,NY,NZ)
668	C
669	C *** ROW 19
670	CALL CR(PC,O,O,1,NX,19,19,1,3,NX,NY,NZ)
671	CALL CR(PN,O,O,1,NX,19,19,1,3,NX,NY,NZ)
672	CALL CR(PE,O,O,1,NX,19,19,1,3,NX,NY,NZ)
673	CALL CR(PH,O,O,1,NX,19,19,1,3,NX,NY,NZ)
674	C
675	CALL CR(PC,.75,1,NX,19,19,4,4,NX,NY,NZ)
676	CALL CR(PN,1,O,1,NX,19,19,4,4,NX,NY,NZ)
677	CALL CR(PE,.75,1,NX,19,19,4,4,NX,NY,NZ)
678	CALL CR(PH,1,O,1,NX,19,19,4,4,NX,NY,NZ)
679	C
680	CALL CR(PC,.75,1,NX,19,19,25,25,NX,NY,NZ)
681	CALL CR(PN,.75,1,NX,19,19,25,25,NX,NY,NZ)
682	CALL CR(PE,.75,1,NX,19,19,25,25,NX,NY,NZ)
683	CALL CR(PH,O,O,1,NX,19,19,25,25,NX,NY,NZ)
684	C
685	CALL CR(PC,O,O,1,NX,19,19,26,28,NX,NY,NZ)
686	CALL CR(PN,O,O,1,NX,19,19,26,28,NX,NY,NZ)
687	CALL CR(PE,O,O,1,NX,19,19,26,28,NX,NY,NZ)
688	CALL CR(PH,O,O,1,NX,19,19,26,28,NX,NY,NZ)
689	C
690	C *** ROW 20
691	CALL CR(PC,O,O,1,NX,20,20,1,3,NX,NY,NZ)
692	CALL CR(PN,O,O,1,NX,20,20,1,3,NX,NY,NZ)
693	CALL CR(PE,O,O,1,NX,20,20,1,3,NX,NY,NZ)
694	CALL CR(PH,O,O,1,NX,20,20,1,3,NX,NY,NZ)
695	C
696	CALL CR(PC,O,9,1,NX,20,20,4,4,NX,NY,NZ)
697	CALL CR(PN,O,5,1,NX,20,20,4,4,NX,NY,NZ)
698	CALL CR(PE,O,9,1,NX,20,20,4,4,NX,NY,NZ)
699	CALL CR(PH,1,O,1,NX,20,20,4,4,NX,NY,NZ)
700	C
701	CALL CR(PC,O,5,1,NX,20,20,25,25,NX,NY,NZ)
702	CALL CR(PN,O,4,1,NX,20,20,25,25,NX,NY,NZ)
703	CALL CR(PE,O,5,1,NX,20,20,25,25,NX,NY,NZ)
704	CALL CR(PH,O,O,1,NX,20,20,25,25,NX,NY,NZ)
705	C
706	CALL CR(PC,O,O,1,NX,20,20,26,28,NX,NY,NZ)
707	CALL CR(PN,O,O,1,NX,20,20,26,28,NX,NY,NZ)
708	CALL CR(PE,O,O,1,NX,20,20,26,28,NX,NY,NZ)
709	CALL CR(PH,O,O,1,NX,20,20,26,28,NX,NY,NZ)
710	C
711	C *** ROW 21
712	CALL CR(PC,O,O,1,NX,21,21,1,3,NX,NY,NZ)
713	CALL CR(PN,O,O,1,NX,21,21,1,3,NX,NY,NZ)
714	CALL CR(PE,O,O,1,NX,21,21,1,3,NX,NY,NZ)
715	CALL CR(PH,O,O,1,NX,21,21,1,3,NX,NY,NZ)
716	C
717	CALL CR(PC,.05,1,NX,21,21,4,4,NX,NY,NZ)
718	CALL CR(PN,O,O,1,NX,21,21,4,4,NX,NY,NZ)
719	CALL CR(PE,.05,1,NX,21,21,4,4,NX,NY,NZ)

780	CALL CR(PC,O.2,1,NX,22,22,21,21,NX,NY,NZ)
781	CALL CR(PH,O.1,1,NX,22,22,21,21,NX,NY,NZ)
782	
783	CALL CR(PC,O.1,1,NX,22,22,22,22,NX,NY,NZ)
784	CALL CR(PN,O.1,1,NX,22,22,22,22,NX,NY,NZ)
785	CALL CR(PE,O.1,1,NX,22,22,22,22,NX,NY,NZ)
786	CALL CR(PH,O.1,1,NX,22,22,22,22,NX,NY,NZ)
787	
788	CALL CR(PC,O.O.1,NX,22,22,23,28,NX,NY,NZ)
789	CALL CR(PN,O.O.1,NX,22,22,23,28,NX,NY,NZ)
790	CALL CR(PE,O.O.1,NX,22,22,23,28,NX,NY,NZ)
791	CALL CR(PH,O.O.1,NX,22,22,23,28,NX,NY,NZ)
792	
793	C *** ROW 23
794	CALL CR(PC,O.O.1,NX,23,23, 1, 8,NX,NY,NZ)
795	CALL CR(PN,O.O.1,NX,23,23, 1, 8,NX,NY,NZ)
796	CALL CR(PE,O.O.1,NX,23,23, 1, 8,NX,NY,NZ)
797	CALL CR(PH,O.O.1,NX,23,23, 1, 8,NX,NY,NZ)
798	
799	CALL CR(PC,O.5,1,NX,23,23, 9, 9,NX,NY,NZ)
800	CALL CR(PN,O.O.1,NX,23,23, 9, 9,NX,NY,NZ)
801	CALL CR(PE,O.5,1,NX,23,23, 9, 9,NX,NY,NZ)
802	CALL CR(PH,1.O.1,NX,23,23, 9, 9,NX,NY,NZ)
803	
804	CALL CR(PC,O.O.1,NX,23,23,21,28,NX,NY,NZ)
805	CALL CR(PN,O.O.1,NX,23,23,21,28,NX,NY,NZ)
806	CALL CR(PE,O.O.1,NX,23,23,21,28,NX,NY,NZ)
807	CALL CR(PH,O.O.1,NX,23,23,20,28,NX,NY,NZ)
808	
809	C *** ROW 24
810	CALL CR(PC,O.O.1,NX,24,24, 1, 9,NX,NY,NZ)
811	CALL CR(PN,O.O.1,NX,24,24, 1, 9,NX,NY,NZ)
812	CALL CR(PE,O.O.1,NX,24,24, 1, 9,NX,NY,NZ)
813	CALL CR(PH,O.O.1,NX,24,24, 1, 9,NX,NY,NZ)
814	
815	CALL CR(PC,O.5,1,NX,24,24,10,10,NX,NY,NZ)
816	CALL CR(PN,O.O.1,NX,24,24,10,10,NX,NY,NZ)
817	CALL CR(PE,O.5,1,NX,24,24,10,10,NX,NY,NZ)
818	CALL CR(PH,1.O.1,NX,24,24,10,10,NX,NY,NZ)
819	
820	CALL CR(PC,O.O.1,NX,24,24,21,28,NX,NY,NZ)
821	CALL CR(PN,O.O.1,NX,24,24,21,28,NX,NY,NZ)
822	CALL CR(PE,O.O.1,NX,24,24,21,28,NX,NY,NZ)
823	CALL CR(PH,O.O.1,NX,24,24,20,28,NX,NY,NZ)
824	
825	C *** ROW 25
826	CALL CR(PC,O.O.1,NX,25,25, 1,10,NX,NY,NZ)
827	CALL CR(PN,O.O.1,NX,25,25, 1,10,NX,NY,NZ)
828	CALL CR(PE,O.O.1,NX,25,25, 1,10,NX,NY,NZ)
829	CALL CR(PH,O.O.1,NX,25,25, 1,10,NX,NY,NZ)
830	
831	CALL CR(PC,O.5,1,NX,25,25,11,11,NX,NY,NZ)
832	CALL CR(PN,O.O.1,NX,25,25,11,11,NX,NY,NZ)
833	CALL CR(PE,O.5,1,NX,25,25,11,11,NX,NY,NZ)
834	CALL CR(PH,1.O.1,NX,25,25,11,11,NX,NY,NZ)
835	
836	CALL CR(PC,O.O.1,NX,25,25,21,28,NX,NY,NZ)
837	CALL CR(PN,O.O.1,NX,25,25,21,28,NX,NY,NZ)
838	CALL CR(PE,O.O.1,NX,25,25,21,28,NX,NY,NZ)
839	CALL CR(PH,O.O.1,NX,25,25,20,28,NX,NY,NZ)

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840 CALL CR(PE.O.O.1,NX,25,25,21,28,NX,NY,NZ)
841 CALL CR(PH.O.O.1,NX,25,25,20,28,NX,NY,NZ)
842
843 C *** ROW 26
844 CALL CR(PC.O.O.1,NX,26,26, 1,11,NX,NY,NZ)
845 CALL CR(PN.O.O.1,NX,26,26, 1,11,NX,NY,NZ)
846 CALL CR(PE.O.O.1,NX,26,26, 1,11,NX,NY,NZ)
847 CALL CR(PH.O.O.1,NX,26,26, 1,11,NX,NY,NZ)
848
849 C
850 CALL CR(PC.O.5,1,NX,26,26,12,12,NX,NY,NZ)
851 CALL CR(PN.O.O.1,NX,26,26,12,12,NX,NY,NZ)
852 CALL CR(PE.O.5,1,NX,26,26,12,12,NX,NY,NZ)
853 CALL CR(PH,1.O,1,NX,26,26,12,12,NX,NY,NZ)
854
855 C
856 CALL CR(PC.O.O.1,NX,26,26,21,28,NX,NY,NZ)
857 CALL CR(PN.O.O.1,NX,26,26,21,28,NX,NY,NZ)
858 CALL CR(PE.O.O.1,NX,26,26,21,28,NX,NY,NZ)
859 CALL CR(PH.O.O.1,NX,26,26,20,28,NX,NY,NZ)
860 C *** ROW 27
861 CALL CR(PC.O.O.1,NX,27,27, 1,12,NX,NY,NZ)
862 CALL CR(PN.O.O.1,NX,27,27, 1,12,NX,NY,NZ)
863 CALL CR(PE.O.O.1,NX,27,27, 1,12,NX,NY,NZ)
864 CALL CR(PH.O.O.1,NX,27,27, 1,12,NX,NY,NZ)
865
866 C
867 CALL CR(PC.O.5,1,NX,27,27,13,13,NX,NY,NZ)
868 CALL CR(PN.O.O.1,NX,27,27,13,13,NX,NY,NZ)
869 CALL CR(PE.O.5,1,NX,27,27,13,13,NX,NY,NZ)
870 CALL CR(PH,1.O,1,NX,27,27,13,13,NX,NY,NZ)
871
872 C
873 CALL CR(PC.O.O.1,NX,27,27,21,28,NX,NY,NZ)
874 CALL CR(PN.O.O.1,NX,27,27,21,28,NX,NY,NZ)
875 CALL CR(PE.O.O.1,NX,27,27,20,28,NX,NY,NZ)
876 CALL CR(PH.O.O.1,NX,27,27,20,28,NX,NY,NZ)
877 C *** ROW 28
878 CALL CR(PC.O.O.1,NX,28,28, 1,13,NX,NY,NZ)
879 CALL CR(PN.O.O.1,NX,28,28, 1,13,NX,NY,NZ)
880 CALL CR(PE.O.O.1,NX,28,28, 1,13,NX,NY,NZ)
881 CALL CR(PH.O.O.1,NX,28,28, 1,13,NX,NY,NZ)
882
883 C
884 CALL CR(PC.O.5,1,NX,28,28,14,14,NX,NY,NZ)
885 CALL CR(PN.O.O.1,NX,28,28,14,14,NX,NY,NZ)
886 CALL CR(PE.O.5,1,NX,28,28,14,14,NX,NY,NZ)
887 CALL CR(PH,1.O,1,NX,28,28,14,14,NX,NY,NZ)
888
889 C
890 CALL CR(PC.O.O.1,NX,28,28,21,28,NX,NY,NZ)
891 CALL CR(PN.O.O.1,NX,28,28,21,28,NX,NY,NZ)
892 CALL CR(PE.O.O.1,NX,28,28,21,28,NX,NY,NZ)
893 CALL CR(PH.O.O.1,NX,28,28,20,28,NX,NY,NZ)
894 C *** ROW 29
895 CALL CR(PC.O.O.1,NX,29,29, 1,14,NX,NY,NZ)
896 CALL CR(PN.O.O.1,NX,29,29, 1,14,NX,NY,NZ)
897 CALL CR(PE.O.O.1,NX,29,29, 1,14,NX,NY,NZ)
898 CALL CR(PH.O.O.1,NX,29,29, 1,14,NX,NY,NZ)
899
900 C
901 CALL CR(PC,25,1,NX,29,29,15,15,NX,NY,NZ)
902 CALL CR(PN.O.O.1,NX,29,29,15,15,NX,NY,NZ)

```

900 CALL CR(PE,25,1,NX,29,29,15,15,NX,NY,NZ)
901 CALL CR(PH,75,1,NX,29,29,15,15,NX,NY,NZ)
902
903 C
904 CALL CR(PC,O,O,1,NX,29,29,21,28,NX,NY,NZ)
905 CALL CR(PN,O,O,1,NX,29,29,21,28,NX,NY,NZ)
906 CALL CR(PE,O,O,1,NX,29,29,21,28,NX,NY,NZ)
907 CALL CR(PH,O,O,1,NX,29,29,20,28,NX,NY,NZ)
908
909 C *** ROW 30
910 CALL CR(PC,O,O,1,NX,30,30,1,15,NX,NY,NZ)
911 CALL CR(PN,O,O,1,NX,30,30,1,15,NX,NY,NZ)
912 CALL CR(PE,O,O,1,NX,30,30,1,15,NX,NY,NZ)
913 CALL CR(PH,O,O,1,NX,30,30,1,15,NX,NY,NZ)
914
915 C
916 CALL CR(PC,O,6,1,NX,30,30,16,16,NX,NY,NZ)
917 CALL CR(PN,O,6,1,NX,30,30,16,16,NX,NY,NZ)
918 CALL CR(PE,O,6,1,NX,30,30,16,16,NX,NY,NZ)
919 CALL CR(PH,1,O,1,NX,30,30,16,16,NX,NY,NZ)
920
921 C
922 CALL CR(PC,O,O,1,NX,30,30,21,28,NX,NY,NZ)
923 CALL CR(PN,O,O,1,NX,30,30,21,28,NX,NY,NZ)
924 CALL CR(PE,O,O,1,NX,30,30,21,28,NX,NY,NZ)
925 CALL CR(PH,O,O,1,NX,30,30,21,28,NX,NY,NZ)
926
927 C *** ROW 31
928 CALL CR(PC,O,O,1,NX,31,31,1,15,NX,NY,NZ)
929 CALL CR(PN,O,O,1,NX,31,31,1,15,NX,NY,NZ)
930 CALL CR(PE,O,O,1,NX,31,31,1,15,NX,NY,NZ)
931 CALL CR(PH,O,O,1,NX,31,31,1,15,NX,NY,NZ)
932
933 C
934 CALL CR(PC,O,1,1,NX,31,31,16,16,NX,NY,NZ)
935 CALL CR(PN,O,1,1,NX,31,31,16,16,NX,NY,NZ)
936 CALL CR(PE,O,1,1,NX,31,31,16,16,NX,NY,NZ)
937 CALL CR(PH,1,O,1,NX,31,31,16,16,NX,NY,NZ)
938
939 C
940 CALL CR(PC,O,O,1,NX,31,31,21,28,NX,NY,NZ)
941 CALL CR(PN,O,O,1,NX,31,31,21,28,NX,NY,NZ)
942 CALL CR(PE,O,O,1,NX,31,31,21,28,NX,NY,NZ)
943 CALL CR(PH,O,O,1,NX,31,31,20,28,NX,NY,NZ)
944
945 C *** ROW 32
946 CALL CR(PC,O,O,1,NX,32,32,1,16,NX,NY,NZ)
947 CALL CR(PN,O,O,1,NX,32,32,1,16,NX,NY,NZ)
948 CALL CR(PE,O,O,1,NX,32,32,1,16,NX,NY,NZ)
949 CALL CR(PH,O,O,1,NX,32,32,1,16,NX,NY,NZ)
950
951 C
952 CALL CR(PC,O,8,1,NX,32,32,17,17,NX,NY,NZ)
953 CALL CR(PN,75,1,NX,32,32,17,17,NX,NY,NZ)
954 CALL CR(PE,O,8,1,NX,32,32,17,17,NX,NY,NZ)
955 CALL CR(PH,1,O,1,NX,32,32,17,17,NX,NY,NZ)
956
957 C *** NOTE: ROWS 32-40 CONTAIN THE HOT GAS PASSAGES THROUGH
958 THE TURBINE BLADE SHANKS. THE POROSITIES FOR THESE CELLS
959 (ROWS 32-40, COLUMNS 21-25) DEPEND ON THE RATIO OF THE HOT
    GAS INLET AREA TO THE CORRESPONDING GRID AREA (RAT)
    RAT= AINH1/ARGRD1
960
961 C
962 CALL CR(PC,RAT,1,NX,32,32,21,28,NX,NY,NZ)
963 CALL CR(PN,RAT,1,NX,32,32,21,28,NX,NY,NZ)
964 CALL CR(PE,1,O,1,NX,32,32,21,28,NX,NY,NZ)
965
966 C
967 CALL CR(PC,RAT,1,NX,32,32,21,28,NX,NY,NZ)
968 CALL CR(PN,RAT,1,NX,32,32,21,28,NX,NY,NZ)
969 CALL CR(PE,1,O,1,NX,32,32,21,28,NX,NY,NZ)
970
971 C
972 CALL CR(PC,RAT,1,NX,32,32,21,28,NX,NY,NZ)
973 CALL CR(PN,RAT,1,NX,32,32,21,28,NX,NY,NZ)
974 CALL CR(PE,1,O,1,NX,32,32,21,28,NX,NY,NZ)
975
976 C
977 CALL CR(PC,RAT,1,NX,32,32,21,28,NX,NY,NZ)
978 CALL CR(PN,RAT,1,NX,32,32,21,28,NX,NY,NZ)
979 CALL CR(PE,1,O,1,NX,32,32,21,28,NX,NY,NZ)
980
981 C
982 CALL CR(PC,RAT,1,NX,32,32,21,28,NX,NY,NZ)
983 CALL CR(PN,RAT,1,NX,32,32,21,28,NX,NY,NZ)
984 CALL CR(PE,1,O,1,NX,32,32,21,28,NX,NY,NZ)
985
986 C
987 CALL CR(PC,RAT,1,NX,32,32,21,28,NX,NY,NZ)
988 CALL CR(PN,RAT,1,NX,32,32,21,28,NX,NY,NZ)
989 CALL CR(PE,1,O,1,NX,32,32,21,28,NX,NY,NZ)
990
991 C
992 CALL CR(PC,RAT,1,NX,32,32,21,28,NX,NY,NZ)
993 CALL CR(PN,RAT,1,NX,32,32,21,28,NX,NY,NZ)
994 CALL CR(PE,1,O,1,NX,32,32,21,28,NX,NY,NZ)
995
996 C
997 CALL CR(PC,RAT,1,NX,32,32,21,28,NX,NY,NZ)
998 CALL CR(PN,RAT,1,NX,32,32,21,28,NX,NY,NZ)
999 CALL CR(PE,1,O,1,NX,32,32,21,28,NX,NY,NZ)
1000

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960 CALL CR(PH,RAT, 1,NX,32,32,20,28,NX,NY,NZ)
961
962 C *** ROW 33
963 CALL CR(PC,O.O, 1,NX,33,33, 1,16,NX,NY,NZ)
964 CALL CR(PN,O.O, 1,NX,33,33, 1,16,NX,NY,NZ)
965 CALL CR(PE,O.O, 1,NX,33,33, 1,16,NX,NY,NZ)
966 CALL CR(PH,O.O, 1,NX,33,33, 1,16,NX,NY,NZ)
967
968 C
969 CALL CR(PC, .75, 1,NX,33,33, 17,17,NX,NY,NZ)
970 CALL CR(PN,O.6, 1,NX,33,33, 17,17,NX,NY,NZ)
971 CALL CR(PE, .75, 1,NX,33,33, 17,17,NX,NY,NZ)
972 CALL CR(PH, 1.O, 1,NX,33,33, 17,17,NX,NY,NZ)
973
974 C
975 CALL CR(PC,RAT, 1,NX,33,33,21,28,NX,NY,NZ)
976 CALL CR(PN,RAT, 1,NX,33,33,21,28,NX,NY,NZ)
977 CALL CR(PE, 1.O, 1,NX,33,33,21,28,NX,NY,NZ)
978 CALL CR(PH,RAT, 1,NX,33,33,20,28,NX,NY,NZ)
979
980 C *** ROW 34
981 CALL CR(PC,O.O, 1,NX,34,34, 1,16,NX,NY,NZ)
982 CALL CR(PN,O.O, 1,NX,34,34, 1,16,NX,NY,NZ)
983 CALL CR(PE,O.O, 1,NX,34,34, 1,16,NX,NY,NZ)
984 CALL CR(PH,O.O, 1,NX,34,34, 1,16,NX,NY,NZ)
985
986 C
987 CALL CR(PC,O.6, 1,NX,34,34, 17,17,NX,NY,NZ)
988 CALL CR(PN,O.5, 1,NX,34,34, 17,17,NX,NY,NZ)
989 CALL CR(PE,O.6, 1,NX,34,34, 17,17,NX,NY,NZ)
990 CALL CR(PH, 1.O, 1,NX,34,34, 17,17,NX,NY,NZ)
991
992 C
993 CALL CR(PC,RAT, 1,NX,34,34,20,28,NX,NY,NZ)
994
995 C *** ROW 35
996 CALL CR(PC,O.O, 1,NX,35,35, 1,16,NX,NY,NZ)
997 CALL CR(PN,O.O, 1,NX,35,35, 1,16,NX,NY,NZ)
998 CALL CR(PE,O.O, 1,NX,35,35, 1,16,NX,NY,NZ)
999 CALL CR(PH,O.O, 1,NX,35,35, 1,16,NX,NY,NZ)
1000
1001 C
1002 CALL CR(PC,O.5, 1,NX,35,35, 17,17,NX,NY,NZ)
1003 CALL CR(PN,O.4, 1,NX,35,35, 17,17,NX,NY,NZ)
1004 CALL CR(PE,O.5, 1,NX,35,35, 17,17,NX,NY,NZ)
1005 CALL CR(PH, 1.O, 1,NX,35,35, 17,17,NX,NY,NZ)
1006
1007 C
1008 CALL CR(PC,RAT, 1,NX,35,35,21,28,NX,NY,NZ)
1009 CALL CR(PN,RAT, 1,NX,35,35,21,28,NX,NY,NZ)
1010 CALL CR(PE, 1.O, 1,NX,35,35,21,28,NX,NY,NZ)
1011 CALL CR(PH,RAT, 1,NX,35,35,20,28,NX,NY,NZ)
1012
1013 C *** ROW 36
1014 CALL CR(PC,O.O, 1,NX,36,36, 1,16,NX,NY,NZ)
1015 CALL CR(PN,O.O, 1,NX,36,36, 1,16,NX,NY,NZ)
1016 CALL CR(PE,O.O, 1,NX,36,36, 1,16,NX,NY,NZ)
1017 CALL CR(PH,O.O, 1,NX,36,36, 1,16,NX,NY,NZ)
1018
1019 C
1020 CALL CR(PC,O.3, 1,NX,36,36, 17,17,NX,NY,NZ)
1021 CALL CR(PN,O.3, 1,NX,36,36, 17,17,NX,NY,NZ)
1022 CALL CR(PE,O.3, 1,NX,36,36, 17,17,NX,NY,NZ)
1023 CALL CR(PH, 1.O, 1,NX,36,36, 17,17,NX,NY,NZ)

1020	C	
1021		CALL CR(PC,RAT,1,NX,36,36,21,28,NX,NY,NZ)
1022		CALL CR(PN,RAT,1,NX,36,36,21,28,NX,NY,NZ)
1023		CALL CR(PE,1,O,1,NX,36,36,21,28,NX,NY,NZ)
1024		CALL CR(PH,RAT,1,NX,36,36,20,28,NX,NY,NZ)
1025	C	
1026	C ***	ROW 37
1027		CALL CR(PC,O,O,1,NX,37,37, 1,16,NX,NY,NZ)
1028		CALL CR(PN,O,O,1,NX,37,37, 1,16,NX,NY,NZ)
1029		CALL CR(PE,O,O,1,NX,37,37, 1,16,NX,NY,NZ)
1030		CALL CR(PH,O,O,1,NX,37,37, 1,16,NX,NY,NZ)
1031	C	
1032		CALL CR(PC,O,2,1,NX,37,37,17,17,NX,NY,NZ)
1033		CALL CR(PN,O,O,1,NX,37,37,17,17,NX,NY,NZ)
1034		CALL CR(PE,O,2,1,NX,37,37,17,17,NX,NY,NZ)
1035		CALL CR(PH,1,O,1,NX,37,37,17,17,NX,NY,NZ)
1036	C	
1037		CALL CR(PC,RAT,1,NX,37,37,21,28,NX,NY,NZ)
1038		CALL CR(PN,RAT,1,NX,37,37,21,28,NX,NY,NZ)
1039		CALL CR(PE,1,O,1,NX,37,37,21,28,NX,NY,NZ)
1040		CALL CR(PH,RAT,1,NX,37,37,20,28,NX,NY,NZ)
1041	C	
1042	C ***	ROW 38
1043		CALL CR(PC,O,O,1,NX,38,38, 1,17,NX,NY,NZ)
1044		CALL CR(PN,O,O,1,NX,38,38, 1,17,NX,NY,NZ)
1045		CALL CR(PE,O,O,1,NX,38,38, 1,17,NX,NY,NZ)
1046		CALL CR(PH,O,O,1,NX,38,38, 1,17,NX,NY,NZ)
1047	C	
1048		CALL CR(PC,RAT,1,NX,38,38,21,28,NX,NY,NZ)
1049		CALL CR(PN,RAT,1,NX,38,38,21,28,NX,NY,NZ)
1050		CALL CR(PE,1,O,1,NX,38,38,21,28,NX,NY,NZ)
1051		CALL CR(PH,RAT,1,NX,38,38,20,28,NX,NY,NZ)
1052	C	
1053	C ***	ROW 39
1054		CALL CR(PC,O,O,1,NX,39,39, 1,17,NX,NY,NZ)
1055		CALL CR(PN,O,O,1,NX,39,39, 1,17,NX,NY,NZ)
1056		CALL CR(PE,O,O,1,NX,39,39, 1,17,NX,NY,NZ)
1057		CALL CR(PH,O,O,1,NX,39,39, 1,17,NX,NY,NZ)
1058	C	
1059		CALL CR(PC,RAT,1,NX,39,39,21,28,NX,NY,NZ)
1060		CALL CR(PN,RAT,1,NX,39,39,21,28,NX,NY,NZ)
1061		CALL CR(PE,1,O,1,NX,39,39,21,28,NX,NY,NZ)
1062		CALL CR(PH,RAT,1,NX,39,39,20,28,NX,NY,NZ)
1063	C	
1064	C ***	ROW 40
1065		CALL CR(PC,O,O,1,NX,40,40, 1,16,NX,NY,NZ)
1066		CALL CR(PN,O,O,1,NX,40,40, 1,16,NX,NY,NZ)
1067		CALL CR(PE,O,O,1,NX,40,40, 1,16,NX,NY,NZ)
1068		CALL CR(PH,O,O,1,NX,40,40, 1,16,NX,NY,NZ)
1069	C	
1070	C	
1071		CALL CR(PC,1,O,1,NX,40,40,17,17,NX,NY,NZ)
1072		CALL CR(PN,O,O,1,NX,40,40,17,20,NX,NY,NZ)
1073		CALL CR(PE,1,O,1,NX,40,40,17,17,NX,NY,NZ)
1074		CALL CR(PH,1,O,1,NX,40,40,17,17,NX,NY,NZ)
1075	C	
1076		CALL CR(PC,RAT,1,NX,40,40,21,28,NX,NY,NZ)
1077		CALL CR(PN,O,O,1,NX,40,40,21,28,NX,NY,NZ)
1078		CALL CR(PE,1,O,1,NX,40,40,21,28,NX,NY,NZ)
1079		CALL CR(PH,RAT,1,NX,40,40,20,28,NX,NY,NZ)


```

1080 C
1081 C
1082 C --- GROUP 8. DEPENDENT VARIABLES TO BE SOLVED FOR OR STORED :
1083 C SOLVAR(1-25)<25*.F.>.STOVAR(1-25)<25*.F.>.CONC(1-4)<4*.T.>
1084 C USE FOLLOWING NAMED INTEGERS FOR ARRAY ELEMENTS 1-20:
1085 C P1,PP,U1,U2,V1,V2,W1,W2,M1,M2,RS,KE,EP,H1,H2,H3,C1,C2,C3,C4.
1086 C SOLVAR(P1)= .TRUE.
1087 C SOLVAR(PP)= .TRUE.
1088 C SOLVAR(U1)= .TRUE.
1089 C SOLVAR(V1)= .TRUE.
1090 C SOLVAR(W1)= .TRUE.
1091 C SOLVAR(KE)= .TRUE.
1092 C SOLVAR(EP)= .TRUE.
1093 C SOLVAR(H1)= .TRUE.
1094 C SOLVAR(C1)= .TRUE.
1095 CC
1096 C STOVAR(18)= .TRUE.
1097 C STOVAR(19)= .TRUE.
1098 C STOVAR(21)= .TRUE.
1099 C STOVAR(22)= .TRUE.
1100 C STOVAR(23)= .TRUE.
1101 C
1102 C --- GROUP 9. VARIABLE LABELS :
1103 C TITLE(1-25)<2HP1,2HPP,2HU1,2HU2,2HV1,2HV2,2HW1,2HW2,2HR1,
1104 C 2HR2,2HRS,2HKE,2HEP,2HH1,2HH2,2HH3,2HC1,2HC2,
1105 C 2HC3,2HC4,2HRX,2HRY,2HRZ, 2*4H***>
1106 C CC *** ENTHALPY OF THE MIXTURE
1107 C TITLE(H1)= 4HMHX
1108 C CC *** MASS FRACTION OF THE WATER
1109 C TITLE(C1)= 4MHM20
1110 C CC *** TEMPERATURE OF THE MIXTURE
1111 C TITLE(18)= 4HTMIX
1112 C CC *** TOTAL PRESSURE
1113 C TITLE(19)= 4HPTOT
1114 C CC *** DENSITY OF THE MIXTURE
1115 C TITLE(2)= 4HRMIX
1116 C CC *** DENSITY OF THE WATER
1117 C TITLE(15)= 4HRH20
1118 C CC *** DENSITY OF THE 'HYDROGEN
1119 C TITLE(16)= 4HRH2
1120 C CC *** EFFECTIVE VISCOSITY
1121 C TITLE(21)= 4HEMU
1122 C CC *** PRESSURE CORRECTION
1123 C TITLE(22)= 4HPP
1124 C CC *** CONTINUITY ERROR
1125 C TITLE(23)= 4HCONT
1126 C
1127 C --- GROUP 10. PROPERTIES:
1128 C IRHO1<1>,IRHO2<1>,RHO1<1.O>,RHO2<1.O>,
1129 C ARHO1<1.O>,BRHO1<1.O>,CRHO1<1.O>
1130 C IEMU1<1>,EMU1<1.O>,EMULAM<1.E-10>
1131 C IHSAT,H1SAT,H2SAT,PSATEX<1.O>
1132 C SIGMA(1-25)<1.O,2.O,1.,1.,1.E10,1.,1.E10,
1133 C 4*1.O,1.314,1.O,1.E10,10*1.O>
1134 CC
1135 C *** UNITS ARE IN LBF, SLUGS, FEET, AND DEGREES RANKINE
1136 CC
1137 C *** THE DENSITY IS CALCULATED IN GROUND CH. 10.
1138 C IRHO1=-1
1139 C *** SETTING IEMU1 = 2 IMPLIES THE K-EPSILON MODEL IS ACTIVE

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1140 IEMU1= 2
1141 CC *** SIGMA = TURB. PRANDTL OR SCHMIDT NO.
1142 C FOR H1 AND C1 THEY ARE .9 BASED ON CHAM TR/75, PAGE 3.2-26
1143 SIGMA(H1)= 0.9
1144 SIGMA(C1)= 0.9
1145 CC *** LAM VISCOSITY FOR WALL FRICTION IS CALCULATED IN GROUND CH. 10
1146 EMULAM= -1.
1147 C-----
1148 C--- GROUP 11 INTER-PHASE TRANSFER PROCESSES :
1149 C ICFIP,CFIPS,IMDOT,CMDOT,CA11<1.E6>,CA21<1.E6>
1150 C-----
1151 C--- GROUP 12 SPECIAL SOURCES :
1152 C ISPCS0(1-25),AGRAVX,AGRAVY,AGRAVZ,ABUDY,HREF
1153 C-----
1154 C--- GROUP 13 INITIAL FIELDS :
1155 C FIINIT(1-25)<25*1.E-10>
1156 C
1157 C OMEGA = RPM*2.*PI/60.
1158 C
1159 C FIINIT(U1)=0.4*OMEGA
1160 C FIINIT(V1)=0.0
1161 C FIINIT(W1)=0.0
1162 C FIINIT(C1)=0.1
1163 CC *** SET TEMP AT INTERMEDIATE VALUE (LMSC-HREC TR D697954)
1164 C FIINIT(18) = 400.
1165 CC *** FIINIT (P1), (H1), (KE) & (EP) ARE SET BELOW IN GROUP 15
1166 C-----
1167 C--- GROUP 14 BOUNDARY/INTERNAL CONDITIONS :
1168 C ILOOP1,ILOOPN,XCYCLE<F>,>PBAR,REGION(1-10)<10*.T.>
1169 C *N.B. ALL 10 REGIONS ARE DEFAULTED .TRUE.. THE USER SHOULD
1170 C SET REGION(I)=.FALSE. FOR UNUSED REGIONS 'I'.
1171 DO 140 I=1,10
1172 140 REGION(I)= .FALSE.
1173 XCYCLE = .TRUE.
1174 C-----
1175 C--- GROUP 15 TO 24 REGIONS 1 TO 10
1176 C--- ONLY THOSE REGIONS ARE ACTIVE WHICH ARE SPECIFIED BY THE
1177 C USER, PREFERABLY BY WAY OF :
1178 C CALL PLACE(IREGN,TYPE,IXF,IXL,IYF,IYL,IZF,IZL) &
1179 C CALL COVAL(IREGN,VARBLE,COEFF,VALUE)
1180 C
1181 CC *** 'COLD' H2 , INLET ***
1182 C
1183 CC *** FEEDC1 IS SET TO THE TOTAL MASS FLOWRATE (LBM/S)
1184 CC AT THE COLD INLET, (SEE LMSC-HREC TR D697954),
1185 CC THEN CONVERTED TO SLUGS/SEC OVER SOLUTION SEGMENT
1186 FEEDC = FEEDC1/(G*SLICES)
1187 CCC AS OF 3/85 THE FLOW THROUGH THE LABY SEAL IS VARIED AS
1188 CCC AS A FUNCTION OF THE ECCENTRICITY OF THE ROTOR:
1189 C
1190 C WEIGHTED FLOWRATE (PER SEGMENT) =(TOTAL FLOWRATE/NX)*
1191 C ((SM GAP HT)-COS(ANGLE))*(ECCENTRICITY)/(ISM GAP HT)
1192 C
1193 C FOR EIGHT CELLS IN THE X DIRECTION:
1194 FEDC1 = FEEDC*(GINC1S-COS(0.)*ECCENT)/GINC1S
1195 FEDC2 = FEEDC*(GINC1S-COS(2.*PI/8.)*ECCENT)/GINC1S
1196 FEDC3 = FEEDC*(GINC1S-COS(2.*PI/4.)*ECCENT)/GINC1S
1197 FEDC4 = FEEDC*(GINC1S-COS(2.*PI*3./8.)*ECCENT)/GINC1S
1198 FEDC5 = FEEDC*(GINC1S-COS(PI)*ECCENT)/GINC1S
1199 FEDC6 = FEEDC*(GINC1S-COS(2.*PI*5./8.)*ECCENT)/GINC1S

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1200 FEDC7 = FEEDC*(GINC1S-COS(2.*PI*.3./4.)*ECCENT)/GINC1S
1201 FEDC8 = FEEDC*(GINC1S-COS(2.*PI*.7./8.)*ECCENT)/GINC1S
1202
1203 CC *** H1INC1 IS SET TO THE ENTHALPY (BTU/LBM) AT THE COLD
1204 CC INLET (TR D697954) THEN CONVERTED TO FT-LBF/SLUGS
1205 H1INC = H1INC1*778.16*G
1206
1207 CC *** ROINC IS THE DENSITY (SLUG/CU FT) AT THE COLD INLET
1208 ROINC = ROINC1/G
1209
1210 CC *** RADINC IS THE AVERAGE RADIUS (FT) OF THE COLD INLET
1211 RADINC = RINNER +O.05/12.
1212
1213 CC *** GINC1 IS SET TO THE (LARGE) GAP HT (INCHES) AT COLD INLET
1214 CC *** CALCULATE THE INLET AREA (SQ IN) & (SQ FT/SEGMENT)
1215 AINC1 = GINC1 * RADINC *12.*2.*PI
1216 AINC = AINC1/(144.*O*SLICES)
1217
1218 CC *** CALCULATE THE AVERAGE FEED VELOCITY AT THE COLD INLET
1219 W1INC = FEEDC/(ROINC*AINC)
1220
1221 VELSQ=W1INC**2 + (O.5*OMEGA*RADINC)**2
1222
1223 C
1224 CALL PLACE(1,CELL,1,1,1,1,13,13)
1225 CALL COVAL(1,M1,FIXFLU,FEDC1/FLOAT(NX))
1226 CALL COVAL(1,U1,ONLYMS,O.5*OMEGA*(RADINC**2))
1227 CALL COVAL(1,W1,ONLYMS,W1INC)
1228 CALL COVAL(1,KE,ONLYMS,.O1*VELSQ)
1229 CALL COVAL(1,EP,ONLYMS,O.16433*(.O1*VELSQ)**1.5/(.1*GINC1/12.))
1230 CALL COVAL(1,H1,ONLYMS,H1INC)
1231 CALL COVAL(1,C1,ONLYMS,O.O)
1232
1233 C
1234 CALL PLACE(2,CELL,2,2,1,1,13,13)
1235 CALL COVAL(2,M1,FIXFLU,FEDC2/FLOAT(NX))
1236 CALL COVAL(2,U1,ONLYMS,O.5*OMEGA*(RADINC**2))
1237 CALL COVAL(2,W1,ONLYMS,W1INC)
1238 CALL COVAL(2,KE,ONLYMS,.O1*VELSQ)
1239 CALL COVAL(2,EP,ONLYMS,O.16433*(.O1*VELSQ)**1.5/(.1*GINC1/12.))
1240 CALL COVAL(2,H1,ONLYMS,H1INC)
1241 CALL COVAL(2,C1,ONLYMS,O.O)
1242
1243 C
1244 CALL PLACE(3,CELL,3,3,1,1,13,13)
1245 CALL COVAL(3,M1,FIXFLU,FEDC3/FLOAT(NX))
1246 CALL COVAL(3,U1,ONLYMS,O.5*OMEGA*(RADINC**2))
1247 CALL COVAL(3,W1,ONLYMS,W1INC)
1248 CALL COVAL(3,KE,ONLYMS,.O1*VELSQ)
1249 CALL COVAL(3,EP,ONLYMS,O.16433*(.O1*VELSQ)**1.5/(.1*GINC1/12.))
1250 CALL COVAL(3,H1,ONLYMS,H1INC)
1251 CALL COVAL(3,C1,ONLYMS,O.O)
1252
1253 C
1254 CALL PLACE(4,CELL,4,4,1,1,13,13)
1255 CALL COVAL(4,M1,FIXFLU,FEDC4/FLOAT(NX))
1256 CALL COVAL(4,U1,ONLYMS,O.5*OMEGA*(RADINC**2))
1257 CALL COVAL(4,W1,ONLYMS,W1INC)
1258 CALL COVAL(4,KE,ONLYMS,.O1*VELSQ)
1259 CALL COVAL(4,EP,ONLYMS,O.16433*(.O1*VELSQ)**1.5/(.1*GINC1/12.))
1260 CALL COVAL(4,C1,ONLYMS,O.O)
1261
1262 C
1263 CALL PLACE(5,CELL,5,5,1,1,13,13)
1264 CALL COVAL(5,M1,FIXFLU,FEDC5/FLOAT(NX))
1265 CALL COVAL(5,U1,ONLYMS,O.5*OMEGA*(RADINC**2))
1266 CALL COVAL(5,W1,ONLYMS,W1INC)
1267 CALL COVAL(5,KE,ONLYMS,.O1*VELSQ)
1268 CALL COVAL(5,EP,ONLYMS,O.16433*(.O1*VELSQ)**1.5/(.1*GINC1/12.))
1269 CALL COVAL(5,C1,ONLYMS,O.O)
1270

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1260 CALL COVAL(5,H1,ONLYMS,H1INC)
1261 CALL COVAL(5,C1,ONLYMS,O.O)
1262
1263 CALL PLACE(6,CELL,6, 6,1,1,13,13)
1264 CALL COVAL(6,M1,FIXFLU,FEDC7/FLOAT(NX))
1265 CALL COVAL(6,U1,ONLYMS,O.5*OMEGA*(RADINC**2))
1266 CALL COVAL(6,W1,ONLYMS,W1INC)
1267 CALL COVAL(6,KE,ONLYMS,.01*VELSQ)
1268 CALL COVAL(6,EP,ONLYMS,O.16433*(.01*VELSQ)**1.5/(.1*GINC1/12.))
1269 CALL COVAL(6,H1,ONLYMS,H1INC)
1270 CALL COVAL(6,C1,ONLYMS,O.O)
1271
1272 CALL PLACE(7,CELL,7, 7,1,1,13,13)
1273 CALL COVAL(7,M1,FIXFLU,FEDC7/FLOAT(NX))
1274 CALL COVAL(7,U1,ONLYMS,O.5*OMEGA*(RADINC**2))
1275 CALL COVAL(7,W1,ONLYMS,W1INC)
1276 CALL COVAL(7,KE,ONLYMS,.01*VELSQ)
1277 CALL COVAL(7,EP,ONLYMS,O.16433*(.01*VELSQ)**1.5/(.1*GINC1/12.))
1278 CALL COVAL(7,H1,ONLYMS,H1INC)
1279 CALL COVAL(7,C1,ONLYMS,O.O)
1280
1281 CALL PLACE(8,CELL,8, 8,1,1,13,13)
1282 CALL COVAL(8,M1,FIXFLU,FEDC8/FLOAT(NX))
1283 CALL COVAL(8,U1,ONLYMS,O.5*OMEGA*(RADINC**2))
1284 CALL COVAL(8,W1,ONLYMS,W1INC)
1285 CALL COVAL(8,KE,ONLYMS,.01*VELSQ)
1286 CALL COVAL(8,EP,ONLYMS,O.16433*(.01*VELSQ)**1.5/(.1*GINC1/12.))
1287 CALL COVAL(8,H1,ONLYMS,H1INC)
1288 CALL COVAL(8,C1,ONLYMS,O.O)
1289
1290 C
1291 CC *** 'HOT' H2 & H2O INLET ***
1292 CC
1293 CC *** FEEDH1 IS SET TO THE TOTAL MASS FLOWRATE (LBM/S)
1294 CC AT THE HOT INLET, (SEE LMSC-HREC TR D697954),
1295 CC THEN CONVERTED TO SLUGS/SEC OVER SOLUTION SEGMENT
1296 FEEDH = FEEDH1/(G*SLICES)
1297 CC *** H1INH1 IS SET TO THE ENTHALPY (BTU/LBM) AT THE HOT
1298 CC INLET (TR D697954) THEN CONVERTED TO FT-LBF/SLUGS
1299 H1INH = H1INH1*778.16*G
1300 CC *** ROINH IS THE DENSITY (SLUG/CU FT) AT THE HOT INLET
1301 ROINH = ROINH1/G
1302 CC *** RADINH IS THE AVERAGE RADIUS (FT) OF THE HOT INLET
1303 RADINH = RINNER + 2.45/12.
1304 CC *** AINH1 IS SET TO THE AREA (SQ IN) AT THE HOT INLET
1305 CC THEN CONVERTED TO THE INLET AREA (SQ FT) PER SEGMENT
1306 AINH = AINH1/(144.O*SLICES)
1307 CC *** CALCULATE THE FEED VELOCITY AT THE HOT INLET
1308 W1INH = -FEEDH/(ROINH*AINH)
1309 CC *** TOTAL NOMINAL GRID AREA PER SEGMENT AT HOT INLET
1310 ARGRID=ARGRD1/(144.*SLICES)
1311 C
1312 CALL PLACE(9,HIGH,1,NX,32,40,28,28)
1313 CALL COVAL(9,M1,FIXFLU,FEEDH/ARGRID)
1314 CALL COVAL(9,W1,ONLYMS,W1INH)
1315 C
1316 CC *** INITIALIZE ENTHALPY, TURBULENCE, AND DISSIPATION
1317 FIINIT(H1)=3.E7
1318 FIINIT(KE)=.01*((OMEGA*RADINH)**2+W1INH**2)
1319 FIINIT(EP)=.16433*(FIINIT(KE))**1.5/(.1*AINH/(RADINH*XULAST))

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1320 VELSQ=WIINH**2
1321 CALL COVAL(9,KE,ONLYMS,.01*VELSQ)
1322 CALL COVAL(9,EP,ONLYMS,FIINIT(EP)*(.01*VELSQ/FIINIT(KE))**1.5)
1323 CALL COVAL(9,H1,ONLYMS,H1INH)
1324 CALL COVAL(9,C1,ONLYMS,H20INH)
1325
1326 C
1327 CC *** OUTLETS ***
1328 CC
1329 CC ** THE EXIT PRESSURES AROUND THE PERIPHERY OF THE
1330 CC AFT-PLATFORM SEAL ARE SPECIFIED IN SATELLITE, BUT
1331 CC ARE APPLIED AS A BOUNDARY CONDITION IN GROUND.
1332 CC ** BEFORE THE VALUES OF U1,KE,... AT THE EXIT ARE CALCULATED
1333 CC BE SPECIFIED IN CASE THERE IS IN-FLOW AT THE PERIPHERY
1334 CC OF THE SEAL (EITHER TEMPORARY OR STEADY), OR NEAR BOLTS.
1335 CC ** CALCULATE THE RADIUS AND AREA AT THE PRIMARY EXIT
1336 RADXIT = RINNER + YVLAST
1337 AEXIT=(GEXIT1/12.)*RADXIT*XULAST
1338 CC ** ESTIMATE THE VELOCITIES AT PRIMARY EXIT
1339 FEEDT=FEEDC + FEEDH
1340 W1EXIT=-FEEDT/(ROINH*AEXIT)
1341 U1EXIT=OMEGA*RADXIT**2
1342
1343 C
1344 VELSQ=W1EXIT**2+(U1EXIT/RADXIT)**2
1345 VALKE=.01*VELSQ
1346 VALEP=.16433*VALKE**1.5/(.1*GEXIT1/12.)
1347 HEXIT=HEXIT1*778.16*G
1348 CC ** INITIALIZE PRESSURE (PEXIT+HALF EXPECTED LOSS AT PRIMARY EXIT)
1349 FIINIT(P1)= PEXIT+0.5*GLOSK1*ROINH*W1EXIT**2/2.
1350
1351 C
1352 C*** ROTATING WALL AND WALL FRICTION ***
1353 CC
1354 CC ALL ROTATION AND WALL FRICTION EFFECTS SET UP IN GROUND CH. 5
1355 C
1356 C---
1357 C--- GROUP 25 GROUND STATION :
1358 C GROSTA<.F.>.NAMLST<.F.>
1359 C *NAMLST ACTIVATES NAMELIST IN GROUND.
1360 GROSTA=.TRUE.
1361
1362 C---
1363 C--- GROUP 26 SOLUTION TYPE AND RELATED PARAMETERS :
1364 C WHOLEP<.F.>.SUBPST<.F.>.DONACC<.F.>
1365 WHOLEP=.TRUE.
1366
1367 C---
1368 C--- GROUP 27 SWEEP AND ITERATION NUMBERS :
1369 C FSWEPT<1>,LSWEPT<1>,LITHYD<1>,LITC<1>,LITKE<1>,LITH<1>,
1370 C LITER(1-25)<9*1,-1,15*1>
1371 C IVELF<1>,NVEL<1>,IVELL<10000>,
1372 C IKEF<1>,NKE<1>,IKEL<10000>,
1373 C IENTF<1>,NENT<1>,IENTL<10000>,
1374 C ICNCF<1>,NCNC<1>,ICNCL<10000>,
1375 C IRH01F<1>,NRH01<1>,IRH01L<10000>,
1376 C IRH02F<1>,NRH02<1>,IRH02L<10000>,
1377 C LSWEPT= 200
1378 C LITER(PP)= 15
1379
1380 C---
1381 C--- GROUP 28 TERMINATION CRITERIA :
1382 C ENDIT(1-25)<9*1,E-10,O.5,15*1,E-10>
1383
1384 C---

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1380 C--- GROUP 29 RELAXATION
1381 C RLXP<1.>,RLXPXY<1.>,RLXPZ<1.>,RLXRHO<1.>,RLXMDT<1.>,
1382 C DTFALS(3-25)<23*1.E10>
1383 C U1MAX=ABS(U1EXIT)
1384 C W1MAX=ABS(W1INH)
1385 C V1MAX=W1MAX
1386 C DTFALS(V1)=YVLAST/(FLOAT(NY)*V1MAX+TINY)
1387 C DTFALS(W1)=ZVLAST/(FLOAT(NZ)*W1MAX+TINY)
1388 C DTFALS(KE)=1.E5*AMAX1(DTFALS(V1),DTFALS(W1))
1389 C DTFALS(EP)=DTFALS(KE)
1390 C---
1391 C--- GROUP 30 LIMITS :
1392 C VELMAX<1.E10>,VELMIN<1.E10>,RHOMAX<1.E10>,RHOMIN<1.E10>,
1393 C TKEMAX<1.E10>,TKEMIN<1.E10>,EMUMAX<1.E10>,EMUMIN<1.E10>,
1394 C EPSMAX<1.E10>,EPSMIN<1.E10>,AMDTMX<1.E10>,AMDTMN<1.E10>,
1395 C EMUMIN=100.*0.5E-5/G
1396 C EMUMAX=1.E4*1.2E-3/G
1397 C EPSMAX=1.E20
1398 C---
1399 C--- GROUP 31 SLOWING DEVICES : SLORHO<1.>,SLOEMU<1.>
1400 C---
1401 C--- GROUP 32 PRINT-OUT OF VARIABLES :
1402 C PRINT(1-25)<.T.,.F.,23*.T.>,SUBWGR<.F.>
1403 C PRINT(2)=.TRUE.
1404 C---
1405 C--- GROUP 33 MONITOR PRINT-OUT :
1406 C IXMNON<1>,IYMON<1>,IZMON<1>,NPRMON<1>,NPRMNT<1>
1407 C IZMON=9
1408 C IYMON=13
1409 C IXMNON=1
1410 C---
1411 C--- GROUP 34 FIELD PRINT-OUT CONTROL :
1412 C NPRINT<100>,NTPRIN<100>,NXPRIN<1>,NYPRIN<1>,NZPRIN<1>,
1413 C IZPRF<1>,ISTPRF<1>,IZPRL<10000>,ISTPRL<10000>
1414 C NUMCLS<10>,KOUTPT
1415 C NPRINT = LSWEEP
1416 C---
1417 C--- GROUP 35 TABLE CONTROL :
1418 C TABLES<.F.>,NTABLE,NTABVR,LINTAB,NPRTAB,NMON,
1419 C ITAB(1-8),MTABVR(1-8)
1420 C---
1421 C--- GROUP 36-38 ARE NOT DOCUMENTED IN THE INSTRUCTION
1422 C MANUAL AND ARE INTENDED FOR MAINTENANCE PURPOSES ONLY
1423 C--- GROUP 36 DEBUG PRINT-OUT SLAB AND TIME-STEP :
1424 C IZPR1<1>,IZPR2<1>,ISTPR1<1>,ISTPR2<1>
1425 C---
1426 C--- GROUP 37 DEBUG SWEEP AND SUBROUTINES :
1427 C KEMU,KMAIN,KINDEX,KGEOM,KINPUT,KSODAT,KCOMPFF,KSORCE,
1428 C KSOLV1,KSOLV2,KSOLV3,KCOMPV,KADJST,KFLUX,KSHIFT,KDIF,
1429 C KCOMPU,KCOMPV,KCOMPW,KCOMPR,KWALL,KDBRHO<-1>,KDBEXP,KDBMDT
1430 C KDBGEN
1431 C---
1432 C--- GROUP 38 MONITOR,TEST,AND FLAG :
1433 C MONITR<.F.>,FLAG<.F.>,TEST<.T.>,KFLAG<1>
1434 C END OF MAINTENANCE-ONLY SECTION
1435 C---
1436 C--- GROUP 39 ERROR AND RESIDUAL PRINT-OUT :
1437 C IERRP<1000>,RESREF(1,3-24)<25*1.>,RESMAP<.F.>,
1438 C RESID(1-25)<2*.F.,23*.T.>,KOUTPT
1439 C IERRP=25

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ORIGINAL PAGE IS
OF POOR QUALITY

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1440 RESREF(P1)=FEEDT/ROINH
1441 RESREF(U1)=FEEDT*U1MAX
1442 RESREF(V1)=FEEDT*V1MAX
1443 RESREF(W1)=FEEDT*W1MAX
1444 RESREF(KE)=FEEDT*FIINIT(KE)
1445 RESREF(EP)=FEEDT*FIINIT(EP)
1446 RESREF(H1)=FEEDT*FIINIT(H1)
1447 RESREF(C1)=FEEDT*H2OINH
1448
1449 C-----
1450 C--- GROUP 40 SPECIAL DATA : LOGIC(1..10),INTGR(1..10),RE(21..30),
1451 C NLSP<1>,NISP<1>,NRSP<1>,SPDATA<F>,>,LSPDA(1),ISPDA(1),RSPDA(1)
1452 C USE FIRST 10 ELEMENTS OF ARRAYS LOGIC & INTGR AND 21ST
1453 C TO 30TH OF ARRAY RE FOR TRANSFERRING SPECIAL DATA FROM
1454 C SATELLITE TO GROUND, BUT IF REQUIREMENTS EXCEED THIS
1455 C PROVISION SET SPDATA = .T., AND DIMENSION ARRAYS LSPDA,
1456 C ISPDA, RSPDA ABOVE AND IN GROUND AS NEEDED, AND SET HERE
1457 C NLSP, NISP, NRSP TO DIMENSION VALUES.
1458
1459 C ** PASS THE FOLLOWING INPUT GEOMETRIES, PROPERTIES, AND BOUNDARY
1460 C CONDITIONS TO GROUND VIA RSPDA (FOR PRINTING ETC.)
1461 C SPDATA=.TRUE.
1462 RSPDA(1)=GINC1
1463 RSPDA(2)=GEXIT1
1464 RSPDA(3)=AINH1
1465 RSPDA(4)=RINNER
1466 RSPDA(5)=HIINC1
1467 RSPDA(6)=HIINH1
1468 RSPDA(7)=ROINC1
1469 RSPDA(8)=ROINH1
1470 RSPDA(9)=ECCENT
1471 RSPDA(10)=RPM
1472 RSPDA(11)=FEEDC1
1473 RSPDA(12)=FEEDH1
1474 RSPDA(13)=H2OINH
1475 RSPDA(14)=W1INC
1476 RSPDA(15)=W1INH
1477 C * VARIABLES FOR EXIT AT O.D. OF AFT-PLATFORM SEAL
1478 RSPDA(16)=GLOSK1
1479 C NB. PEXIT(8) ARRAY IS EQUIVALENCED TO RSPDA(17)
1480 RSPDA(25)=VALKE
1481 RSPDA(26)=VALEP
1482 RSPDA(27)=HEXIT
1483 RSPDA(28)=SLICES
1484 RSPDA(29)=H2OXIT
1485 C NB. GEXIT(8) ARRAY IS EQUIVALENCED TO RSPDA(30)
1486 C-----
1487 C--- GROUP 42 RESTARTS AND DUMPS : SAVEM<F>,>,RESTR<F>,>,KINPUT
1488 C SAVEM = .TRUE.
1489 C RESTR = .TRUE.
1490 C-----
1491 C--- GROUP 43 GRAFFIC :
1492 C GRAPHS<F>,>,ORTHOG<I>,>,ITITL<5*4H>+*+*+>
1493 C FOR A GRAFFIC RUN, DIMENSION PHI1 & PHI2 AS FOLLOWS:
1494 C PHI1(NX*NY*NZ*NM)
1495 C PHI2((NX+2)*(NY+2)*(NZ+2)*(NM+IBLK)) . WHERE
1496 C NM=NO. OF VARIABLES STORED + DENSITY(-IES)
1497 C IBLK=0 IF BLOCK=.FALSE.,4 IF A 3D RUN,
1498 C =3 IF A 2D.YZ RUN.
1499 C GRAPHS = .TRUE.
1500 C-----

```


ORIGINAL PAGE IS
OF POOR QUALITY

```
1560 C---- ALL RUNS
1561 CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX USER SECTION 3 ENDS.
1562 CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX STANDARD SECTION 4 STARTS:
1563 C-----
1564 C WRITE GENERAL DATA ON TO THE GUSIE1 DTA TAPE, ETC....
1565 IF(SPDATA) CALL WRTSPC(LSPDA,NLSP,ISPDA,NISP,RSPDA,NRSP)
1566 IF(BLOCK) CALL WRTPOR(PE,PN,PH,PC,NX,NY,NZ,IPLANE)
1567 C OLD PRACTICES RETAINED FOR REFERENCE:
1568 C IF(SPDATA) CALL SPCDAT(IRUN)
1569 C IF(BLOCK) CALL PORDAT(IRUN)
1570 IF(GRAPH) CALL SORT(IRUN)
1571 IF(RESTRT) GO TO 902
1572 DO 901 INDVAR=1,25
1573 IF(IFI(FIINIT(INDVAR)+O.1).NE.10101) GO TO 901
1574 CALL FLDDAT(IRUN)
1575 GO TO 902
1576 901 CONTINUE
1577 902 CALL DATAIO(WRT,10)
1578 IF(MONITR) CALL DATAIO(WRT,-6)
1579 999 CONTINUE
1580 STOP
1581 END
1582 P!
```

@BRKPT PRINT\$

```

RUNKLEBIN197*TPF$(O).SLPRT
1 $BATCH
2 C$DIRECTIVE**MAIN
3 C ***
4 C *FILE NAME: DSK32GRD.FTN
5 C ***
6 C *ABSTRACT: GROUND STATION FOR SSME HPFTP APS 3-D MODEL (2 EXITS)
7 C ***
8 C *INCLUDED SUBROUTINES: THE MODELS OF MAIN, GROUND
9 C *DOCUMENTATION: PHOENICS INSTRUCTION MANUAL (SPRING 1983).
10 C *SATELLITE FILE NAME: DSKSAT.FTN
11 COMMON/ISHIFT/III(57) NFMAX
12 C SET F-ARRAY DIMENSION AS NEEDED, & SET NFMAX ACCORDINGLY.
13 COMMON F(324000)
14 NFMAX=324000
15 CALL MAIN1
16 STOP
17 END
18 C$DIRECTIVE**GROUND
19 SUBROUTINE GROUND(IRN,ICHAP,ISTP,ISWP,IZED,INDVAR)
20 $INCLUDE 9,CWNGUSST.FTN/G
21 $INCLUDE 9,GUSSEQUI.FTN/G
22 $INCLUDE 9,NMLIST.FTN/G
23 CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX STANDARD SECTION 1 STARTS:
24 C-----
25 C *****MEANING OF SUBROUTINE ARGUMENTS:
26 C IRN=RUN NUMBER
27 C ISWP=SOLUTION SWEEP
28 C *****USER-INTRODUCED VARIABLES & ARRAYS:
29 C TO AVOID CONFLICT WITH VARIABLE NAMES USED IN COMMON, ALL
30 C VARIABLES INTRODUCED BY THE USER SHOULD HAVE NAMES STARTING
31 C WITH 'G' IF REAL, 'J' IF INTEGER, AND 'G' OR 'J' IF LOGICAL.
32 C THUS GDZ(IZ) MIGHT BE A Z-INTERVAL ARRAY
33 C GW1(IY,IX) A 2-D ARRAY FOR AXIAL VELOCITY
34 C USER-GENERATED SUBROUTINES SHOULD BE NAMED CORRESPONDINGLY, EG
35 C SUBROUTINE GVISC(GTEMP,GCNC,GVSC), FOR COMPUTING VISCOSITY
36 C FROM CONCENTRATION & TEMPERATURE.
37 C *****GROUND-TO-EARTH CONNECTING SUBROUTINES:
38 C *USE GET(NAME,GARRAY,NY,NX) TO PUT VALUES OF VARIABLE NAMED
39 C 'NAME' INTO ARRAY 'GARRAY' DIMENSIONED GARRAY(NY,NX).
40 C *USE SET(NAME,IXF,IXL,IYF,IYL,GARRAY,NY,NX) TO SET VARIABLE
41 C 'NAME' TO GARRAY(IY,IX) OVER THE REGION: IXF-IXL & IYF-IYL.
42 C *USE PRNSLB(NAME) TO PRINT VARIABLE 'NAME' OVER X-Y PLANE.
43 C *USE ADD(NAME,IXF,IXL,IYF,IYL,TYPE,CM,VM,CVAR,VVAR,NY,NX)
44 C TO ADD SOURCE TO VARIABLE NAMED 'NAME' (SEE CHAPTER 5).
45 C *USE READIZ(IZED) IN CHAPTERS 1, 2, 8, & 9 TO ACCESS P1....DM
46 C & VOL....AHDZ. (SEE FOOTNOTE TO LEGALITY TABLE)
47 C *USE GET1D(NAME,GARRAY,NDIM) TO PUT VARIABLE NAMED 'NAME' IN
48 C ONE-D ARRAY 'GARRAY' DIMENSIONED NDIM. THUS:
49 C CALL GET1D(NAME,GNX,NY) FOR XG....DXG & DIMENSION GNX(NY)
50 C CALL GET1D(NAME,GNV,NY) FOR YG....RV & DIMENSION GNV(NY)
51 C CALL GET1D(NAME,GNZ,NZ) FOR ZG....WGRID & DIMENSION GNZ(NZ).
52 C *****LEGALITY TABLE FOR USE OF EARTH-CONNECTING SUBROUTINES:
53 C ENTRIES IN TABLE GIVE CHAPTERS IN WHICH SUBROUTINES CAN BE
54 C USED FOR VARIABLES IN LEFT-HAND COLUMN. (SUBROUTINE
55 C STRIDE IS REGARDED AS BEING IN CHAPTER 3)
56 C
57 C : VARIABLE : GET & : SET : ADD : READIZ : GET1D :
58 C : : : PRNSLB : : : : :
59 C :-----

```

ISTP=TIME STEP
INDVAR: SEE CHAPTERS BELOW.

ETC.

```

60 C :P1 - RZ : : ALL : 6 & 7 : 5 : 1,2,8,9 : NONE :
61 C :P10 - RZH::3-7, 10-16: 3 : NONE : NONE : NONE :
62 C :VOL -AHDZ:: ALL : 3 : NONE : 1,2,8,9 : NONE :
63 C :D1DP : : NONE : 10 : NONE : NONE : NONE :
64 C :D2DP : : NONE : 11 : NONE : NONE : NONE :
65 C :MU1,MU1H : : 5,13-16 : 12 : NONE : NONE : NONE :
66 C :EXCO(L,H):: NONE : 13 : NONE : NONE : NONE :
67 C :CFP : : 5 : 14 : NONE : NONE : NONE :
68 C :MDT : : 5 : 15 : NONE : NONE : NONE :
69 C :HST1,HST2:: 5 & 15 : 16 : NONE : NONE : NONE :
70 C :XG -WGRID:: NONE : NONE : NONE : NONE : ALL :
71 C -----
72 C NOTES ON ABOVE TABLE:
73 C *IN CHAPTERS 1, 2, 8, & 9 VARIABLES P1...DM & GEOMETRY
74 C VOL...AHDZ CAN BE ACCESSED BUT ONLY IN CONJUNCTION WITH
75 C USE OF READIZ, THUS:
76 C DO 1 IZED=1,NZ
77 C CALL READIZ(IZED)
78 C 1 CALL GET(... AS REQUIRED...)
79 C *GEOMETRY ACCESSED BY READIZ IS THAT AT INITIAL TIME
80 C *D1DP & D2DP ONLY ACCESSIBLE IN UNSTEADY FLOWS.
81 C *****GROUND SERVICE SUBROUTINES:
82 C *USE CONTOUR(NAME,IPLANE,ILOC,NINT,I1,I2,J1,J2,GARRAY,NDIM) FOR
83 C LINE-PRINTER PLOTS OF CONTOURS. 'NAME' = U1,...,C4
84 C 'IPLANE' = XPLANE, YPLANE, OR ZPLANE
85 C IZ LOCATION OF IPLANE
86 C CELLS IN HORIZ. & VERT. ON PLOT GARRAY IS 1-D WORKING ARRAY
87 C OF DIMENSION NX*NY, NX*NZ, OR NY*NZ DICTATED BY IPLANE
88 C NDIM SETS VALUE OF DIMENSION OF GARRAY.
89 C *USE FLD2DA(TITLE,GARRAY,NY,NX) TO PRINT ANY ARRAY DIMENSIONED
90 C GARRAY(NY,NX) SET 'TITLE' TO REQUIRED NAME ( 4 HOLLERITH
91 C CHARACTERS ONLY).
92 C *USE FLD3DA(TITLE,GARRAY,NX,NY,NZ,IPLANE,ILOC) TO PRINT ANY
93 C ARRAY DIMENSIONED GARRAY(NX,NY,NZ) IN PLANE SPECIFIED BY
94 C 'IPLANE' & 'ILOC' AS FOR CONTOUR ABOVE
95 C FLD2DA.
96 C VARIABLE NAMES FOR USE IN GROUND:
97 C COMMON/TYPE/CELL,EAST,WEST,NORTH,SOUTH,HIGH,LOW,VOLUME,WALL
98 C COMMON/VAR/P1,PP,U1,U2,V1,V2,W1,W2,R1,R2,RS,
99 C &KE,EP,H1,H2,H3,C1,C2,C3,C4,RX,RY,RZ,S1,S2
100 C COMMON/VAROLD/P10,PP0,U10,U20,V10,V20,W10,W20,R10,R20,RS0,
101 C &KE0,EP0,H10,H20,H30,C10,C20,C30,C40,RX0,RY0,RZ0,S10,S20
102 C COMMON/VARLOW/P1L,PP1,U1L,U2L,V1L,V2L,W1L,W2L,R1L,R2L,RSL,
103 C &KE1,EP1,H1L,H2L,H3L,C1L,C2L,C3L,C4L,RXL,RYL,RZL,S1L,S2L
104 C COMMON/VARHI/P1H,PPH,U1H,U2H,V1H,V2H,W1H,W2H,R1H,R2H,RSH,
105 C &KEH,EPH,H1H,H2H,H3H,C1H,C2H,C3H,C4H,RXH,RYH,RZH,S1H,S2H
106 C COMMON/GMTRY/VOL,VOLO,AEAST,ANORTH,AHIGH,AEDX,ANDY,AHDZ
107 C COMMON/PROP/D1,D2,D1DP,D2DP,MU1,MU1LAM,EXCO,CFP,MDT,HST1,HST2
108 C COMMON/PRPOLD/D10,D20
109 C COMMON/PRPLOW/D1L,D2L,EXCOL
110 C COMMON/PRPHI/D1H,D2H,MU1H,EXCOH
111 C COMMON/VARNY/XG,XU,DXU,DYG
112 C COMMON/VARNY/YG,YV,DYV,DYG,R,RV
113 C COMMON/VARNZ/ZG,ZW1,DZW,DZG,WGRID
114 C COMMON/GDMSC1/XPLANE,YPLANE,ZPLANE,ITNO
115 C COMMON/GDMSC1/LSLAB,MSLAB,HSLAB,LAMMU
116 C REAL NORTH,LOW
117 C INTEGER P1,PP,U1,U2,V1,V2,W1,W2,R1,R2,RS,
118 C &EP,H1,H2,H3,C1,C2,C3,C4,RX,RY,RZ,S1,S2
119 C INTEGER P10,PP0,U10,U20,V10,V20,W10,W20,R10,R20,RS0,

```

ILOC SETS IX, IY, OR
8

SET 'TITLE' AS FOR


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180 C ** DATA FOR SECOND EXIT
181 C LOSS COEFFICIENT
182 C NB. MAKE SURE EXIT AREA IS PERTINENT TO CHOSEN CALCULATION DOMAIN
183 C DATA GLOSK2,GAXIT2,JIXE2F,JIXE2L/1.5,0.0, 0.0/
184 C
185 CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX USER SECTION 1 ENDS.
186 CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX STANDARD SECTION 2 STARTS:
187 CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX
188 C PLEASE DO NOT ALTER, OR RE-SET, ANY OF THE REMAINING
189 C STATEMENTS OF THIS SECTION.
190 C IF(SPDATA)
191 &CALL RDSPC(IRN,INTGR(12),LSPDA,NLSP,ISPD,NISP,RSPDA,NRSP)
192 CALL GRDUTY(IRN,ICHAP,IZED,INDVAR)
193 IF(ICHAP.EQ.-5) GO TO 10
194 IF(ICHAP.LE.0.OR.ICHAP.GT.16) RETURN
195 GO TO (100,200,300,400,500,600,700,800,900,1000,1100,1200,
196 &1300,1400,1500,1600),ICHAP
197 RETURN
198 CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX STANDARD SECTION 2 ENDS.
199 CXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXXX
200 C-----
201 C CHAPTER 0: MODIFY SATLIT DATA, AT START OF EACH IRN.
202 C-----
203 C
204 C 10 CONTINUE
205 C IF(.NOT.NAMLST) RETURN
206 C IF(IRN.EQ.NRUN) DATFIL=.FALSE.
207 C-----
208 C READ SATLIT DATA NAMELIST HERE
209 C CALL WRIT40(40ENTER NAMELIST DATA FOR GROUPS 1 TO 24 )
210 C READ(20,G1G24)
211 C CALL WRIT40(40ENTER NAMELIST DATA FOR GROUPS 25 TO 42 )
212 C READ(20,G25G42)
213 C
214 C ** SUMMARY PRINTOUT OF INPUT DATA
215 C WRITE(6,21)
216 C WRITE(6,22) RSPDA(10),RSPDA(1),RSPDA(9),RSPDA(3),RSPDA(2),
217 &RSPDA(16)
218 C WRITE(6,23) RSPDA(5),RSPDA(6),RSPDA(27)/(778.16+G),RSPDA(11),
219 &RSPDA(12)
220 C WRITE(6,24) RSPDA(7),RSPDA(8),RSPDA(14),RSPDA(15),
221 &RSPDA(13),RSPDA(29)
222 C WRITE(6,28) RSPDA(37),RSPDA(36),RSPDA(35),RSPDA(34),RSPDA(33),
223 &RSPDA(32),RSPDA(31),RSPDA(30)
224 C WRITE(6,25) RSPDA(24),RSPDA(23),RSPDA(22),RSPDA(21)
225 C WRITE(6,26) RSPDA(20),RSPDA(19),RSPDA(18),RSPDA(17)
226 C WRITE(6,27) GLOSK2,GAXIT2,JIXE2F,JIXE2L
227 C
228 C 21 FORMAT(//////25X,21HSUMMARY OF INPUT DATA,/25X,21(1H-))
229 C 22 FORMAT(
230 &/1X,1PE12.3,2X,36HROTATIONAL SPEED OF THE DISC. (RPM)...
231 &/1X,1PE12.3,2X,41HGAP SIZE AT THE LABYRINTH SEAL. (INCHES)..
232 &/1X,1PE12.3,2X,46HECCENTRICITY IN THE 11:30 DIRECTION. (INCHES)..
233 &/1X,1PE12.3,2X,70HTOTAL FLOW AREA (OVER 360 DEG) BETWEEN TURBINE B
234 &LADE SHANKS. (SQ INS)...
235 &/1X,1PE12.3,2X,85H(AVERAGE) CLEARANCE BETWEEN AFT-PLATFORM SEAL OD
236 & AND THE TURBINE BLADE LIP. (INCHES)..
237 &/1X,1PE12.3,2X,64HLOSS COEFFICIENT FOR ADDITIONAL LOSSES AT EXIT N
238 &EAR BLADE ROOTS.)
239 C 23 FORMAT(
240 &/1X,1PE12.3,2X,53HENTHALPY OF H2 ENTERING AT LABYRINTH SEAL. (BTU/
241 &LBM)..

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FIRST, LAST IX-LOCATION

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240 $/1X,E12.3.2X,78HENTHALPY OF H2 + H2O MIXTURE ENTERING BETWEEN TURB
241 $INE BLADE SHANKS. (BTU/LBM)
242 $/1X,E12.3.2X,40HENTHALPY OF TURBINE DISCHARGE (BTU/LBM)..
243 $/1X,1PE12.3.2X,74HTOTAL MASS FLOWRATE OF THE H2 ENTERING THROUGH L
244 $ABYRINTH SEAL (LBM/CU FT)..
245 $/1X,1PE12.3.2X,83HTOTAL MASS FLOWRATE OF H2 + H2O MIXTURE ENTERING
246 $ BETWEEN BLADE SHANKS. (LBM/CU FT.)
247
248 24 FORMAT(
249 $/1X,1PE12.3.2X,63HDENSITY OF THE H2 ENTERING THROUGH LABYRINTH SEA
250 $L, (LBM/CU FT)..
251 $/1X,1PE12.3.2X,75HDENSITY OF THE H2 + H2O MIXTURE ENTERING BETWEEN
252 $ BLADE SHANKS. (LBM/CU FT)..
253 $/1X,1PE12.3.2X,68HCALCULATED INLET VELOCITY OF THE H2 AT THE LABYR
254 $INTH SEAL. (FT/SEC)..
255 $/1X,1PE12.3.2X,90HCALCULATED INLET VELOCITY OF THE H2 + H2O MIXTUR
256 $E ENTERING BETWEEN BLADE SHANKS. (FT/SEC)..
257 $/1X,1PE12.3.2X,51HMASS FRACTION OF H2O ENTERING BETWEEN BLADE SHAN
258 $KS..
259 $/1X,1PE12.3.2X,36HMASS FRACTION OF H2O EXITING TURBINE.)
260
261 28 FORMAT(
262 $/1X,1PE12.3.2X,33HEXIT GAP CLEARANCE (FEET) AT 1:00,
263 $/1X,1PE12.3.2X,33HEXIT GAP CLEARANCE (FEET) AT 2:30,
264 $/1X,1PE12.3.2X,33HEXIT GAP CLEARANCE (FEET) AT 4:00,
265 $/1X,1PE12.3.2X,33HEXIT GAP CLEARANCE (FEET) AT 5:30,
266 $/1X,1PE12.3.2X,33HEXIT GAP CLEARANCE (FEET) AT 7:00,
267 $/1X,1PE12.3.2X,33HEXIT GAP CLEARANCE (FEET) AT 8:30,
268 $/1X,1PE12.3.2X,34HEXIT GAP CLEARANCE (FEET) AT 10:00,
269 $/1X,1PE12.3.2X,34HEXIT GAP CLEARANCE (FEET) AT 11:30 )
270
271 25 FORMAT(
272 $/1X,1PE12.3.2X,27HEXIT PRESSURE (PSF) AT 1:00,
273 $/1X,1PE12.3.2X,27HEXIT PRESSURE (PSF) AT 2:30,
274 $/1X,1PE12.3.2X,27HEXIT PRESSURE (PSF) AT 4:00,
275 $/1X,1PE12.3.2X,27HEXIT PRESSURE (PSF) AT 5:30)
276
277 26 FORMAT(
278 $ 1X,1PE12.3.2X,27HEXIT PRESSURE (PSF) AT 7:00,
279 $/1X,1PE12.3.2X,27HEXIT PRESSURE (PSF) AT 8:30,
280 $/1X,1PE12.3.2X,28HEXIT PRESSURE (PSF) AT 10:00,
281 $/1X,1PE12.3.2X,28HEXIT PRESSURE (PSF) AT 11:30 )
282
283 27 FORMAT(
284 $/1X,1PE12.3.2X,32HLOSS COEFFICIENT AT SECOND EXIT..
285 $/5X,12.4H TO .12.2X,40HIX-CELLS OVER WHICH SECOND EXIT LOCATED..
286 $///// )
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300 GVALKE = RSPDA(25)
301 GVALEP = RSPDA(26)
302 GHEXIT = RSPDA(27)
303 H20XIT = RSPDA(29)
304 CC *** NEED TO CHECK ON VALUE OF H AND H20
305 C GVALKE=0.01*WHEXIT**2
306 WIXITM=SQRT(100.*GVALKE)/10.
307 RETURN
308
309 C-----
310 C CHAPTER 1: CALLED AT THE START OF EACH TIME STEP.
311 C SET 'DT' HERE WHEN TLAST SET NEGATIVE IN BLOCK DATA.
312 C 'ATIME + DT' GIVES THE END TIME OF THE CURRENT TIME STEP.
313 C NOT ACCESSED IF STEADY OR PARABOLIC.
314 C-----
315 100 CONTINUE
316 RETURN
317
318 C-----
319 C CHAPTER 2: CALLED AT THE START OF EACH SWEEP.
320 C-----
321 200 CONTINUE
322 RETURN
323
324 C-----
325 C CHAPTER 3: CALLED AT THE START OF EACH SLAB
326 C NOT ACCESSED IF PARABOLIC, BUT 'STRIDE' IS.
327 C-----
328 300 CONTINUE
329 C ***
330 IF(.NOT.(RESTRT.AND.ISWP.EQ.FSWEEP)) RETURN
331 CALL GET(C1,GC1,NY,NX)
332 CALL GET(T1,GT1,NY,NX)
333 CALL GVISC(GT1,GC1,GMU1L,NY,NX)
334
335 C ***
336 RETURN
337
338 C-----
339 C CHAPTER 4: CALLED AT THE START OF EACH RE-CALCULATION OF
340 C VARIABLES P1,...,C4 AT CURRENT SLAB. ITND= ITERATION NUMBER.
341 C-----
342 400 CONTINUE
343 RETURN
344
345 C-----
346 C CHAPTER 5: GROUND CALLED WHEN SOURCE TERM IS COMPUTED.
347 C INDVAR GIVES DEPENDENT VARIABLE IN QUESTION IE. U1,...,C4.
348 C TO ADD SOURCE TO DEPENDENT VARIABLE C1(SAY) FOR IX=IXF,IXL
349 C AND IV=IVF,IVL INSERT STATEMENT:
350 C IF(INDVAR.EQ.C1)
351 C &CALL ADD(INDVAR,IXF,IXL,IVF,IVL,TYPE,CM,VM,CVAR,VVAR,NY,NX)
352 C NOTES ON 'ADD':
353 C *SOURCE= (CVAR(IV,IX)+AMAX1(0.0,MASFLO))*(VVAR(IV,IX)-PHI),
354 C WHERE 'PHI' IS IN-CELL VALUE OF VARIABLE IN QUESTION.
355 C *MASFLO= CM(IV,IX)*(VM(IV,IX)-P).
356 C WHERE 'P' IS THE IN-CELL PRESSURE.
357 C *FOR INDVAR= M1, OR =M2, SOURCE ADDED IS 'MASFLO' ONLY.
358 C EXCEPT FOR ONEPHS=.F. & MASFLO < 0.0 (IE. OUTFLOW) WHEN
359 C CM(IV,IX) IS MULTIPLIED BY R1*D1 (FOR M1) & R2*D2 (FOR M2).
360 C *BOTH 'CVAR' & 'CM' ARE MULTIPLIED BY CELL-GEOMETRY QUANTITY
361 C DICTATED BY SETTING OF 'TYPE' (=CELL, EAST AREA,...,VOLUME).
362 C *TYPE-SPECIFIED AREAS ARE CALCULATED AS IF BLOCKAGE ABSENT.
363 C BUT 'VOLUME' WITH ACCOUNT FOR ITS PRESENCE.
364 C *FOR ALL SOLVED VARIABLES, INCLUDING M1 ( & M2 WHEN ONEPHS=.F),
365 C IF 'CM' > 0.0 CALL 'ADD' FOR M1 & M2 ALTHOUGH 'CVAR' & 'VVAR'

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360 C HAVE NO SIGNIFICANCE THEY MUST BE ENTERED AS ARGUMENTS.
361 C *'CVAR', 'VVAR', 'CM' & 'VM' MUST BE DIMENSIONED NY,NX.
362 C -----
363 C
364 C 500 CONTINUE
365 C ***
366 C IF(INDVAR.NE.U1) GO TO 502
367 C FIX ANGULAR MOMENTUM IN CELL(S) COMPLETELY ENFRAMED BY BLADES
368 IF(IZED.LT.21) GO TO 502
369 CALL GET1D(R,GR,NY)
370 JIYF = 32
371 JIYL = 40
372 DO 501 JIX=1,NX
373 DO 501 JIY=JIYF,JIYL
374 CVAR(JIY,JIX)=FIXVAL
375 VVAR(JIY,JIX)=GOMEGA*GR(JIY)**2
376 CALL ADD(U1,1,NX,JIYF,JIYL,CELL,CM,VM,CVAR,VVAR,NY,NX)
377 C
378 502 IF(INDVAR.NE.C1) GO TO 503
379 C
380 C GET ADDITIONAL VARIABLES REQUIRED FOR TOTAL PRESSURE CALCULATIONS
381 CALL GET(P1,GPT,NY,NX)
382 CALL GET(W1L,GW1L,NY,NX)
383 C
384 C SAVE CALCULATED EFFECTIVE VISCOSITIES FOR PRINTOUT
385 CALL GET(MU1,GMU1,NY,NX)
386 C
387 C GET VARIABLES REQUIRED FOR SUBROUTINE GWALL (IN COMMON/WALLG/)
388 CALL GET(U1,GU1,NY,NX)
389 CALL GET(V1,GV1,NY,NX)
390 CALL GET(W1,GW1,NY,NX)
391 CALL GET(D1,GD1,NY,NX)
392 C!! NB. THE "GET" COMMAND CANNOT BE USED FOR MU1LAM IN CH. 5 AND
393 C!! SO THE LOCAL LAMINAR VISCOSITY ARRAY (GMU1L) MUST BE SET-UP
394 C!! ELSEWHERE IN GROUND. FOR THE CURRENT PROBLEM IT IS CALCULATED (FOR
395 C!! CONVENIENCE) IN CH. 10, AND THEN "SET" IN CH. 12 (FOR PASSING
396 C!! BACK TO EARTH).
397 C
398 CALL GET1D(DXU,GDXU,NX)
399 CALL GET1D(DYV,GDYV,NY)
400 CALL GET1D(DZW,GDZW,NZ)
401 CALL GET1D(R,GR,NY)
402 C
403 C *** CALCULATE WALL FRICTION EFFECTS ***
404 C
405 503 GVELUW=INDVAR.EQ.U1.OR.INDVAR.EQ.W1
406 GVELVW=INDVAR.EQ.V1.OR.INDVAR.EQ.W1
407 GVELUV=INDVAR.EQ.U1.OR.INDVAR.EQ.V1
408 GKEEP=INDVAR.EQ.KE.OR.INDVAR.EQ.EP
409 C
410 C *** ROTATING WALL(S) ***
411 C
412 C *** ROW 1
413 IF(.NOT.(IZED.GE.13.AND.IZED.LE.19)) GO TO 504
414 IF(.NOT.GVELUW) GO TO 5040
415 CALL GWALL(INDVAR,1,NX,1,1,IZED,SOUTH,GOMEGA,O.O.,O.,-1.)
416 CALL ADD(INDVAR,1,NX,1,1,SOUTH,CM,VM,CVAR,VVAR,NY,NX)
417 IF(.NOT.GKEEP) GO TO 504
418 CALL GWALL(INDVAR,1,NX,1,1,IZED,SOUTH,GOMEGA,O.O.,O.,-1.)
419 CALL ADD(INDVAR,1,NX,1,1,CELL,CM,VM,CVAR,VVAR,NY,NX)

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420 504 IF(.NOT.(IZED.EQ.19)) GO TO 505
421 IF(.NOT.GVELUV) GO TO 5050
422 CALL GWALL(INDVAR,1,NX,1,1,IZED,HIGH,GOMEGA,O.O.O.,-1.)
423 CALL ADD(INDVAR,1,NX,1,1,HIGH,CM,VM,CVAR,VVAR,NY,NX)
424 5050 IF(.NOT.GKEEP) GO TO 505
425 CALL GWALL(INDVAR,1,NX,1,1,IZED,HIGH,GOMEGA,O.O.O.,-1.)
426 CALL ADD(INDVAR,1,NX,1,1,CELL,CM,VM,CVAR,VVAR,NY,NX)
427 C
428 C *** ROWS 2 TO 3
429 505 IF(.NOT.(IZED.EQ.21)) GO TO 506
430 IF(.NOT.GVELUV) GO TO 5060
431 CALL GWALL(INDVAR,1,NX,2,3,IZED,HIGH,GOMEGA,O.O.O.,-1.)
432 CALL ADD(INDVAR,1,NX,2,3,HIGH,CM,VM,CVAR,VVAR,NY,NX)
433 5060 IF(.NOT.GKEEP) GO TO 506
434 CALL GWALL(INDVAR,1,NX,2,3,IZED,HIGH,GOMEGA,O.O.O.,-1.)
435 CALL ADD(INDVAR,1,NX,2,3,CELL,CM,VM,CVAR,VVAR,NY,NX)
436 C
437 506 IF(.NOT.(IZED,GE.20,AND,IZED.LE.21)) GO TO 507
438 IF(.NOT.GVELUV) GO TO 5070
439 CALL GWALL(INDVAR,1,NX,2,2,IZED,SOUTH,GOMEGA,O.O.O.,-1.)
440 CALL ADD(INDVAR,1,NX,2,2,SOUTH,CM,VM,CVAR,VVAR,NY,NX)
441 5070 IF(.NOT.GKEEP) GO TO 507
442 CALL GWALL(INDVAR,1,NX,2,2,IZED,SOUTH,GOMEGA,O.O.O.,-1.)
443 CALL ADD(INDVAR,1,NX,2,2,CELL,CM,VM,CVAR,VVAR,NY,NX)
444 C
445 507 IF(.NOT.(IZED,GE.17,AND,IZED.LE.21)) GO TO 508
446 IF(.NOT.GVELUV) GO TO 5080
447 CALL GWALL(INDVAR,1,NX,3,3,IZED,NORTH,GOMEGA,O.O.O.,-1.)
448 CALL ADD(INDVAR,1,NX,3,3,NORTH,CM,VM,CVAR,VVAR,NY,NX)
449 5080 IF(.NOT.GKEEP) GO TO 508
450 CALL GWALL(INDVAR,1,NX,3,3,IZED,NORTH,GOMEGA,O.O.O.,-1.)
451 CALL ADD(INDVAR,1,NX,3,3,CELL,CM,VM,CVAR,VVAR,NY,NX)
452 C
453 C *** ROW 4
454 508 IF(.NOT.(IZED.EQ.16)) GO TO 509
455 IF(.NOT.GVELUV) GO TO 5090
456 CALL GWALL(INDVAR,1,NX,4,4,IZED,HIGH,GOMEGA,O.O.O.,-1.)
457 CALL ADD(INDVAR,1,NX,4,4,HIGH,CM,VM,CVAR,VVAR,NY,NX)
458 5090 IF(.NOT.GKEEP) GO TO 509
459 CALL GWALL(INDVAR,1,NX,4,4,IZED,HIGH,GOMEGA,O.O.O.,-1.)
460 CALL ADD(INDVAR,1,NX,4,4,CELL,CM,VM,CVAR,VVAR,NY,NX)
461 C
462 C *** ROWS 5 TO 10
463 509 IF(.NOT.(IZED,GE.17,AND,IZED.LE.20)) GO TO 510
464 IF(.NOT.GVELUV) GO TO 5100
465 CALL GWALL(INDVAR,1,NX,5,5,IZED,SOUTH,GOMEGA,O.O.O.,-1.)
466 CALL ADD(INDVAR,1,NX,5,5,SOUTH,CM,VM,CVAR,VVAR,NY,NX)
467 5100 IF(.NOT.GKEEP) GO TO 510
468 CALL GWALL(INDVAR,1,NX,5,5,IZED,SOUTH,GOMEGA,O.O.O.,-1.)
469 CALL ADD(INDVAR,1,NX,5,5,CELL,CM,VM,CVAR,VVAR,NY,NX)
470 C
471 510 IF(.NOT.(IZED.EQ.20)) GO TO 511
472 IF(.NOT.GVELUV) GO TO 5110
473 CALL GWALL(INDVAR,1,NX,5,10,IZED,HIGH,GOMEGA,O.O.O.,-1.)
474 CALL ADD(INDVAR,1,NX,5,10,HIGH,CM,VM,CVAR,VVAR,NY,NX)
475 5110 IF(.NOT.GKEEP) GO TO 511
476 CALL GWALL(INDVAR,1,NX,5,10,IZED,HIGH,GOMEGA,O.O.O.,-1.)
477 CALL ADD(INDVAR,1,NX,5,10,CELL,CM,VM,CVAR,VVAR,NY,NX)
478 C
479 511 IF(.NOT.(IZED.EQ.21)) GO TO 512

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C
512 IF(.NOT.GVELUW) GO TO 5120
CALL GWALL(INDVAR,1,NX,10,10,10,ZED,SOUTH,GOMEGA,O.,O.O.,-1.)
CALL ADD(INDVAR,1,NX,10,10,SOUTH,CM,VM,CVAR,VVAR,NY,NX)
5120 IF(.NOT.GKEEP) GO TO 512
CALL GWALL(INDVAR,1,NX,10,10,10,ZED,SOUTH,GOMEGA,O.,O.O.,-1.)
CALL ADD(INDVAR,1,NX,10,10,CELL,CM,VM,CVAR,VVAR,NY,NX)
C
513 IF(.NOT.(IZED.EQ.22)) GO TO 513
IF(.NOT.GVELUV) GO TO 5130
CALL GWALL(INDVAR,1,NX,10,10,10,ZED,HIGH,GOMEGA,O.,O.O.,-1.)
CALL ADD(INDVAR,1,NX,10,10,HIGH,CM,VM,CVAR,VVAR,NY,NX)
5130 IF(.NOT.GKEEP) GO TO 513
CALL GWALL(INDVAR,1,NX,10,10,10,ZED,HIGH,GOMEGA,O.,O.O.,-1.)
CALL ADD(INDVAR,1,NX,10,10,CELL,CM,VM,CVAR,VVAR,NY,NX)
C
C *** ROW 11
514 IF(.NOT.(IZED.EQ.23)) GO TO 514
IF(.NOT.GVELUW) GO TO 5140
CALL GWALL(INDVAR,1,NX,11,11,11,ZED,SOUTH,GOMEGA,O.,O.O.,-1.)
CALL ADD(INDVAR,1,NX,11,11,SOUTH,CM,VM,CVAR,VVAR,NY,NX)
5140 IF(.NOT.GKEEP) GO TO 514
CALL GWALL(INDVAR,1,NX,11,11,11,ZED,SOUTH,GOMEGA,O.,O.O.,-1.)
CALL ADD(INDVAR,1,NX,11,11,CELL,CM,VM,CVAR,VVAR,NY,NX)
C
515 IF(.NOT.(IZED.EQ.24)) GO TO 515
IF(.NOT.GVELUV) GO TO 5150
CALL GWALL(INDVAR,1,NX,11,11,11,ZED,HIGH,GOMEGA,O.,O.O.,-1.)
CALL ADD(INDVAR,1,NX,11,11,HIGH,CM,VM,CVAR,VVAR,NY,NX)
5150 IF(.NOT.GKEEP) GO TO 515
CALL GWALL(INDVAR,1,NX,11,11,11,ZED,HIGH,GOMEGA,O.,O.O.,-1.)
CALL ADD(INDVAR,1,NX,11,11,CELL,CM,VM,CVAR,VVAR,NY,NX)
C
C *** ROWS 12 TO 13
516 IF(.NOT.(IZED.EQ.24)) GO TO 516
IF(.NOT.GVELUV) GO TO 5160
CALL GWALL(INDVAR,1,NX,12,13,13,ZED,HIGH,GOMEGA,O.,O.O.,-1.)
CALL ADD(INDVAR,1,NX,12,13,HIGH,CM,VM,CVAR,VVAR,NY,NX)
5160 IF(.NOT.GKEEP) GO TO 516
CALL GWALL(INDVAR,1,NX,12,13,13,ZED,HIGH,GOMEGA,O.,O.O.,-1.)
CALL ADD(INDVAR,1,NX,12,13,CELL,CM,VM,CVAR,VVAR,NY,NX)
C
517 IF(.NOT.(IZED.GE.21.AND.IZED.LE.24)) GO TO 517
IF(.NOT.GVELUW) GO TO 5170
CALL GWALL(INDVAR,1,NX,13,13,13,ZED,NORTH,GOMEGA,O.,O.O.,-1.)
CALL ADD(INDVAR,1,NX,13,13,NORTH,CM,VM,CVAR,VVAR,NY,NX)
5170 IF(.NOT.GKEEP) GO TO 517
CALL GWALL(INDVAR,1,NX,13,13,13,ZED,NORTH,GOMEGA,O.,O.O.,-1.)
CALL ADD(INDVAR,1,NX,13,13,CELL,CM,VM,CVAR,VVAR,NY,NX)
C
C *** ROW 14
518 IF(.NOT.(IZED.EQ.20)) GO TO 518
IF(.NOT.GVELUV) GO TO 5180
CALL GWALL(INDVAR,1,NX,14,14,14,ZED,HIGH,GOMEGA,O.,O.O.,-1.)
CALL ADD(INDVAR,1,NX,14,14,HIGH,CM,VM,CVAR,VVAR,NY,NX)
5180 IF(.NOT.GKEEP) GO TO 518
CALL GWALL(INDVAR,1,NX,14,14,14,ZED,HIGH,GOMEGA,O.,O.O.,-1.)
CALL ADD(INDVAR,1,NX,14,14,CELL,CM,VM,CVAR,VVAR,NY,NX)
C
C *** ROW 15
519 IF(.NOT.(IZED.GE.21.AND.IZED.LE.23)) GO TO 519
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DO 5241 JIX=1,NX
DO 5241 JIY=32,40
5241 CVAR(JIY,JIX)=CVAR(JIY,JIX)*GBCELL
CALL ADD(INDVAR,1,NX,32,40,EAST,CM,VM,CVAR,VVAR,NY,NX)
C
CALL GWALL(INDVAR,1,NX,32,40,IZED,WEST,GOMEGA,O.O.O.,GONEBL)
DO 5242 JIX=1,NX
DO 5242 JIY=32,40
5242 CVAR(JIY,JIX)=CVAR(JIY,JIX)*GBCELL
CALL ADD(INDVAR,1,NX,32,40,WEST,CM,VM,CVAR,VVAR,NY,NX)
C
5250 IF(.NOT.GKEEP) GO TO 5251
CALL GWALL(INDVAR,1,NX,32,40,IZED,EAST,GOMEGA,O.O.O.,GONEBL)
CALL ADD(INDVAR,1,NX,32,40,CELL,CM,VM,CVAR,VVAR,NY,NX)
C
C
5251 IF(.NOT.(IZED,GE,21,AND,IZED,LE,28)) GO TO 525
IF(.NOT.GVELUW) GO TO 5252
CALL GWALL(INDVAR,1,NX,32,32,IZED,SOUTH,GOMEGA,O.O.O.,-1.)
CALL ADD(INDVAR,1,NX,32,32,SOUTH,CM,VM,CVAR,VVAR,NY,NX)
5252 IF(.NOT.GKEEP) GO TO 525
CALL GWALL(INDVAR,1,NX,32,32,IZED,SOUTH,GOMEGA,O.O.O.,-1.)
CALL ADD(INDVAR,1,NX,32,32,CELL,CM,VM,CVAR,VVAR,NY,NX)
C
525 IF(.NOT.(IZED,GE,17,AND,IZED,LE,28)) GO TO 526
IF(.NOT.GVELUW) GO TO 5260
CALL GWALL(INDVAR,1,NX,40,40,IZED,NORTH,GOMEGA,O.O.O.,-1.)
CALL ADD(INDVAR,1,NX,40,40,NORTH,CM,VM,CVAR,VVAR,NY,NX)
5260 IF(.NOT.GKEEP) GO TO 526
CALL GWALL(INDVAR,1,NX,40,40,IZED,NORTH,GOMEGA,O.O.O.,-1.)
CALL ADD(INDVAR,1,NX,40,40,CELL,CM,VM,CVAR,VVAR,NY,NX)
C
C *** NON-ROTATING WALLS ***
C
C *** ROW 1
526 IF(.NOT.(IZED,EQ,13)) GO TO 530
IF(.NOT.GVELUW) GO TO 5300
CALL GWALL(INDVAR,1,NX,1,1,IZED,NORTH,O.O.O.,-1.)
CALL ADD(INDVAR,1,NX,1,1,NORTH,CM,VM,CVAR,VVAR,NY,NX)
5300 IF(.NOT.GKEEP) GO TO 530
CALL GWALL(INDVAR,1,NX,1,1,IZED,NORTH,O.O.O.,-1.)
CALL ADD(INDVAR,1,NX,1,1,CELL,CM,VM,CVAR,VVAR,NY,NX)
C
C *** ROWS 2 TO 5
530 IF(.NOT.(IZED,EQ,14)) GO TO 531
IF(.NOT.GVELUW) GO TO 5310
CALL GWALL(INDVAR,1,NX,2,5,IZED,LOW,O.O.O.,-1.)
CALL ADD(INDVAR,1,NX,2,5,LOW,CM,VM,CVAR,VVAR,NY,NX)
5310 IF(.NOT.GKEEP) GO TO 531
CALL GWALL(INDVAR,1,NX,2,5,IZED,LOW,O.O.O.,-1.)
CALL ADD(INDVAR,1,NX,2,5,CELL,CM,VM,CVAR,VVAR,NY,NX)
C
531 IF(.NOT.(IZED,EQ,13)) GO TO 532
IF(.NOT.GVELUW) GO TO 5320
CALL GWALL(INDVAR,1,NX,5,5,IZED,SOUTH,O.O.O.,-1.)
CALL ADD(INDVAR,1,NX,5,5,SOUTH,CM,VM,CVAR,VVAR,NY,NX)
5320 IF(.NOT.GKEEP) GO TO 532
CALL GWALL(INDVAR,1,NX,5,5,IZED,SOUTH,O.O.O.,-1.)
CALL ADD(INDVAR,1,NX,5,5,CELL,CM,VM,CVAR,VVAR,NY,NX)
C

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660 532 IF(.NOT.(IZED.EQ.12)) GO TO 533
661 IF(.NOT.GVELUV) GO TO 5330
662 CALL GWALL(INDVAR,1,NX,3,5,IZED,HIGH,O.O.O.O.O.,-1.)
663 CALL ADD(INDVAR,1,NX,3,5,HIGH,CM,VM,CVAR,VVAR,NY,NX)
664 5330 IF(.NOT.GKEEP) GO TO 533
665 CALL GWALL(INDVAR,1,NX,3,5,IZED,HIGH,O.O.O.O.O.,-1.)
666 CALL ADD(INDVAR,1,NX,3,5,CELL,CM,VM,CVAR,VVAR,NY,NX)
667 C
668 533 IF(.NOT.(IZED.GE.5.AND.IZED.LE.12)) GO TO 534
669 IF(.NOT.GVELUV) GO TO 5340
670 CALL GWALL(INDVAR,1,NX,3,3,IZED,SOUTH,O.O.O.O.O.,-1.)
671 CALL ADD(INDVAR,1,NX,3,3,SOUTH,CM,VM,CVAR,VVAR,NY,NX)
672 5340 IF(.NOT.GKEEP) GO TO 534
673 CALL GWALL(INDVAR,1,NX,3,3,IZED,SOUTH,O.O.O.O.O.,-1.)
674 CALL ADD(INDVAR,1,NX,3,3,CELL,CM,VM,CVAR,VVAR,NY,NX)
675 C
676 534 IF(.NOT.(IZED.EQ.5)) GO TO 535
677 IF(.NOT.GVELUV) GO TO 5350
678 CALL GWALL(INDVAR,1,NX,3,3,IZED,LOW,O.O.O.O.O.,-1.)
679 CALL ADD(INDVAR,1,NX,3,3,LOW,CM,VM,CVAR,VVAR,NY,NX)
680 5350 IF(.NOT.GKEEP) GO TO 535
681 CALL GWALL(INDVAR,1,NX,3,3,IZED,LOW,O.O.O.O.O.,-1.)
682 CALL ADD(INDVAR,1,NX,3,3,CELL,CM,VM,CVAR,VVAR,NY,NX)
683 C
684 535 IF(.NOT.(IZED.EQ.4)) GO TO 537
685 IF(.NOT.GVELUV) GO TO 5360
686 CALL GWALL(INDVAR,1,NX,4,5,IZED,SOUTH,O.O.O.O.O.,-1.)
687 CALL ADD(INDVAR,1,NX,4,5,SOUTH,CM,VM,CVAR,VVAR,NY,NX)
688 5360 IF(.NOT.GKEEP) GO TO 536
689 CALL GWALL(INDVAR,1,NX,4,5,IZED,SOUTH,O.O.O.O.O.,-1.)
690 CALL ADD(INDVAR,1,NX,4,5,CELL,CM,VM,CVAR,VVAR,NY,NX)
691 536 IF(.NOT.GVELUV) GO TO 5370
692 CALL GWALL(INDVAR,1,NX,4,4,IZED,LOW,O.O.O.O.O.,-1.)
693 CALL ADD(INDVAR,1,NX,4,4,LOW,CM,VM,CVAR,VVAR,NY,NX)
694 5370 IF(.NOT.GKEEP) GO TO 537
695 CALL GWALL(INDVAR,1,NX,4,4,IZED,LOW,O.O.O.O.O.,-1.)
696 CALL ADD(INDVAR,1,NX,4,4,CELL,CM,VM,CVAR,VVAR,NY,NX)
697 C
698 C *** ROWS 6 TO 9
699 537 IF(.NOT.(IZED.EQ.3)) GO TO 539
700 IF(.NOT.GVELUV) GO TO 5380
701 CALL GWALL(INDVAR,1,NX,6,7,IZED,SOUTH,O.O.O.O.O.,-1.)
702 CALL ADD(INDVAR,1,NX,6,7,SOUTH,CM,VM,CVAR,VVAR,NY,NX)
703 5380 IF(.NOT.GKEEP) GO TO 538
704 CALL GWALL(INDVAR,1,NX,6,7,IZED,SOUTH,O.O.O.O.O.,-1.)
705 CALL ADD(INDVAR,1,NX,6,7,CELL,CM,VM,CVAR,VVAR,NY,NX)
706 538 IF(.NOT.GVELUV) GO TO 5390
707 CALL GWALL(INDVAR,1,NX,6,7,IZED,LOW,O.O.O.O.O.,-1.)
708 CALL ADD(INDVAR,1,NX,6,7,LOW,CM,VM,CVAR,VVAR,NY,NX)
709 5390 IF(.NOT.GKEEP) GO TO 539
710 CALL GWALL(INDVAR,1,NX,6,7,IZED,LOW,O.O.O.O.O.,-1.)
711 CALL ADD(INDVAR,1,NX,6,7,CELL,CM,VM,CVAR,VVAR,NY,NX)
712 C
713 539 IF(.NOT.(IZED.EQ.2)) GO TO 5411
714 IF(.NOT.GVELUV) GO TO 5400
715 CALL GWALL(INDVAR,1,NX,8,8,IZED,SOUTH,O.O.O.O.O.,-1.)
716 CALL ADD(INDVAR,1,NX,8,8,SOUTH,CM,VM,CVAR,VVAR,NY,NX)
717 5400 IF(.NOT.GKEEP) GO TO 540
718 CALL GWALL(INDVAR,1,NX,8,8,IZED,SOUTH,O.O.O.O.O.,-1.)
719 CALL ADD(INDVAR,1,NX,8,8,CELL,CM,VM,CVAR,VVAR,NY,NX)

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540 IF(.NOT.GVELUV) GO TO 5410
CALL GWALL(INDVAR,1,NX,8,8,IZED,LOW,O.O.,O.,-1.)
CALL ADD(INDVAR,1,NX,8,8,LOW,CM,VM,CVAR,VVAR,NY,NX)
5410 IF(.NOT.GKEEP) GO TO 5411
CALL GWALL(INDVAR,1,NX,8,8,IZED,LOW,O.O.,O.,-1.)
CALL ADD(INDVAR,1,NX,8,8,CELL,CM,VM,CVAR,VVAR,NY,NX)
C
5411 IF(.NOT.(IZED.EQ.2)) GO TO 541
IF(.NOT.GVELUV) GO TO 5414
CALL GWALL(INDVAR,1,NX,9,9,IZED,LOW,O.O.,O.,-1.)
CALL ADD(INDVAR,1,NX,9,9,LOW,CM,VM,CVAR,VVAR,NY,NX)
5414 IF(.NOT.GKEEP) GO TO 541
CALL GWALL(INDVAR,1,NX,9,9,IZED,LOW,O.O.,O.,-1.)
CALL ADD(INDVAR,1,NX,9,9,CELL,CM,VM,CVAR,VVAR,NY,NX)
C
C *** ROW 10
541 IF(.NOT.(IZED.EQ.1)) GO TO 545
IF(.NOT.GVELUV) GO TO 5450
CALL GWALL(INDVAR,1,NX,10,10,IZED,SOUTH,O.O.,O.,-1.)
CALL ADD(INDVAR,1,NX,10,10,SOUTH,CM,VM,CVAR,VVAR,NY,NX)
CALL GWALL(INDVAR,1,NX,10,10,IZED,NORTH,O.O.,O.,-1.)
CALL ADD(INDVAR,1,NX,10,10,NORTH,CM,VM,CVAR,VVAR,NY,NX)
5450 IF(.NOT.GKEEP) GO TO 545
CALL GWALL(INDVAR,1,NX,10,10,IZED,SOUTH,O.O.,O.,-1.)
CALL ADD(INDVAR,1,NX,10,10,CELL,CM,VM,CVAR,VVAR,NY,NX)
C
545 IF(.NOT.(IZED.GE.2.AND.IZED.LE.4)) GO TO 546
IF(.NOT.GVELUV) GO TO 5460
CALL GWALL(INDVAR,1,NX,10,10,IZED,NORTH,O.O.,O.,-1.)
CALL ADD(INDVAR,1,NX,10,10,NORTH,CM,VM,CVAR,VVAR,NY,NX)
5460 IF(.NOT.GKEEP) GO TO 546
CALL GWALL(INDVAR,1,NX,10,10,IZED,NORTH,O.O.,O.,-1.)
CALL ADD(INDVAR,1,NX,10,10,CELL,CM,VM,CVAR,VVAR,NY,NX)
546 IF(.NOT.GVELUV) GO TO 5470
CALL GWALL(INDVAR,1,NX,10,10,IZED,LOW,O.O.,O.,-1.)
CALL ADD(INDVAR,1,NX,10,10,LOW,CM,VM,CVAR,VVAR,NY,NX)
5470 IF(.NOT.GKEEP) GO TO 547
CALL GWALL(INDVAR,1,NX,10,10,IZED,LOW,O.O.,O.,-1.)
CALL ADD(INDVAR,1,NX,10,10,CELL,CM,VM,CVAR,VVAR,NY,NX)
C
C *** ROW 11
547 IF(.NOT.(IZED.GE.3.AND.IZED.LE.4)) GO TO 549
IF(.NOT.GVELUV) GO TO 5480
CALL GWALL(INDVAR,1,NX,11,11,IZED,LOW,O.O.,O.,-1.)
CALL ADD(INDVAR,1,NX,11,11,LOW,CM,VM,CVAR,VVAR,NY,NX)
5480 IF(.NOT.GKEEP) GO TO 548
CALL GWALL(INDVAR,1,NX,11,11,IZED,LOW,O.O.,O.,-1.)
CALL ADD(INDVAR,1,NX,11,11,CELL,CM,VM,CVAR,VVAR,NY,NX)
548 IF(.NOT.GVELUV) GO TO 5490
CALL GWALL(INDVAR,1,NX,11,11,IZED,SOUTH,O.O.,O.,-1.)
CALL ADD(INDVAR,1,NX,11,11,SOUTH,CM,VM,CVAR,VVAR,NY,NX)
5490 IF(.NOT.GKEEP) GO TO 549
CALL GWALL(INDVAR,1,NX,11,11,IZED,SOUTH,O.O.,O.,-1.)
CALL ADD(INDVAR,1,NX,11,11,CELL,CM,VM,CVAR,VVAR,NY,NX)
C
C *** ROWS 12 TO 17
549 IF(.NOT.(IZED.EQ.3)) GO TO 550
IF(.NOT.GVELUV) GO TO 5500
CALL GWALL(INDVAR,1,NX,12,17,IZED,LOW,O.O.,O.,-1.)
CALL ADD(INDVAR,1,NX,12,17,LOW,CM,VM,CVAR,VVAR,NY,NX)

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780 5500 IF(.NOT.GKEEP) GO TO 550
781 CALL GWALL(INDVAR,1,NX,12,17,1ZED,LOW,O.O.,O.O.,-1.)
782 CALL ADD(INDVAR,1,NX,12,17,CELL,CM,VM,CVAR,VVAR,NV,NX)
783
784 C
785 550 IF(.NOT.(1ZED.GE.3.AND.1ZED.LE.4)) GO TO 551
786 IF(.NOT.GVELUW) GO TO 5510
787 CALL GWALL(INDVAR,1,NX,17,17,1ZED,NORTH,O.O.,O.O.,-1.)
788 CALL ADD(INDVAR,1,NX,17,17,NORTH,CM,VM,CVAR,VVAR,NV,NX)
789 IF(.NOT.GKEEP) GO TO 551
790 CALL GWALL(INDVAR,1,NX,17,17,1ZED,NORTH,O.O.,O.O.,-1.)
791 CALL ADD(INDVAR,1,NX,17,17,CELL,CM,VM,CVAR,VVAR,NV,NX)
792 C
793 C *** ROWS 18 TO 21
794 551 IF(.NOT.(1ZED.EQ.4)) GO TO 552
795 IF(.NOT.GVELUW) GO TO 5520
796 CALL GWALL(INDVAR,1,NX,18,20,1ZED,LOW,O.O.,O.O.,-1.)
797 CALL ADD(INDVAR,1,NX,18,20,LOW,CM,VM,CVAR,VVAR,NV,NX)
798 IF(.NOT.GKEEP) GO TO 552
799 CALL GWALL(INDVAR,1,NX,18,20,1ZED,LOW,O.O.,O.O.,-1.)
800 CALL ADD(INDVAR,1,NX,18,20,CELL,CM,VM,CVAR,VVAR,NV,NX)
801 C
802 552 IF(.NOT.(1ZED.EQ.4)) GO TO 553
803 IF(.NOT.GVELUW) GO TO 5530
804 CALL GWALL(INDVAR,1,NX,21,21,1ZED,NORTH,O.O.,O.O.,-1.)
805 CALL ADD(INDVAR,1,NX,21,21,NORTH,CM,VM,CVAR,VVAR,NV,NX)
806 IF(.NOT.GKEEP) GO TO 553
807 CALL GWALL(INDVAR,1,NX,21,21,1ZED,NORTH,O.O.,O.O.,-1.)
808 CALL ADD(INDVAR,1,NX,21,21,CELL,CM,VM,CVAR,VVAR,NV,NX)
809 C
810 553 IF(.NOT.(1ZED.GE.5.AND.1ZED.LE.6)) GO TO 555
811 IF(.NOT.GVELUW) GO TO 5540
812 CALL GWALL(INDVAR,1,NX,21,21,1ZED,NORTH,O.O.,O.O.,-1.)
813 CALL ADD(INDVAR,1,NX,21,21,NORTH,CM,VM,CVAR,VVAR,NV,NX)
814 IF(.NOT.GKEEP) GO TO 555
815 CALL GWALL(INDVAR,1,NX,21,21,1ZED,NORTH,O.O.,O.O.,-1.)
816 CALL ADD(INDVAR,1,NX,21,21,CELL,CM,VM,CVAR,VVAR,NV,NX)
817 C
818 C *** ROWS 22 TO 29
819 555 IF(.NOT.(1ZED.GE.6.AND.1ZED.LE.8)) GO TO 556
820 IF(.NOT.GVELUW) GO TO 5560
821 CALL GWALL(INDVAR,1,NX,22,22,1ZED,NORTH,O.O.,O.O.,-1.)
822 CALL ADD(INDVAR,1,NX,22,22,NORTH,CM,VM,CVAR,VVAR,NV,NX)
823 IF(.NOT.GKEEP) GO TO 556
824 CALL GWALL(INDVAR,1,NX,22,22,1ZED,NORTH,O.O.,O.O.,-1.)
825 CALL ADD(INDVAR,1,NX,22,22,CELL,CM,VM,CVAR,VVAR,NV,NX)
826 C
827 556 IF(.NOT.(1ZED.EQ.9)) GO TO 557
828 IF(.NOT.GVELUW) GO TO 5570
829 CALL GWALL(INDVAR,1,NX,23,23,1ZED,NORTH,O.O.,O.O.,-1.)
830 CALL ADD(INDVAR,1,NX,23,23,NORTH,CM,VM,CVAR,VVAR,NV,NX)
831 IF(.NOT.GKEEP) GO TO 557
832 CALL GWALL(INDVAR,1,NX,23,23,1ZED,NORTH,O.O.,O.O.,-1.)
833 CALL ADD(INDVAR,1,NX,23,23,CELL,CM,VM,CVAR,VVAR,NV,NX)
834 C
835 557 IF(.NOT.(1ZED.EQ.10)) GO TO 558
836 IF(.NOT.GVELUW) GO TO 5580
837 CALL GWALL(INDVAR,1,NX,24,24,1ZED,NORTH,O.O.,O.O.,-1.)
838 CALL ADD(INDVAR,1,NX,24,24,NORTH,CM,VM,CVAR,VVAR,NV,NX)
839 IF(.NOT.GKEEP) GO TO 558
840 CALL GWALL(INDVAR,1,NX,24,24,1ZED,NORTH,O.O.,O.O.,-1.)

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840 CALL ADD(INDVAR, 1, NX, 24, 24, CELL, CM, VM, CVAR, VVAR, NY, NX)
841
842 IF(.NOT.(IZED.EQ.11)) GO TO 559
843 IF(.NOT.GVELUW) GO TO 5590
844 CALL GWALL(INDVAR, 1, NX, 25, 25, IZED, NORTH, O., O., O., -1.)
845 CALL ADD(INDVAR, 1, NX, 25, 25, NORTH, CM, VM, CVAR, VVAR, NY, NX)
846 IF(.NOT.GKEEP) GO TO 559
847 CALL GWALL(INDVAR, 1, NX, 25, 25, IZED, NORTH, O., O., O., -1.)
848 CALL ADD(INDVAR, 1, NX, 25, 25, CELL, CM, VM, CVAR, VVAR, NY, NX)
849
850 IF(.NOT.(IZED.EQ.12)) GO TO 560
851 IF(.NOT.GVELUW) GO TO 5600
852 CALL GWALL(INDVAR, 1, NX, 26, 26, IZED, NORTH, O., O., O., -1.)
853 CALL ADD(INDVAR, 1, NX, 26, 26, NORTH, CM, VM, CVAR, VVAR, NY, NX)
854 IF(.NOT.GKEEP) GO TO 560
855 CALL GWALL(INDVAR, 1, NX, 26, 26, IZED, NORTH, O., O., O., -1.)
856 CALL ADD(INDVAR, 1, NX, 26, 26, CELL, CM, VM, CVAR, VVAR, NY, NX)
857
858 IF(.NOT.(IZED.EQ.13)) GO TO 561
859 IF(.NOT.GVELUW) GO TO 5610
860 CALL GWALL(INDVAR, 1, NX, 27, 27, IZED, NORTH, O., O., O., -1.)
861 CALL ADD(INDVAR, 1, NX, 27, 27, NORTH, CM, VM, CVAR, VVAR, NY, NX)
862 IF(.NOT.GKEEP) GO TO 561
863 CALL GWALL(INDVAR, 1, NX, 27, 27, IZED, NORTH, O., O., O., -1.)
864 CALL ADD(INDVAR, 1, NX, 27, 27, CELL, CM, VM, CVAR, VVAR, NY, NX)
865
866 IF(.NOT.(IZED.EQ.14)) GO TO 562
867 IF(.NOT.GVELUW) GO TO 5620
868 CALL GWALL(INDVAR, 1, NX, 28, 28, IZED, NORTH, O., O., O., -1.)
869 CALL ADD(INDVAR, 1, NX, 28, 28, NORTH, CM, VM, CVAR, VVAR, NY, NX)
870 IF(.NOT.GKEEP) GO TO 562
871 CALL GWALL(INDVAR, 1, NX, 28, 28, IZED, NORTH, O., O., O., -1.)
872 CALL ADD(INDVAR, 1, NX, 28, 28, CELL, CM, VM, CVAR, VVAR, NY, NX)
873
874 IF(.NOT.(IZED.EQ.15)) GO TO 563
875 IF(.NOT.GVELUW) GO TO 5630
876 CALL GWALL(INDVAR, 1, NX, 29, 29, IZED, NORTH, O., O., O., -1.)
877 CALL ADD(INDVAR, 1, NX, 29, 29, NORTH, CM, VM, CVAR, VVAR, NY, NX)
878 IF(.NOT.GKEEP) GO TO 563
879 CALL GWALL(INDVAR, 1, NX, 29, 29, IZED, NORTH, O., O., O., -1.)
880 CALL ADD(INDVAR, 1, NX, 29, 29, CELL, CM, VM, CVAR, VVAR, NY, NX)
881
882 C *** ROWS 30 TO 31
883 IF(.NOT.(IZED.EQ.16)) GO TO 565
884 IF(.NOT.GVELUW) GO TO 5640
885 CALL GWALL(INDVAR, 1, NX, 30, 31, IZED, NORTH, O., O., O., -1.)
886 CALL ADD(INDVAR, 1, NX, 30, 31, NORTH, CM, VM, CVAR, VVAR, NY, NX)
887 IF(.NOT.GKEEP) GO TO 564
888 CALL GWALL(INDVAR, 1, NX, 30, 31, IZED, NORTH, O., O., O., -1.)
889 CALL ADD(INDVAR, 1, NX, 30, 31, CELL, CM, VM, CVAR, VVAR, NY, NX)
890 IF(.NOT.GVELUW) GO TO 5650
891 CALL GWALL(INDVAR, 1, NX, 30, 31, IZED, LOW, O., O., O., -1.)
892 CALL ADD(INDVAR, 1, NX, 30, 31, LOW, CM, VM, CVAR, VVAR, NY, NX)
893 IF(.NOT.GKEEP) GO TO 565
894 CALL GWALL(INDVAR, 1, NX, 30, 31, IZED, LOW, O., O., O., -1.)
895 CALL ADD(INDVAR, 1, NX, 30, 31, CELL, CM, VM, CVAR, VVAR, NY, NX)
896
897 C *** ROWS 32 TO 37
898 IF(.NOT.(IZED.EQ.17)) GO TO 567
899 IF(.NOT.GVELUW) GO TO 5670
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900 CALL GWALL(INDVAR,1,NX,32,37,IZED,LOW,O.,O.,O.,O.,-1.)
901 CALL ADD(INDVAR,1,NX,32,37,LOW,CM,VM,CVAR,VVAR,NY,NX)
902 IF(.NOT.GKEEP) GO TO 567
903 CALL GWALL(INDVAR,1,NX,32,37,IZED,LOW,O.,O.,O.,O.,-1.)
904 CALL ADD(INDVAR,1,NX,32,37,CELL,CM,VM,CVAR,VVAR,NY,NX)
905
906 C *** ROWS 38 TO 39
907 IF(.NOT.(IZED.EQ.18)) GO TO 568
908 IF(.NOT.GVELUV) GO TO 5680
909 CALL GWALL(INDVAR,1,NX,38,39,IZED,LOW,O.,O.,O.,O.,-1.)
910 CALL ADD(INDVAR,1,NX,38,39,LOW,CM,VM,CVAR,VVAR,NY,NX)
911 IF(.NOT.GKEEP) GO TO 568
912 CALL GWALL(INDVAR,1,NX,38,39,IZED,LOW,O.,O.,O.,O.,-1.)
913 CALL ADD(INDVAR,1,NX,38,39,CELL,CM,VM,CVAR,VVAR,NY,NX)
914
915 C *** ROW 40
916 IF(.NOT.(IZED.EQ.17)) GO TO 575
917 IF(.NOT.GVELUV) GO TO 5690
918 CALL GWALL(INDVAR,1,NX,40,40,IZED,SOUTH,O.,O.,O.,O.,-1.)
919 CALL ADD(INDVAR,1,NX,40,40,SOUTH,CM,VM,CVAR,VVAR,NY,NX)
920 IF(.NOT.GKEEP) GO TO 575
921 CALL GWALL(INDVAR,1,NX,40,40,IZED,SOUTH,O.,O.,O.,O.,-1.)
922 CALL ADD(INDVAR,1,NX,40,40,CELL,CM,VM,CVAR,VVAR,NY,NX)
923
924 C
925 C
926 C
927 C *** ACCOUNT FOR MOMENTUM LOSSES AT EXIT(S) ***
928
929 C *** EXIT NEAR BLADE ROOTS (O.D. OF AFT-PLATFORM SEAL)
930 IF(.NOT.(IZED.EQ.17)) GO TO 582
931 JIY = NY
932 CALL GET(AHIGH,GAHIGH,NY,NX)
933 CALL GET(DYV,GDVV,NY)
934 CALL GET(W1,GW1,NY,NX)
935
936 C ** USE A LOSS COEFFICIENT (GLOSK1) TO COMPUTE THE PRESSURE
937 C LOSS ACROSS THE EXIT AT THE O.D. OF THE AFT-PLATFORM SEAL
938 C MASSFLOW = CM (EXIT PRESS - CELL PRESS)
939 C CM = 2 * (EXIT AREA)/(GLOSK1*EXIT VELOCITY)
940 C NOTE: SUB. FOR VELOCITY, VELOCITY =
941 C W1(FULL CELL AXIAL VELOCITY)*(CELL HEIGHT/GAP SIZE)
942 C SUB. FOR EXIT AREA, EXIT AREA =
943 C GAHIGH(FULL CELL AREA)*(GAP SIZE/CELL HEIGHT)
944
945 C DO 580 JIX = 1,NX
946 C PREVENT LARGE CM BY LIMITING SMALLEST W1 (=0.1*NOMINAL EXIT W1)
947 C ABSGW1=AMAX1(W1XITM,ABS(GW1(JIY,JIX)))
948 C (CALCULATE THE LOSS COEFFICIENT CM)
949 C CM(JIY,JIX)=(2.0*GAHIGH(JIY,JIX))/(GLOSK1*ABSGW1+GTINY))
950 C * (GGEXIT(JIX)/GDVV(JIY))**2.
951 C PREVENT CM FROM BEHAVING ERRATICALLY IN FIRST FEW (5) SWEEPS
952 C NB. THE .0025 IS A 'LARGE' VALUE SUFFICIENT TO FIX P=PEXIT
953 C IF (ISWP.LE.5) CM(JIY,JIX)=0.0025*GAHIGH(JIY,JIX)
954 C GIVE SAVED CM A FINITE VALUE AT SWEEP 1
955 C IF (ISWP.LE.1) CM1S(JIX)=CM(JIY,JIX)
956 C UNDER-RELAX CM TO PREVENT INSTABILITY
957 C CM(JIY,JIX)=CMRLX1*CM(JIY,JIX)+(1.-CMRLX1)*CM1S(JIX)
958 C SAVE CM VALUE FOR RELAXATION
959 C CM1S(JIX)=CM(JIY,JIX)
960 C (ASSIGN VM THE CIRCUMFERENTIAL EXIT PRESSURES)

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960 VM(JIY,JIX)=GPEXIT(JIX)
961
962 C ** SET THE VALUES OF U1,V1,W1,H1,KE,AND EP AT THE O.D. OF
963 C THE AFT-PLATFORM SEAL IN CASE OF INFLOW.
964 C ** CM & VM HAVE BEEN SET ABOVE FOR PRESCRIBED MASS FLOW
965 C CVAR IS SET TO ZERO FOR ZERO DIFFUSION FLUX
966 C CVAR(JIY,JIX) = 0.0
967 C SET VVAR TO EXTERNAL VALUE APPROPRIATE FOR THE VARIABLE
968 C VVAR(JIY,JIX) = 0.0
969 IF (INDVAR.EQ.H1) VVAR(JIY,JIX) = GHEXIT
970 IF (INDVAR.EQ.C1) VVAR(JIY,JIX) = H2EXIT
971 IF (INDVAR.EQ.KE) VVAR(JIY,JIX) = GVALKE
972 IF (INDVAR.EQ.EP) VVAR(JIY,JIX) = GVALEP
973 C ** NOTE: THE VALUES OF CVAR AND VVAR NEED NOT BE DEFINED FOR M1
974 C AS THEY DO FOR OTHER VARIABLES (REF. CHAM TR/75 SEC.4.2-9)
975 580 CONTINUE
976 C **** ADD SOURCE TERM ****
977 CALL ADD(INDVAR,1,NX,JIY,CELL,CM,VM,CVAR,VVAR,NY,NX)
978
979 C SUM THE MASSFLOW OUT EXIT1
980 IF(.NOT.(ISWP.EQ.LSWEEP.AND.INDVAR.EQ.W1)) GO TO 582
981 EMOUT1=0.0
982 DO 581 JIX=1,NX
983 EMOUT1=EMOUT1-GD1(JIY,JIX)+GW1(JIY,JIX)*GAHIGH(JIY,JIX)*G
984 581 CONTINUE
985 IF(NX.EQ.1) EMOUT1=EMOUT1+2.*GP1/XULAST
986
987 C
988 C **** SECOND EXIT ***
989 582 IF(.NOT.(JIXE2F.GE.1.AND.JIXE2F.LE.NX)) GO TO 587
990 IF(IZED.NE.1) GO TO 587
991 JIY=10
992 CALL GET(AHIGH,GAHIGH,NY,NX)
993 CALL GET(W1,GW1,NY,NX)
994
995 C SUM UP THE TOTAL HIGH FACE AREA BEING CONSIDERED
996 GAHSUM = 0.0
997 DO 583 JIX =JIXE2F,JIXE2L
998 583 GAHSUM= GAHSUM + GAHIGH(JIY,JIX)
999
1000 C USE A LOSS COEFFICIENT (GLOSK2) TO COMPUTE THE PRESSURE
1001 C LOSS ACROSS THE EXIT
1002 C MASSFLOW = CM (EXIT PRESS - CELL PRESS)
1003 C CM = 2 * (EXIT AREA)/(GLOSK2*EXIT VELOCITY)
1004 C NOTE:SUBSTITUTE VEL. = W1 (FULL CELL AXIAL VELOCITY)
1005 C * (FULL CELL AREA/EXIT AREA)
1006
1007 DO 584 JIX =JIXE2F,JIXE2L
1008 (CALCULATE THE LOSS COEFFICIENT CM)
1009 (FIRST NEED TO CALCULATE EXIT AREA PER CELL (GAREAC))
1010 GAREAC= (GAXIT2/144.0)*(GAHIGH(JIY,JIX)/GAHSUM)
1011 C PREVENT LARGE CM BY LIMITING SMALLEST W1 (=0.1*NOMINAL EXIT W1+
1012 ABSGW1=AMAX1(W1XITM*GAREAC/GAHIGH(JIY,JIX),ABS(GW1(JIY,JIX)))
1013 CM(JIY,JIX)=(2.0*GAREAC/(GLOSK2*ABSGW1+GTINY))
1014 * (GAREAC/(GAHIGH(JIY,JIX)))
1015
1016 C PREVENT CM FROM BEHAVING ERRATICALLY IN FIRST FEW (5) SWEEPS
1017 C NB. THE .02 IS A 'LARGE' VALUE SUFFICIENT TO FIX P=PEXIT
1018 IF(ISWP.LE.5) CM(JIY,JIX)=0.02*GAHIGH(JIY,JIX)
1019 C GIVE SAVED CM A FINITE VALUE AT SWEEP 1
1020 IF(ISWP.LE.1) CM2S(JIX)=CM(JIY,JIX)

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1020 C UNDER-RELAX CM TO PREVENT INSTABILITY
1021 CM(JIY,JIX)=CMRLX2*CM(JIY,JIX)+(1.-CMRLX2)*CM2S(JIX)
1022 C SAVE CM VALUE FOR RELAXATION
1023 CM2S(JIX)=CM(JIY,JIX)
1024 C (ASSIGN VM THE SPECIFIED EXIT PRESSURE (SAME AS EXIT 1))
1025 VM(JIY,JIX)=GPEXIT(JIX)
1026
1027 C ** SET THE VALUES OF U1,V1,W1,H1,KE,AND EP AT THE EXIT
1028 C IN CASE OF INFLOW.
1029 C ** CM & VM HAVE BEEN SET ABOVE FOR PRESCRIBED MASS FLOW
1030 C CVAR IS SET TO ZERO FOR ZERO DIFFUSION FLUX
1031 CVAR(JIY,JIX) = 0.0
1032 C SET VVAR TO EXTERNAL VALUE APPROPRIATE FOR THE VARIABLE
1033 C OUT OF LAZINESS AND FOR WANT OF ANYTHING BETTER. THE
1034 C VALUES BELOW ARE THE SAME AS FOR EXIT 1
1035 VVAR(JIY,JIX) = 0.0
1036 IF (INDVAR.EQ.H1) VVAR(JIY,JIX) = GHEXIT
1037 IF (INDVAR.EQ.C1) VVAR(JIY,JIX) = H2OXIT
1038 IF (INDVAR.EQ.KE) VVAR(JIY,JIX) = GVALKE
1039 IF (INDVAR.EQ.EP) VVAR(JIY,JIX) = GVALEP
1040
1041 584 CONTINUE
1042 C **** ADD SOURCE TERM ****
1043 CALL ADD(INDVAR,JIXE2F,JIXE2L,JIY,CELL,CM,VM,CVAR,VVAR,NY,NX)
1044
1045 C SUM THE MASSFLOW OUT EXIT2
1046 IF (.NOT.(ISWP.EQ.LSWEEP.AND.INDVAR.EQ.W1)) GO TO 587
1047 EMOUT2=0.0
1048 DO 585 JIX=JIXE2F,JIXE2L
1049 EMOUT2=EMOUT2-GD1(JIY,JIX)*GW1(JIY,JIX)*GAHIGH(JIY,JIX)*G
1050
1051 585 CONTINUE
1052 IF (NX.EQ.1) EMOUT2=EMOUT2+2.*GPI/XULAST
1053
1054 C **** RESET CM AND VM SO THAT THEY DON'T INTERFERE WITH 'Gwall'
1055 587 DO 590 JIX=1,NX
1056 DO 590 JIY=1,NY
1057 CM(JIY,JIX)=0.0
1058 VM(JIY,JIX)=0.0
1059
1060 590 CONTINUE
1061
1062 C *** CALCULATE TOTAL PRESSURES
1063 IF (INDVAR.NE.C1) GO TO 599
1064 DO 595 JIX=1,NX
1065 DO 595 JIY=1,NY
1066 UVEL=GU1(JIY,JIX)/GR(JIY)
1067 VVEL=GV1(JIY,JIX)
1068 WVEL=GW1(JIY,JIX)
1069 IF (JIY.GT.1) VVEL=0.5*(VVEL+GV1(JIY-1,JIX))
1070 WVEL=GW1(JIY,JIX)
1071 IF ((IZED.EQ.17.AND.JIY.EQ.40).OR.(IZED.EQ.13.AND.JIY.EQ.1))
1072 GO TO 594
1073 IF (IZED.GT.1) WVEL=0.5*(WVEL+GW1(JIY,JIX))
1074 VELSQ=UVEL*UVEL+VVEL*VVEL+WVEL*WVEL
1075 GPT(JIY,JIX)=GPT(JIY,JIX)+0.5*GD1(JIY,JIX)*VELSQ
1076
1077 C ***
1078 599 RETURN
1079

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1080 C CHAPTER 6: CALLED AT THE END OF EACH VARIABLE-RECALCULATION
1081 C CYCLE COMMENCED AT CHAPTER 4. ITNO = ITERATION NUMBER.
1082 C -----
1083 C 600 CONTINUE
1084 C RETURN
1085 C -----
1086 C CHAPTER 7: CALLED AT END OF EACH SLAB-WISE CALCULATION.
1087 C -----
1088 C 700 CONTINUE
1089 C ***
1090 C PASS CALCULATED AUXILIARY VARIABLES BACK TO EARTH
1091 C CALL SET(JMU1,1,NX,1,NY,GMU1,NY,NX)
1092 C CALL SET(JPT,1,NX,1,NY,GPT,NY,NX)
1093 C IF(.NOT.(IRHO1.EQ.-1)) RETURN
1094 C CALL SET(JT1M,1,NX,1,NY,GT1M,NY,NX)
1095 C CALL SET(JRH20,1,NX,1,NY,GRH20,NY,NX)
1096 C CALL SET(JRH2,1,NX,1,NY,GRH2,NY,NX)
1097 C ***
1098 C .....AUTOPLOT FILE
1099 C IF(MOD(ISWP,NPRMON).EQ.0.AND.IZED.EQ.IZMON) THEN
1100 C JSTP=ISTP
1101 C JSWP=ISWP
1102 C CALL AUTMON(JSTP,JSWP)
1103 C ENDIF
1104 C -----
1105 C RETURN
1106 C -----
1107 C CHAPTER 8: CALLED AT THE END OF EACH SWEEP
1108 C NOT ACCESSED IF PARABOLIC.
1109 C -----
1110 C 800 CONTINUE
1111 C RETURN
1112 C -----
1113 C CHAPTER 9: CALLED AT THE END OF EACH TIME STEP
1114 C NOT ACCESSED IF PARABOLIC.
1115 C -----
1116 C 900 CONTINUE
1117 C ***
1118 C WRITE(6,991) EMOUT1,EMOUT2
1119 C 991 FORMAT(/////1X,1PE12.3,2X,72HCALCULATED (TOTAL) MASS OUTFLOW RATE
1120 C .AT EXIT NEAR BLADE ROOTS (LBM/SEC).//.
1121 C .//1X,E12.3,2X,62HCALCULATED (TOTAL) MASS OUTFLOW RATE AT SECOND EXI
1122 C .T (LBM/SEC)./////
1123 C ***
1124 C RETURN
1125 C -----
1126 C CHAPTER 10: SET PHASE 1 DENSITY HERE WHEN IRHO1=-1 IN DATA.
1127 C SET CURRENT-Z 'SLAB' DENSITY, D1, IF MSLAB=.T..
1128 C EG. IF(MSLAB) CALL SET(D1,1,NX,1,NY,GD1,NY,NX).
1129 C SET NEXT LARGER-Z 'SLAB' DENSITY, D1H, IF HSLAB=.T. & PARAB=F
1130 C EG. IF(HSLAB) CALL SET(D1H,1,NX,1,NY,GD1H,NY,NX).
1131 C SET D(LN(D1))/DP (IE. D1DP) FOR UNSTEADY FLOW.
1132 C EG. IF(MSLAB) CALL SET(D1DP,1,NX,1,NY,GD1DP,NY,NX).
1133 C -----
1134 C 1000 CONTINUE
1135 C ***
1136 C CALCULATE TEMP, DENSITY AND VISCOSITY OF HYDROGEN/WATER MIXTURE
1137 C IF(MSLAB) GO TO 1001
1138 C JH1=H1H
1139 C JC1=C1H

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1140 JD1=D1H
1141 JT1=T1H
1142 GO TO 1002
1143
1144 1001 JH1=H1
1145 JC1=C1
1146 JD1=D1
1147 JT1=T1
1148
1149 C
1150 1002 CALL GET(JH1,GH1,NY,NX)
1151 CALL GET(JT1,GT1,NY,NX)
1152 CALL GET(JC1,GC1,NY,NX)
1153
1154 C DEDUCE TEMPERATURE OF MIXTURE FROM CALCULATED MIXTURE ENTHALPY
1155 CALL GTEMP(GH1,GC1,GT1,NY,NX,MSLAB)
1156
1157 C CALCULATE DENSITIES FROM DEDUCED MIXTURE TEMPERATURE
1158 CALL GRHO(GT1,GC1,GD1,GRH2O,GRH2,NY,NX,MSLAB)
1159
1160 C PASS CALCULATED MIXTURE DENSITY BACK TO EARTH
1161 CALL SET(JD1,1,NX,1,NY,GD1,NY,NX)
1162
1163 C IF(.NOT.MSLAB) RETURN
1164
1165 C CALCULATE THE LAMINAR VISCOSITY OF THE MIXTURE ("SET" IN CH. 12)
1166 CALL GVISC(GT1,GC1,GMU1L,NY,NX)
1167
1168 C SAVE MSLAB TEMPERATURES
1169 DO 1010 IX=1,NX
1170 DO 1010 IY=1,NY
1171 1010 GT1M(IY,IX)=GT1(IY,IX)
1172 C ***
1173 RETURN
1174
1175 C CHAPTER 11: SET PHASE 2 DENSITY HERE WHEN IRHO2=-1 IN DATA.
1176 C SET CURRENT-Z 'SLAB' DENSITY, D2, IF MSLAB=.T.,
1177 C EG. IF(MSLAB) CALL SET(D2,1,NX,1,NY,GD2,NY,NX).
1178 C SET NEXT LARGER-Z 'SLAB' DENSITY, D2H, IF HSLAB=.T. & PARAB=F
1179 C EG. IF(HSLAB) CALL SET(D2H,1,NX,1,NY,GD2H,NY,NX).
1180 C SET D(LN(D2))/DP FOR UNSTEADY FLOW.
1181 C EG. IF(MSLAB) CALL SET(D2DP,1,NX,1,NY,GD2DP,NY,NX).
1182
1183 1100 CONTINUE
1184 RETURN
1185
1186 C CHAPTER 12: SET PHASE 1 VISCOSITY HERE WHEN IEMU1=-1 IN DATA.
1187 C SET CURRENT-Z 'SLAB' VISCOSITY (MU1), IF MSLAB=.T.,
1188 C EG. IF(MSLAB) CALL SET(MU1,1,NX,1,NY,GVISC,NY,NX).
1189 C SET NEXT LARGER-Z 'SLAB' VISC. (MU1H), IF HSLAB=.T. & PARAB=F
1190 C EG. IF(HSLAB) CALL SET(MU1H,1,NX,1,NY,GVSCHE,NY,NX).
1191
1192 C CHAPTER ALSO ACCESSED WHEN EMULAM=-1.0 IN DATA, SO THAT THE
1193 C LAMINAR VISCOSITY WHICH APPEARS IN WALL FUNCTIONS & IN THE
1194 C KE-EP TURBULENCE MODEL (IEMU1=2) MAY BE SET NON-CONSTANT.
1195 C SET CURRENT-Z 'SLAB' VALUE (MU1LAM) WHEN LAMMU=.T.,
1196 C EG. IF(LAMMU) CALL SET(MU1LAM,1,NX,1,NY,GVSCL,NY,NX).
1197
1198 1200 CONTINUE
1199
1200 C ***
1201 C PASS CALCULATED MIXTURE VISCOSITY BACK TO EARTH
1202 IF(LAMMU) CALL SET(MU1LAM,1,NX,1,NY,GMU1L,NY,NX)

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C *** RETURN
C
C CHAPTER 13: SET EXCHANGE COEFFICIENT (E.C.) FOR VARIABLE
C INDVAR WHEN SIGMA(INDVAR)=-1.0 IN DATA.
C SET CURRENT-Z 'SLAB' E.C. (EXCO) IF MSLAB=T..
C EG. IF(MSLAB) CALL SET(EXCO,1,NX,1,NY,GEXCO,NY,NX).
C SET NEXT SMALLER-Z 'SLAB' E.C. (EXCOL) IF LSLAB=T..
C EG. IF(LSLAB) CALL SET(EXCOL,1,NX,1,NY,GEXCOL,NY,NX).
C SET NEXT LARGER-Z 'SLAB' E.C. (EXCOH) IF HSLAB=T..
C EG. IF(HSLAB) CALL SET(EXCOH,1,NX,1,NY,GEXCOH,NY,NX).
C NOTE: FOR MSLAB, INDVAR=U1...C4 FOR LSLAB, INDVAR=U1L...C4L
C & FOR HSLAB, INDVAR=U1H...C4H. IF PARAB=T. SET MSLAB ONLY.
C
C 1300 CONTINUE
C RETURN
C
C CHAPTER 14: SET INTER-PHASE FRICTION COEFFICIENT (CFP) HERE
C WHEN ICFIP = -1 IN DATA ITS UNITS = FORCE / (CELL * RELATIVE
C SPEED OF PHASES).
C
C 1400 CONTINUE
C RETURN
C
C CHAPTER 15: SET INTER-PHASE MASS-TRANSFER RATE PER CELL (MDT)
C HERE WHEN IMDOT = -1 IN DATA.
C
C 1500 CONTINUE
C RETURN
C
C CHAPTER 16: SET HERE PHASE 1 & 2 SATURATION ENTHALPIES
C ( HST1 & HST2) WHEN IHSAT = -1 IN DATA.
C
C 1600 CONTINUE
C RETURN
C END
C SUBROUTINE GTEMP(GH1,GC1,GT1,NY,NX,MSLAB)
C
C PURPOSE: - TO DETERMINE THE TEMPERATURE OF THE HYDROGEN/WATER MIXTURE
C FROM THE CALCULATED MIXTURE ENTHALPY
C
C CURVE FITS OF THE ANALYTICAL FORM: -
C HH2=CH2+BH2*T+AH2*T**2
C HH20=CH20+BH20*T+AH20*T**2
C
C REFERENCES: -
C H2:
C H20:
C
C RANGES OF VALIDITY: -
C H2: T=170 TO 2000 DEG R
C H20: T=490 TO 2060 DEG R (BUT EXTRAPOLATION BELOW THIS O.K.)
C
C UNITS: -
C H IN BTU/LBM AND T IN DEG R
C H'S CONVERTED TO FT-LBF/SLUG BEFORE RETURN TO GROUND
C
C DIMENSION GH1(NY,NX),GC1(NY,NX),GT1(NY,NX),CH20(6),BH20(6),
C AH20(6),CH2(2),BH2(2),AH2(2)

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1260 LOGICAL MSLAB
1261 -----
1262 C
1263 C HYDROGEN ENTHALPY CURVE FIT DATA
1264 DATA CH2/-357.6903,-45.88906/
1265 DATA BH2/4.468995,3.557702/
1266 DATA AH2/-5.92706E-4,-7.15694E-6/
1267 C WATER ENTHALPY CURVE FIT DATA
1268 DATA CH2O
1269 ./-424.5938,2289.552,-7363.69,599.5881,-307.5449,-96.3053/
1270 DATA BH2O
1271 . /0.82414,-4.577089,6.913,-1.27177,1.190721,1.285063/
1272 DATA AH2O
1273 . /1.3067E-4,2.815249E-3,0.0,1.369267E-3,0.0,-1.75707E-4/
1274 C
1275 C UNIT CONVERSION FACTOR
1276 DATA CONVH/25036.52/
1277 C CONVH = CONVERSION FACTOR FROM BTU/LBM TO FT.LBF/SLUG = 778.16*G
1278 C
1279 DATA TINY/1.E-10/
1280 -----
1281 C
1282 DO 50 IX=1,NX
1283 DO 50 IY=1,NY
1284 ENTH=GH1(IY,IX)/CONVH
1285 IF (ENTH.LE.TINY) GO TO 35
1286 TEMP=GT1(IY,IX)
1287 XH2O=GC1(IY,IX)
1288 C
1289 C DETERMINE WHICH OF THE SIX WATER ENTHALPY/TEMP CURVE FITS TO USE
1290 IF (TEMP.GE.10..AND.TEMP.LT.975.) GO TO 12
1291 IF (TEMP.GE.975..AND.TEMP.LT.1184.6) GO TO 13
1292 IF (TEMP.GE.1184.6.AND.TEMP.LT.1223.3) GO TO 14
1293 IF (TEMP.GE.1223.3.AND.TEMP.LT.1281.4) GO TO 15
1294 IF (TEMP.GE.1281.4.AND.TEMP.LT.1400.) GO TO 16
1295 IF (TEMP.GE.1400..AND.TEMP.LT.2000.) GO TO 161
1296 GO TO 90
1297 12 IHW=1
1298 GO TO 17
1299 13 IHW=2
1300 GO TO 17
1301 14 IHW=3
1302 GO TO 17
1303 15 IHW=4
1304 GO TO 17
1305 16 IHW=5
1306 GO TO 17
1307 161 IHW=6
1308 C
1309 C DETERMINE WHICH OF THE TWO HYDROGEN ENTHALPY/TEMP CURVE FITS TO USE
1310 17 IF (TEMP.GE.10..AND.TEMP.LT.508.) GO TO 18
1311 IF (TEMP.GE.508..AND.TEMP.LT.2000.) GO TO 19
1312 18 IHH=1
1313 GO TO 20
1314 19 IHH=2
1315 C
1316 C SOLVE QUADRATIC IN T TO DETERMINE LOCAL MIXTURE TEMPERATURE (DEG R)
1317 20 CC=CH2(IHH)*(1.-XH2O)+XH2O*CH2O(IHW)-ENTH
1318 BB=BH2(IHH)*(1.-XH2O)+XH2O*BH2O(IHW)
1319 AA=AH2(IHH)*(1.-XH2O)+XH2O*AH2O(IHW)

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1320 C
1321 IF (ABS(AA).LE.TINY) GO TO 28
1322 ROOT=SQRT(BB*BB-4.*AA*CC)
1323 T1=(-BB+ROOT)/(2.*AA)
1324 T2=(-BB-ROOT)/(2.*AA)
1325 IF (AA.LT.O.) GO TO 27
1326 C AA POSITIVE
1327 TEMP=AMAX1(T1,T2)
1328 GO TO 40
1329 C AA NEGATIVE
1330 27 TEMP=AMIN1(T1,T2)
1331 GO TO 40
1332 C AA ZERO
1333 28 TEMP=-CC/BB
1334 GO TO 40
1335
1336 C SET TEMP TO ZERO IN FULLY BLOCKED CELLS
1337 35 TEMP=O.O
1338 C
1339 40 GT1(IY,IX)=TEMP
1340 C
1341 50 CONTINUE
1342 C
1343 RETURN
1344 C----- DE-BUG -----
1345 90 WRITE(6,91)
1346 WRITE(6,92) IY,IX,TEMP,ENTH,MSLAB
1347 FORMAT(///IX,2I4,1P2E12.3,1I1)
1348 91 FORMAT(///IX,8H*** TEMPERATURE OUT OF RANGE OF CURVE FITS IN SUBR
1349 OUTLINE GTEMP, EXECUTION TERMINATED ***)
1350 STOP
1351 END
1352 SUBROUTINE GRHO(GT1,GC1,GD1,GRH2O,GRH2,NY,NX,MSLAB)
1353 C-----
1354 C PURPOSE:- TO CALCULATE THE DENSITIES OF THE MIXTURE, HYDROGEN AND
1355 C WATER AT THE MIXTURE TEMPERATURE DERIVED FROM THE
1356 C CALCULATED MIXTURE ENTHALPY (IN SUBROUTINE GTEMP)
1357 C-----
1358 C
1359 C CURVE FITS OF THE ANALYTICAL FORM:-
1360 C RH2=EXP(CH2*BH2+LN(TEMP)+AH2+LN(TEMP)**2)
1361 C RH2O=EH2O+EH2O*T+DH2O*T**2+CH2O*T**3+BH2O*T**4+AH2O*T**5
1362 C
1363 C REFERENCES:-
1364 C H2:
1365 C H2O:
1366 C
1367 C RANGES OF VALIDITY:-
1368 C H2: T=170 TO 2000 DEG R (BUT EXTRAPOLATION DOWN TO 150 O.K.)
1369 C H2O: T=490 TO 2060 DEG R
1370 C (NB. H2O AT T BELOW 490 GIVEN DENSITY OF H2O AT FREEZING)
1371 C
1372 C UNITS:-
1373 C RHO IN LBM/FT**3 AND T IN DEG R
1374 C RHO'S CONVERTED TO SLUG/CU FT BEFORE RETURNING TO GROUND
1375 C-----
1376 C DIMENSION GT1(NY,NX),GRH2O(NY,NX),GRH2(NY,NX),GC1(NY,NX),
1377 C GD1(NY,NX),FH2O(4),EH2O(4),DH2O(4),CH2O(4),BH2O(4),AH2O(4)
1378 C LOGICAL MSLAB
1379 C-----

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1380 C
1381 C HYDROGEN DENSITY CURVE FIT DATA
1382 DATA CH2,BH2,AH2/4.579578,-0.5199177,-2.86885E-2/
1383 C WATER DENSITY CURVE FITS DATA
1384 DATA FH20/-82.117,-2177.783,119.1372,30.17724/
1385 DATA EH20/0.62353,7.12733,-4.770357E-2,-2.573409E-2/
1386 DATA DH20/-6.77963E-4,-4.54395E-3,-1.00694E-4,6.195714E-6/
1387 DATA CH20/-3.41207E-7,-1.91391E-6,5.516186E-8,0.0/
1388 DATA BH20/9.23406E-10,1.686E-9,0.0,0.0/
1389 DATA AH20/-3.9688E-13,0.0,0.0,0.0/
1390 C
1391 C UNIT CONVERSION FACTOR
1392 DATA CONVR/32.174/
1393 C CONVR = G = 32.174, TO CONVERT LBM/FT**3 TO SLUG/FT**3
1394 C
1395 DATA RH20F/62.578/
1396 C RH20F = WATER DENSITY AT FREEZING (APPROX 490 DEG R), IN LBM/FT**3
1397 DATA TINY/1.E-10/
1398 C
1399 C
1400 DO 20 IX=1,NX
1401 DO 20 IY=1,NY
1402 TEMP=GT1(IY,IX)
1403 CONC=GC1(IY,IX)
1404 IF(TEMP.LE.TINY) GO TO 18
1405 TEMPLN=ALOG(TEMP)
1406 C
1407 C DETERMINE WHICH OF THE 4 WATER DENSITY/TEMPERATURE CURVE FITS TO USE
1408 IF(TEMP.GE.10..AND.TEMP.LT.1180.) GO TO 12
1409 IF(TEMP.GE.1180..AND.TEMP.LT.1250.) GO TO 13
1410 IF(TEMP.GE.1250..AND.TEMP.LT.1380.) GO TO 14
1411 IF(TEMP.GE.1380..AND.TEMP.LT.2000.) GO TO 141
1412 GO TO 50
1413 IT=1
1414 GO TO 15
1415 IT=2
1416 GO TO 15
1417 IT=3
1418 GO TO 15
1419 IT=4
1420 C
1421 15 IF(TEMP.LE.490.) GO TO 16
1422 C DENSITY OF WATER (IN SLUG/FT**3)
1423 RH20=(FH20(IT)+EH20(IT)+TEMP+DH20(IT)+TEMP**2
1424 +CH20(IT)+TEMP**3+BH20(IT)+TEMP**4+AH20(IT)+TEMP**5)/CONVR
1425 GO TO 17
1426 C TRAP WATER DENSITY TO ITS VALUE AT FREEZING FOR TEMPS BELOW FREEZING
1427 16 RH20=RH20F/CONVR
1428 C
1429 C DENSITY OF HYDROGEN (IN SLUG/FT**3)
1430 RH2=(EXP(CH2+BH2*TEMPLN+AH2*TEMPLN**2))/CONVR
1431 GO TO 19
1432 C
1433 C SET DENSITIES TO TINY IN FULLY BLOCKED CELLS
1434 18 RH2=TINY
1435 RH2=TINY
1436 C
1437 C CALCULATE THE MIXTURE DENSITY
1438 19 GD1(IY,IX)=1./((CONC/RH20*(1.-CONC)/RH2)
1439 C

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1440 IF(.NOT.MSLAB) GO TO 20
1441 C SAVE MSLAB DENSITIES FOR PRINTOUT FROM EARTH
1442 GRH2D(IY,IX)=RH2O
1443 GRH2(IY,IX)=RH2
1444 C
1445 20 CONTINUE
1446 C
1447 RETURN
1448 C----- DE-BUG -----
1449 50 WRITE(6,51)
1450 WRITE(6,52) IY,IX,TEMP,CONC,MSLAB
1451 FORMAT(///IX,87H** TEMPERATURE OUT OF RANGE OF CURVE FITS IN SUBR
1452 OUTLINE GRHO, EXECUTION TERMINATED ***)
1453 52 FORMAT(///IX,214,1P2E12.3,1L1)
1454 STOP
1455 END
1456 SUBROUTINE GVISC(GT1,GC1,GMU1L,NY,NX)
1457 C
1458 C PURPOSE:- TO CALCULATE THE LAMINAR VISCOSITY OF THE MIXTURE
1459 C-----
1460 C
1461 C CURVE FITS OF THE ANALYTICAL FORM:-
1462 C EMU42=DH2+CH2+TEMP+BH2+TEMP**2+AH2+TEMP**3
1463 C EMU420=EXP(FH20+EH20+TEMP+DH20+TEMP**2+CH20+TEMP**3+BH20+TEMP**4
1464 C +AH20+TEMP**5)
1465 C
1466 C REFERENCES:-
1467 C H2:
1468 C H20:
1469 C
1470 C RANGES OF VALIDITY:-
1471 C H2: T=170 TO 2000 DEG R (BUT EXTRAPOLATION DOWN TO 150 O.K.)
1472 C H20: T=490 TO 1752 DEG R
1473 C (NB. H20 AT T BELOW 490 GIVEN VISCOSITY OF H20 AT FREEZING)
1474 C
1475 C UNITS:-
1476 C EMU IN LBM/FT.SEC AND T IN DEG R
1477 C EMU'S CONVERTED TO SLUG/FT.SEC BEFORE RETURNING TO GROUND
1478 C-----
1479 C DIMENSION GT1(NY,NX),GC1(NY,NX),GMU1L(NY,NX)
1480 C-----
1481 C
1482 C HYDROGEN VISCOSITY CURVE FIT DATA
1483 DATA DH2,CH2,BH2,AH2/O.4989,-5.4575E-5,5.1824E-7,-1.4948E-10/
1484 C WATER VISCOSITY CURVE FIT DATA
1485 DATA FH20,EH20,DH20,CH20,BH20,AH20/20.5532,-6.52199E-2,
1486 .3.2726E-5,6.6687E-8,-8.3627E-11,2.6237E-14/
1487 DATA FH20A,EH20A/6.5334525E-3,1.11E-5/
1488 C
1489 C UNIT CONVERSION FACTOR
1490 DATA CONVM/32.174/
1491 C CONVM = G = 32.174, TO CONVERT LBM TO SLUG
1492 DATA EMULWF/1.2446E-3/
1493 C EMULWF=LAM VISCOSITY OF WATER AT FREEZING (490 DEG R)
1494 C-----
1495 DO 20 IX=1,NX
1496 DO 20 IY=1,NY
1497 TEMP=GT1(IY,IX)
1498 CONC=GC1(IY,IX)
1499

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IN LBM/FT.SEC

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1500 C
1501 C VISCOSITY OF HYDROGEN (IN LBM/FT.SEC)
1502 EMUH2=(DH2+CH2*TEMP+BH2*TEMP**2+AH2*TEMP**3)*1.E-5
1503 C
1504 IF(TEMP.LE.490.) GO TO 17
1505 IF(TEMP.GE.1392.) GO TO 16
1506 C VISCOSITY OF WATER (IN LBM/FT.SEC)
1507 EMUH20=EXP(FH20+EH20*TEMP+DH20*TEMP**2+CH20*TEMP**3+BH20*TEMP**4
1508 +AH20*TEMP**5)*1.E-3
1509 GO TO 18
1510 16 EMUH20=FH20A+EH20A*TEMP
1511 GO TO 18
1512 C
1513 C TRAP WATER VISCOSITY TO ITS VALUE AT FREEZING FOR TEMPS BELOW FREEZING
1514 17 EMUH20=EMULWF
1515 C
1516 C CALCULATE THE MIXTURE VISCOSITY (IN SLUGS/FT.SEC)
1517 18 GMU1L(IV,IX)=1./(CONC/EMUH20+(1.-CONC)/EMUH2)/CONVM
1518 C
1519 20 CONTINUE
1520 C
1521 RETURN
1522 END
1523 C--- OCTOBER, 1984, CHAM (NA) GROUND SUBPROGRAM "GWALL", TO FACILITATE
1524 C THE SETTING OF AN UNLIMITED NUMBER OF WALL SURFACES IN THE SPRING
1525 C 1983 VERSION OF PHOENICS.
1526 C
1527 SUBROUTINE GWALL(JVAR,JIXF,JIXL,JIFY,JIVL,JIZ,GWTYPE,
1528 GWALL,GWALL,GWALL,GWALL,GDELTA)
1529 C-----
1530 $INCLUDE 9,CMNGUSSI.FTN/G (NLIST)
1531 $INCLUDE 9,GUSSEQUI.FTN/G (NLIST)
1532 C-----
1533 C
1534 C PURPOSE:- TO COMPUTE CVAR (=GCVAR) AND VVAR (=GVVAR) FOR TURBULENT
1535 C AND LAMINAR WALL FUNCTIONS
1536 C
1537 C-----
1538 C ANY QUESTIONS (OR PROBLEMS) ON THE USE OF THIS SUBPROGRAM SHOULD BE
1539 C ADDRESSED TO:
1540 C L.W. KEETON, CHAM (NA) INC.,
1541 C 1525-A SPARKMAN DRIVE,
1542 C HUNTSVILLE, AL 35802, U.S.A.
1543 C TEL: (205) 830-2620
1544 C-----
1545 C RESTRICTIONS:-
1546 C 1. GWALL IS NOT VALID FOR 2-FLUID MODEL CALCULATIONS.
1547 C 2. PROVISION FOR A MOVING GRID HAS NOT YET BEEN INCLUDED.
1548 C-----
1549 C NOTES:-
1550 C 1. THIS GROUND SUBPROGRAM IS INTENDED TO FACILITATE THE SETTING OF
1551 C APPROPRIATE WALL BOUNDARY CONDITIONS VIA GROUND FOR THOSE CASES
1552 C WHEN THE 10 REGIONS OF THE SATELLITE ARE INSUFFICIENT. INSTEAD
1553 C OF USING A SPECIAL REGION TO SPECIFY THE PRESENCE OF A WALL THE
1554 C GROUND USER SUBPROGRAM GWALL CAN NOW BE USED INSTEAD. THE MODELS
1555 C EMPLOYED ARE IDENTICAL TO THOSE CURRENTLY INCORPORATED IN EARTH
1556 C SUBPROGRAM "WALL" (SEE NOTE 3 BELOW).
1557 C
1558 C 2. TO FACILITATE CROSS-CHECKING, WHERE FEASIBLE, ALL VARIABLE NAMES
1559 C AND CODING IN GWALL ARE SIMILAR TO THOSE USED IN EARTH SUBPROGRAM

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"WALL".

3. THE WALL BOUNDARY CONDITION TREATMENT USED HEREIN IS EXACTLY AS DESCRIBED IN THE SPRING 1983 PHOENICS USER'S MANUAL (CHAM TR/75), ON PAGES 3.2-47 TO 49. ITS MAIN FEATURES ARE OUTLINED BELOW.

4. THE QUANTITIES GCVAR (=GCOEFF) AND GVVAR (=GVALUE) COMPUTED IN GWALL ARE EQUIVALENT TO THE "COEFFICIENT" AND "VALUE" QUANTITIES (CP1R1, VP1R1 ETC.) DISCUSSED IN THE USER'S MANUAL ON PAGES 3.2-41 TO 49. THE GWALL ARRAYS GCVAR AND GVVAR ARE IDENTICALLY EQUIVALENT TO THE GROUND ARRAYS CVAR AND VVAR, RESPECTIVELY, AND MUST BE EQUIVALENCED TO EACH OTHER IN GROUND (SEE NOTES 5 AND 6 BELOW). SPECIFIC EXAMPLES OF THE USES OF CVAR AND VVAR IN GROUND ARE GIVEN IN SECTION 4 OF THE USER'S MANUAL ON PAGE 4.3-2.

5. TO USE GWALL, THE USER MUST PROVIDE, IN GROUND CH. 5
----- (FOR EACH SEPARATE REGION OF WALL, AT EACH IZ-SLAB):-----

- A. VIA SUBROUTINE ARGUMENTS: THE VARIABLE INDEX (E.G. U1,KE,...), JVAR THE FIRST AND LAST IX AND IY-CELL COORDINATES OF THE REGION OF CELLS CONTAINING (OR NEIGHBOURING) THE WALL, JIXF, JIXL, JIYF, JIYL THE CURRENT IZ-SLAB COORDINATE, JIZ THE WALL 'TYPE' (E.G. NORTH, SOUTH,...), GWTYPE THE 3 COMPONENTS OF WALL VELOCITY, GUWALL, GVVALL, GWWALL (SEE NOTE 8 BELOW) THE WALL ENTHALPY, GHWALL AND THE PERPENDICULAR DISTANCE FROM THE WALL, GDELTA (SEE NOTE 12 BELOW)
- B. VIA "CALL GET" STATEMENTS IN GROUND CH. 5: THE 3 COMPONENTS OF FLUID VELOCITIES, GU1, GV1, GW1 AND THE DENSITIES, GD1
- C. VIA "CALL GET10" STATEMENTS IN GROUND CH.5: THE CELL WIDTHS IN THE 3 COORDINATE DIRECTIONS, GD1U, GD1V, GD1W AND THE RADII AT EACH CELL GRID NODE, GR
- D. VIA LOCAL CALCULATION IN GROUND CH.5 (SEE NOTES 9 AND 10): THE CURRENT IZ-SLAB LAMINAR VISCOSITIES, GMU1L.

THE REQUIRED CVAR AND VVAR VALUES ARE THEN RETURNED TO GROUND FOR EACH VARIABLE, THROUGH COMMON/WALLG/, VIA THE GCVAR AND GVVAR ARRAYS (WHICH ARE EQUIVALENCED TO CVAR AND VVAR), RESPECTIVELY.

6. SUBROUTINE GWALL SHOULD BE CALLED, SEPARATELY, FOR EACH CONTINUOUS REGION OF CELLS AT THE CURRENT SLAB CONTAINING (OR NEIGHBOURING) A WALL. CONSEQUENTLY, THE QUANTITIES IN GROUP A ABOVE MUST BE PROVIDED ON A REGION-BY-REGION BASIS. THE VARIABLES IN GROUPS B, C AND D, HOWEVER, SHOULD BE OBTAINED ONCE ONLY FOR EACH IZ-SLAB VIA "CALL GET" OR "CALL GET10" STATEMENTS (SEE USER'S MANUAL, PAGE 4.2-26) OR LOCAL CALCULATION, RESPECTIVELY, AS DESCRIBED IN NOTE 5 ABOVE. THESE VARIABLES ARE STORED IN GROUND IN THE LOCAL ARRAY NAMES GIVEN AND ARE THEN PASSED TO SUBROUTINE GWALL VIA THE GROUND/WALL COMMON BLOCK "WALLG". THE NAMES AND SEQUENCE OF THE ELEVEN ARRAYS IN COMMON/WALLG/ MUST NOT BE ALTERED BY THE USER. FURTHERMORE, THEY MUST BE APPROPRIATELY AND CONSISTENTLY DIMENSIONED IN BOTH GROUND AND GWALL, VIZ: GU1, GV1, GW1, GD1, GMU1L, GCVAR, GVVAR(NY, NX) GDXU(NX)

ADDITION, THE GCVAR AND GVVAR ARRAYS MUST BE EQUIVALENCED IN GROUND TO CVAR AND VVAR, RESPECTIVELY, SO THAT THEIR VALUES AS CALCULATED IN GWALL CAN BE PASSED BACK TO GROUND (VIA COMMON/WALLG/) FOR USE IN THE CORRESPONDING CALLS TO "ADD".

GD1V, GR(NY) AND GD1W(NZ). IN

7. GROUND SUBPROGRAM GWALL MUST BE CALLED FOR EACH CELL OR REGION OF CELLS WHERE A SPECIAL WALL BOUNDARY TREATMENT IS REQUIRED. GWALL MUST BE CALLED SEPARATELY FOR EACH VARIABLE INFLUENCED BY

1620 C THE WALL, I.E. FOR U1,V1,W1,H1,KE AND EP AS NECESSARY, FOLLOWED BY
 1621 C A CALL TO ADD TO INCLUDE THE APPROPRIATE CVAR AND VVAR SOURCE
 1622 C MODIFICATION TO THE RELEVANT F.O. EQUATIONS. IT SHOULD BE STRESSED
 1623 C THAT EVERY CALL TO GWALL IN GROUND FOR ANY VARIABLE MUST BE
 1624 C FOLLOWED IMMEDIATELY BY A CORRESPONDING CALL TO ADD, I.E. WITH
 1625 C SAME VARIABLE INDEX, REGION OF CELLS AND CELL TYPE (UNLESS EITHER:
 1626 C A. AREAS CALCULATED LOCALLY - SEE NOTE 9 BELOW
 1627 C INDEX (JVAR) IS EITHER KE OR EP, IN WHICH CASE THE CALL TO ADD
 1628 C TYPE MUST ALWAYS BE "CELL" (DUE TO THEIR VALUES BEING FIXED)).
 1629 C NOTE ALSO THAT GWALL MUST BE CALLED SEPARATELY (AND REPEATEDLY)
 1630 C FOR EACH DIFFERENT WALL TYPE (E.G. NORTH,HIGH,...) THAT MIGHT
 1631 C OCCUR IN ANY CELL OR CELLS.
 1632 C
 1633 C 8. FOR POLAR COORDINATES (WHEN UR IS SOLVED-FOR RATHER THAN U) THE
 1634 C GWALL AND GU1 QUANTITIES ARE ASSUMED (IN GWALL) TO BE
 1635 C ANGULAR VELOCITY ($\Omega = U/R$) AND UR-AT-THE-CELL, RESPECTIVELY.
 1636 C THE GWALL (=OMEGA) IS THEN MULTIPLIED (WITHIN GWALL, WHENEVER
 1637 C $CARTES = F.$) BY THE LOCAL $RADIUS+2$ TO GIVE THE REQUIRED LOCAL
 1638 C UR-AT-THE-WALL VALUE. IF THIS IS NOT APPROPRIATE FOR ANY
 1639 C PARTICULAR PROBLEM THEN THE MULTIPLICATION BY $R+2$ SHOULD BE
 1640 C SUPPRESSED BY THE USER IN GWALL AND THE DESIRED GUWALL VALUE,
 1641 C RATHER THAN OMEGA, SHOULD THEN BE FED VIA THE GUWALL ARGUMENT.
 1642 C
 1643 C 9. GCVAR IS NOT MULTIPLIED BY THE APPROPRIATE AREAS OF CONTACT WITHIN
 1644 C GWALL. THIS MUST BE DONE BY THE USER WITHIN GROUND CH. 5 ITSELF,
 1645 C FOR EACH PARTICULAR VARIABLE, AS NECESSARY. AFTER CVAR
 1646 C HAS BEEN RETURNED FROM GWALL, THIS CAN BE DONE EITHER BY
 1647 C EXPLICITLY CALCULATING THE APPROPRIATE AREAS OR VIA THE "TYPE"
 1648 C SPECIFICATION IN THE CALL TO ADD. IF THE AREAS ARE CALCULATED
 1649 C LOCALLY (AND THEN MULTIPLIED TO CVAR) THEN THE CALL TO ADD "TYPE"
 1650 C SHOULD BE PER "CELL" FOR EVERY VARIABLE (AND REGION) SO TREATED.
 1651 C
 1652 C 10. THE LAMINAR VISCOSITIES AT EACH 12-SLAB WHERE GWALL IS TO BE CALLED
 1653 C MUST BE SET-UP AND STORED IN THE LOCAL ARRAY GMU1L, WITHIN GROUND
 1654 C CH.5 (SEE NOTE 5 ABOVE). THESE CAN BE SET EITHER: A. TO A CONSTANT
 1655 C VALUE EVERYWHERE (E.G. EMULAM) OR, B. DETERMINED LOCALLY (BASED
 1656 C ON LOCAL CONDITIONS) AS DESCRIBED IN NOTE 11 BELOW.
 1657 C
 1658 C 11. THE LAMINAR VISCOSITIES USED IN THE WALL FUNCTIONS WITHIN THE
 1659 C PHOENICS SUBPROGRAM WALL CAN BE SET TO A NON-CONSTANT VALUE BY
 1660 C SETTING EMULAM= -1. IN THE SATELLITE, AND INSERTING APPROPRIATE
 1661 C CODING IN GROUND CH.12, AS DESCRIBED ON PAGE 4.3-14 OF THE USER'S
 1662 C MANUAL. IF GWALL IS TO BE USED, HOWEVER, THE CODING FOR VARYING
 1663 C LAMINAR VISCOSITY (LOCAL ARRAY: GMU1L) MUST BE INCLUDED IN CH.5
 1664 C (AND NOT CH. 12). THIS IS BECAUSE THE CALL TO CH.12 ORIGINATES
 1665 C FROM WITHIN THE PHOENICS WALL SUBPROGRAM, WHICH WILL NOT BE
 1666 C ACCESSED IF GWALL IS USED INSTEAD. THE CALCULATED GMU1L VALUES
 1667 C MUST, HOWEVER, STILL BE "SET" IN CH. 12.
 1668 C
 1669 C 12. FOR THOSE CASES WHEN THE WALLS ARE ALIGNED WITH CELL FACES, THE
 1670 C PERPENDICULAR DISTANCES FROM THE WALL (GDELTA) ARE NORMALLY
 1671 C EXACTLY EQUAL TO ONE HALF THE APPROPRIATE CELL WIDTH (I.E. $DX/2$
 1672 C ETC.). WHEN SUCH A TREATMENT IS APPROPRIATE THE USER OF GWALL
 1673 C NEEDS SIMPLY TO SET GDELTA TO ANY NEGATIVE VALUE (E.G. -1.) AND
 1674 C THE APPROPRIATE HALF-CELL WIDTH(S) WILL THEN BE AUTOMATICALLY
 1675 C USED INSIDE GWALL. IF THIS TREATMENT IS NOT DESIRED, HOWEVER,
 1676 C THE APPROPRIATE NORMAL DISTANCES MUST BE SPECIFIED AS AN
 1677 C ARGUMENT (CELL-BY-CELL OR REGION-BY-REGION) IN THE GWALL CALL
 1678 C STATEMENT. HOWEVER, IT SHOULD BE NOTED THAT, IN POLAR GEOMETRIES
 1679 C WHEN THE NORMAL DISTANCE FROM AN EAST OR WEST WALL IS BEING

OR B. THE VARIABLE

1680 C SPECIFIED EXPLICITLY ONLY THE ANGLE (I.E. $DX/2$) BETWEEN THE GRID
1681 C NODE AND WALL SURFACE NEEDS TO BE SPECIFIED AS THE CORRESPONDING
1682 C NORMAL DISTANCE IS DEDUCED WITHIN GWALL ITSELF BY MULTIPLYING
1683 C THE SPECIFIED ANGLE BY THE LOCAL RADIUS.
1684 C
1685 C -----
1686 C DESCRIPTION OF THE WALL BOUNDARY TREATMENT EMPLOYED:-
1687 C
1688 C A. THE TURBULENT WALL SHEAR STRESS IS CALCULATED FROM A WALL FUNCTION
1689 C BASED ON THE LOGARITHMIC LAW OF THE WALL (REF: LAUNDER AND
1690 C SPALDING (1972)). "MATHEMATICAL MODELS OF TURBULENCE". THE
1691 C SO-CALLED "LOG LAW OF THE WALL" IS GIVEN BY:
1692 C
1693 C $UPLUS = (1./AK) * LOG(EWALL * YPLUS)$
1694 C
1695 C WHERE
1696 C $UPLUS = UGRID / USTAR$
1697 C $YPLUS = RHO * USTAR * DELTA / EMUL$
1698 C AND
1699 C $AK = \text{VON KARMANN CONSTANT } (=0.435)$
1700 C $EWALL = \text{EMPIRICAL CONSTANT } (=9.0 \text{ FOR SMOOTH WALL})$
1701 C $UGRID = \text{VELOCITY AT THE NEAR-WALL GRID NODE}$
1702 C $USTAR = \text{WALL SHEAR VELOCITY } (= \sqrt{TAUW / RHO})$
1703 C $RHO = \text{DENSITY}$
1704 C $DELTA = \text{PERPENDICULAR DISTANCE OF NEAR-WALL NODE FROM WALL}$
1705 C $EMUL = \text{LAMINAR VISCOSITY}$
1706 C
1707 C THE TURBULENT WALL SHEAR STRESS IS THEN GIVEN BY:
1708 C
1709 C $TAUW = EMUL * YPLUS / UPLUS$
1710 C
1711 C THE QUANTITIES YPLUS AND UPLUS ARE COMMONLY REFERRED TO AS
1712 C THE NORMALISED DISTANCE AND VELOCITY, RESPECTIVELY. IN THE
1713 C CODING OF GWALL BELOW UPLUS AND YPLUS ARE NOT SEEN EXPLICITLY.
1714 C HOWEVER, THEY CAN BE DEDUCED AS FOLLOWS:
1715 C
1716 C $UPLUS = 1. / \sqrt{GS}$
1717 C $YPLUS = REYN * \sqrt{GS} = REYN * YPLUS$
1718 C
1719 C WHERE
1720 C $\sqrt{GS} = USTAR / UGRID$
1721 C THAT IS
1722 C $GS = TAUW / (RHO * UGRID ** 2)$
1723 C AND
1724 C $REYN = RHO * UGRID * DELTA / EMUL$
1725 C
1726 C B. DUE TO THE IMPLICIT RELATIONSHIP BETWEEN UPLUS AND YPLUS THEIR
1727 C VALUES ARE OBTAINED ITERATIVELY. THE ITERATIVE PROCEDURE'S
1728 C INITIAL GUESS FOR GS (WHERE $UPLUS = 1. / \sqrt{GS}$) IS TAKEN FROM
1729 C KUTATELADZE AND LEONTIEV "TURBULENT BOUNDARY LAYERS", VIZ:
1730 C $GS = A * (REYNOLDS NO) ** B$
1731 C
1732 C WHERE A ($=8.74$) AND B ($=0.142857$) ARE TAKEN FROM TABLE 3-1 OF
1733 C THE ABOVE REFERENCE.
1734 C
1735 C C. THE TURBULENT KINETIC ENERGY AND DISSIPATION RATE VALUES ARE THEN
1736 C FIXED AT THE VALUES WHICH WOULD PREVAIL AT THE NEAR-WALL GRID
1737 C NODES IF THE SUPPOSED UNIVERSAL LOGARITHMIC VELOCITY PROFILE
1738 C PREVAILED.
1739 C

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1740 C D. FOR LAMINAR WALL SHEAR STRESS (REYNOLDS NO .LE. 132.25) A
1741 C LINEAR VELOCITY PROFILE IS ASSUMED NEAR TO THE WALL.
1742 C
1743 C E. THE WALL HEAT TRANSFER RATE IS EVALUATED FROM THE CHILTON-
1744 C COLBURN FORM OF THE REYNOLD'S ANALOGY, AS DESCRIBED IN THE
1745 C PHOENICS USER'S MANUAL, PAGE 3.2-48.
1746 C
1747 C
1748 C -----
1749 C COMMON/WALLG/ GU1(40,8),GV1(40,8),GW1(40,8),GDU1(40,8),
1750 C GCVAR(40,8),GVVAR(40,8),GDXU(8),GDYV(40),GR(40),GDZW(28)
1751 C -----
1752 C DATA JVISIT,JSOUTH,JU1,JV1,JW1,JKE,JEP,JH1/O,4,3,5,7,12,13,14/
1753 C DATA GAFRIC,GBFRIC,GAK,GEWALL,GTAUDK/8,74,0,142857,0,435,9,0,0,3/
1754 C DATA GREAT/1,E10/
1755 C -----
1756 C CHAPTER O PRELIMINARIES
1757 C -----
1758 C IF(JVISIT,GT,0) GO TO 10
1759 C JVISIT=JVISIT+1
1760 C GACON=1./GAFRIC**2./((1.+GBFRIC))
1761 C GBCON=(1.-GBFRIC)/((1.+GBFRIC)
1762 C GAKRA=1./SIGMA(24)**0.666667
1763 C GWALC=0.16433/GAK
1764 C
1765 C 10 DO 390 JIX=JIXF,JIXL
1766 C DO 390 JIV=JIVF,JIVL
1767 C
1768 C RWDPR2=1.
1769 C GRGRID=GR(JIV)
1770 C JWTYPE=IFX(GWTYPE)
1771 C GDEL=GDELTA
1772 C
1773 C GWALLU=GUWALL
1774 C
1775 C FOLLOWING STATEMENT SHOULD BE SUPPRESSED (IE. "COMMENTED OUT") IF
1776 C NOT APPROPRIATE (SEE NOTE 8 ABOVE)
1777 C IF(.NOT.CARTES) GWALLU=GUWALL*GRGRID**2
1778 C
1779 C GOTO (13,13,12,12,11,11), JWTYPE
1780 C DETERMINE DISTANCE FROM WALL AND RELATIVE VELOCITY PARALLEL TO WALL
1781 C HIGH OR LOW WALL
1782 C 11 IF(GDELTA,LT,Q.) GDEL=0.5*GDZW(JIZ)
1783 C GV1WAL=GVWALL
1784 C GV2WAL=GWALLU/GRGRID
1785 C GV1CEL=GV1(JIV,JIX)
1786 C GV2CEL=GU1(JIV,JIX)/GRGRID
1787 C GO TO 17
1788 C
1789 C NORTH OR SOUTH WALL
1790 C 12 IF(GDELTA,LT,O.) GDEL=0.5*GDYV(JIY)
1791 C GV1WAL=GWALL
1792 C GV2WAL=GWALLU/GRGRID
1793 C GV1CEL=GV1(JIV,JIX)
1794 C GV2CEL=GU1(JIV,JIX)/GRGRID
1795 C IF(.NOT.(.NOT.CARTES.AND.JVAR.EQ,JU1)) GO TO 17
1796 C WHEN SOLVING FOR UR, MODIFY U SO THAT NEAR-WALL U IS EMPLOYED
1797 C GFAC=0.5
1798 C IF(JWTYPE.EQ,JSOUTH) GFAC=-0.5
1799 C RWDPR2=(1.+GFAC*GDYV(JIV)/GRGRID)**2

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1800 GO TO 17
1801 C
1802 C EAST OR WEST WALL
1803 13 IF(GDELTA.LT.O.) GDEL=0.5*GDXU(JIX)
1804 IF(.NOT.CARTES) GDEL=GDEL*GRGRID
1805 GV1WAL=GWWALL
1806 GV2WAL=GWWALL
1807 GV1CEL=GM1(JIY,JIX)
1808 GV2CEL=GV1(JIY,JIX)
1809 C
1810 C CALCULATE RELATIVE VELOCITY OF FLUID PARALLEL TO WALL.
1811 17 CONTINUE
1812 GSPEED=SQRT((GV1CEL-GV1WAL)**2+(GV2CEL-GV2WAL)**2)
1813 C
1814 C SET APPROPRIATE WALL VALUE (I.E. ITS VELOCITY OR ENTHALPY)
1815 GVPHI=O.O
1816 IF(JVAR.EQ.JKE.OR.JVAR.EQ.JEP) GO TO 18
1817 IF(JVAR.EQ.JU1) GVPHI=GWALLU/RWDRP2
1818 IF(JVAR.EQ.JV1) GVPHI=GWWALL
1819 IF(JVAR.EQ.JW1) GVPHI=GWWALL
1820 IF(JVAR.EQ.JH1) GVPHI=GHWALL
1821 C
1822 18 GRHO=GD1(JIY,JIX)
1823 GDELMU=GDEL/GMU1L(JIY,JIX)
1824 GREYNO=GRHO*GSPEED*GDELMU
1825 GVALUE=O.O
1826 GCOEFF=O.O
1827 C
1828 IF(JVAR.EQ.JKE.OR.JVAR.EQ.JEP) GO TO 100
1829 IF(JVAR.EQ.JU1.OR.JVAR.EQ.JV1.OR.JVAR.EQ.JW1) GO TO 300
1830 IF(JVAR.EQ.JH1) GO TO 301
1831 GO TO 350
1832 C
1833 CHAPTER 1 FIX TURBULENT KINETIC ENERGY (KE)
1834 C
1835 100 GS=GACON*AMAX1(GREYNO,1.O)**((GBCON-1.)
1836 DO 101 JITS=1,3
1837 GSHALF=SQRT(GS)
1838 GS=(GAK/ALOG(1.+GSHALF*GREYNO*GSHALF))*2
1839 GTAU=GS*GREYNO*GSPEED/GDELMU
1840 GTKE=AMIN1(AMAX1(GTAU/(GRHO*GTAUDK),TKEMIN),TKEMAX)
1841 C
1842 IF(JVAR.EQ.JEP) GO TO 200
1843 C
1844 GVALUE=GTKE
1845 GCOEFF=GREAT
1846 C
1847 GO TO 350
1848 C
1849 CHAPTER 2 FIX KE DISSIPATION RATE (EP)
1850 C
1851 200 GVALUE=GWALC*SQRT(GTKE)*GTKE/GDEL
1852 GCOEFF=GREAT
1853 C
1854 GO TO 350
1855 C
1856 CHAPTER 3 WALL FRICTION (U1,V1,W1) AND HEAT TRANSFER (H1)
1857 C
1858 C--- LAMINAR
1859 C WALL FRICTION

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1860 300 GCOEFF=RWRP2/GDELMU
1861 GO TO 302
1862 C HEAT TRANSFER
1863 301 GCOEFF=GAKRA*RWRP2/GDELMU
1864 C
1865 302 IF(GREYND.LE.132.25) GO TO 310
1866 C--- TURBULENT
1867 GS=GACON*GREYND**(.GBCON-1.)
1868 DO 303 JITS=1,3
1869 GSHALF=SQRT(GS)
1870 303 GS=(GAK/ALOG(1.01+GEWALL*GREYND*GSHALF))**.2
1871 GCOEFF=GCOEFF*GS*GREYND
1872 C
1873 310 GVALUE=GVPHI
1874 C
1875 C--- SET UP GVAR (=CVAR) AND GVAR (=VVAR) ARRAYS
1876 350 GCVAR(JIY,JIX)=GCOEFF
1877 GVAR(JIY,JIX)=GVALUE
1878 C
1879 390 CONTINUE
1880 C
1881 RETURN
1882 C-----
1883 END
1884 SUBROUTINE AUTMON(ISTP,ISWP)
1885 $INCLUDE CMNGUSSI.FTN/G (NLIST)
1886 $INCLUDE GUSSEQUI.FTN/G (NLIST)
1887 DIMENSION ISOLV(25)
1888 LOGICAL FIRST
1889 DATA KSTP/O/
1890 DATA KSTP/O/
1891 C... USER DIMENSIONED (NY X NX) ARRAY FOR GETTING VARIABLES
1892 DIMENSION GDUM(40,8)
1893 C
1894 IF(FIRST) THEN
1895 OPEN(20,FILE='AUTOMON.DTA',STATUS='RENEW',RECL=20,FORM=
1896 + 'FORMATTED')
1897 NUMSOL = 0
1898 DO 10 I = 1,25
1899 IF(SOLVAR(I).OR.STOVAR(I)) THEN
1900 ISOLV(NUMSOL+1) = I
1901 NUMSOL = NUMSOL+1
1902 ENDIF
1903 10 CONTINUE
1904 FIRST=.FALSE.
1905 ENDIF
1906 C
1907 IF(KSTP.NE.ISTP) THEN
1908 IF(.NOT.STEADY) WRITE(20,('TIME STEP NO. ',I3')) ISTP
1909 WRITE(20,('I2')) NUMSOL
1910 DO 15 I = 1,NUMSOL
1911 15 WRITE(20,('A4')) TITLE(ISOLV(I))
1912 KSTP = ISTP
1913 ENDIF
1914 C
1915 WRITE(20,('I3')) ISWP
1916 DO 20 II = 1,NUMSOL
1917 CALL GET(ISOLV(II),GDUM,NY,NX)
1918 WRITE(20,('IPE10.3')) GDUM(IYMON,IXMON)
1919 20 CONTINUE

```

1920 C
1921 RETURN
1922 END
1923 P!

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APPENDIX B: PROPERTY CURVE FITS

The individual enthalpy curves for water and hydrogen have been combined in order to calculate a mixture enthalpy, $\text{Enthalpy}_{\text{mix}}$, defined as:

$$\text{Enthalpy}_{\text{mix}}(T) = (\text{Mass Ratio H}_2\text{O}) * \text{Enthalpy Water}(T) + \\ (1 - \text{Mass Ratio H}_2\text{O}) * \text{Enthalpy Hydrogen}(T)$$

This combined property curve is needed to be able to calculate the temperature of any given mixture of water and hydrogen in the aft-platform seal cavity, based on the mixture ratio and enthalpy calculated by the model. From the temperature are then calculated other fluid properties, such as density and viscosity. The curve fits used to compute these properties are depicted in Figures B-1 to B-6.

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ENTHALPY OF WATER¹

CURVE FIT I $H \text{ (Btu/lbm)} = -424.5938 + .82414T + 1.3067 \times 10^{-4}T^2$
(492 ≤ T < 975R)

CURVE FIT II $H = 2289.552 - 4.577089T + 2.815249 \times 10^{-3}T^2$
(975R ≤ T < 1184.6R)

CURVE FIT III $H = -7363.69 + 6.913T$
(1184.6R ≤ T < 1223.3R)

CURVE FIT IV $H = 599.5881 - 1.27177T + 1.369267 \times 10^{-3}T^2$
(1223.3R ≤ T < 1281.4R)

CURVE FIT V $H = -307.5449 + 1.190721T$
(1281.4R ≤ T < 1400R)

STANDARD ERROR = 4.08 Btu/lbm

¹These curves were fit to data taken from Thermodynamic Properties of Steam, Joseph Keenan and Frederick Keyes, (New York: Wiley and Sons, 1936) pp. 72-75.

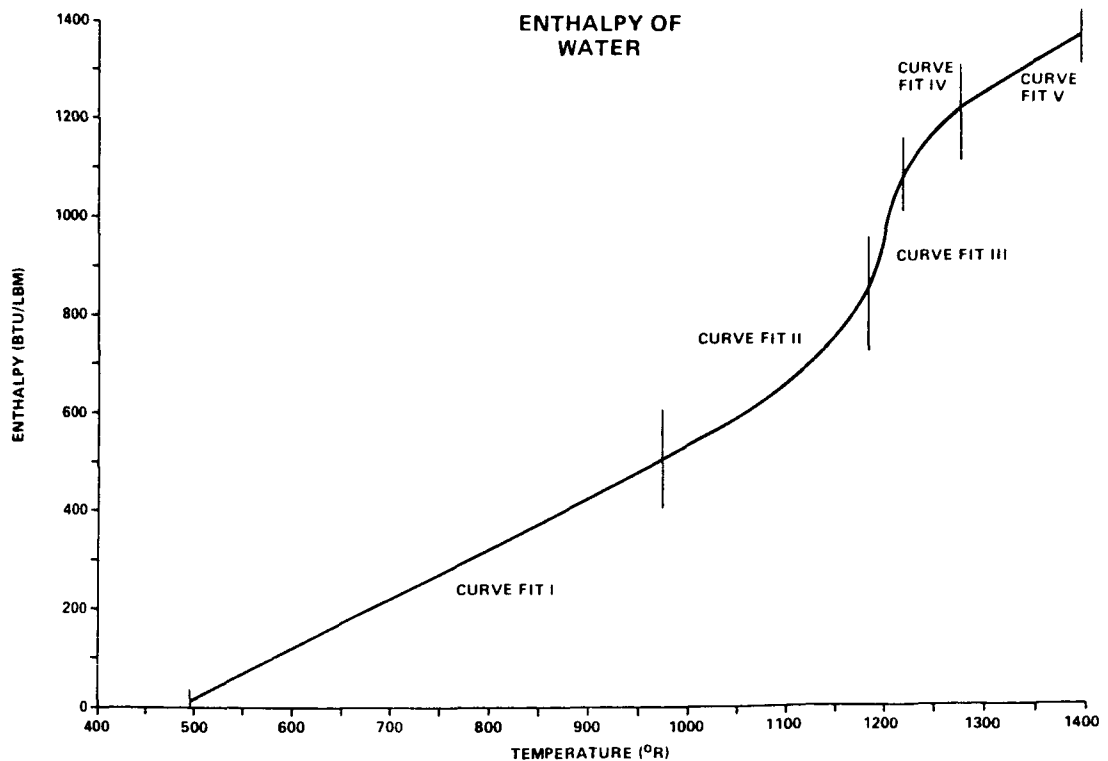


Figure B-1.

DENSITY OF WATER²

CURVE FIT I
(490R ≤ T < 1180R) density (lbm/ft³) = $-82.117 + .62353T - 6.77693 \times 10^{-4}T^2$
 $-3.41207 \times 10^{-7}T^3 + 9.23406 \times 10^{-10}T^4$
 $-3.9688 \times 10^{-13}T^5$

CURVE FIT II density = $-2177.783 + 7.12733T - 4.54395 \times 10^{-3}T^2$
 (1180R ≤ T < 1250R) $-1.91391 \times 10^{-6}T^3 + 1.686 \times 10^{-9}T^4$

CURVE FIT III density = $119.1372 - 4.770357 \times 10^{-2}T - 1.00694 \times 10^{-4}T^2$
 (1250R ≤ T ≤ 1400R) $+ 5.516186 \times 10^{-8}T^3$

STANDARD ERROR = 0.61 lbm/ft³

²These curves are fit to data taken from Keenan, pp. 72-75.

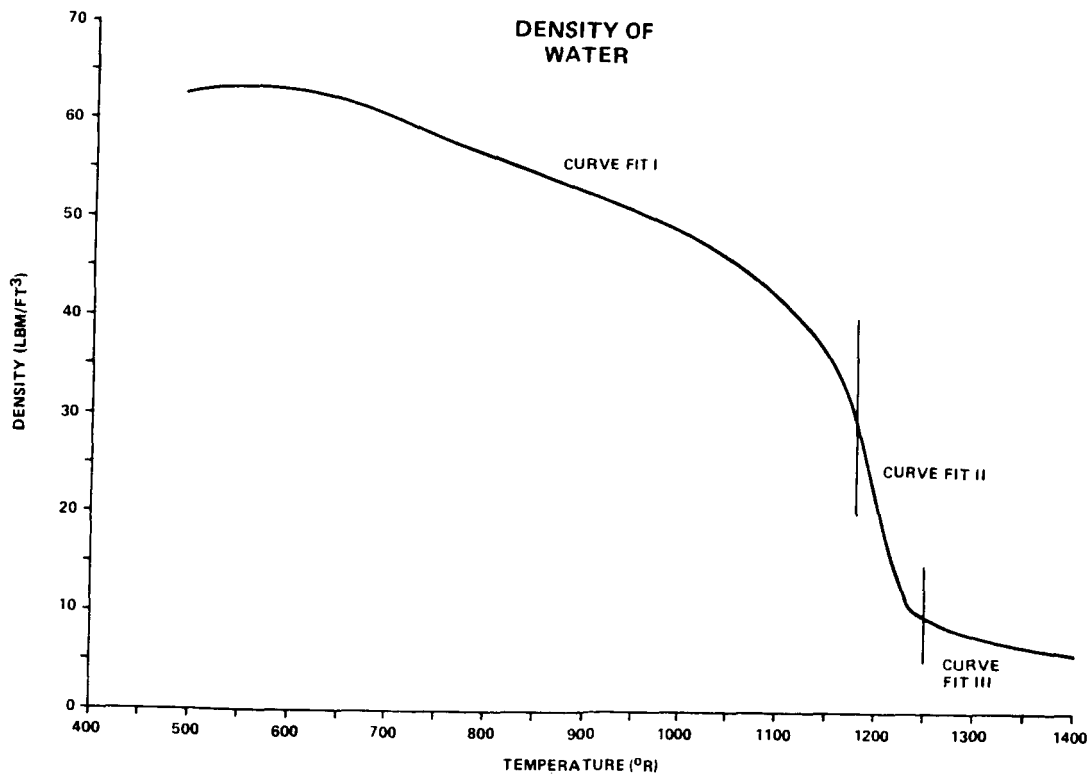


Figure B-2.

VISCOSITY OF WATER³

$$\text{VISC } (\times 10^3) = \frac{\left[20.5532 - 6.52199 \times 10^{-2}T + 3.2726 \times 10^{-5}T^2 + 6.6687 \times 10^{-8}T^3 - 8.3627 \times 10^{-11}T^4 + 2.6237 \times 10^{-14}T^5 \right]}{e}$$

$$\text{STANDARD ERROR } (\times 10^3) = 0.0066 \text{ lb/ft-sec}$$

³This curve is fit to data taken from Steam Tables, Joseph Keenan, et al., (New York: Wiley and Sons, Inc., 1969) p. 113.

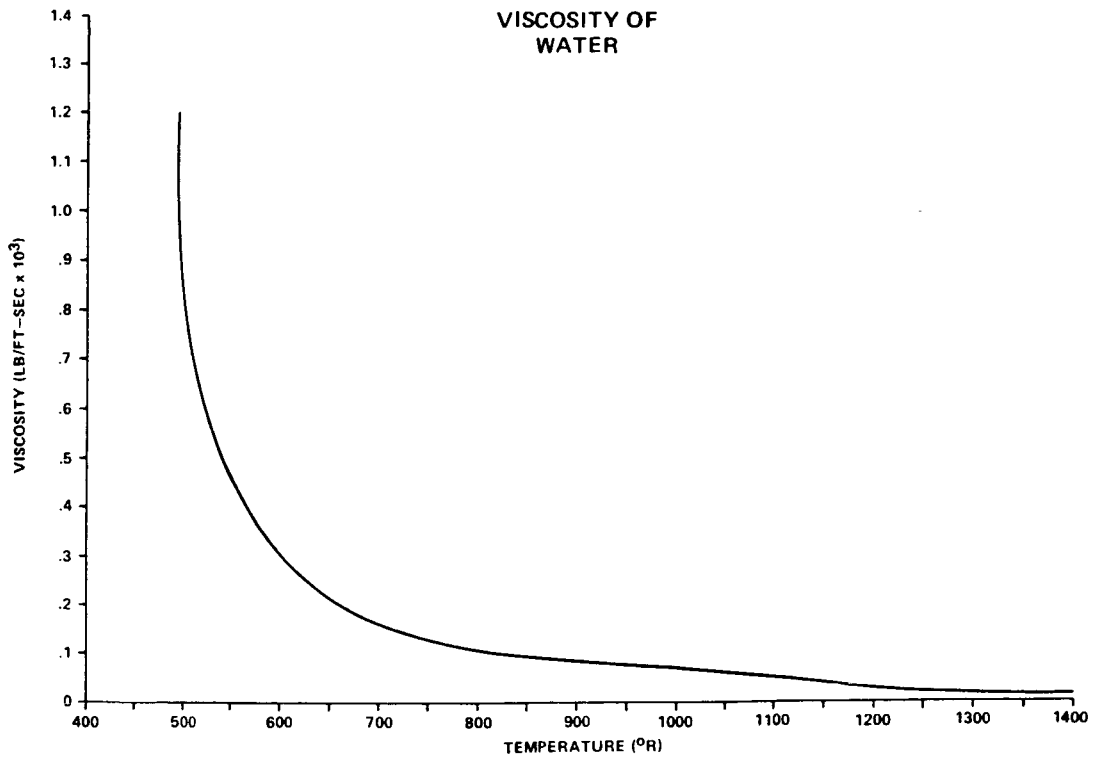


Figure B-3.

ENTHALPY OF HYDROGEN⁴

CURVE FIT I
 (170R ≤ T ≤ 508R) $H \text{ (Btu/lbm)} = -5.92706 \times 10^{-4} T^2 + 4.468995T - 357.6903$

CURVE FIT II
 (508R ≤ T ≤ 2000R) $H = -7.15694 \times 10^{-6} T^2 + 3.557702T - 45.88906$

STANDARD ERROR = 4.39 Btu/lbm

⁴These curves are fit to data taken from the Hydrogen Technological Survey - Thermophysical Properties, Robert D. McCarty, (Washington, D.C.: NASA Scientific and Technical Information Office, 1975) p. 472.

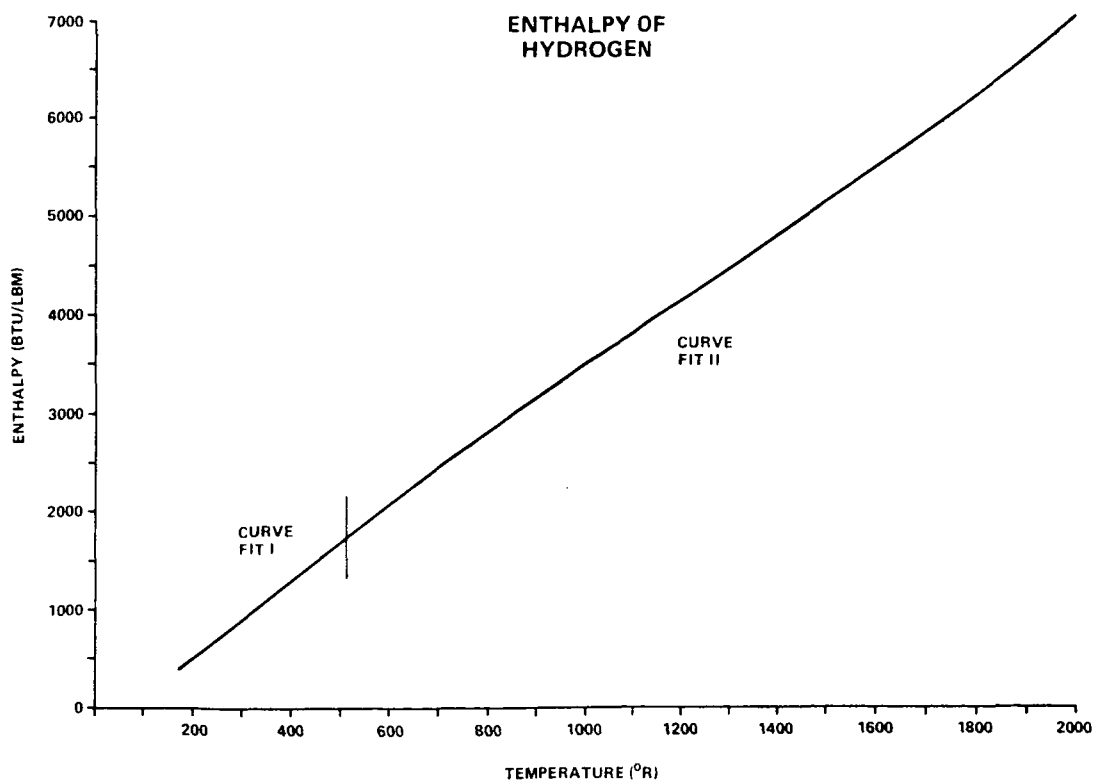


Figure B-4.

DENSITY OF HYDROGEN⁵

$$\text{density (lbm/ft}^3\text{)} = \frac{\left[-5.26685 + 3.049183(\ln H) - .41497(\ln H)^2 \right]}{e^{+ 1.40759 \times 10^{-2}(\ln H)^3}}$$

where H is the enthalpy of hydrogen.

$$\text{STANDARD ERROR} = .0189 \text{ lbm/ft}^3$$

⁵This curve is fit to data taken from McCarty, p. 472.

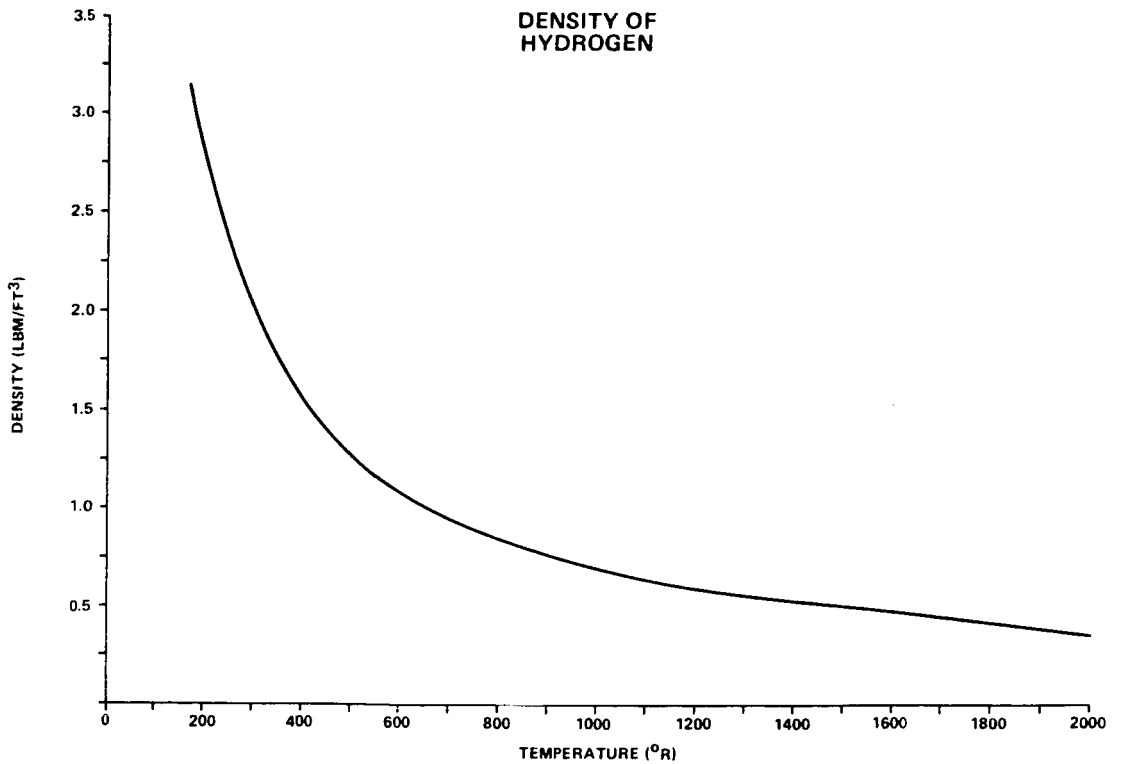


Figure B-5.

VISCOSITY OF HYDROGEN⁶

$$\begin{aligned} \text{VISC. (lbm/ft-sec} \times 10^5) &= .4989 - 5.4575 \times 10^{-5} T \\ &+ 5.1824 \times 10^{-7} T^2 - 1.4948 \times 10^{-10} T^3 \end{aligned}$$

$$\text{STANDARD ERROR (} \times 10^5) = 0.00047 \text{ lbm/ft-sec}$$

⁶This curve is fit to data taken from the Hydrogen Technological Survey - Thermophysical Properties, Robert D. McCarty, (Washington, D.C.: Scientific and Technical Information Office, NASA, 1975) p. 473.

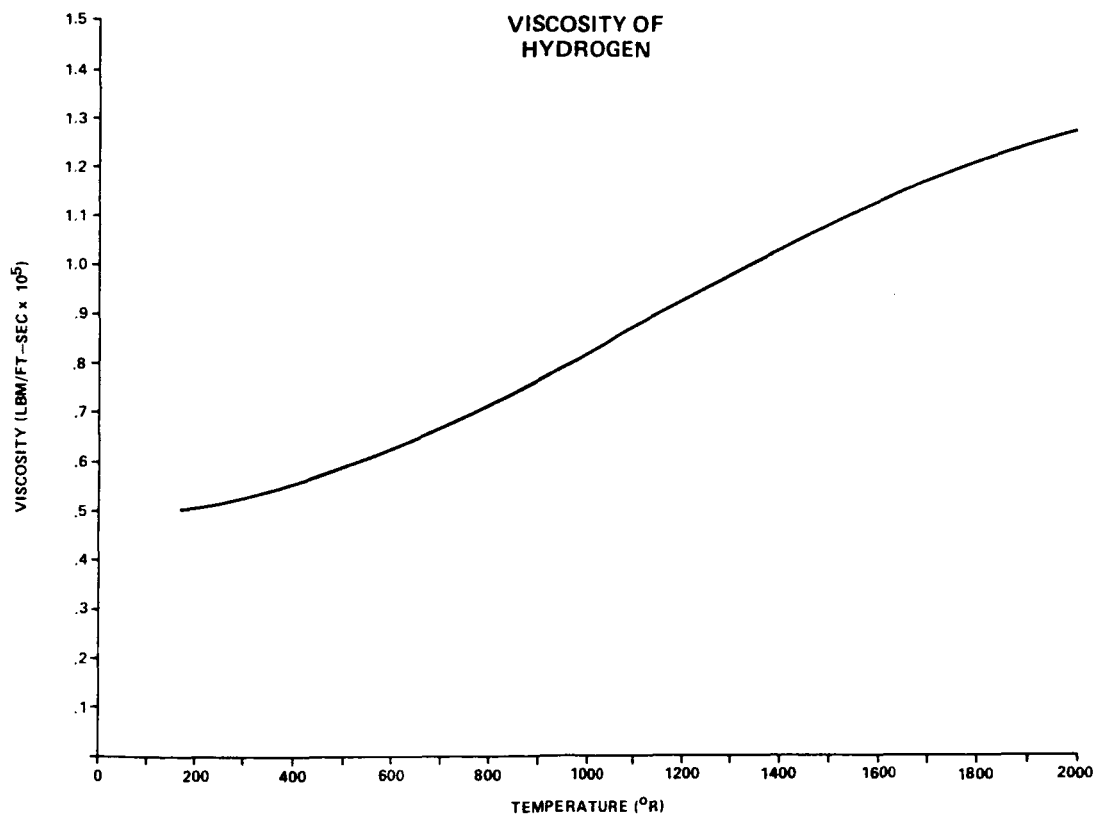


Figure B-6.

APPENDIX C: CONVERGENCE CHARACTERISTICS

The insensitivity of the model to the initial values chosen for temperature and velocity is demonstrated by the solution sets given below. There were four different test cases run using identical boundary conditions but with the different guesses of velocity and temperature listed in the following table. Cases 1 to 3 were run to test the sensitivity of the solution to the initial temperature guess, and case 4 was run to check the sensitivity of the solution to the initial choice of the velocity field.

INITIAL FIELD VALUES

	Temperature	Theta Velocity
CASE 1	Hot Guess	$\Omega = 0.4$ Disk Ω
CASE 2	Best Guess	Same as above
CASE 3	Cold Guess	Same as above
CASE 4	Best Guess	$\Omega = 0$

(Ω in radians/sec)

After 500 sweeps, the values of velocity, temperature, and pressure, at a reference point in the middle of the cavity, have converged to the extent shown in Figures C-1 to C-8. By 500 sweeps the constant pressure lines (Fig. C-2) for all four cases are very similar, as are the streamlines (Fig. C-8), and to a lesser extent the temperature profiles (Figs. C-1 and C-7). Of the three, temperature is the slowest to recover from a poor initial guess. However, even with an initial temperature estimate 1000°R off the final values, the temperature at the monitoring point has converged to within 200° of the final value after 200 sweeps, and to within 75° of the final value after 400 sweeps. This is an acceptable convergence rate for our application, especially since the magnitude of the error is readily apparent from the slope of the temperature convergence curve (Fig. C-1). In the event that greater accuracy were required, the solution could be bracketed or else extended the necessary number of sweeps.

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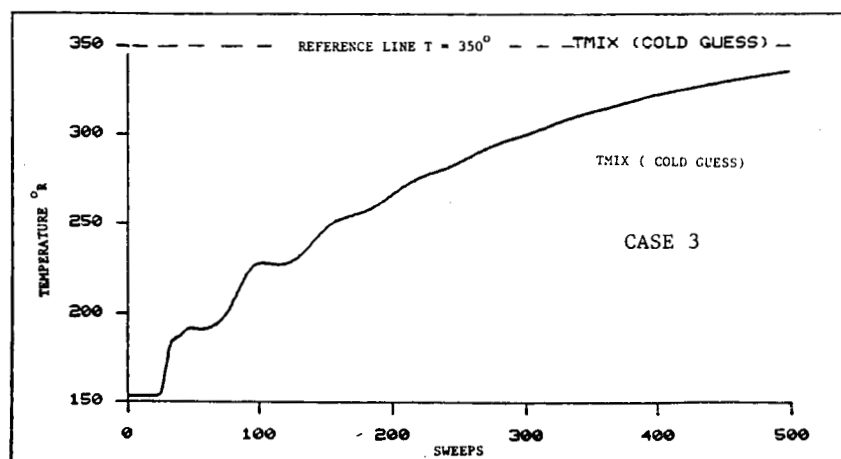
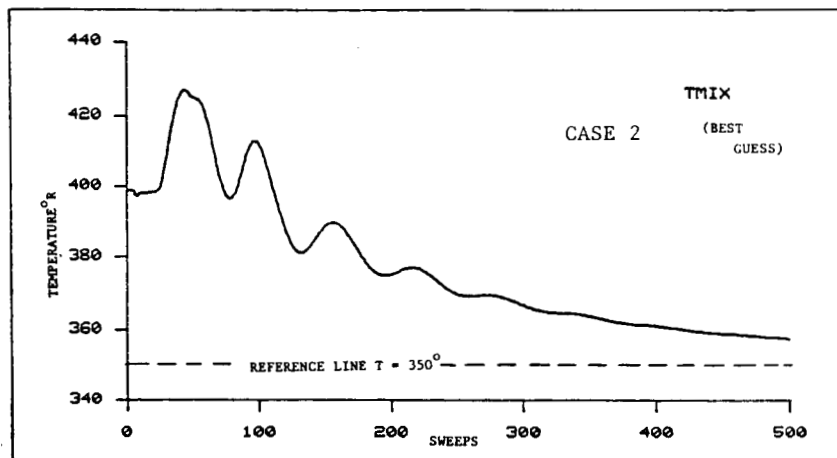
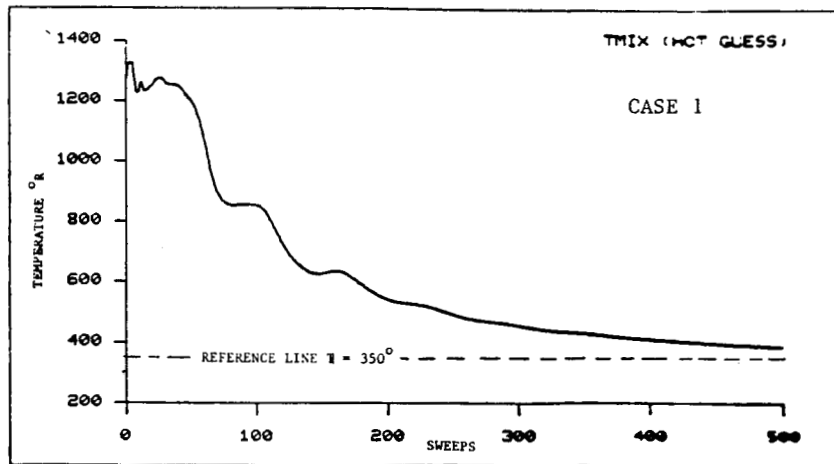


Figure C-1. Temperature convergence, cases 1 to 3.

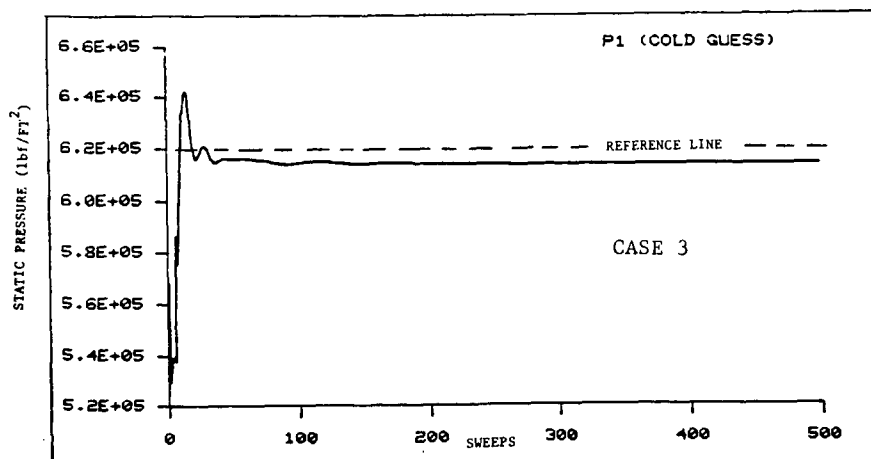
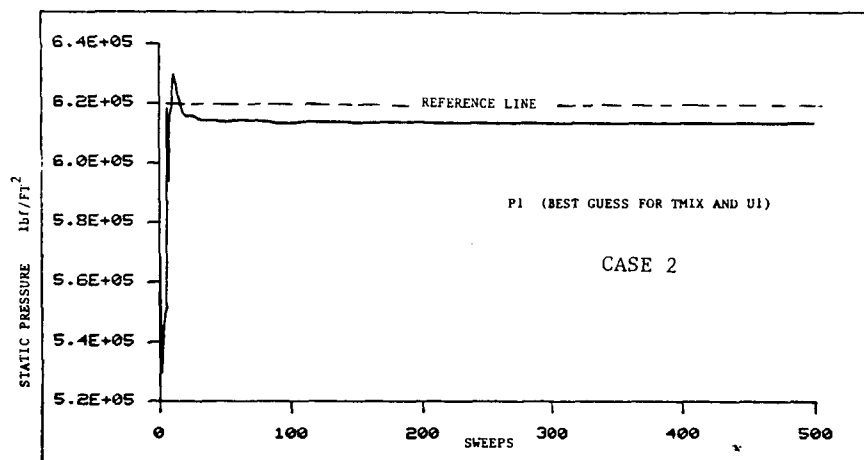
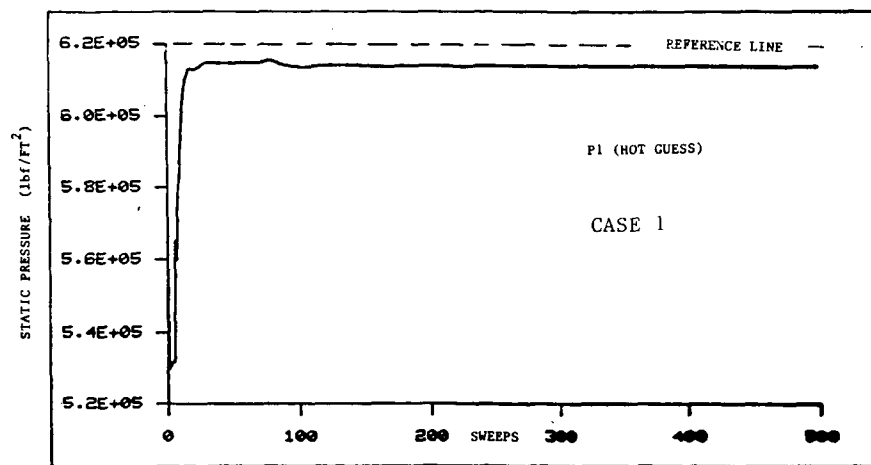


Figure C-2. Pressure convergence, cases 1 to 3.

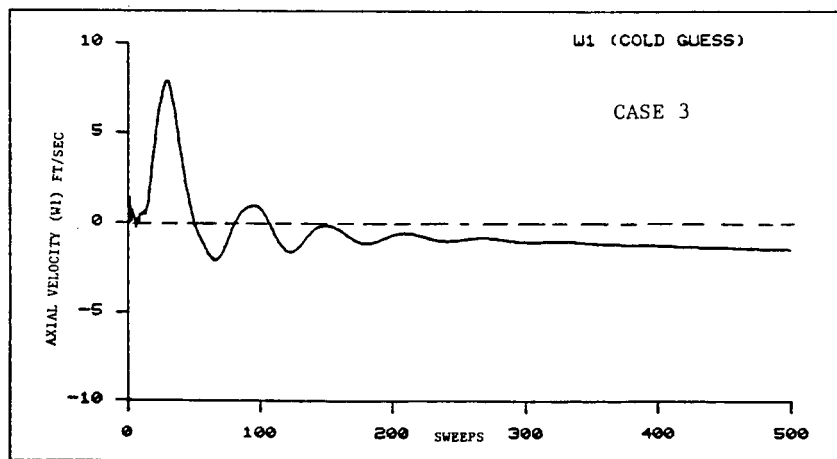
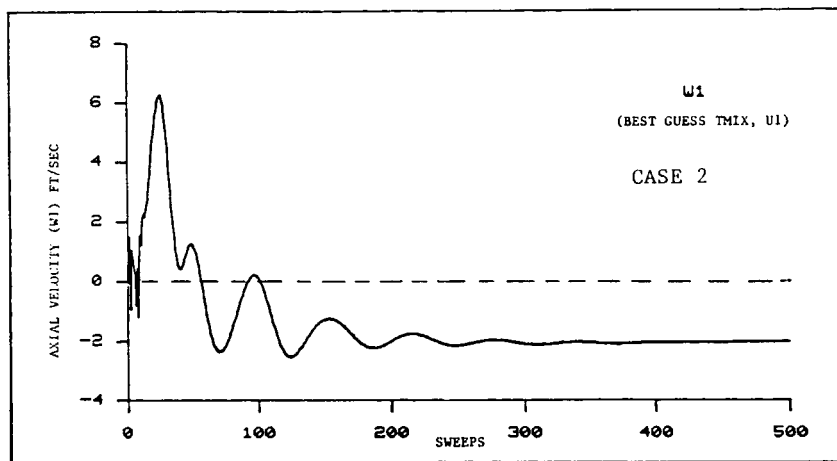
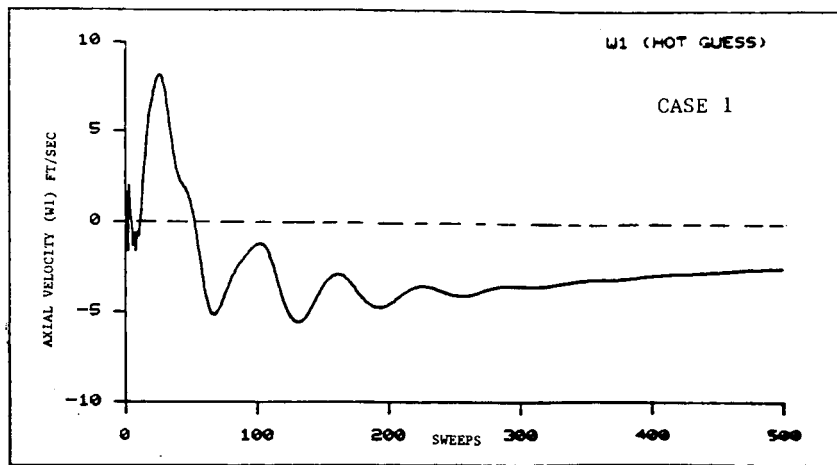


Figure C-3. Circumferential velocity convergence, cases 1 to 3.

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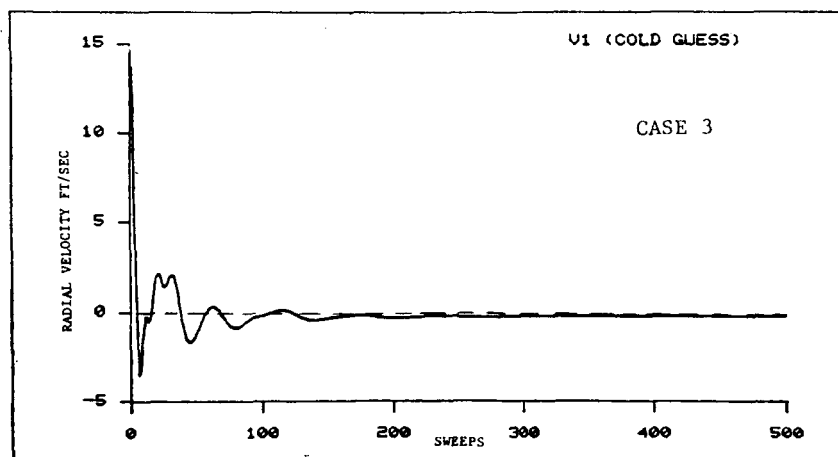
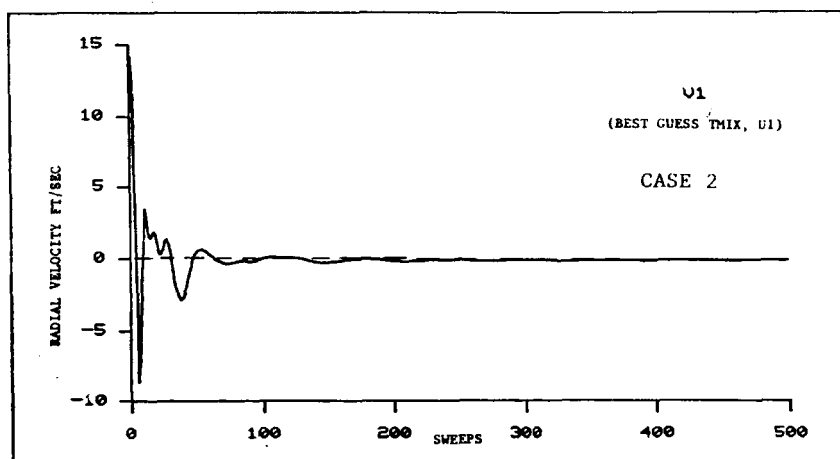
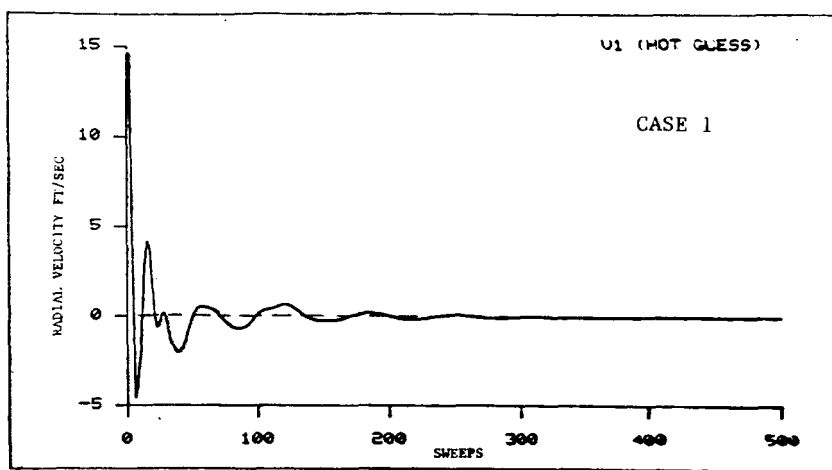


Figure C-4. Radial velocity convergence, cases 1 to 3.

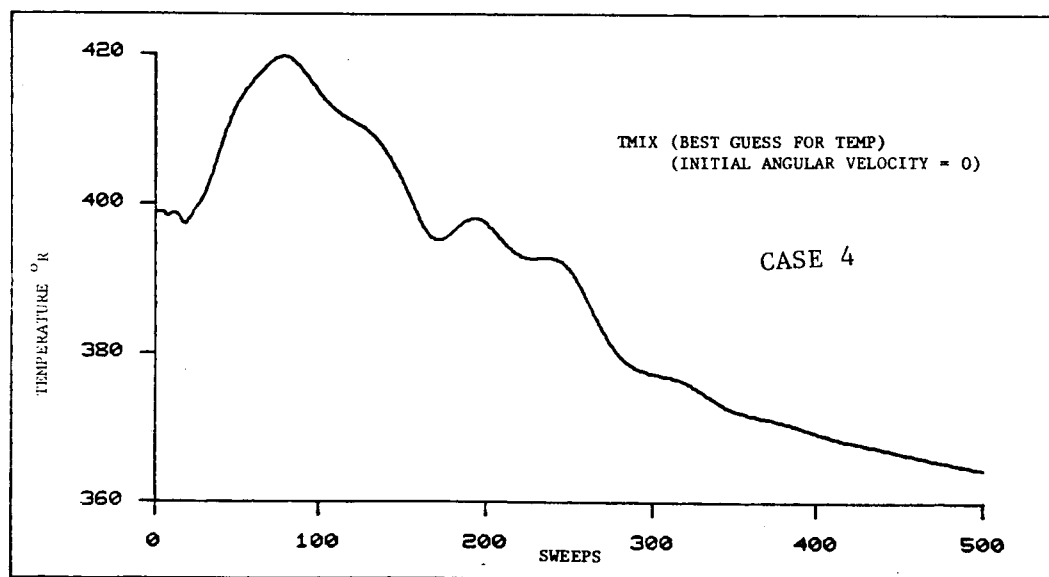
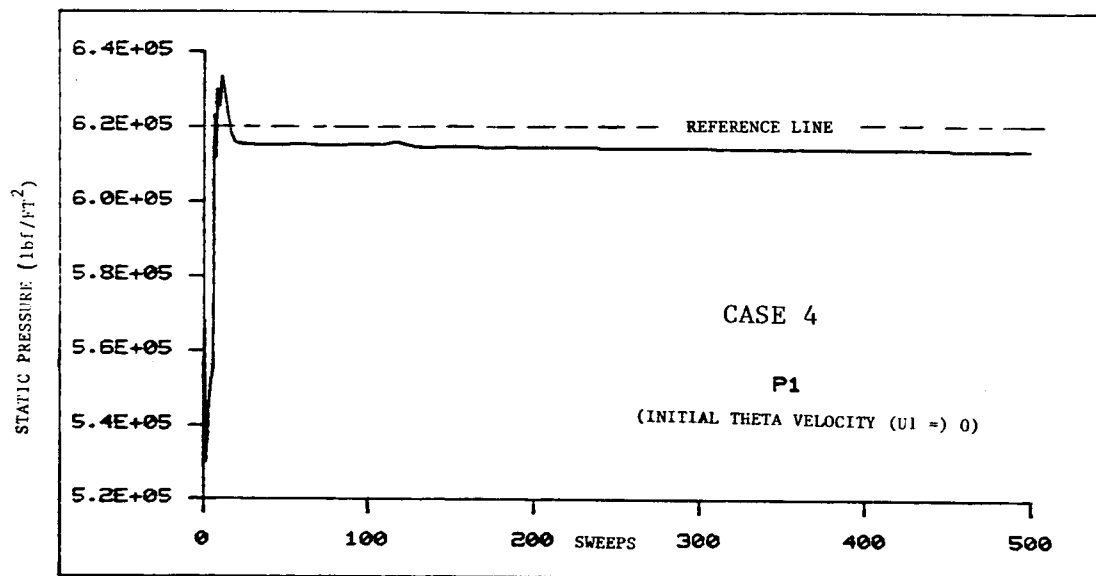


Figure C-5. Pressure and temperature convergence, case 4.

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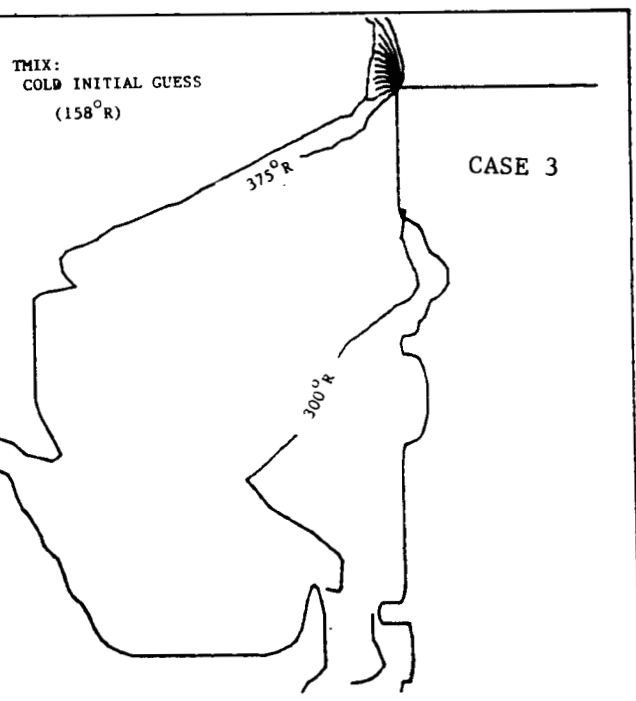
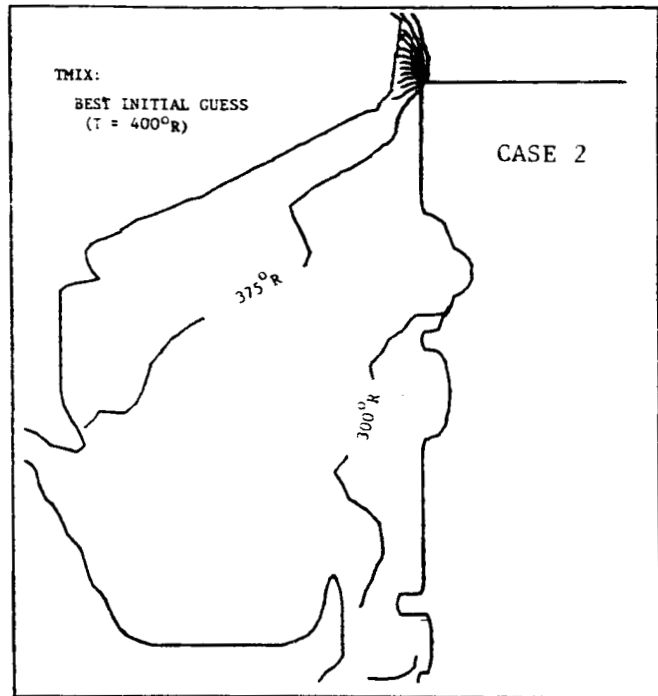
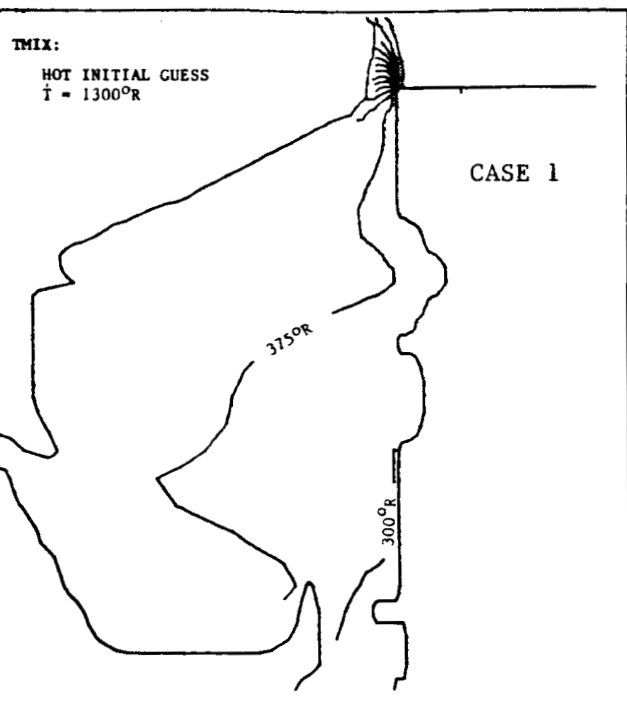


Figure C-6. Temperature fields, cases 1 to 3.

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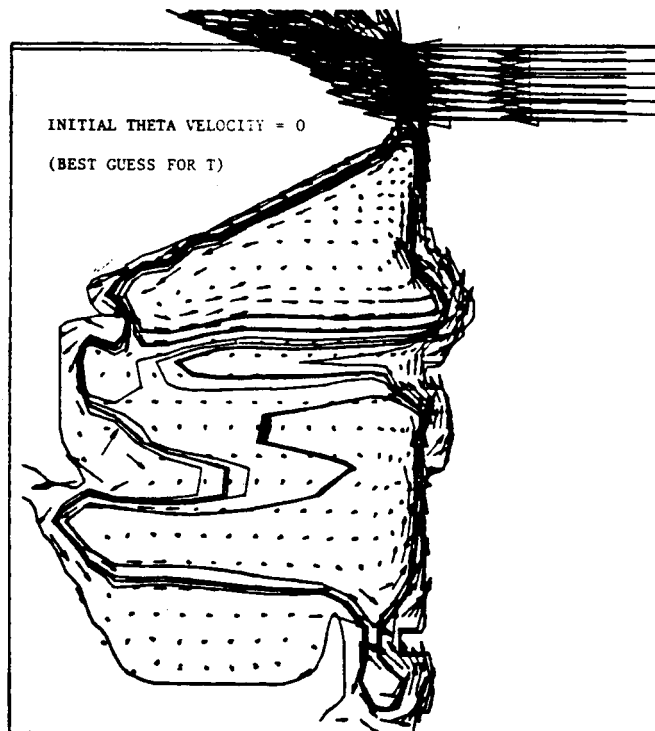
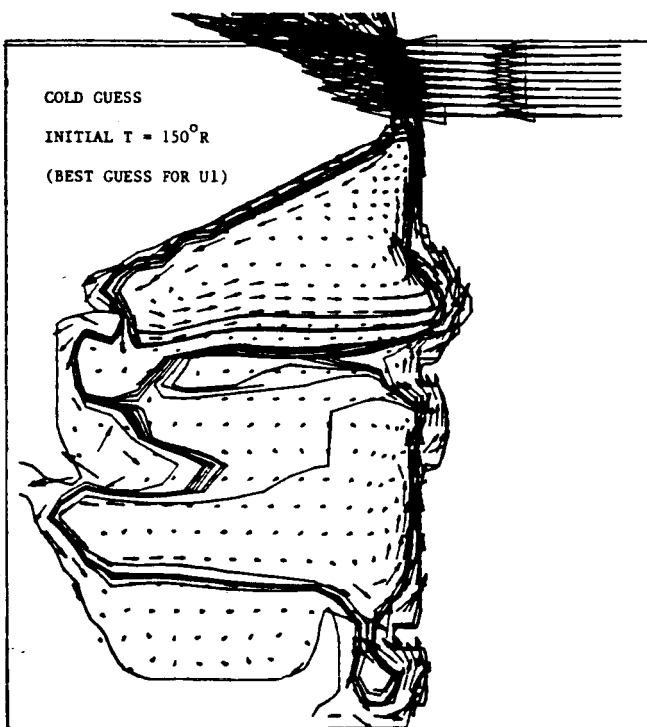
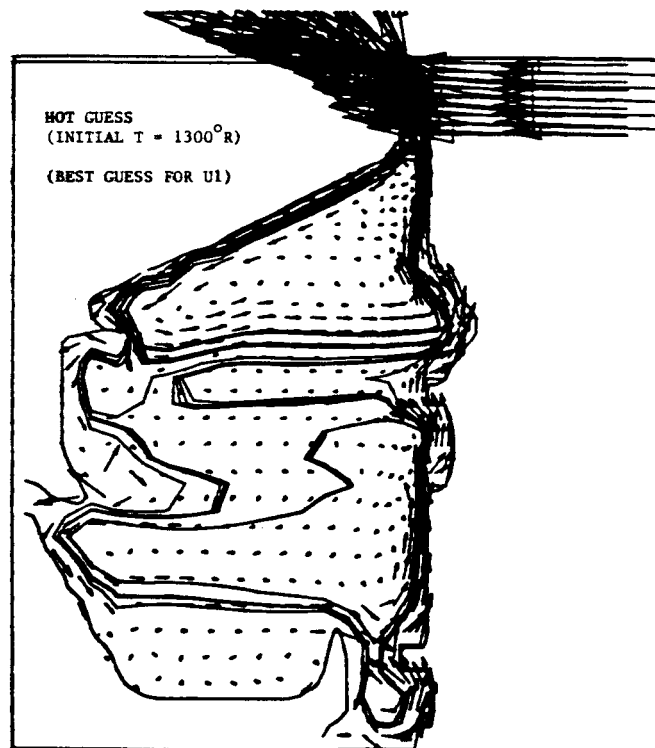
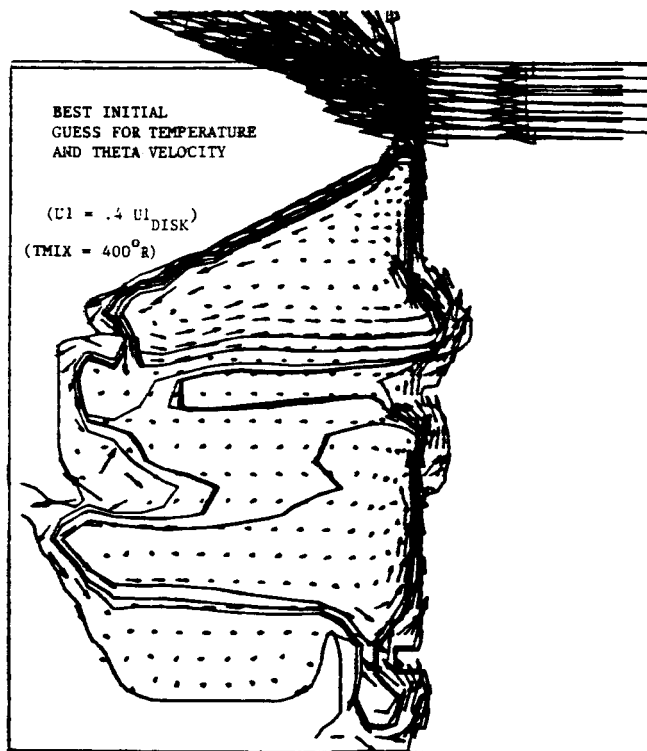


Figure C-7. Velocity field and streamlines, cases 1 to 4.

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